

# **Current Activities on Solid Oxide Cells at DLR**

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Institute of Engineering Thermodynamics  
Stuttgart, Germany**



**Knowledge for Tomorrow**



# Outline

- Brief Introduction of DLR-ITT
- Metal Supported Cell Concepts for SOC
  - Plasma spray concept
  - EVOLVE concept
- SOEC activities
  - Hi2H2 project
  - Degradation study
  - Solar fuels
- Conclusion



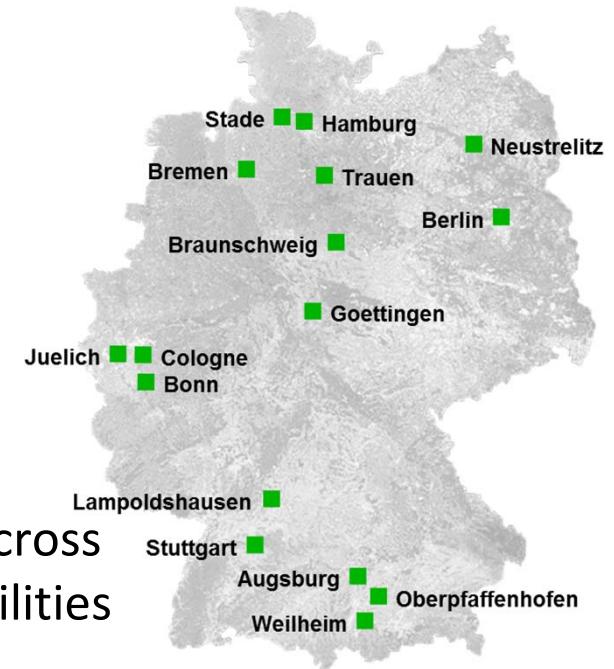
# DLR

## German Aerospace Center

Aeronautics  
Space  
Transport  
Energy

Research Institution

> 7500 employees across  
32 institutes and facilities



Space Agency  
Project Management Agency



# Institute of Engineering Thermodynamics

*Prof. Dr. André Thess*

## Administration

*Jörg Piskurek*



### Electrochemical Energy Technology

*Prof. A. Friedrich*

### Computational Electrochemistry

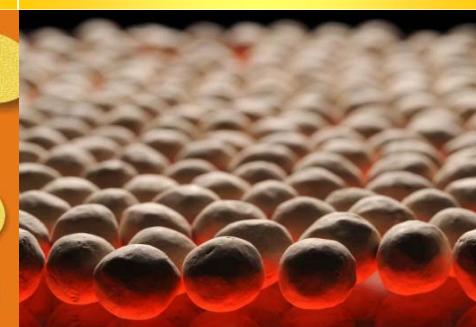
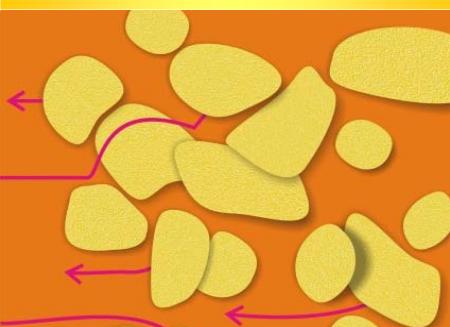
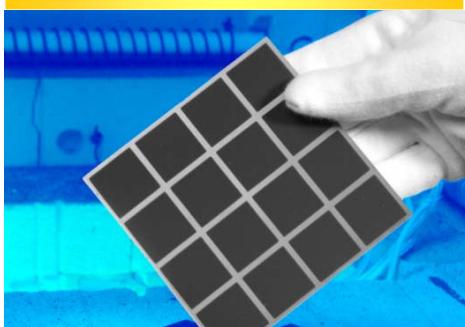
*Prof. A. Latz*

### Thermal Process Technology

*Dr. A. Wörner*

### System Analysis and Techn. Assessment

*Dr. C. Schillings /  
C. Hoyer-Klick (komm.)*



Staff: About 190 in Stuttgart, Köln, Hamburg and Ulm

Yearly budget: About 18 Mio. EUR including 50% third party funding

*„.... innovative solutions for sustainable and environmentally friendly energy storage and conversion processes ...“*



# Electrochemical Energy Technology

R&D of efficient electrochemical energy storage and conversion

## 5 Fields of Research

### Solid Oxide Cells

Realization of durable, powerful and cost effective SOFC-stacks



### Lithium Metal and Lithium Ion Batteries

Development of mobile energy storages

### Modeling & Simulation

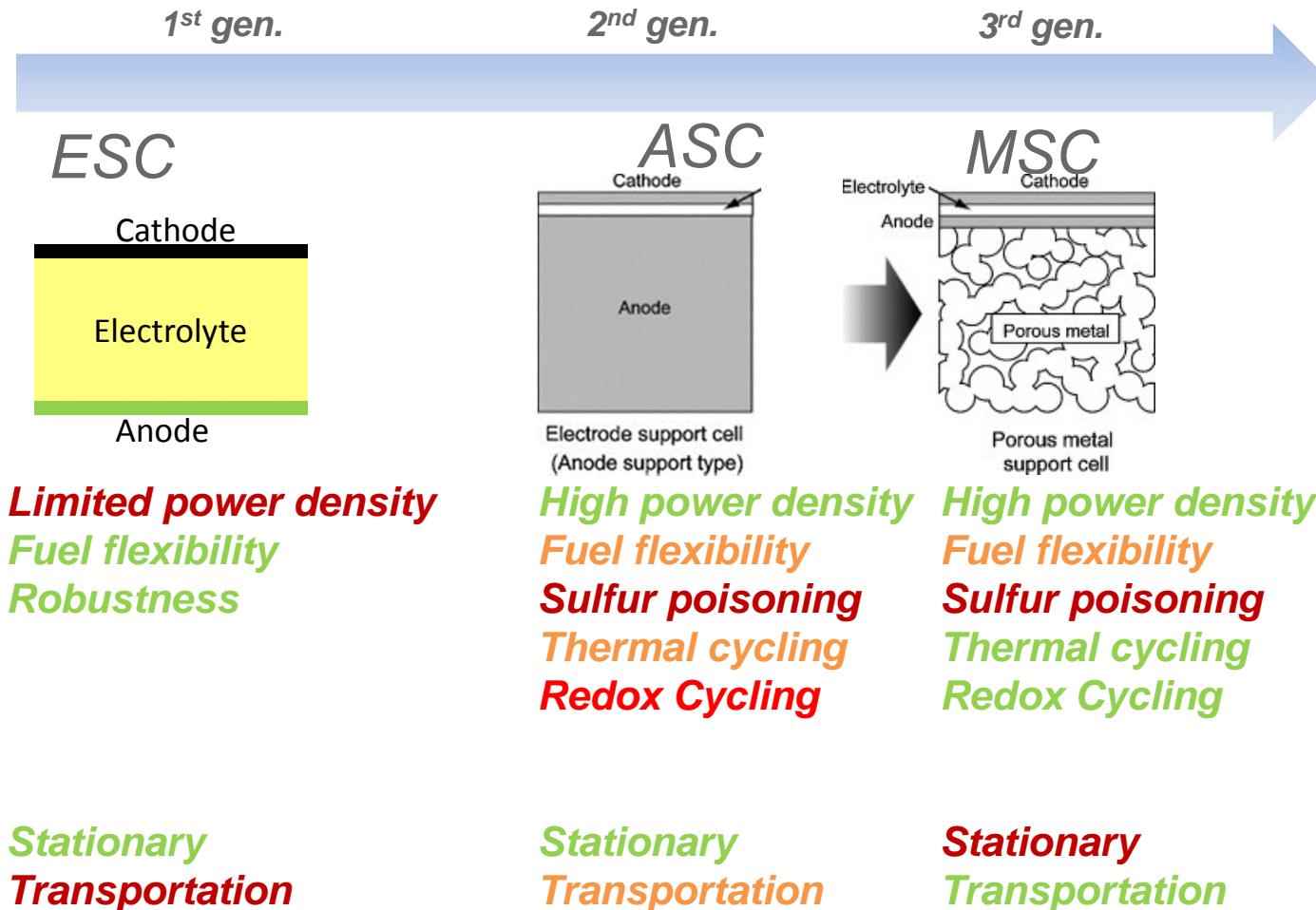
Improvement of the efficiency factor, longevity and costs of fuel cells and batteries

### Electrochemical Systems

Development of efficient and effective, multifunctional fuel cells systems for stationary and mobile applications



# Generations of planar SOFCs



# Metal Supported SOFC

Plasma Spray for Functional Layers

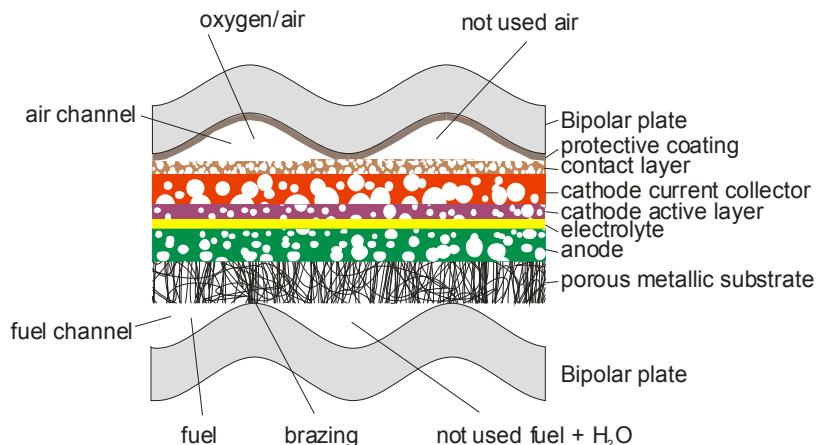
Compact design with thin sheet ferritic substrates and interconnects

100 cm<sup>2</sup> foot print

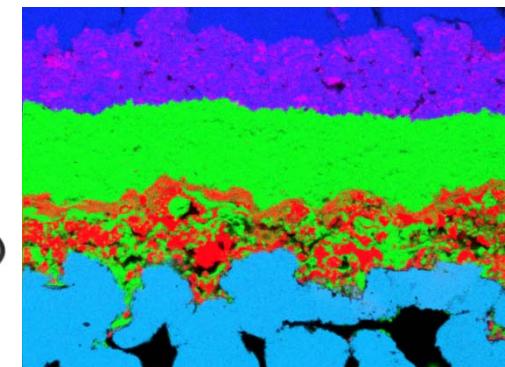
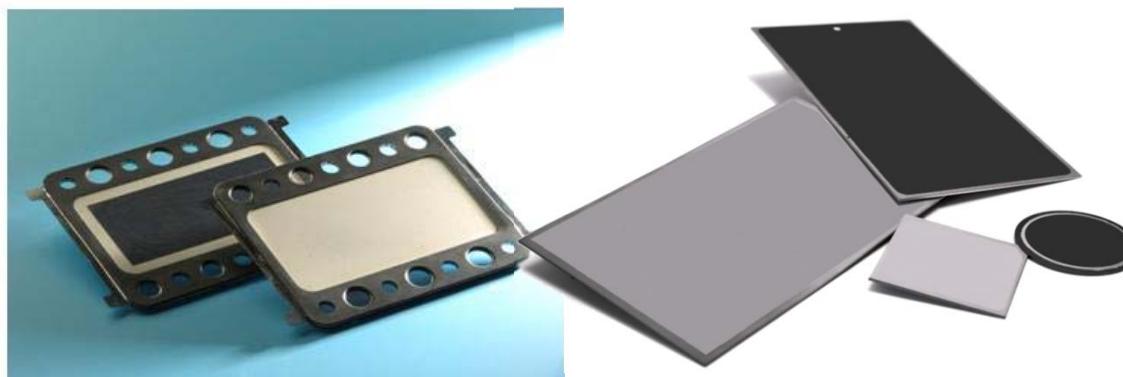
Counter flow stamped gas manifold

