

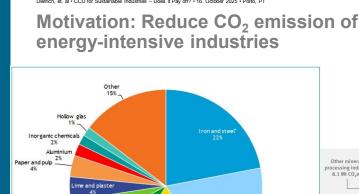
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CCU for Sustainable Industries Agenda





- 1. Motivation and goals
- 2. Techno economic and environmental assessment
 - 1. Technical
 - 2. Economic
 - 3. Environmental
 - 4. Weighing CO₂ reduction versus cost: CO₂ abatement cost
 - 5. Potential use of AI for TEA and LCA
- 3. Technological readiness
- 4. Conclusion and outlook





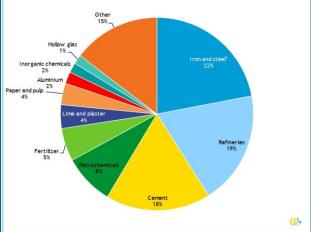


Fig. 1: Share of ${\rm CO_2}$ emissions in the total industrial ${\rm CO_2}$ emissions in the EU ETS in 2018 https://www.researchgate.net/publication/342707922_Energy-intensive_industries_Challenges_and_opportunities_in_energy_transition

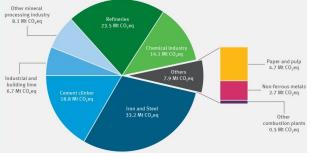


Fig. 2: Distribution of emissions in Germany among individual industrial sectors in 2022 and absolute emissions https://www.dehst.de/SharedDocs/downloads/EN/publications/2022_VET-Report.pdf?__blob=publicationFile&v=3

Dietrich, et. al • CCU for Sustainable Industries - Does it Pay off? • 16. October 2025 • Porto, PT Motivation: Reduce CO₂ emission of energy-intensive industries





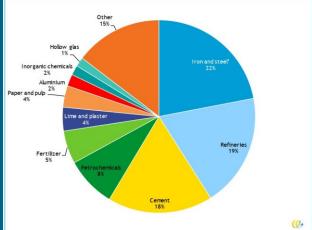


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Glass industry as an example for CCU implementation

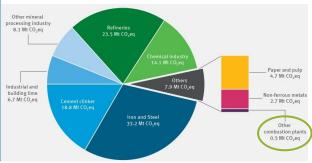
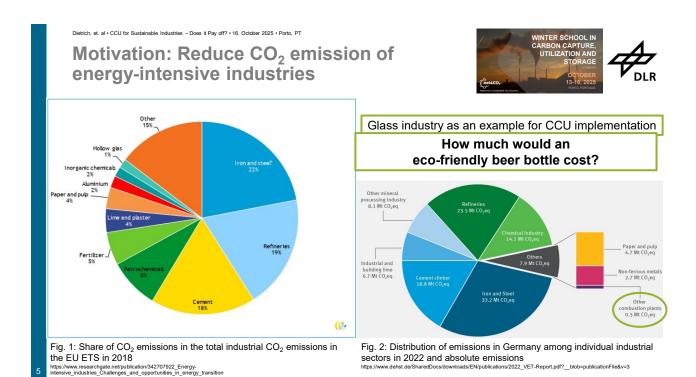
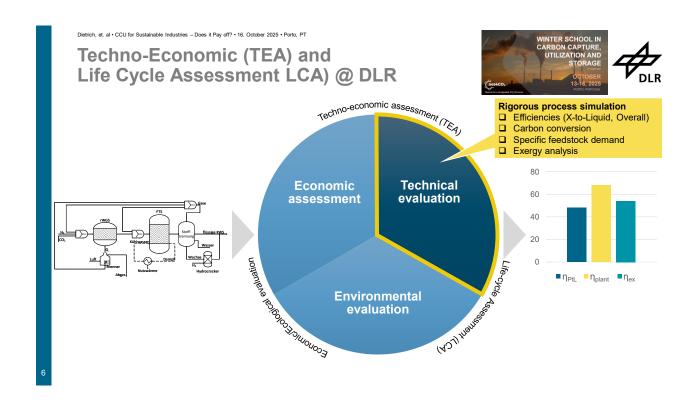
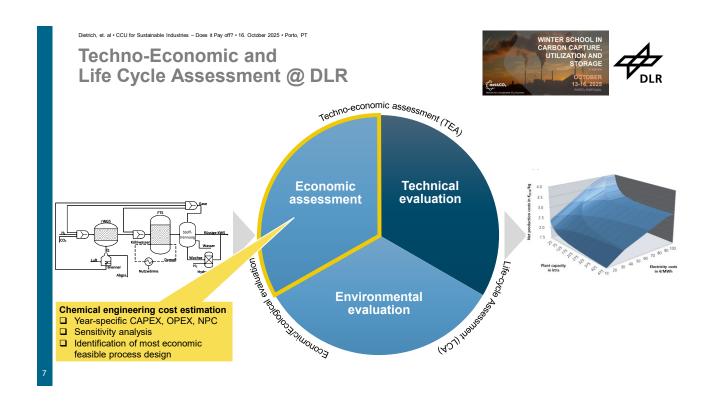
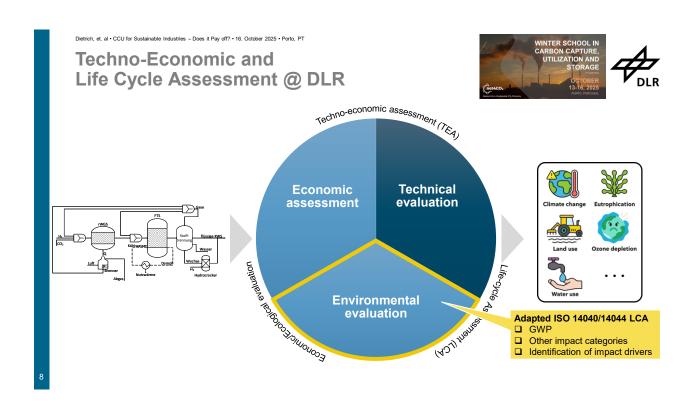


