

Physically based modeling and simulation of a LiFePO₄-based lithium-ion battery

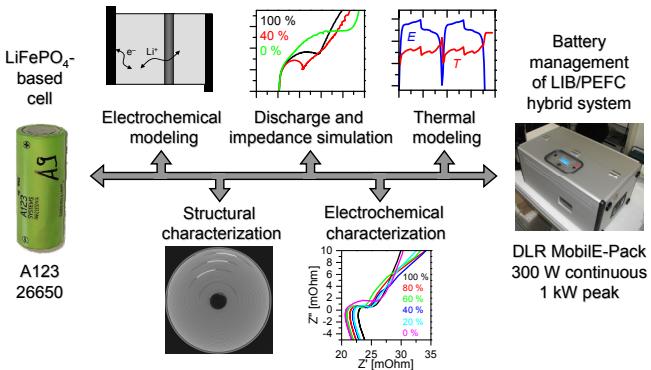
C. Hellwig, D. N. Fronczek*, S. Sörgel and W. G. Bessler

German Aerospace Center (DLR), Institute of Technical Thermodynamics, Stuttgart, Germany

*E-mail: david.fronczek@dlr.de

Goal and approach

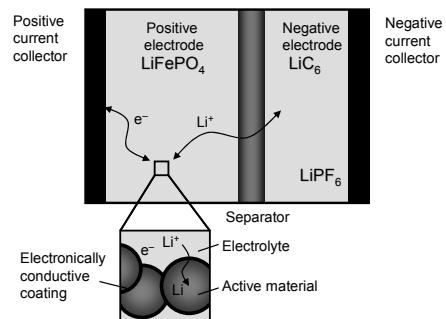
Goal: Impedance-based SOC diagnostics of LiFePO₄ cells



Multi-scale modeling

Mass and charge transport is modeled on particle and repeat unit scale.

- Li⁺ charge transport in electrolyte: 100 μm scale
- Li transport in solid phase: ~100–1000 nm scale



Model

Parameters:

• LiPF ₆ Concentration:	1.5 mol l ⁻¹
• Li ⁺ and PF ₆ ⁻ diffusion coefficient:	1·10 ⁻¹⁰ m ² s ⁻¹
• Thickness (anode / separator / cathode):	40 μm / 20 μm / 80 μm
• Bulk diffusion coefficients (LiC ₆ / LiFePO ₄):	1·10 ⁻¹⁴ m ² s ⁻¹ / 1·10 ⁻¹⁶ m ² s ⁻¹
• Exchange current density:	3·10 ⁵ A m ⁻³
• Particle radius (anode / cathode):	1 μm / 0.1 μm

Thermodynamic data:

- Separation in enthalpy and entropy
- LiC₆: Y. Reynier, R. Yazami, B. Fultz, Journal of Power Sources 119–121 (2003) 850–855
- LiFePO₄: J. L. Dodd, PhD thesis, California Institute of Technology, 2007

Thermodynamics

- Empirical half-cell enthalpy, entropy

Kinetics

- Butler-Volmer kinetics
- Concentration overpotential

Solid-state transport

- Mass conservation
- Spherical diffusion in particle

Electrolyte transport

- Nernst-Planck equation
- Charge neutrality

Heat transport

- Ohmic, chemical heat production
- Heat conduction and convection

Cell voltage

$$\Delta\phi_{eq}(c_{Li}) = -\frac{\Delta G}{zF} = -\frac{\Delta H(c_{Li}) - T\Delta S(c_{Li})}{zF}$$

$$i = i_0 \left(\exp\left(\frac{zF}{RT}\eta_{act}\right) - \exp\left(-\frac{(1-\alpha)zF}{RT}\eta_{act}\right) \right)$$

$$\eta_{conc} = \frac{RT}{zF} \ln\left(\frac{c_0}{c(t)}\right) \quad \eta_{act} = \Delta\phi(t) - \Delta\phi_{eq}(c_{Li}) - \eta_{conc}$$

$$\frac{\partial \eta_{Li}}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 D \frac{\partial \eta_{Li}}{\partial r} \right) - \frac{M_{Li}}{zF} j$$

$$\frac{\partial c(x,t)}{\partial t} = \frac{\partial}{\partial y} \left(D \frac{\partial c}{\partial y} \right) + \frac{zF}{RT} \frac{\partial}{\partial y} \left(D_c c \frac{\partial \phi}{\partial y} \right) + \sum_i c_i z_i V$$

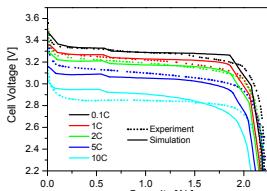
$$\frac{\partial (c_i z_i)}{\partial t} = \frac{\partial}{\partial y} \left(\lambda \frac{\partial T}{\partial y} \right) + Q_{chem} + Q_{ohm} - \alpha(T_{cell} - T_{env})$$

$$E = \phi_{cathode} - \phi_{anode}$$

Electrochemical behavior

Discharge curves

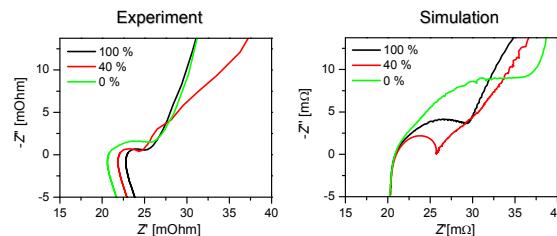
- Discharge curves starting from 100 % SOC at different discharge rates



- Flat discharge curve, voltage variation mainly from C₆ electrode
- Voltage losses at higher discharge rates due to transport limitations in electrodes

Electrochemical impedance spectra

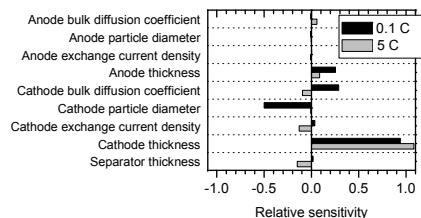
- Impedance spectra of an unpolarized cell at different SOC



- Considerable influence of SOC on impedance spectrum
- Impedance simulations are feasible, so far only qualitative agreement

Sensitivity analysis

- Sensitivity of cell parameters on discharge capacity



- Allows detailed insight into rate-limiting processes.
- Cathode is limiting component

Spatial concentration variations

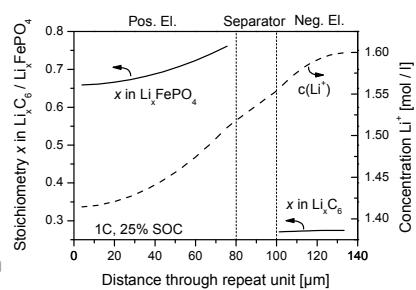
Concentration variation at SOC 25 % with 1C discharge rate:

Electrolyte:

- S-curve behavior of Li⁺ concentration in electrolyte
- No interaction with separator assumed

Bulk:

- Stoichiometry change during discharging in dependence on diffusion limitations in electrolyte



Outlook: Lithium-sulfur batteries

- Promising system for high-energy batteries (5× specific energy)
- Major challenge today: Limited cycle life
- New model will account for side reactions and other degradation mechanisms, allowing the study of cell aging