Welded substrate with the interconnect

Brazing or Glass Seal as joining of repeat units



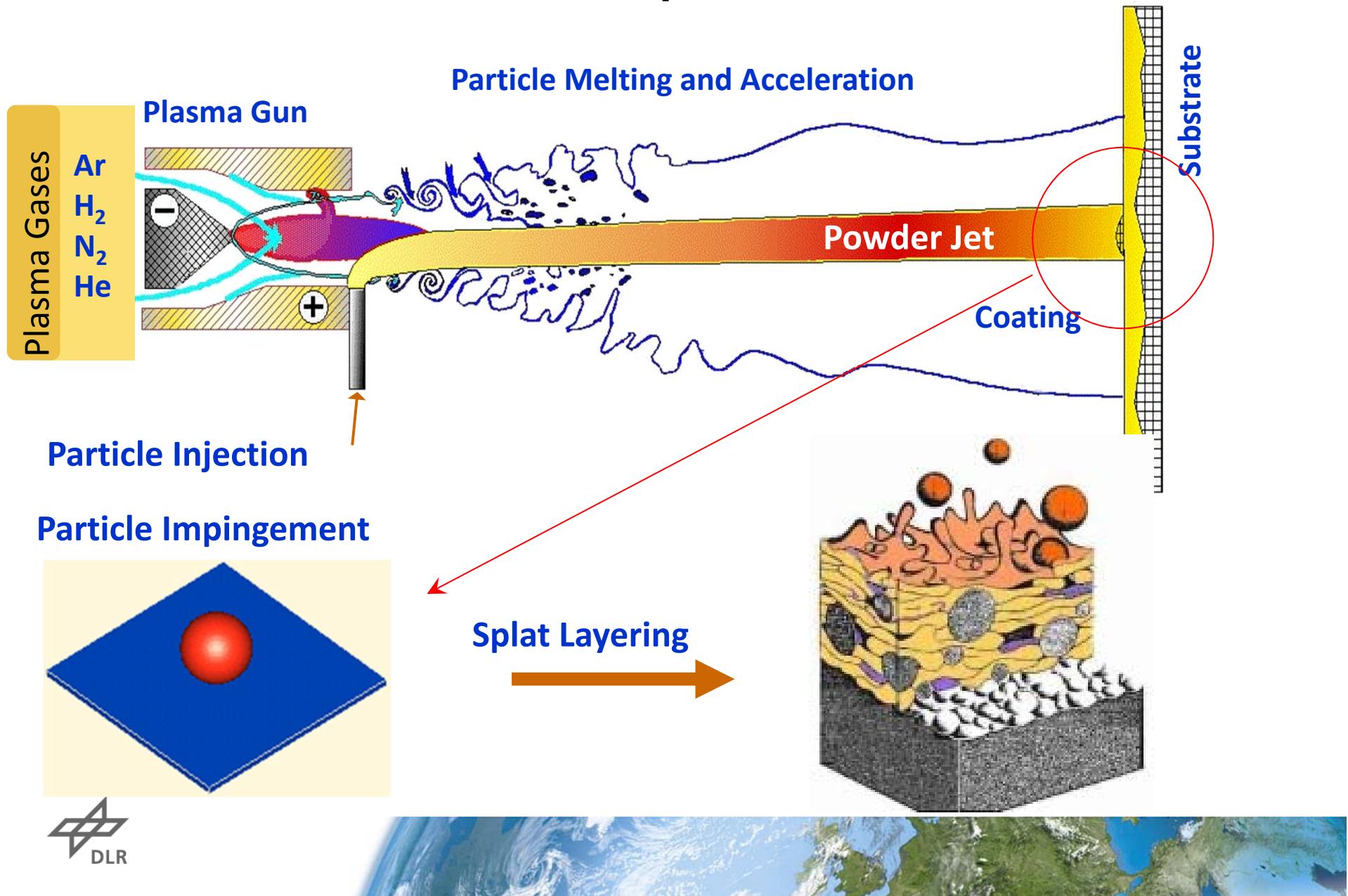
(not in scale)



Cathode 20 µm  
Electrolyte 35 µm  
Anode 35 µm  
Substrate



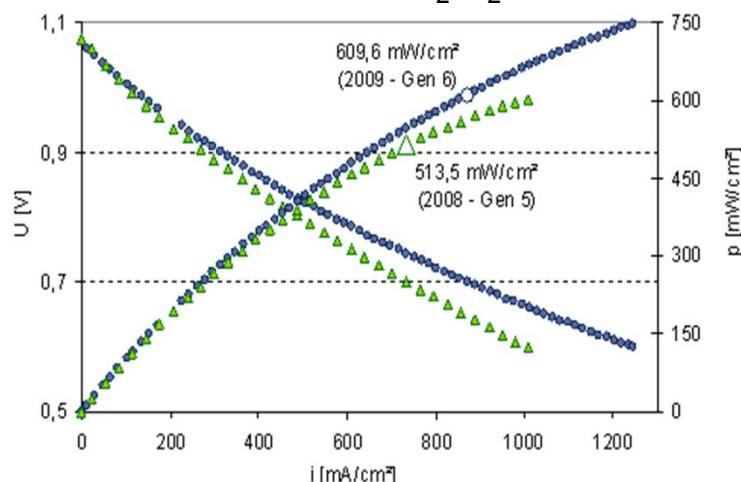
# Functional Principle of DC Plasma



# Metal Supported SOFC - Performance

## MSC Cell

12.5 cm<sup>2</sup> cell at 800°C; H<sub>2</sub>/N<sub>2</sub> and air



**610 mW/cm<sup>2</sup> @ 0.7V (2009- G6)**

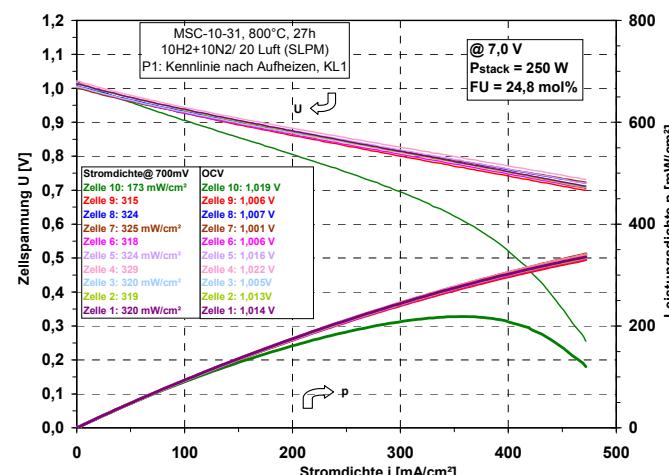
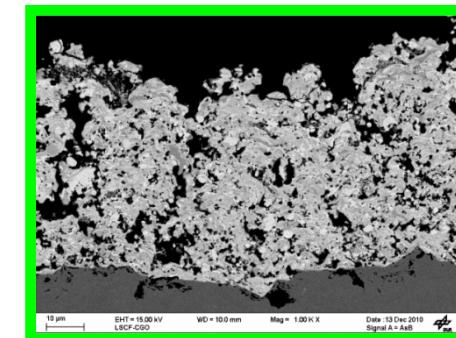
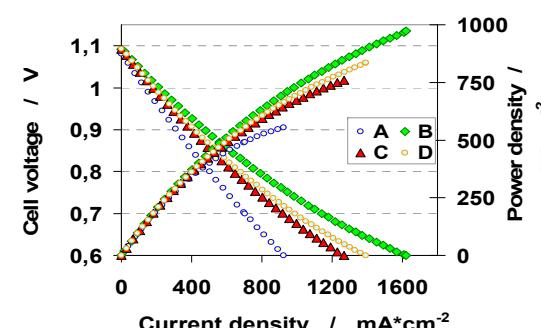
## 10-Cell Stack

100 cm<sup>2</sup> cells at 800°C; H<sub>2</sub>/N<sub>2</sub>; air

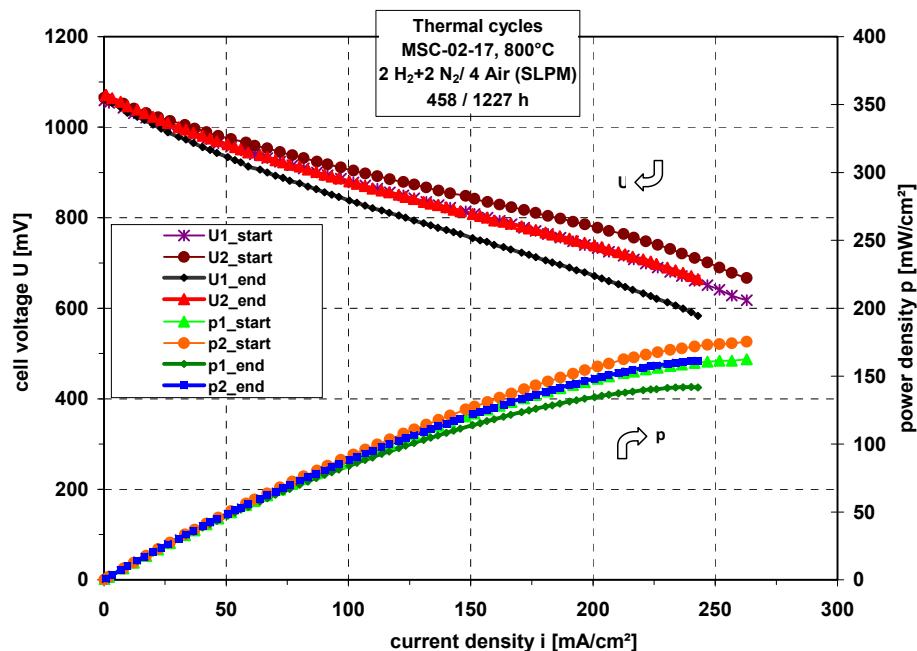
## MSC Cell with Suspension Plasma Spray Electrodes

Power density above 800 mW/cm<sup>2</sup> at 0.7 V

12.5 cm<sup>2</sup> cell at 800°C; H<sub>2</sub>/N<sub>2</sub> and air

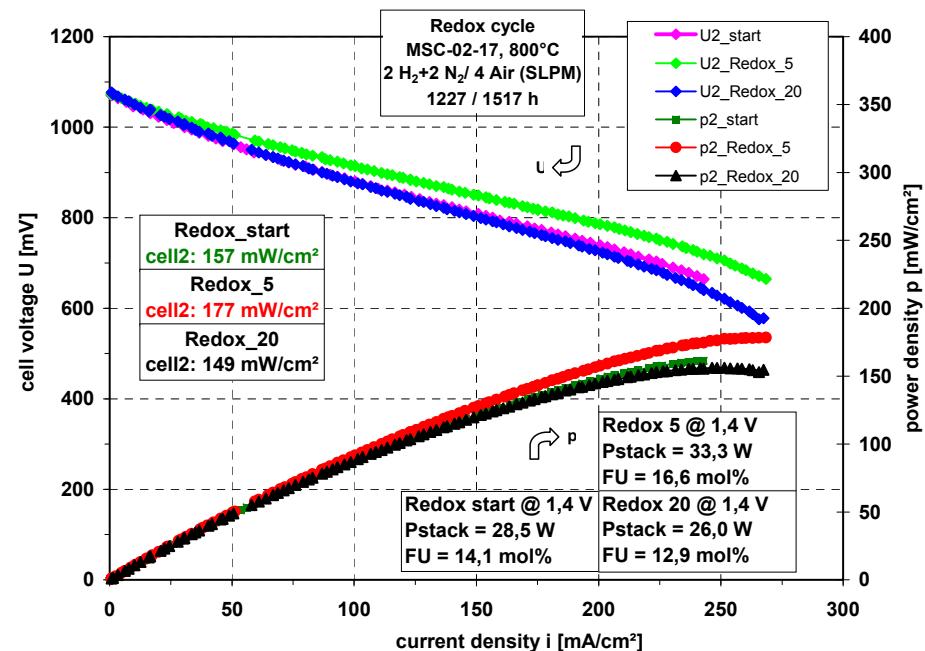


# Cyclability of Metal Supported Cells



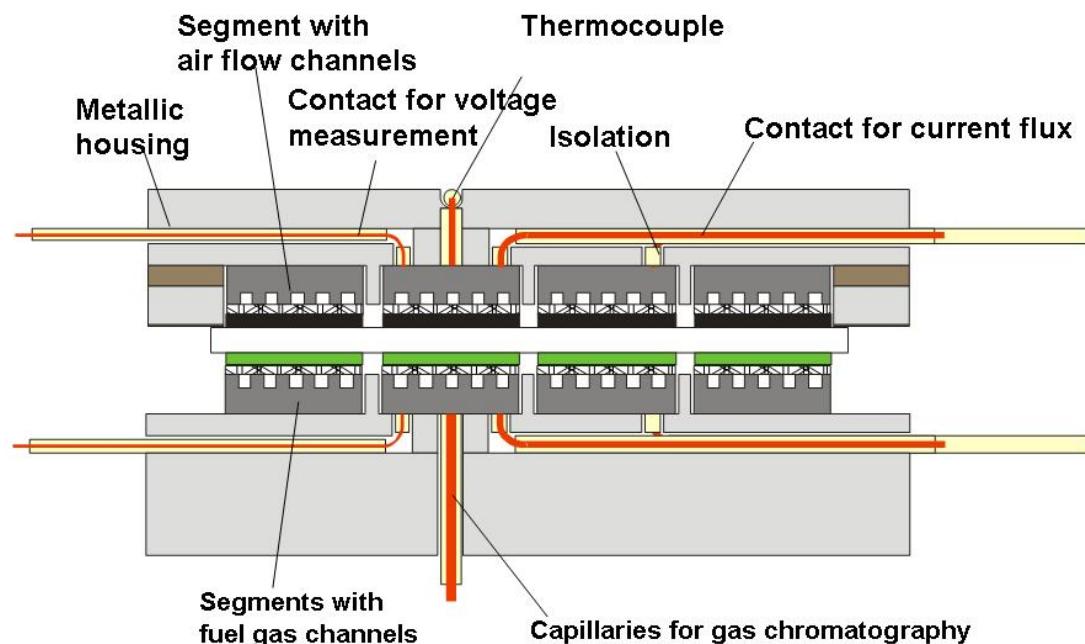
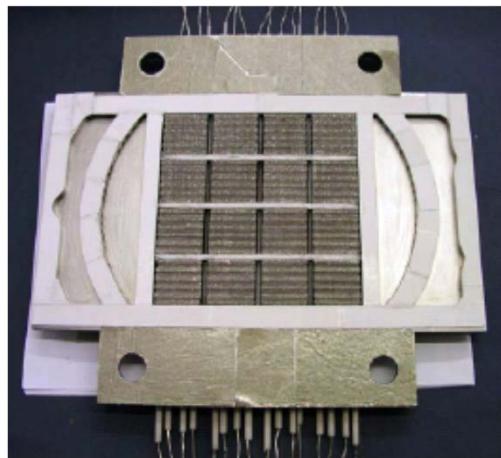
15 thermal cycles performed, 12 down to 350 °C and 3 to ambient temperature