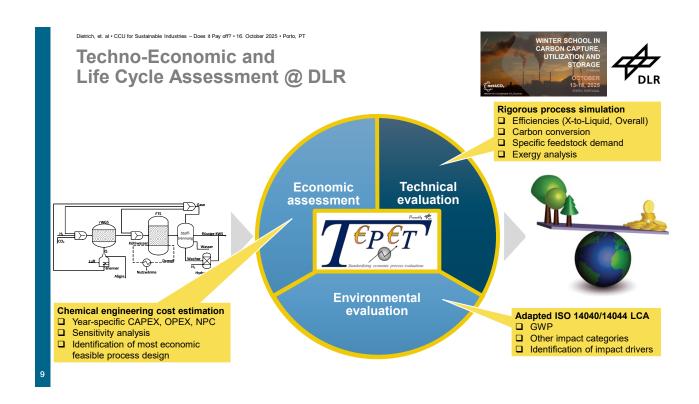
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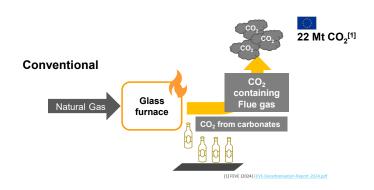
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Technical Assessment ExampleChallenges of Glass Industry



DLR

Glass furnace journey (campaign): 15 years with 24/7 operation



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Technical Assessment ExampleChallenges of Glass Industry



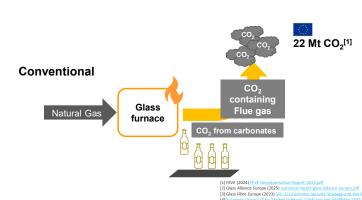
Different glass types / processes for various applications





Expected Growth^[4] ~1 % p.a. until 2035

Glass type	EU Production in 2023 [Mt] ^[2,3]	Market Share ^[2,3]	Key Applications
Container Glass	23.1 🗖	~60 %	Bottles, jars
Flat Glass	10.4 🗖	~27 %	Construction, automotive
Glass Fiber	1.0 🗷	~2-3 %	Reinforcement, insulation
Specialty	0.9 🗷	~2-3 %	Medical, optics, household



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Technical Assessment Example Challenges of Glass Industry



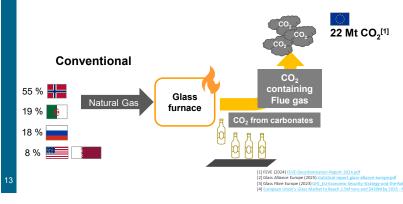
- Different glass types / processes for various applications
- Dependent on the natural gas supply/import^[5]





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[5] Institute for Energy Economics and Financial Analysis (2025) EU Gas Flows Tracker | IEEF

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Technical Assessment ExampleChallenges of Glass Industry





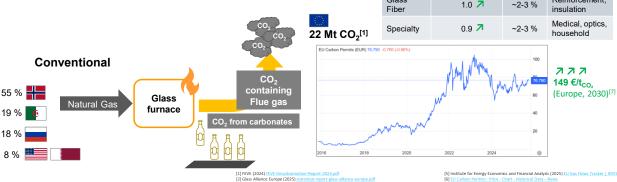
- Different glass types / processes for various applications
- Dependent on the natural gas supply/import^[5]
- CO₂-certificate / EU Emissions Trading System (ETS)^[6] penalty





Expected Growth^[4] ~1 % p.a. until 2035

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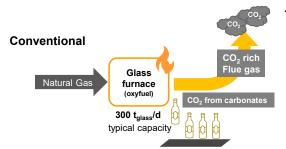
Technical Assessment Example

Glass-CCU concept^[1,2]



Solution options:

- Oxyfuel furnace, ~10 % of all glass furnaces^[3]
 - Potentially reduces 50 % glass CO₂ emissions^[3]



105 t_{CO2}/d

[1] Drünert et al. (2023) Techno-economic assessment of carbon capture and utilization concepts for a CO2 emission-free glass production.
[2] Rahmat et al. (under review) Advancing the defossilication of the glass industry based on the integration of synthetic fuels production. Fuel 3] Reducing the environmental footion of glass manufacturine I plasswapsh-rom.