Degradation after thermal cycles was 10.3 %



20 forced redox cycles performed with 50 ml/min O<sub>2</sub> on the anode side per layer  
Increase of power density after 5 cycles (Improving contact Ni-YSZ?)  
Degradation of the stack was 9.1 % after 20 redox cycles

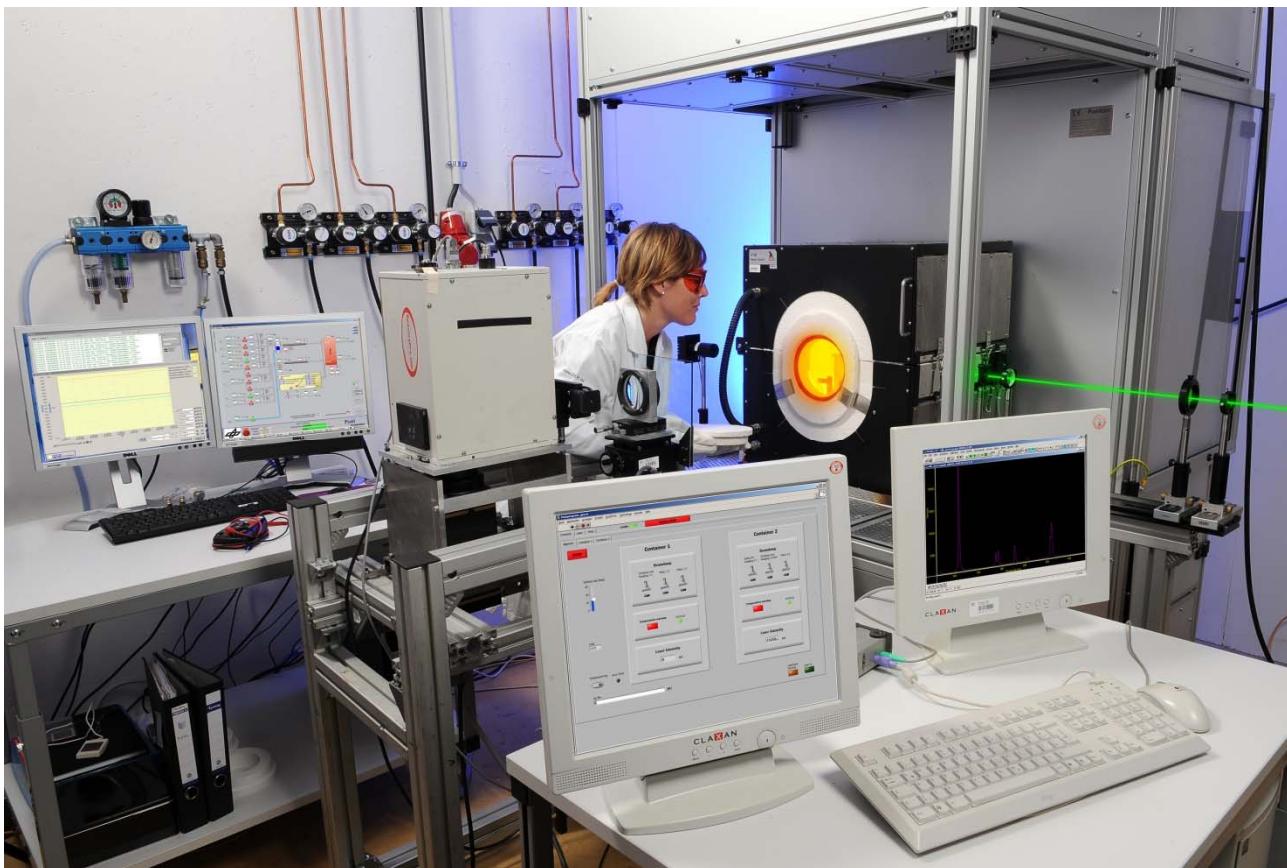
# Measurement Setup for Segmented Cells



- 16 galvanically isolated segments
  - Local and global i-V characteristics
  - Local and global impedance measurements
- Local temperature measurements  
Local fuel concentrations  
Flexible design: substrate-, anode-, and electrolyte-supported cells  
Co- and counter-flow



# Experimental Setup for Raman Spectroscopy Measurements



# **Beyond the 3<sup>rd</sup> Gen. SOFC: Issues to be addressed for improving MSCs**

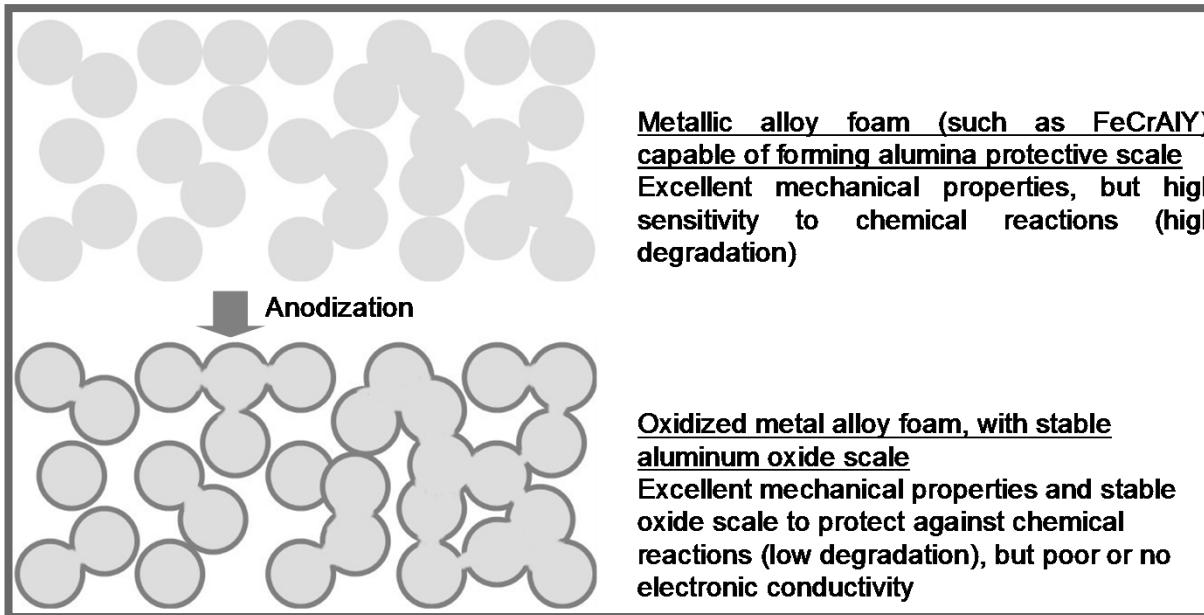
- Cr-poisoning at the cathode side > Protective coating required
- Improve tolerance toward sulfur poisoning
- Lifetime of metal substrate if stationary applications are considered
- Hermetic electrolyte

Which materials and architecture  
for the next generation SO(F)C?



# Beyond the 3<sup>rd</sup> Generation SOFC

*Metal substrate resistant toward oxidation*

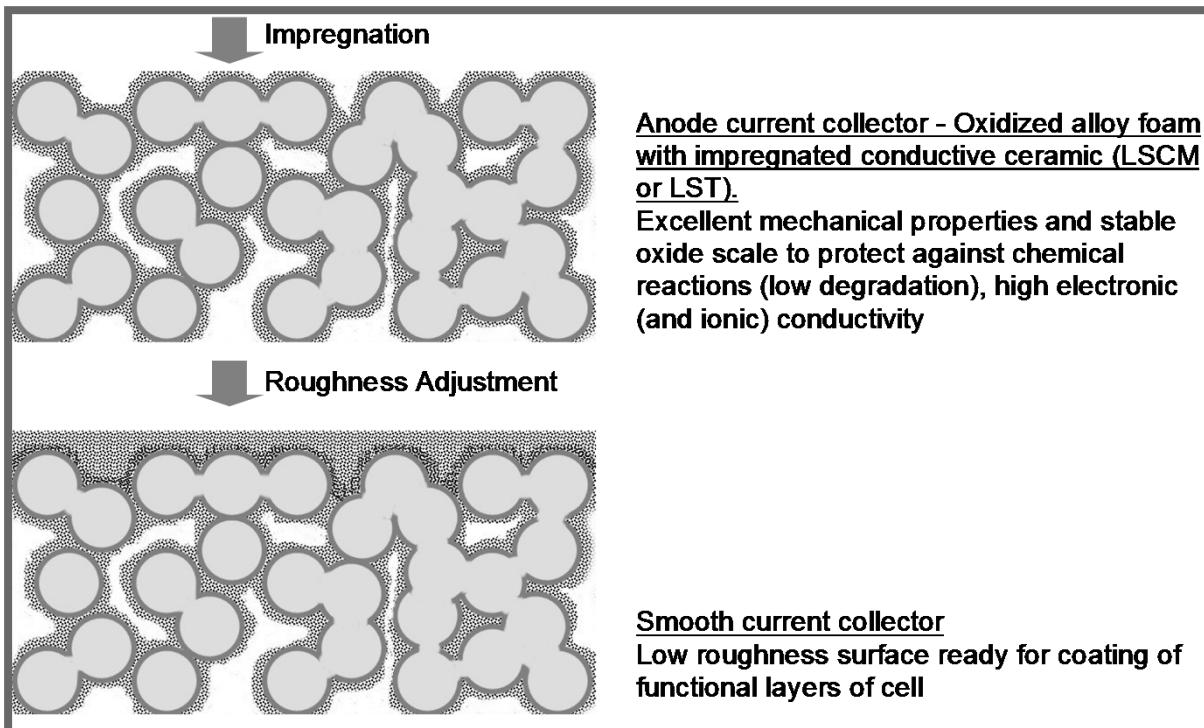


***Formation of an  $Al_2O_3$  layer as a durable protective coating***

***Al rich alloys, on the basis of  $MCrAl(Y)$  with M being Fe, Ni, Co or a mixture***



# Nickel-free Hybrid Metal-Ceramic Supported SOFC



***Infiltration with an electronic conductor (ideally a ceramic)***

**Dense  $\text{La}_{0.1}\text{Sr}_{0.9}\text{TiO}_3$  ( $800^\circ\text{C}$ ): sintering in  $\text{H}_2$ :  $\sigma_{\text{tot}} \approx 150 \text{ S/cm}$**

O. Marina et al. Solid State Ionics, 149 (2002) 21-28.

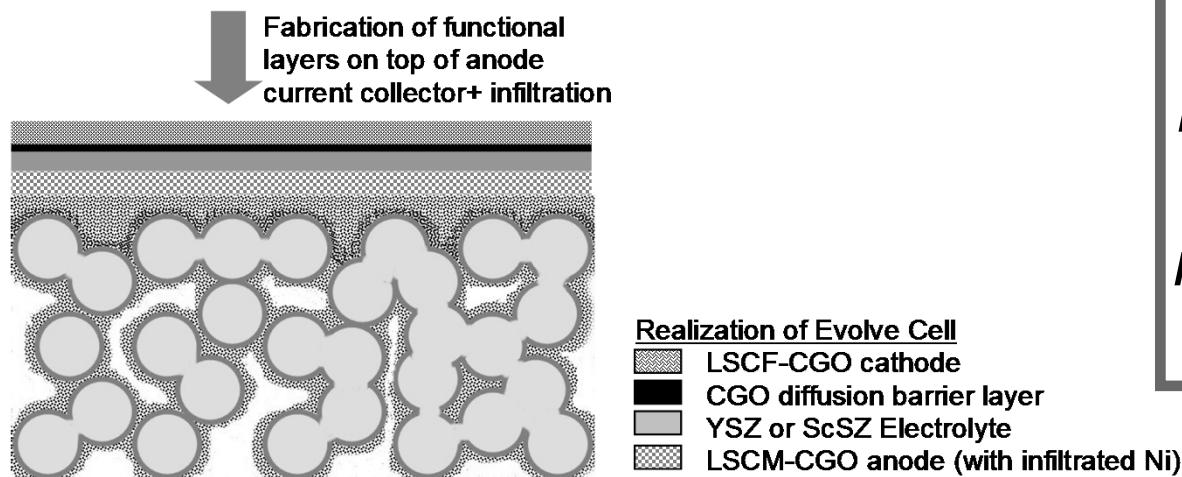
S. Hashimoto et al. Journal of Alloys and Compounds, 397 (2005) 245-249.