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Technical Assessment Example Glass-CCU concept[1,2]



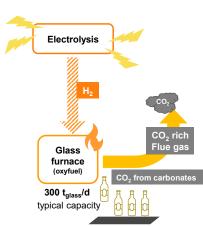


Solution options:

- Oxyfuel furnace, ~10 % of all glass furnaces^[3]
 - Potentially reduces 50 % glass CO₂ emissions^[3]
- Retrofitting strategies: alternative to full electrification
 - only 60-80 % electrification possible (hybrid)



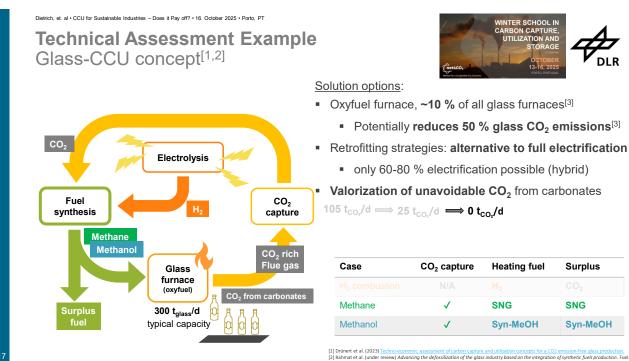


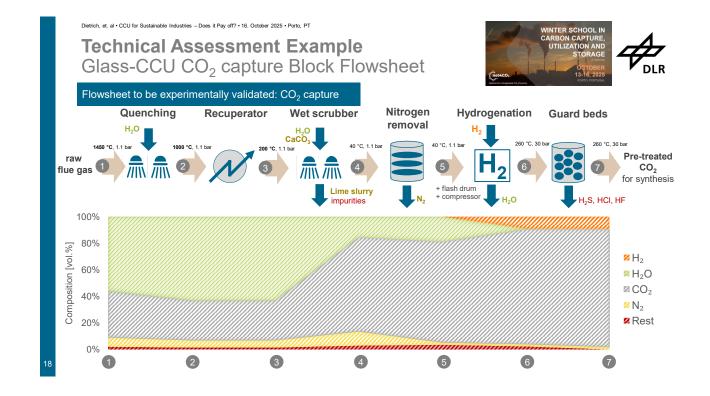


Surplus

SNG

Syn-MeOH





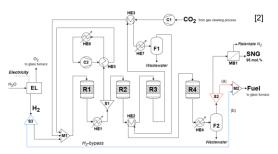
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Technical Assessment Example Glass-CCU Methane PFD^[2]

WINTER SCHOOL IN CARBON CAPTURE, UTILIZATION AND STORAGE OCTOBER 13-16, 2025



Flowsheet: Adapted TREMPTM process design^[1]



AspenPlus® model[2]: RPlug

T_{max,R1}^[4] = 700 °C

 $T_{in,R1}$ = 250 °C

 $p^{[3]} = 20-30 \text{ bar}$

 $GHSV^{[2,7]} = 4,000-10,000 h^{-1}$

Kinetic model: Rönsch et al.[4-6]

- · Combination of WGS and CO-Methanation
- Catalyst^[3] MCR-2X (Ni-based)
 - → CO₂ pre-treatment required
- Topsøe, H., From coal to clean energy. 2011
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- [4] Rönsch et al., 2016, Review on methanation From fundamentals to current projects.
- [5] Klose, J., 1984, Kinetics of the methanation of carbon monoxide on an alumina-supported nickel catalyst. Journal of Catalysis
 [6] Thang L. et al. 2013. Kinetic investigation of carbon monoxide hydrogenation under realistic conditions of methanation of bioma.
- [7] Bartholomew and Farrauto, 2006, Fundamentals of Industrial Catalytic Processes, 2nd Edition.

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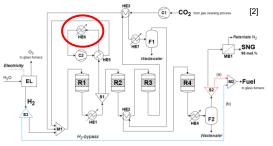
Technical Assessment ExampleGlass-CCU Methane PFD^[2]





Flowsheet: Adapted TREMPTM process design^[1]

high energetic efficiency & steam cycle applicable

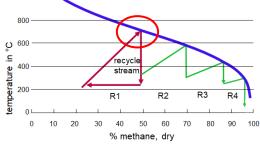


AspenPlus® model[2]: RPlug

 $T_{\text{max,R1}}^{[4]} = 700 \,^{\circ}\text{C}$ $T_{\text{in,R1}} = 250 \,^{\circ}\text{C}$

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- [2] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel.
 [3] Harms, H., B. Höhlein, and A. Skov, 1980, Methanisierung kohlenmonoxidreicher Gase beim Energie-Transport.
- [3] Harms, H., B. Honiein, and A. Skov, 1980, Methaniserung kontentionoxidreicher Gase be
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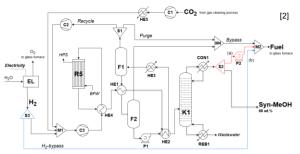
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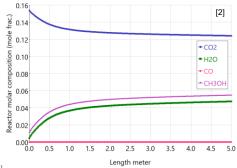
Technical Assessment Example Glass-CCU Methanol PFD^[2]





Flowsheet Lurgi process design^[3]:





AspenPlus® model[1]: RPlug

$$T_{\text{max,R5}}^{[3,5]} = 280-300 \, ^{\circ}\text{C}$$

 $T_{in,R1}^{[1,3]} = 250 \, ^{\circ}C$

 $p^{[1,3]} = 80 \text{ bar}$

GHSV^[4] = 10,000 h⁻¹

Kinetic model: Vanden Bussche and Froment[1,4]

- MeOH synthesis from CO/CO₂/H₂ represented as CO₂ hydrogenation & RWGS reactions
- Catalyst: Cu/ZnO/Al₂O₃
 - → CO₂ pre-treatment required!