Y. Tsvetkova et al. Materials and Design, 30 (2009) 206-209.

***Hybrid current collector mechanically and chemically stable in both oxidant and reducing atmosphere***



## Beyond the 3<sup>rd</sup> Generation SOFC



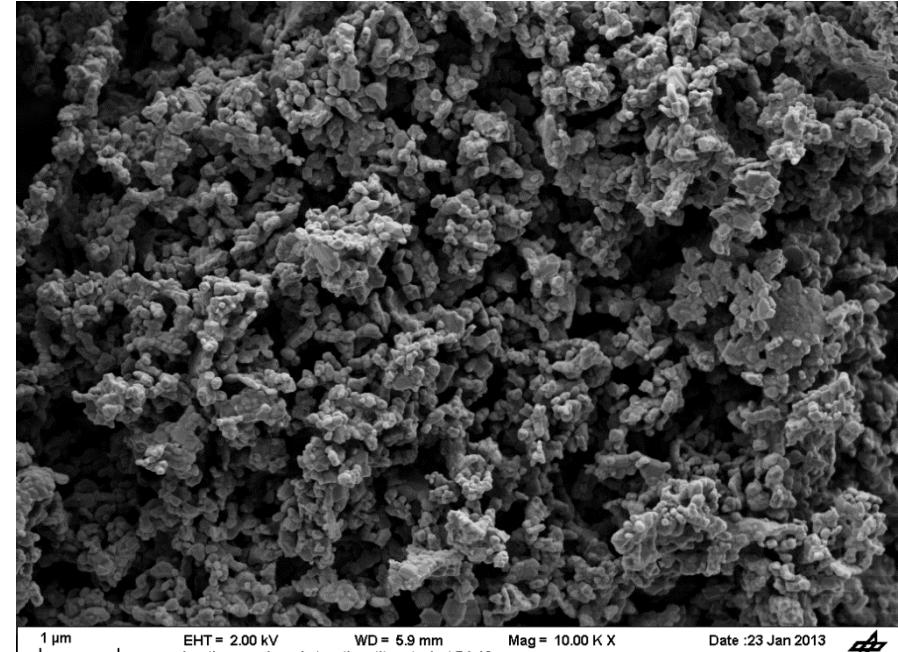
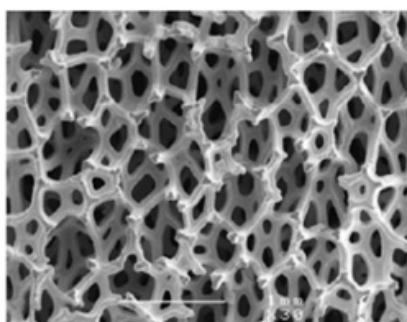
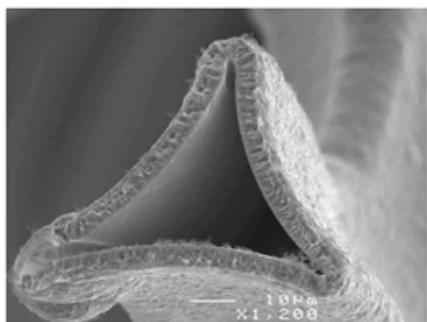
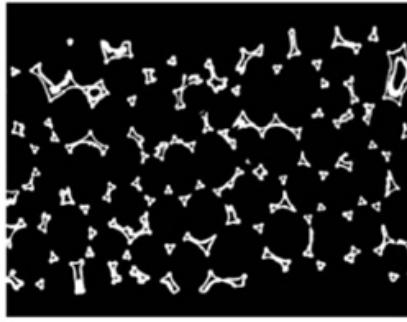
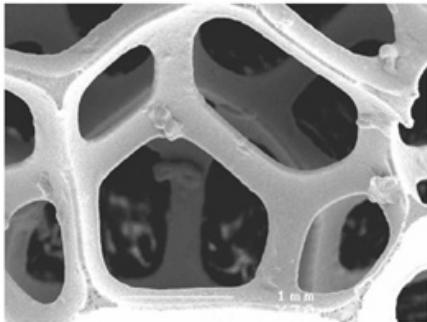
*Use of perovskite materials at the anode and cathode, being modified by addition of suitable catalysts*

***High power density, sulfur resistant, fuel flexibility, thermal cycling, redox cycling***

***Stationary applications ...***



## Beyond the 3<sup>rd</sup> Generation SOFC



Source: Alantum Europe GmbH

Metal Foam: NiCrAl

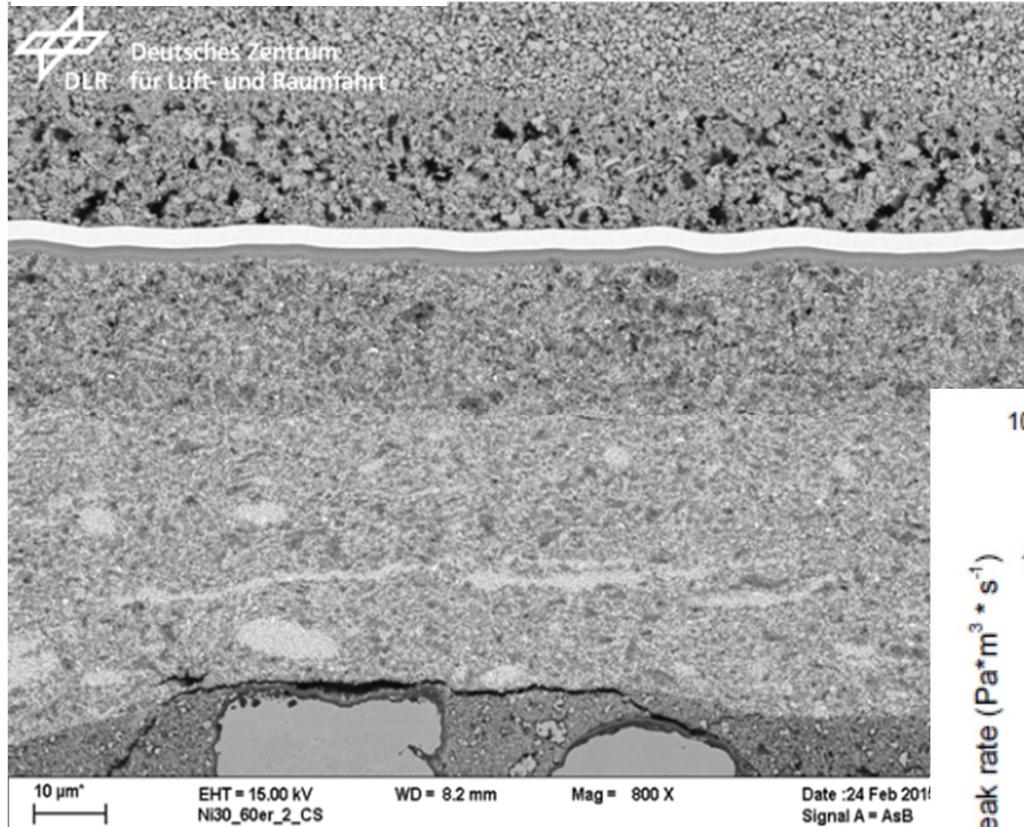
Composition of the anode:  $Ce_{1-x}Gd_xO_{2-\alpha}$  /  $La_{0,1}Sr_{0,9}TiO_{3-\alpha}$

Electrolyte: 8-YSZ / 10-GDC

Cathode :  $La_{0,4}Sr_{0,6}Co_{0,2}Fe_{0,8}O_{3-\alpha}$



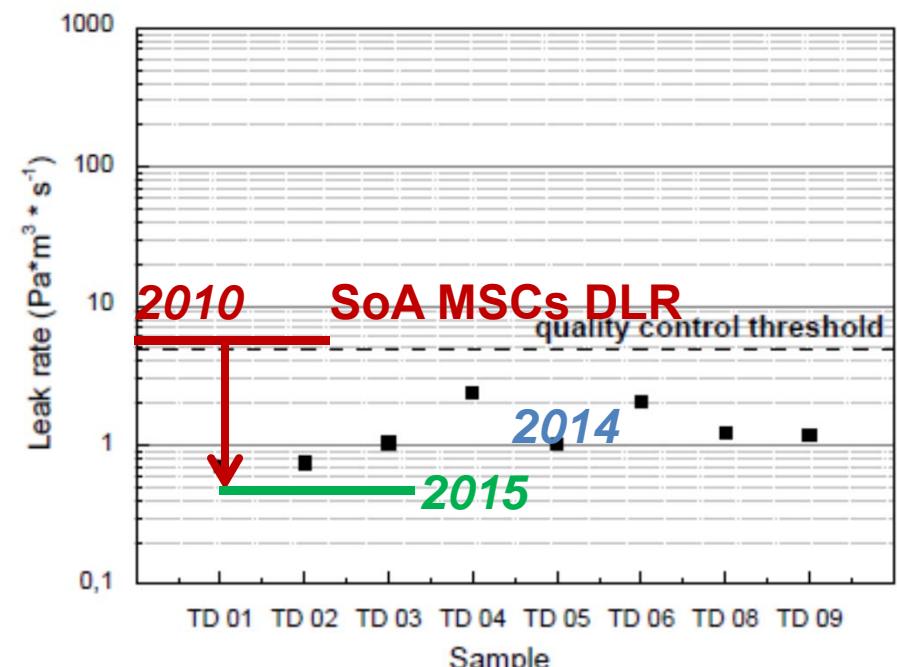
## Beyond the 3<sup>rd</sup> Generation SOFC



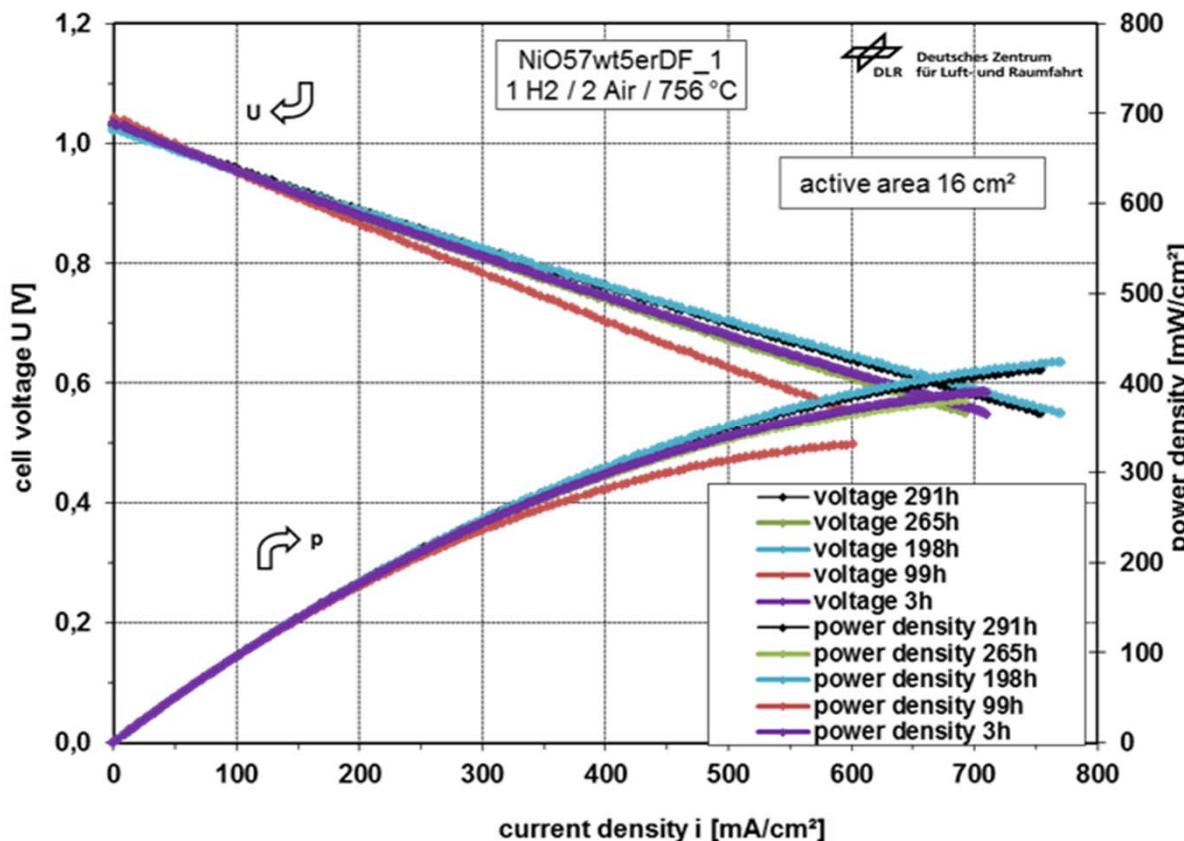
*Manufactured in air (except PVD layer)*

*Perovskite based anode*

*Thin film electrolyte (1  $\mu\text{m}$  YSZ+  
2  $\mu\text{m}$  CGO) with improved  
hermiticity (in collaboration with  
Ceraco GmbH)*



# Beyond the 3<sup>rd</sup> Generation SOFC



50 mm x 50 mm with active surface 16 cm<sup>2</sup>

**P @ 0.7V and 750°C**

- 340 mW /cm<sup>2</sup>
- Redox cycles tested: 10

➤ But... with addition of Nickel!!!

AFL: LST-CGO 50:50  
modified with 5 wt% Nickel  
Current collector: NiCrAl +  
LST 50vol% - Ni 50vol%

- Issue with sulfur poisoning still expected

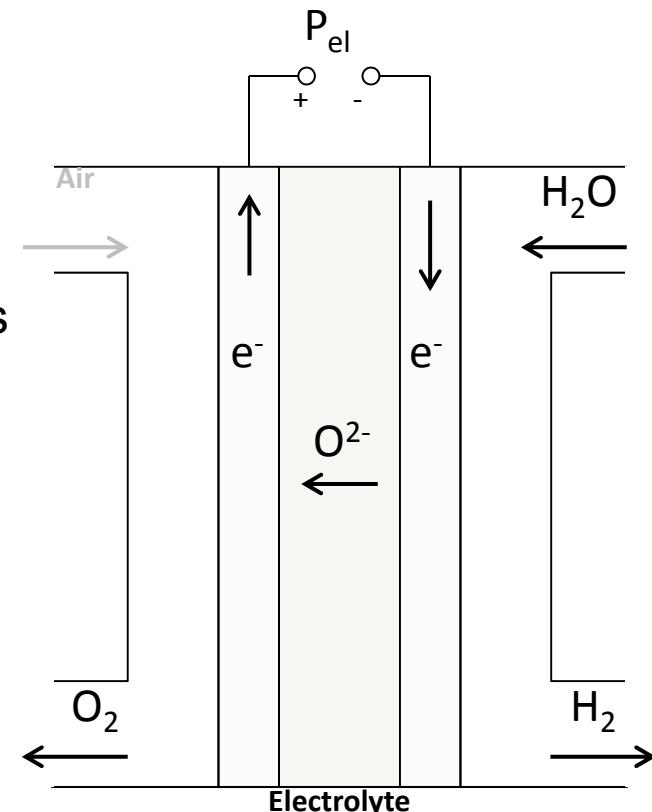
Replacement of Nickel still remains challenging!



# Solid Oxide Electrolysis

## Advantages:

- High temperature (600 - 900°C)
  - Fast reaction kinetics
  - Low overvoltage
  - High efficiency & high current densities
- No noble metals as catalysts
- Fuel versatility:  $\text{CO}_2$  electrolysis
  - Co-electrolysis of  $\text{H}_2\text{O}/\text{CO}_2$  possible
  - Syn-gas production
  - External (or internal) hydrocarbon formation

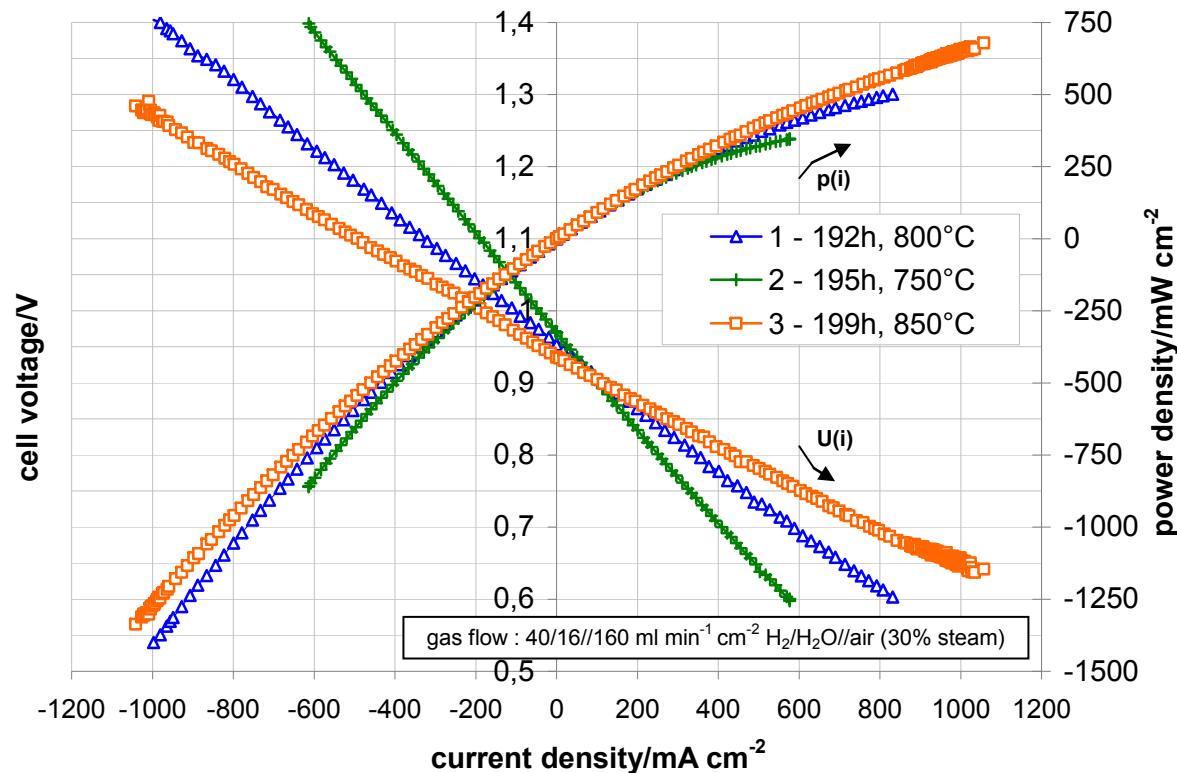


Anode -  
Oxygen electrode

Cathode -  
Fuel electrode

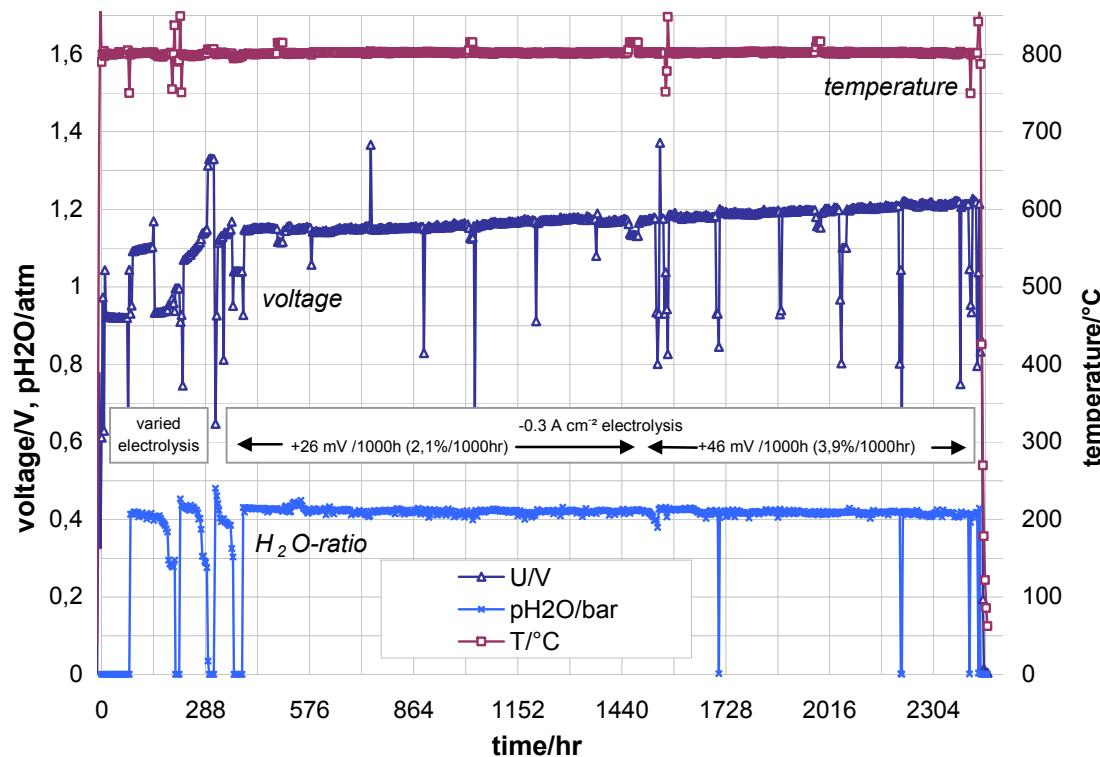


# Hi2H2: I-V Curves of a VPS Cell in SOFC and SOEC Mode as a Function of Temperature



Hi2H2:

# Complete Test Run of a VPS Cell in Electrolysis Mode



Lit: G.Schiller et al., J. Appl. Electrochem., 39, 293-301, 2009



# Challenges in SOEC technology

- Improvement of performance and particularly durability (reduced degradation) by
  - Development of improved materials (cathodes and anodes) for steam electrolysis
  - Study of degradation behaviour and elaboration of mitigation strategies
- Integration of high-temperature heat (solar heat, waste heat from industrial processes)
- Development of operation strategies with use of integrated heat (heat management)
- Development of co-electrolysis process (steam + CO<sub>2</sub>) for production of synthetic fuels
  - Development of cells for co-electrolysis operation
  - Development of electrocatalysts for synthesis of liquid and gaseous fuels
  - Operation at elevated pressure conditions > 10 bar
  - Development of system concepts and demonstration of functionality
- Efficient operation in bi-functional mode

Development work at DLR in the frame of internal project („Future Fuels“) and in POF III phase of Helmholtz Association (HGF) with a transportable research platform („e-Xplore“)



# Motivation and Objective of Systematic Degradation Study

## Problem: low longevity – degradation

A variety of long-term degradation data

- about 3-5% / 1000h at 800°C and 80% absolute humidity (AH)
- about 35% / a

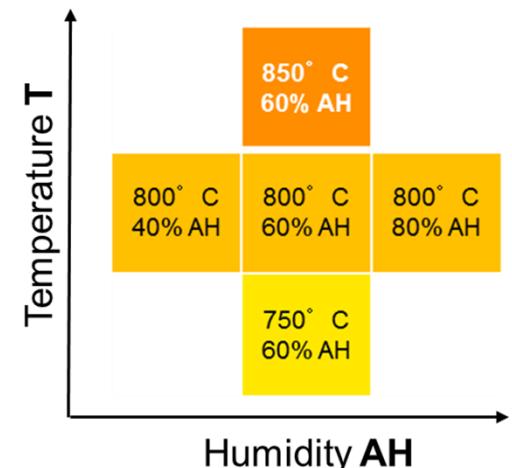
Different studies hard to compare!

Systematic parameter study of:

- Temperature T
- Humidity AH
- Current density i

Test setup – quadruple cell measurement

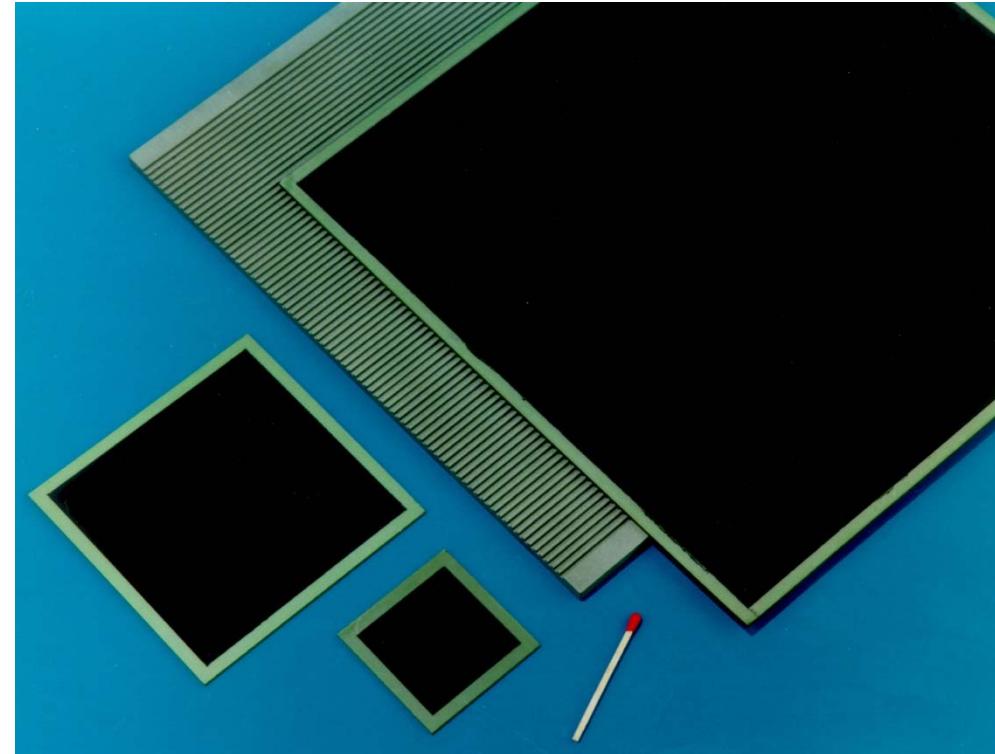
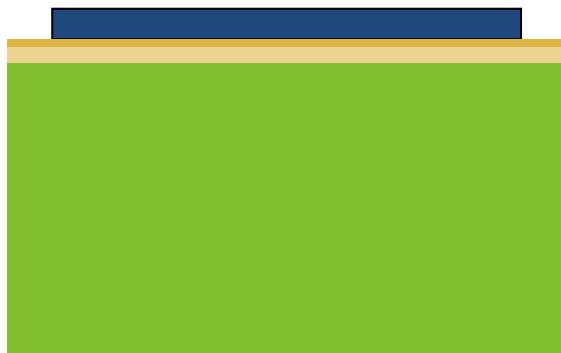
- Four different current densities simultaneously
- Identical temperature, gas supply (and also incidents)