[1] Bahmat et al. (2023) Techno-economic and exercy analysis of e-MeOH production under fixed operating conditions in Germany. Applied Ene (2) Bahmat et al. (1) under review) Advances the defeasibility of the glass and such yoused on the integration of synthetic fixed psynduction. Fuel. (3) Metalligenelischaft AG (1996) – EP 0790.226 BJ. (1) (4) Var-Dal and Soulais(D (2013)) Exercing and simulation of a methanol plant plant from CO2, hydrogenation. Journal of Cleaner Production.

[5] Bartholomew and Farrauto (2006) Fundamentals of Industrial Catalytic Processes, 2. Ed.

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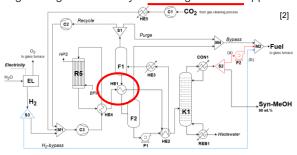
Technical Assessment Example Glass-CCU Methanol PFD^[2]

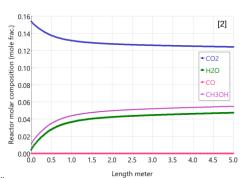




Flowsheet Lurgi process design^[3]:

high energetic efficiency & steam generation applicable





AspenPlus® model[1]: RPlug

= 80 bar

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Technical Assessment ExampleGlass-CCU Methane / Methanol





Equipment Design Parameters^[1]

Equipment ^[1-3,5]	AspenPlus® model	Parameters	Remarks
Heat exchangers	HeatX/Heater	$\Delta p = 0.2 \text{ bar}^{[4]}, \ \Delta T_{approach} = 10 \text{ K}^{[4]}$	U-values ^[6] method
Compressors	Compr/MCompr	Max. compression ratio = $3^{[4]}$ $\eta_{\text{isentropic}} = 80 \%^{[4]}$, $\eta_{\text{mech.}} = 95 \%$	range compression ratio 2.5-4 ^[4]
Pumps	Pump	η_{pump} = 95 %, η_{driver} = 95 %	
Flash drums	Flash2	$Q = 0 \text{ kW}, \Delta p = 0.2 \text{ bar}^{[4]}$	adiabatic
Distillation columns	RadFrac	$p_{cond.} = 1.36 \text{ bar}^{[1,2]}, \Delta p_{col.} = 0.34 \text{ bar}^{[1,2]}$ $n_{stage} = 55, \text{ reflux ratio} = 1$	$d_{col.} = f(\dot{V}_{gas,col.})^{[7]}$
Alkaline Electrolyzer (AEL)	RStoic (Stack) Flash2, Sep, Pump (BoP)	$\eta_{\rm energetic}$ = 53.3 % (LHV) ^[3]	simplified model
Wet scrubber (limestone)	Flash2, Sep	100 % separation of SO ₂ , SO ₃ , HCl, HF ^[8]	black-box
Membrane PMP	Sep	N ₂ separation = 92.75 % ^[9]	black-box

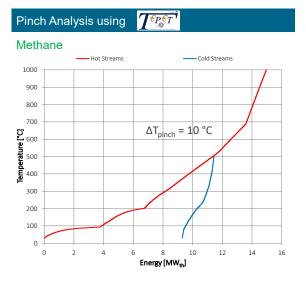
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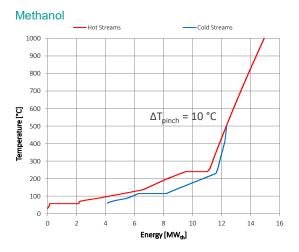
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Technical Assessment ExampleGlass-CCU Methane / Methanol heat integration



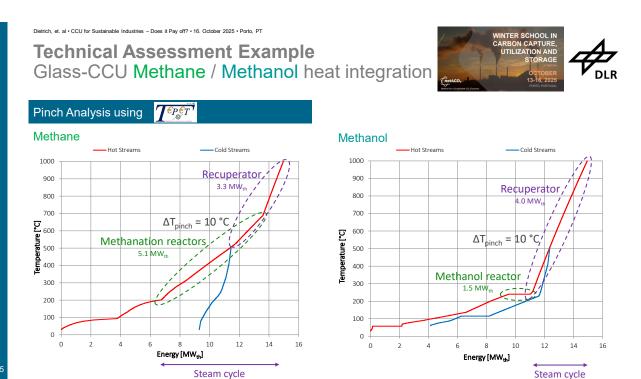


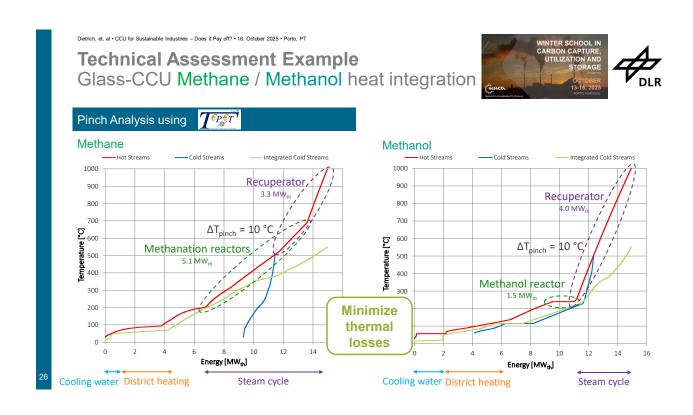




 ^[8] Sorreis (2021) Clemina Engineering Design
 [8] Sorreis (2021) Chapter 1 – Wet and Dry Scrubbers for Acid Gas Control. www.epa
 [9] Samei and Raisi (2022) Separation of nitrogen from methane by multi-stage mem