# Solid Oxide Fuel Cells: Planar Design

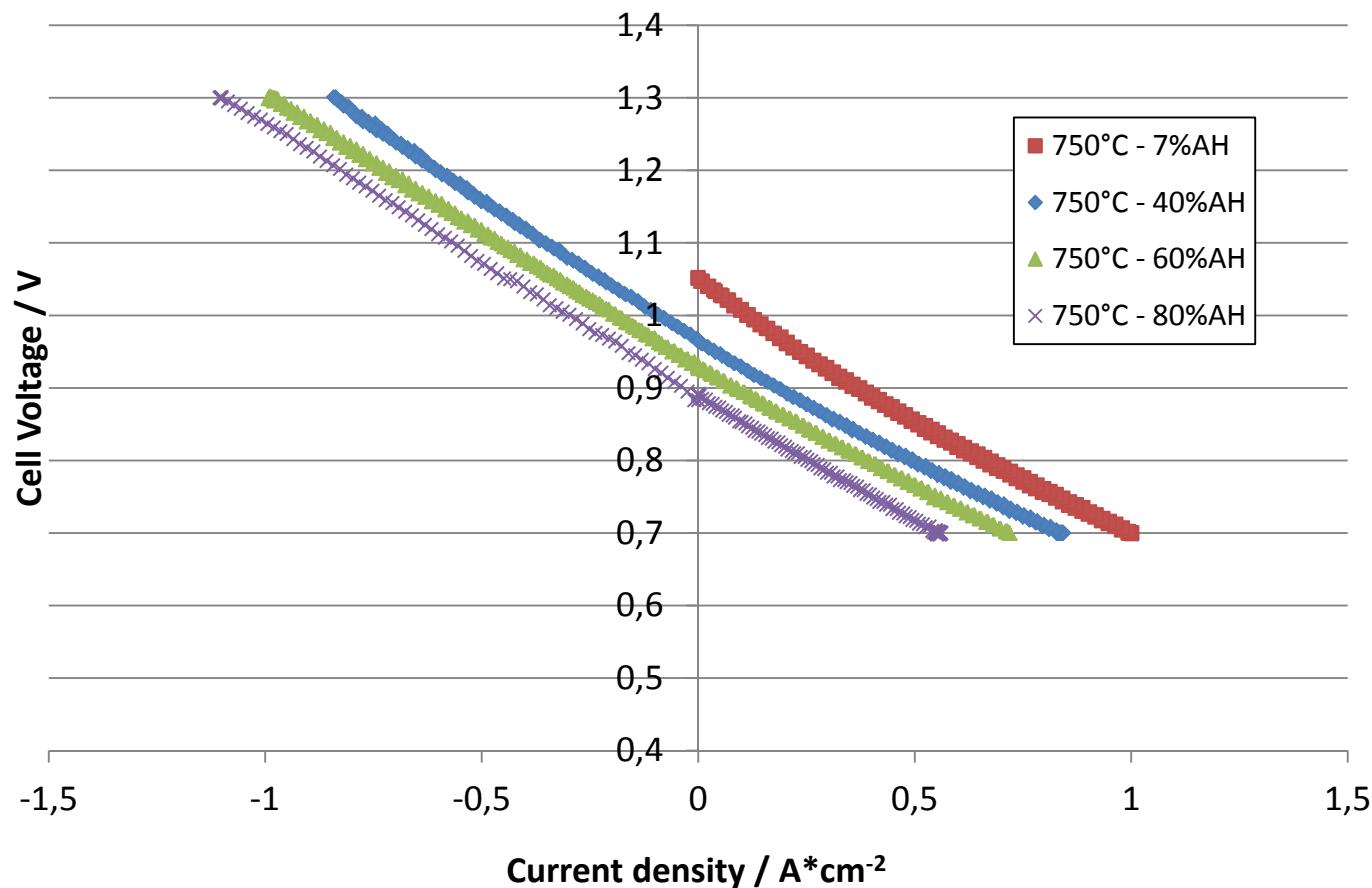
## Materials

Cathode:  $(\text{La}, \text{Sr})(\text{Fe}, \text{Co})\text{O}_3$   
Diffusion barrier: CGO – 1-5  $\mu\text{m}$   
Electrolyte: 8YSZ – 5-10  $\mu\text{m}$   
Anode: Ni/YSZ  
Anode Substrate: Ni/YSZ  
Interconnect: ferritic steel



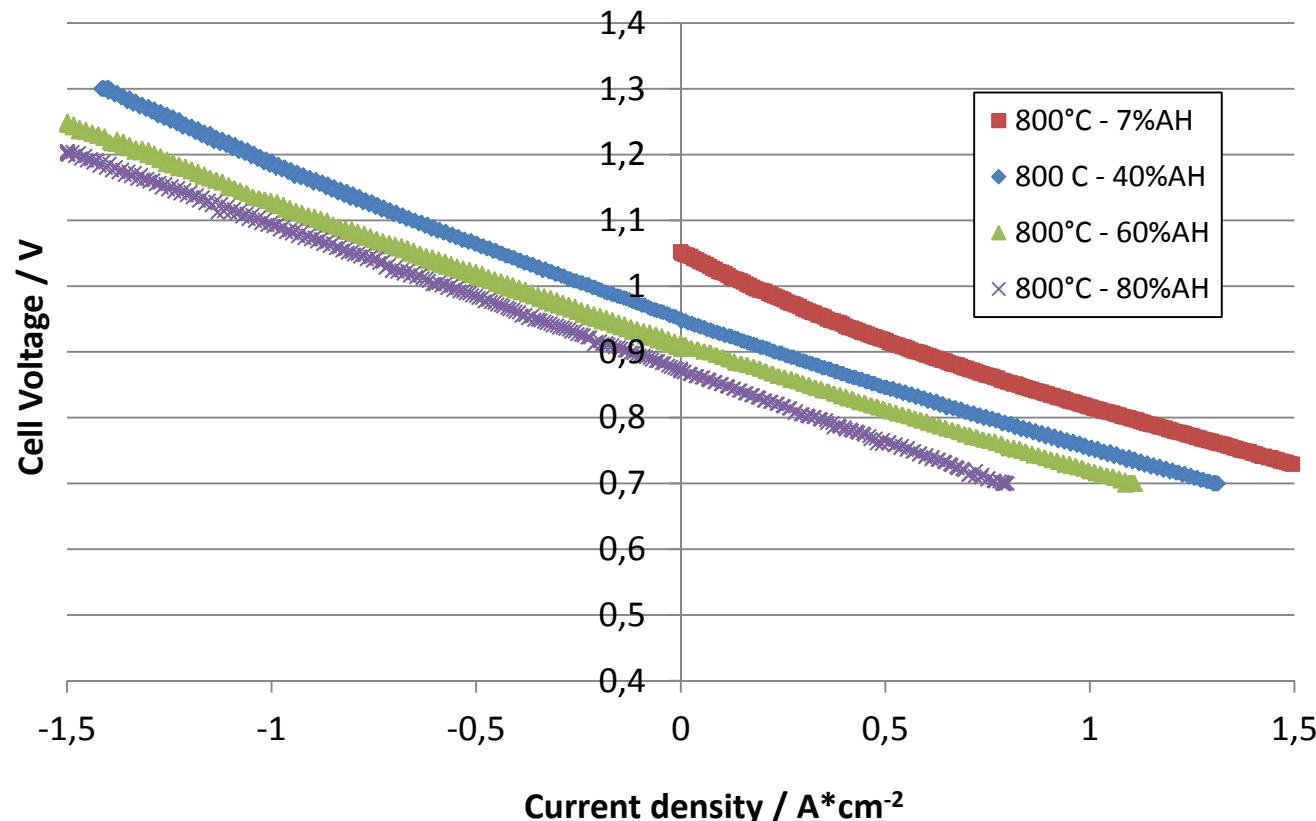
# I-V Curves at 750 °C as a Function of Steam Content

(Flow rates: 2 l/min H<sub>2</sub>/H<sub>2</sub>O, 3 l/min air)

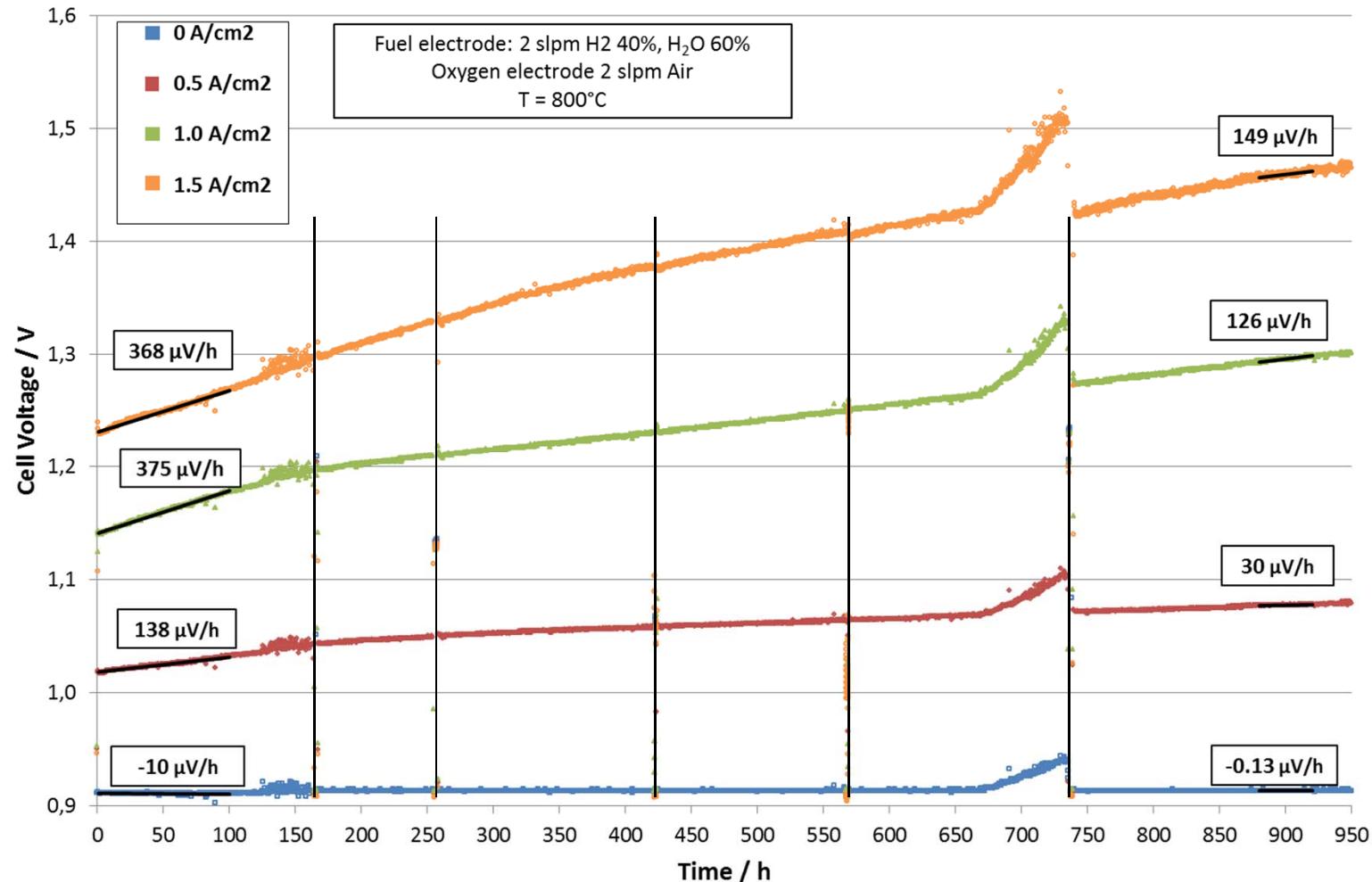


# I-V Curves at 800 °C as a Function of Steam Content

(Flow rates: 2 l/min H<sub>2</sub>/H<sub>2</sub>O, 3 l/min air)



# Degradation Measurements

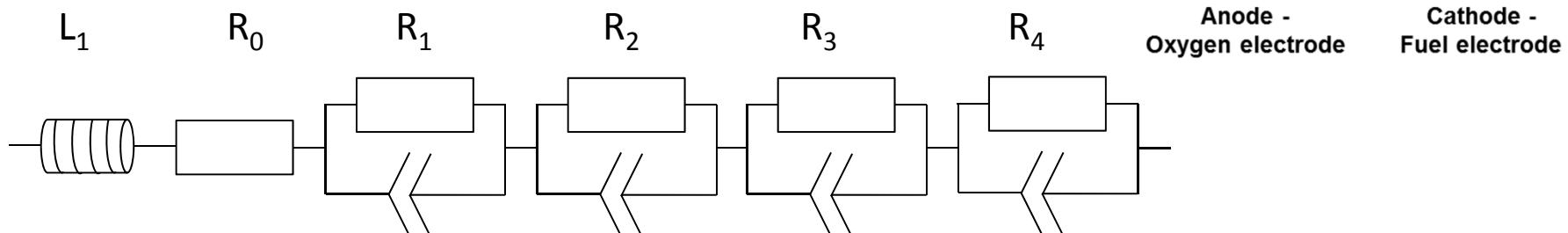
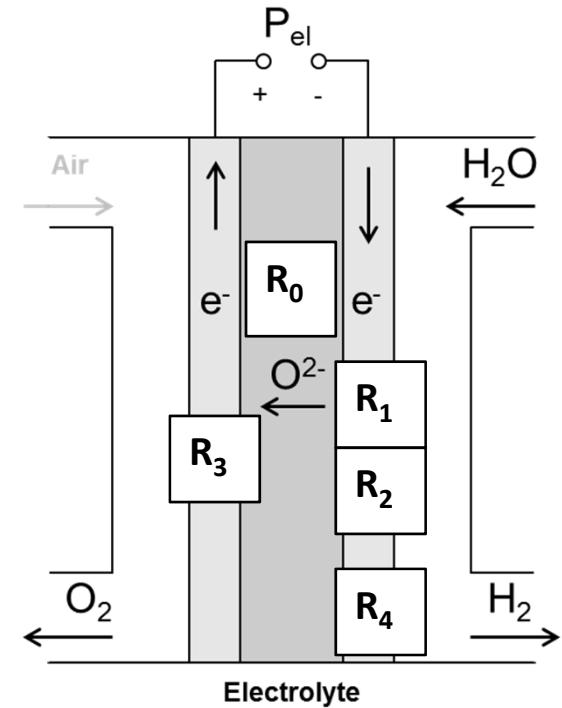


# Degradation Measurements

## Impedance analysis – equivalent circuit

High freq. ( $10^5$  Hz)  $\longrightarrow$  Low freq. (0.5 Hz)

- $L_1$ : High frequency interference ( $\sim 10^5$  Hz)
- $R_0$ : Ohmic resistance ( $\sim 10^5$  Hz)
- $R_1$ : Fuel electrode process A ( $\sim 10^4$  Hz)
- $R_2$ : Fuel electrode process B ( $\sim 10^3 - 10^4$  Hz)
- $R_3$ : Oxygen electrode process ( $\sim 10^2$  Hz)
- $R_4$ : Fuel electrode mass transport ( $\sim 10^1$  Hz)

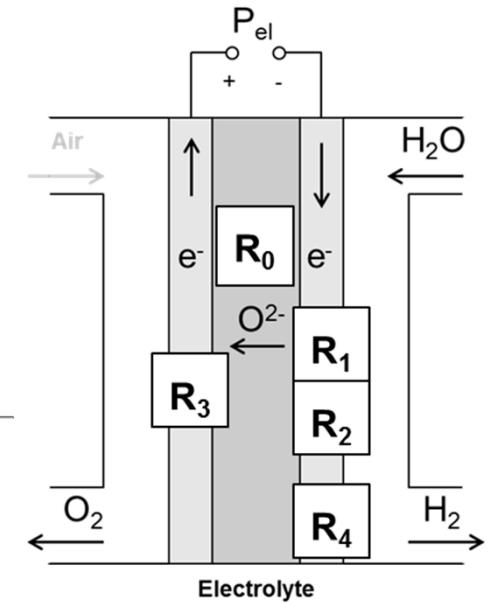
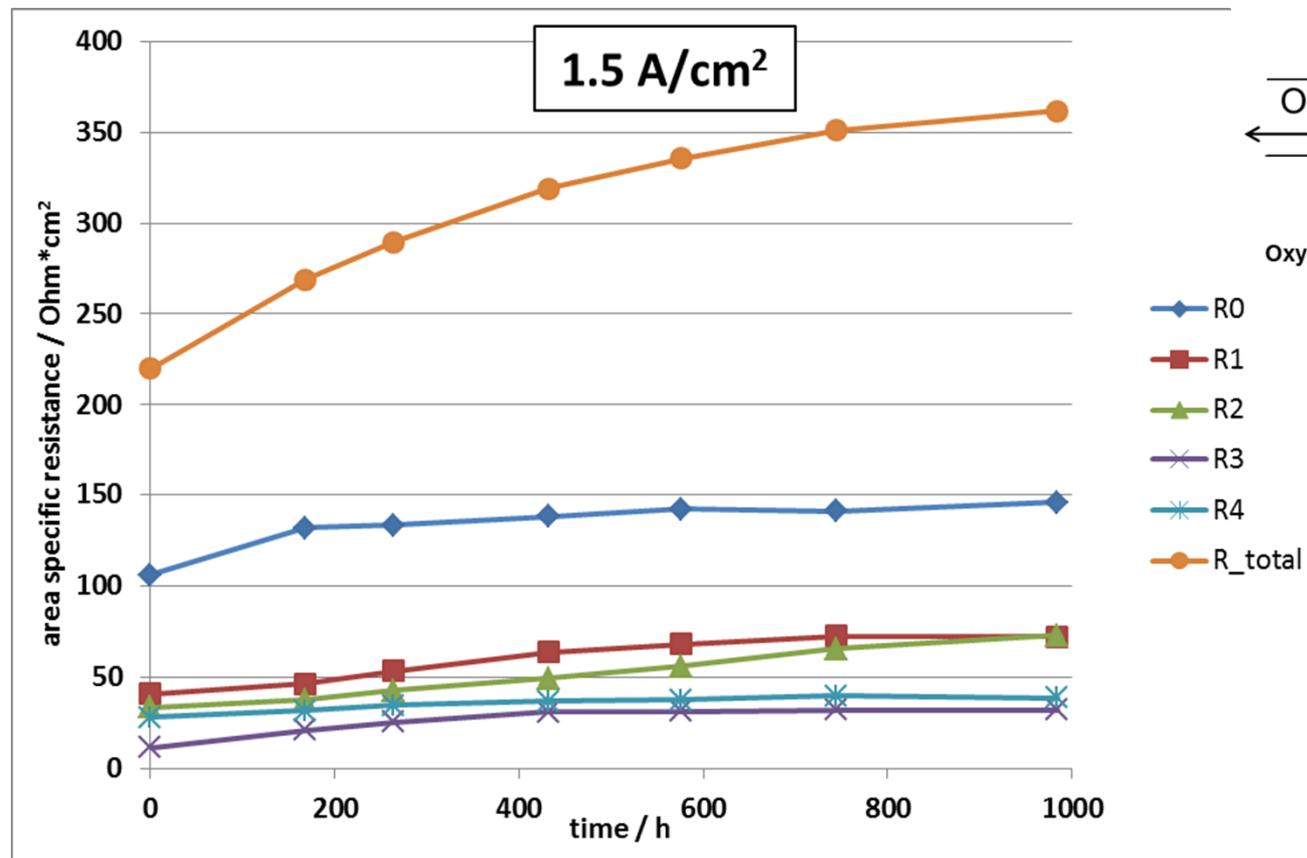


A. Leonide, V. Sonn, A. Weber, and E. Ivers-Tiffée  
Journal of The Electrochemical Society, 155 (1) B36-B41 (2008)



# Degradation Measurements

Change of each resistive process with time



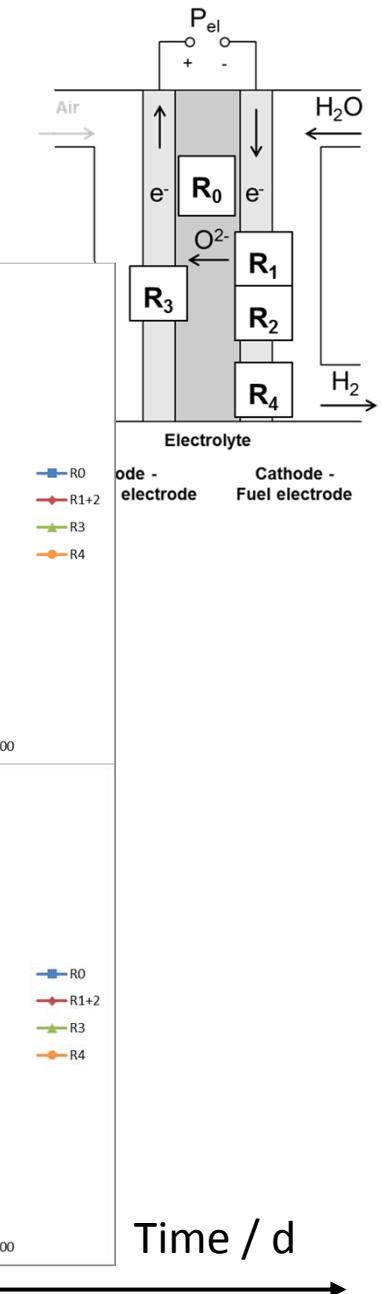
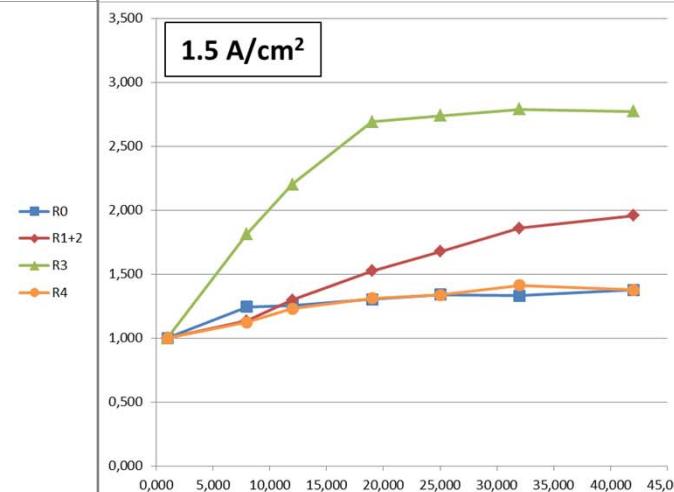
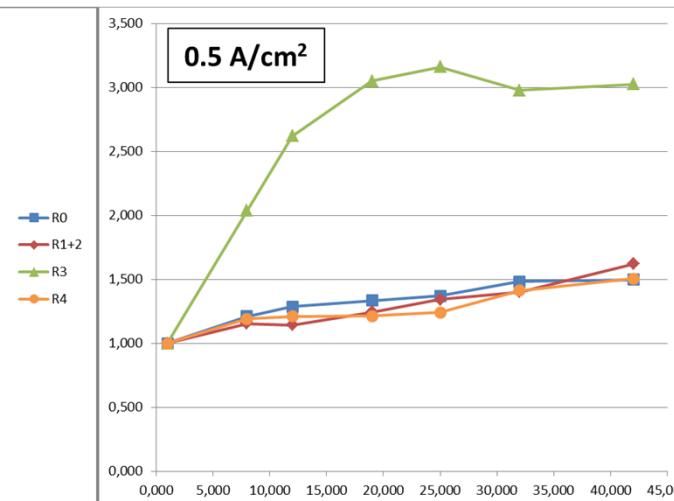
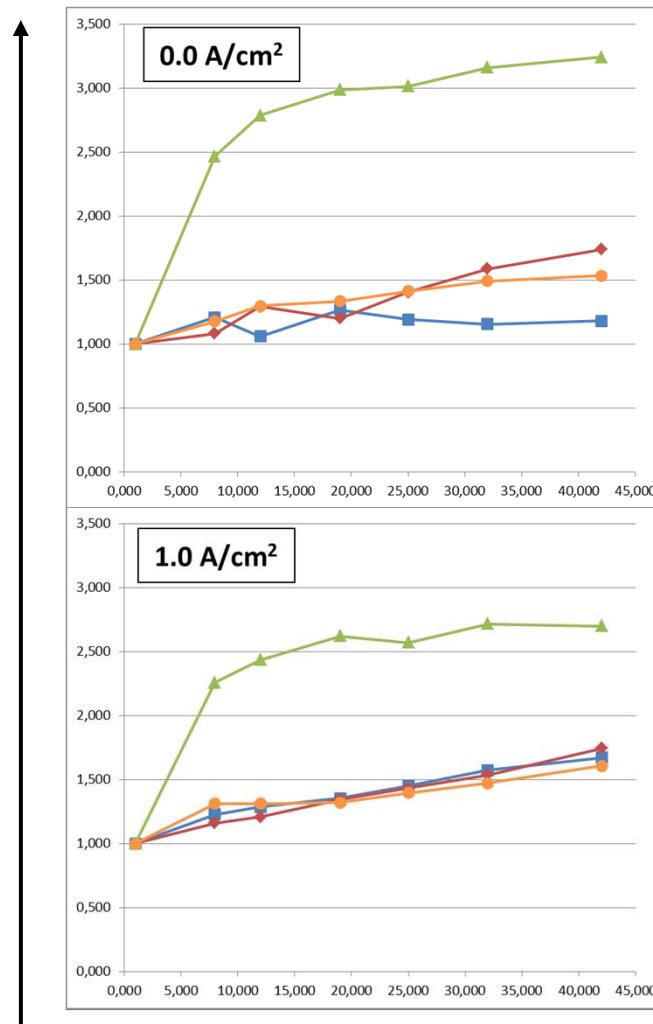
Anode - Oxygen electrode      Cathode - Fuel electrode

- $\diamond$   $R_0$
- $\blacksquare$   $R_1$
- $\blacktriangle$   $R_2$
- $\times$   $R_3$
- $\ast$   $R_4$
- $\bullet$   $R_{\text{total}}$

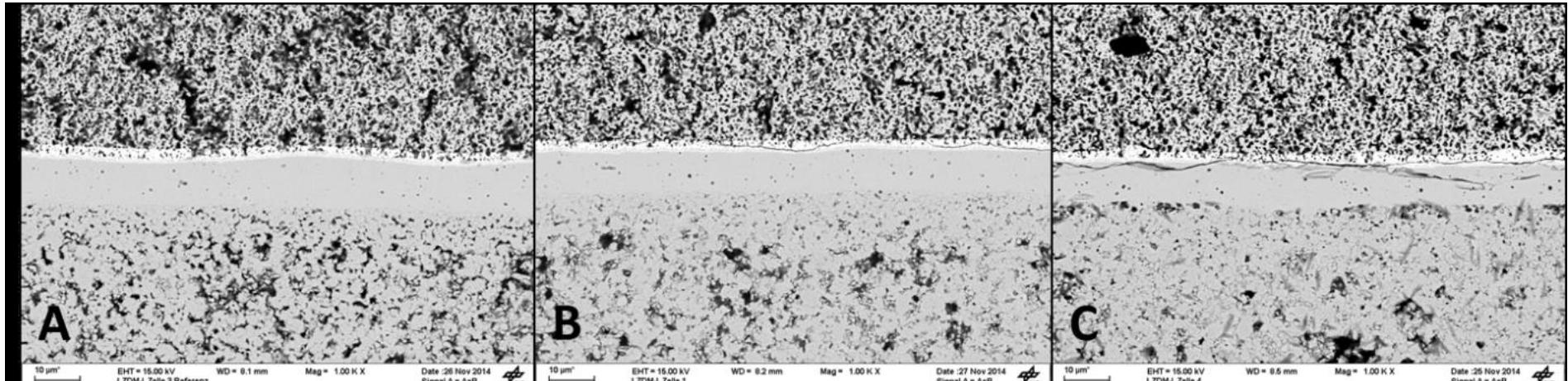
Bias:  $0.5 \text{ A/cm}^2$

# Degradation Measurements

Relative change in resistance / A.U.