^[3] Sánchez et al. (2020) Aspen Plus model of an alkaline electrolysis system for hydrogen production. Journal of Hydrogen Energy.
[4] Woods (2007) Rules of Thumbi in Engineering Practices
[5] Heimann, N. et al (under review), Standardized techno-economic assessment of synthetic natural gas and synthetic hydrogen natural gas production f





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Technical Assessment Methodology



Definition of KPIs such as:

$$\eta_{\rm C} = \frac{\dot{n}_{\rm C,fuel}}{\dot{n}_{\rm C,feedstock}} \qquad \quad \eta_{\rm HtF} = \frac{\dot{m}_{\rm fuel} \cdot LHV_{\rm fuel}}{\dot{m}_{\rm H_2} \cdot LHV_{\rm H_2}} \qquad \quad \eta_{\rm PtF} = \frac{\dot{m}_{\rm fuel} \cdot LHV_{\rm fuel}}{P_{\rm electrolysis} + P_{\rm pumps} + P_{\rm compressors} - P_{\rm heat\,integration}}$$

- Rigorous steady-state process simulation + validation
 - Experimentally validated process models of most processes from research projects available
 - Adaptable to any new configuration / feedstock / ...

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Technical Assessment Methodology

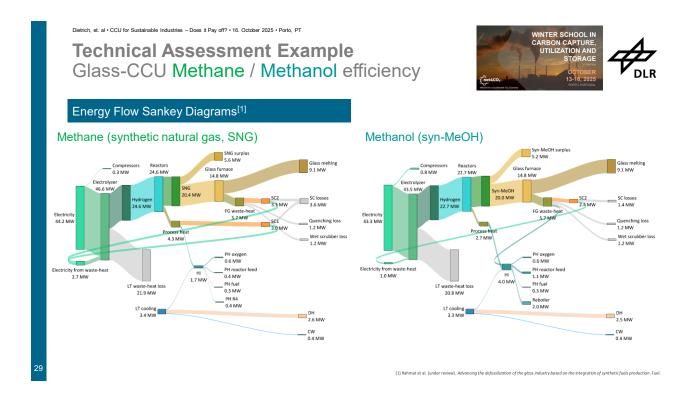


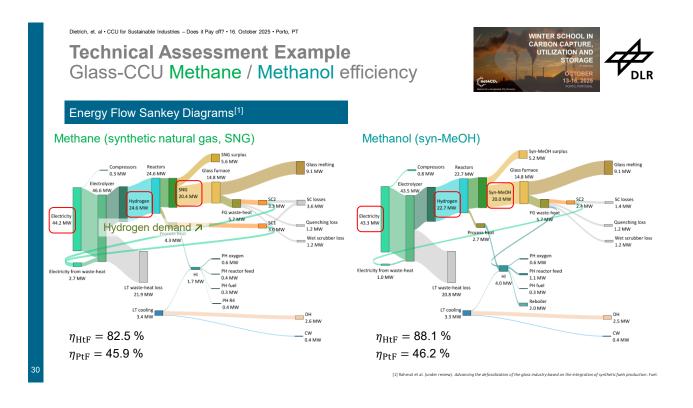


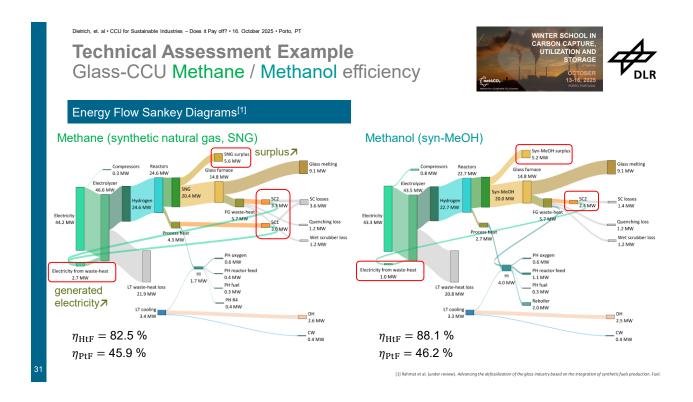
Definition of KPIs such as:

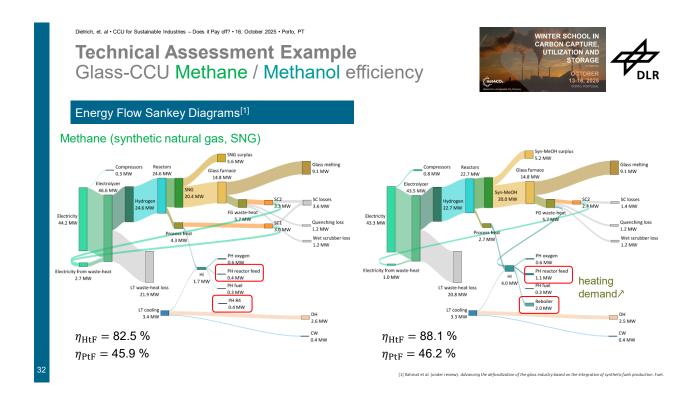
$$\eta_{\rm C} = \frac{\dot{n}_{\rm C,fuel}}{\dot{n}_{\rm C,feedstock}} \qquad \eta_{\rm HtF} = \frac{\dot{m}_{\rm fuel} \cdot LHV_{\rm fuel}}{\dot{m}_{\rm H_2} \cdot LHV_{\rm H_2}} \qquad \eta_{\rm PtF} = \frac{\dot{m}_{\rm fuel} \cdot LHV_{\rm fuel}}{P_{\rm electrolysis} + P_{\rm pumps} + P_{\rm compressors} - P_{\rm heat\,integration}}$$

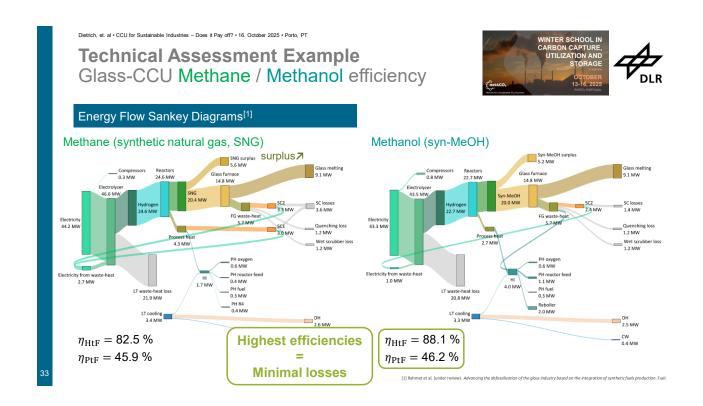
- Rigorous steady-state process simulation + validation
 - Experimentally validated process models of most processes from research projects available
 - Adaptable to any new configuration / feedstock / ...
- Aspen Plus extension and automated parameter variation via \mathcal{L}_{P}
 - Assists to reach convergence of a complex simulation (e.g. multiple recycle streams)
 - Sensitivity of each process parameter on each KPI
 - Automated heat integration flexibility towards configuration changes













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Economic Assessment Methodology

Define each required plant factor (basic conditions → see [1])



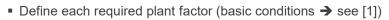


Glass-CCU Basic conditions[2]					
Plant location	Germany				
Base year	2022				
Basis currency	€				
FLh	8000 h a ⁻¹				
Plant lifetime (y)	15 a				
Interest rate (IR)	7 %				
Labor costs	41 €/h				

[1] Heimann et al. (2025) Contribution to the standardization of the economic and ecological analysis of PtX-process [in submission] [2] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel.

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Economic Assessment Methodology





Summarizing annualized CAPEX and OPEX in the following Equation:

$$NPC^{\text{[1]}}[\in_{2022} t_{glass}^{-1}] = \frac{ACC + \sum OPEX + labor\ costs}{12.5\ t_{glass} \cdot FLh\ [h\ a^{-1}]}$$





Glass-CCU Basic conditions[2]						
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36

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Economic Assessment Methodology



Plant location

Basis currency

Plant lifetime (y)

Interest rate (IR)

Labor costs

Base year

FLh



Germany

2022

8000 h a⁻¹

15 a

7 %

41 €/h

€

- Define each required plant factor (basic conditions → see [1])
- Standard chemical cost estimation: based on validated basic design
 - Summarizing annualized CAPEX and OPEX in the following Equation:

$$NPC^{[1]}[\in_{2022} t_{glass}^{-1}] = \underbrace{ACC} + \sum_{12.5} OPEX^{[.3]} + labor \ costs \\ 12.5 \ t_{glass} \cdot FLh \ [h \ a^{-1}]$$

 $ACC = FCI * Annuity factor^{[3]}$

Annualized Capital Costs (ACC) based on Fixed Capital Investment (FCI) and Annuity factor

[1] Heimann et al. (2025) Contribution to the standardization of the economic and ecological analysis of PX-process [in submission] [2] Rahmat et al. (under eview) Advancing the effossilization of the gluss industry based on the integration of synthetic fuels production. Fuel [3] Peters et al. (2002) Design and Economics for Demokrate Engineers. Europe, McGraw-Hill Education.

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Economic Assessment Methodology





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 - Summarizing annualized CAPEX and OPEX in the following Equation:

$$NPC^{[1]} \left[\in_{2022} t_{glass}^{-1} \right] = \underbrace{\frac{ACC}{12.5} + \sum_{glass} OPEX + labor \ costs}_{12.5 \ t_{glass} \cdot FLh \ [h \ a^{-1}]}$$

 $ACC = FCI + Annuity factor^{13}$



- Annualized Capital Costs (ACC) based on Fixed Capital Investment (FCI) and Annuity factor
- All chemical standard equipment cost available^[3]
- New equipment via analogies, exchange with technology suppliers
- All equipment cost plus Lang factors: FCI

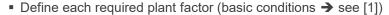
$$FCI_i = EC_i \times \sum Lang \ factors^{[3]}$$

[1] Heimann et al. (2025) Contribution to the standardization of the economic and ecological analysis of PX-process [in submission] [2] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel [3] Peters et al. (2002) Design and Economics for Chemical Engineers: Curpor, McGraw-Hill Education.

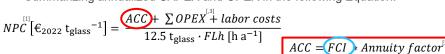
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Economic Assessment Methodology



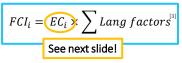


- Standard chemical cost estimation: based on validated basic design
 - Summarizing annualized CAPEX and OPEX in the following Equation:





- Annualized Capital Costs (ACC) based on Fixed Capital Investment (FCI) and Annuity factor
- All chemical standard equipment cost available^[3]
- New equipment via analogies, exchange with technology suppliers
- All equipment cost plus Lang factors: FCI



[2] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel [3] Peters et al. (2002) Design and Economics for Chemical Engineers. Europe: McGraw-Hill Education.