# Post mortem Analysis (SEM)



Solely reduced

1000 h @ OCV

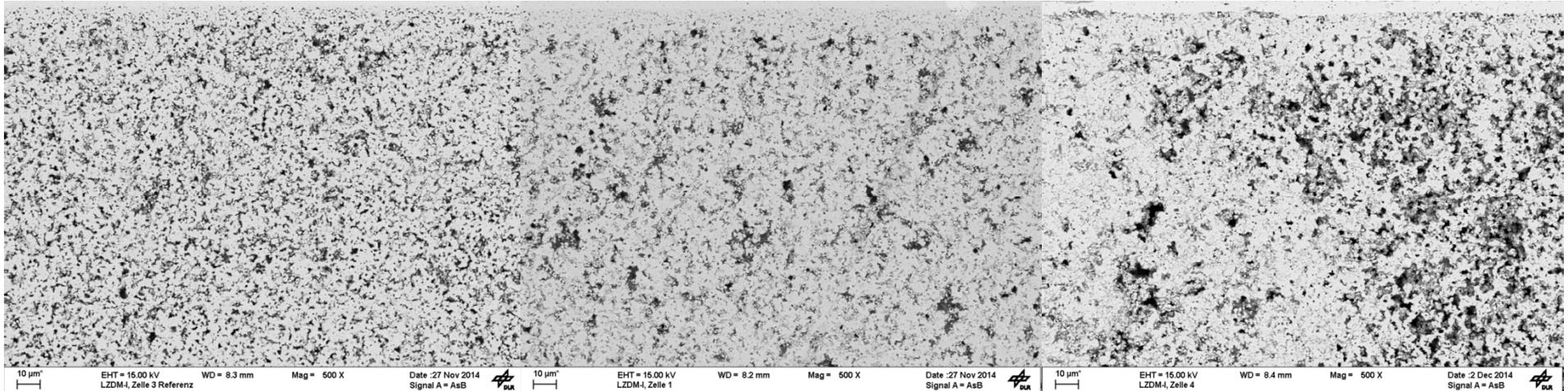
1000 h @ 1.5 A/cm<sup>2</sup>

## Ohmic resistance:

- Weakening of YSZ|CGO|LSCF interface
- Visible cracks probably formed during sample preparation along weakened microstructure



# Post mortem Analysis (SEM)



Solely reduced

1000 h @ OCV

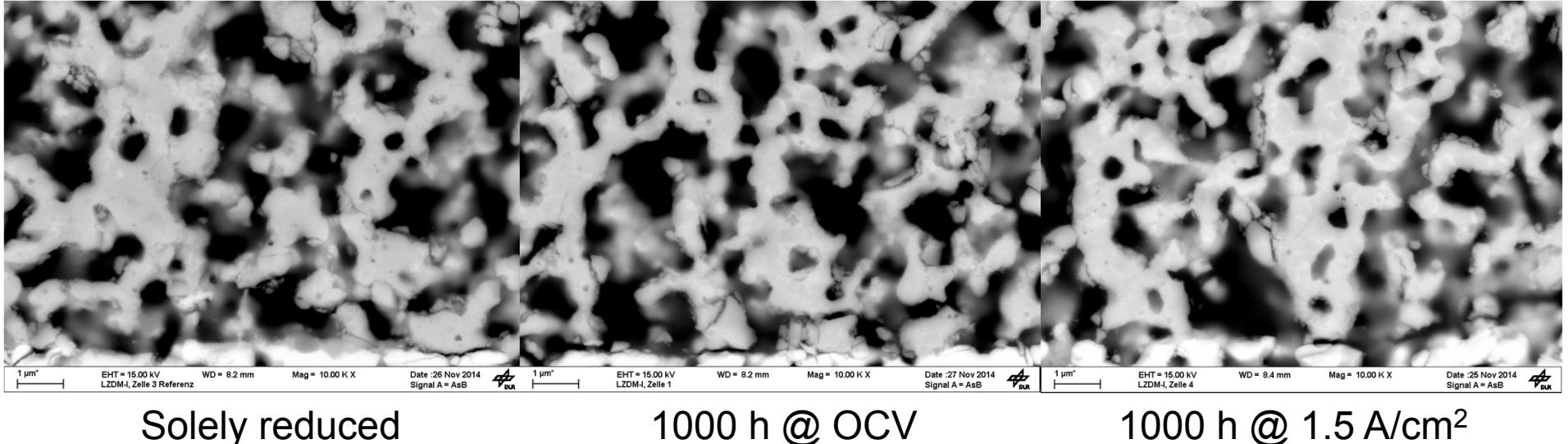
1000 h @ 1.5 A/cm<sup>2</sup>

## Fuel electrode:

- Change in microstructure
- Likely due to Ni-coarsening
- → decrease TPB
- Decreased percolation ?



# Post mortem Analysis (SEM)

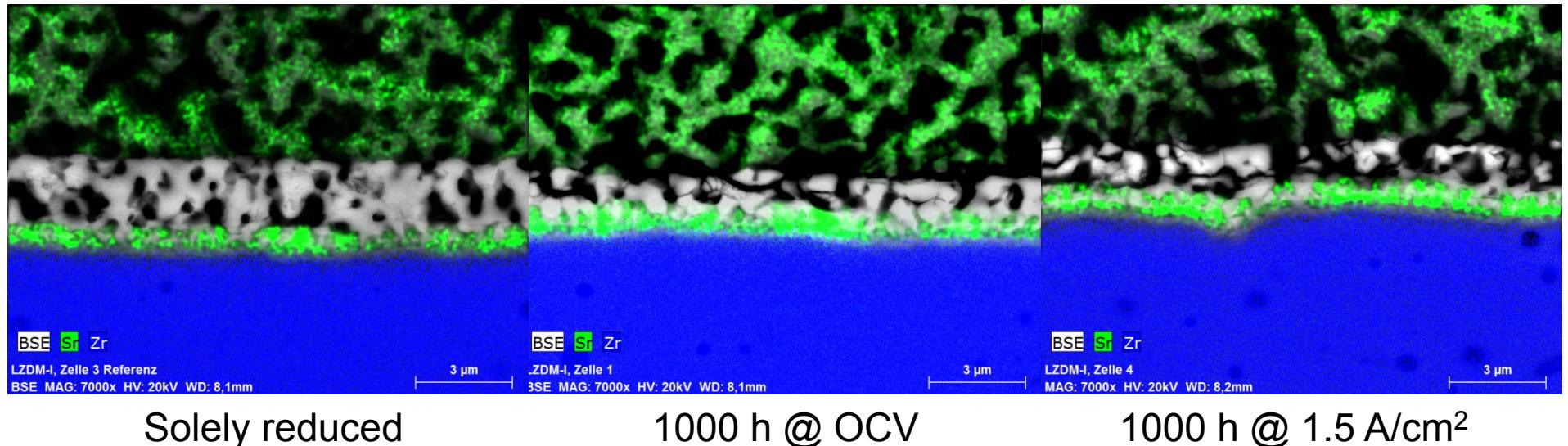


## Oxygen electrode:

- No obvious change in microstructure
- Appearance of brittleness
- Degradation due to change in perovskite stoichiometry close to surface  
→ Sr-rich surface layer?
- Difficult to measure surface sensitively with high focus XPS

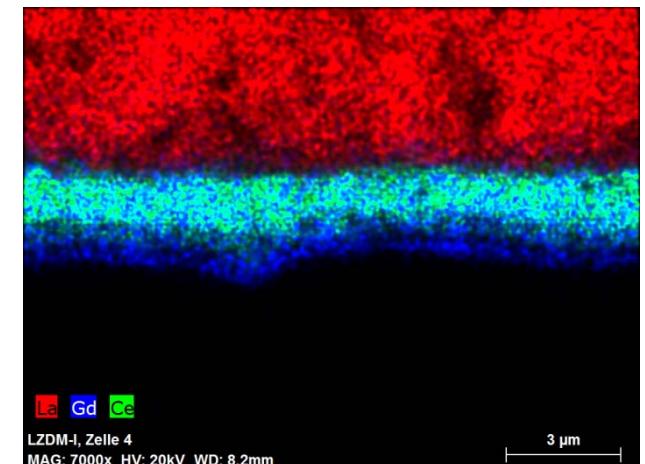


# Post mortem Analysis (SEM)



## Diffusion barrier layer:

- No reaction between Sr and Zr (or generally LSFC with YSZ)
- General Sr-enrichment at CGO|YSZ interface
- Ce depletion at CGO|YSZ interface



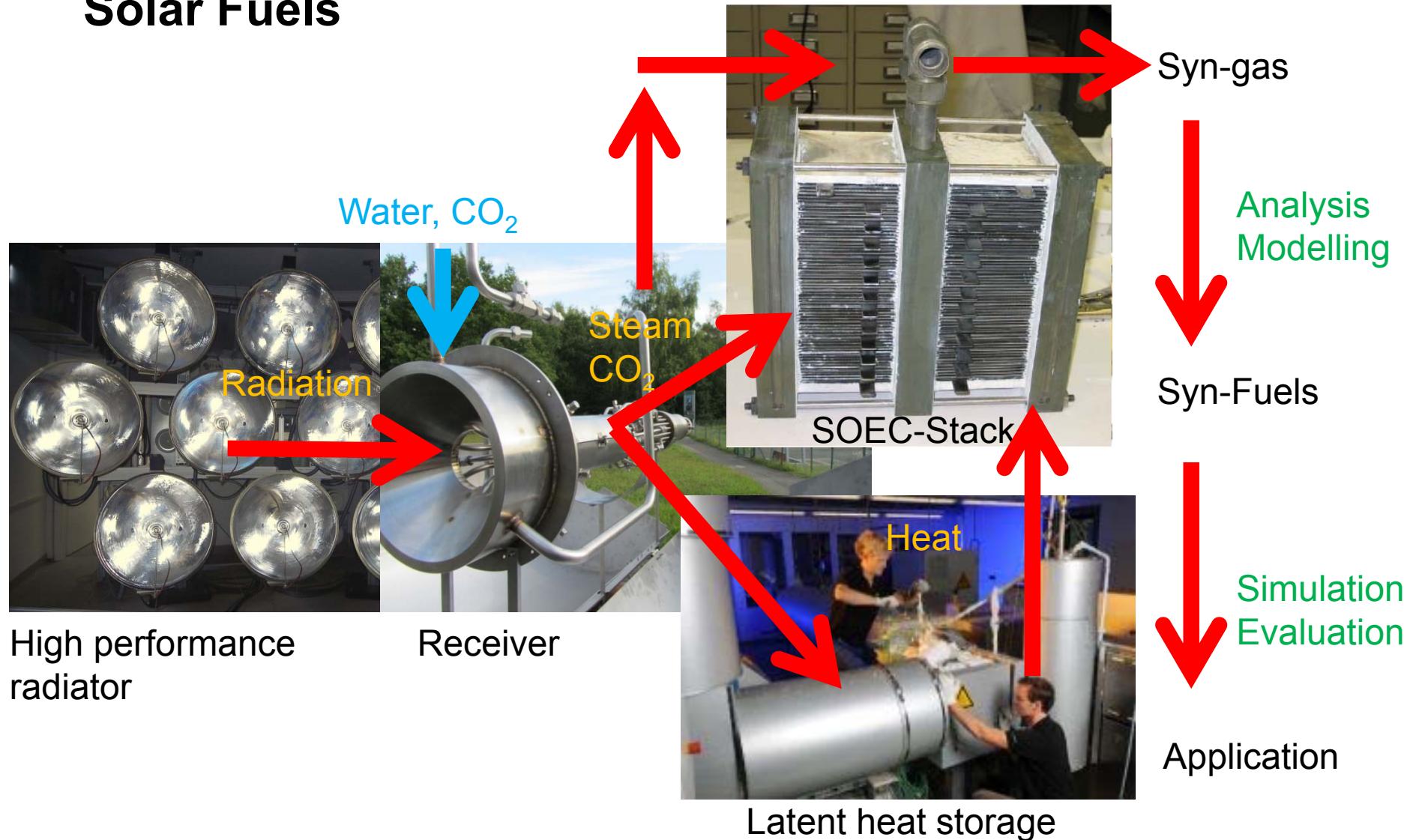
# Future Fuels: TP 3 Solar Fuels

**DLR Internal Project: SF, TT, VT, AT**

- **Objective:**
  - Production of synthetic liquid hydrocarbons through solarthermal and solarelectrical processes
- **Duration: 2015-2017**



# Solar Fuels



# Conclusion

- Plasma sprayed metal supported cell technology has been developed
- Stability of ferritic stainless steel against corrosion remains an issue for long-term operation.
- Use of perovskite as current collector and anodic electro-catalysts are still challenging because of the reduced electronic conductivity and the stringent manufacturing parameters required for high performance
- Current and future SOEC activities in cell degradation, co-electrolysis and synthetic fuel production



## Acknowledgment

I'd like to thank my co-workers Dr. Asif Ansar, Dr. Rémi Costa and PhD student Michael Hörlein for their scientific work as well as all other members of my group for their strong effort.

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