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Economic Assessment Methodology





Germany

2022

€

- Define each required plant factor (basic conditions → see [1])
- Standard chemical cost estimation: based on validated basic design
 - Summarizing annualized CAPEX and OPEX in the following Equation:

$$NPC^{[1]} \Big[\in_{2022} t_{glass}^{-1} \Big] = \underbrace{ACC} + \sum OPEX^{[.3]} + labor \ costs \\ 12.5 \ t_{glass} \cdot FLh \ [h \ a^{-1}]$$

Basis currency FLh 8000 h a-1 Plant lifetime (y) Interest rate (IR) 7 % Labor costs 41 €/h $ACC = FCI \cdot Annuity factor^{\parallel}$

Plant location

Base year

Annualized Capital Costs (ACC) based on Fixed Capital Investment (FCI) and Annuity factor

- All chemical standard equipment cost available^[3]
- New equipment via analogies, exchange with technology suppliers
- All equipment cost plus Lang factors: FCI



Fully automated economic cost estimation using DLR in-house tool

[1] Heithalfille Ed. (2022) Officialization to the samulativation of the economic and econogical start, as of the process [2] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthe [3] Peters et al. (2002) Design and Economics for Chemical Engineers. Europe: McGraw-Hill Education.

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Economic Assessment TEPET database







$$EC_{i,ref} = EC_{ref} \times \left(\frac{sizing_i}{sizing_{ref}}\right)^n \times \left(\frac{CEPCI_i}{CEPCI_{ref}}\right)$$

$$\textit{EC}_{i,poly} = \left[\left.e \cdot \left(\textit{sizing}_{i}\right)^{2} + \left.f \cdot \, \textit{sizing}_{i} + g\right.\right] \times \left(\frac{\textit{CEPCI}_{i}}{\textit{CEPCI}_{ref}}\right)$$

Reference function (EC _{i,ref})	EC _{ref}	Currency	sizing _{ref}	Unit	n	Year _{ref}	Source
Compressor	3 035	\$	1	kW _{el}	0.68	2002	[1]
Centrifugal pump	16 809	\$	1	m³ s-1	0.36	2002	[1]
Distillation column	286 343	\$	100	size factor = HxD ^{1.5} [m ^{2.5}]	0.53	2007	[2,3]
AEL stack	800	k€	0.005	kg/s	1	2019	[4]
AEL balance of plant	1	m€	0.025	kg/s	0.8	2019	[4]
Wet scrubber (limestone)	13 061	k\$	14	MW_th	0.72	2012	[5]
Membrane PMP	9.76	m\$	525.6	kmol/h	0.6	2020	[6]**
Methanation fixed-bed reactor	57 794	\$	14 000	m³/h	0.52	2007	[2]
Polynomial function (EC _{i,poly})	е	f	g	Sizing unit	Currency	Year _{ref}	Source
MeOH Lurgi reactor, D _{tube} 2 in.*	0	156.03	11 910	Number of tubes [-]	\$	2002	[1]**
Shell & tube heat exchanger*	0	201.29	3853.3	Heat transfer area [m²]	\$	2002	[1]
Flash drum	-2.21	369.75	805.42	Length & diameter [m]	\$	2002	[1]

stainless steel as the material construction

[1] Peters et al. (2002) Design and Economics for Chemical Engineers. Europe: McGraw-Hill Education.
[2] Woods (2007) Muleo d'Imbruh in Engineering Practices
[3] Towler (2008) Chemical Engineering Design
[4] Habermayer et al. (2023) Sustainable aviation fuel from forestry residue and hydrogen. https://doi.org/10.1039/d3se003558|
[5] Sorrels (2021) Chapter 1 – Wet and by Scrubbers for Acid Gas Control. www.eps.gov

[6] Samei and Raisi (2022) Separation of nitrogen from methane by multi-stage membrane

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Economic Assessment TEPET database







$$EC_{i,ref} = EC_{ref} \times \left(\frac{sizing_i}{sizing_{ref}}\right)^n \times \left(\frac{CEPCI_i}{CEPCI_{ref}}\right)$$

$$\textit{EC}_{i,poly} = \left[\left. e \cdot (\textit{sizing}_{i})^{2} + \left. f \cdot \textit{sizing}_{i} + g \right. \right] \times \left(\frac{\textit{CEPCI}_{i}}{\textit{CEPCI}_{ref}} \right)$$

Reference function (EC _{i,ref})							
Compressor			1	kW _{el}			
Centrifugal pump			1				
Distillation column							
AEL stack	800	k€	0.005	kg/s	La TEDE	2019	[4]
AEL balance of plant	Co	st func	tions a	re available in t	ne lepe	i databa	ase _[4]
Wet scrubber (limestone)		k\$	14	MW_th			
Membrane PMP	lleare	havo a	full fla	xibility to selec	t/undate	the inni	ıt data
Methanation fixed-bed reactor	03013 57 794	nayc a	14 000	Albility to scied	trupuate	1116 111PC	it data
Polynomial function (EC _{i,poly})		f					
MeOH Lurgi reactor, D _{tube} 2 in.*				Number of tubes [-]			[1]**
Shell & tube heat exchanger*							
Flash drum				Length & diameter [m]			

^{*}stainless steel as the material construction

^{**}with own reformulation

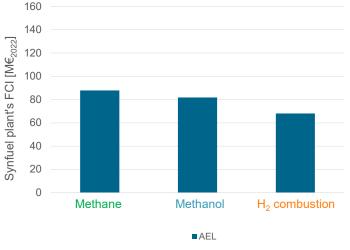
^[1] Peters et al. (2002) Design and Economics for Chemical Engineers. Europe: McGraw-Hill Education. [2] Woods (2007) Rules of Thumb in Engineering Practices. [3] Towler (2008) Chemical Engineering Design. [4] Habermayer et al. (2023) Sustainable aviation fuel from Forestry residue and hydrogen. https://doi. [5] Sorrels (2021) Chapter 1 – Wet and Dry Scrubbers for Acid Gas Control, www.eca.acvv. [6] Samei and Raisi (2022) Separation of nitrogen from methane by multi-stage membrane.

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Economic Assessment ExampleGlass-CCU Methane / Methanol / H₂ FCI^[1]







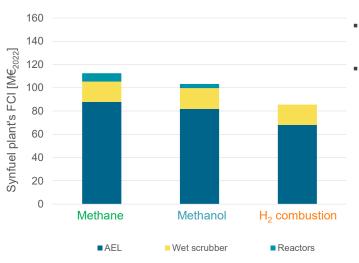
Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fu

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Economic Assessment ExampleGlass-CCU Methane / Methanol / H₂ FCI^[1]







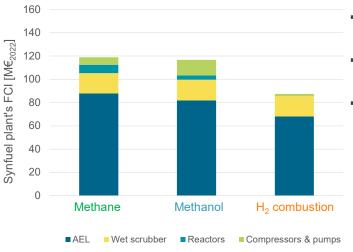
- AEL: Methane requires more H₂ feedstock than Methanol
- Reactors: Methane fixed-bed multi-stage,
 Methanol multi-tube single-stage

[1] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel.

Economic Assessment Example Glass-CCU Methane / Methanol / H₂ FCI^[1]







 AEL: Methane requires more H₂ feedstock than Methanol

 Reactors: Methane fixed-bed multi-stage, Methanol multi-tube single-stage

Compressors:

p_{reactor} Methane 30 bar

p_{reactor} Methanol 80 bar

[1] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel

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Economic Assessment Example Glass-CCU Methane / Methanol / H₂ FCI^[1]





160 140 Synfuel plant's FCI [M€₂₀₂₂] 120 100 80 60 40 20 0 Methane Methanol H₂ combustion ■ Wet scrubber AFI Reactors ■ Compressors & pumps Heat exchangers ■ Steam cycle

• AEL: Methane requires more H₂ feedstock than Methanol

 Reactors: Methane fixed-bed multi-stage, Methanol multi-tube single-stage

Compressors:

preactor Methane 30 bar

p_{reactor} Methanol 80 bar

Steam cycle:

Methane in recuperator & reactor

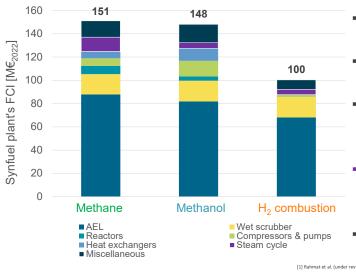
Methanol in recuperator only

[1] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel

Economic Assessment Example
Glass-CCU Methane / Methanol / H₂ FCI^[1]







 AEL: Methane requires more H₂ feedstock than Methanol

Reactors: Methane fixed-bed multi-stage,
 Methanol multi-tube single-stage

Compressors:

p_{reactor} Methane 30 barp_{reactor} Methanol 80 bar

Steam cycle:

Methane in recuperator & reactor Methanol in recuperator only

FCI: Methane ≈ Methanol

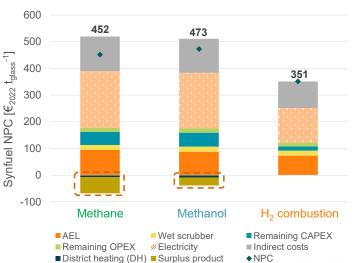
1] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fue

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Economic Assessment ExampleGlass-CCU Methane / Methanol / H₂ NPC^[1]





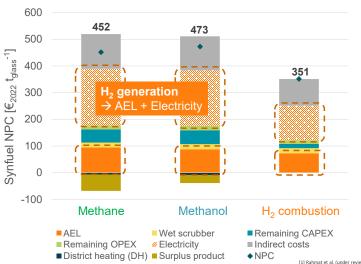


Sales of surplus synfuels as fossil fuels

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Economic Assessment ExampleGlass-CCU Methane / Methanol / H₂ NPC^[1]





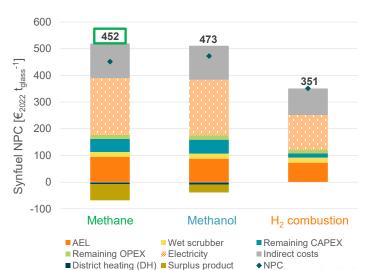
- Sales of surplus synfuels as fossil fuels
- Cost driver is H₂ generation
 - → ca. 60-67 % NPC

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Economic Assessment ExampleGlass-CCU Methane / Methanol / H₂ NPC^[1]



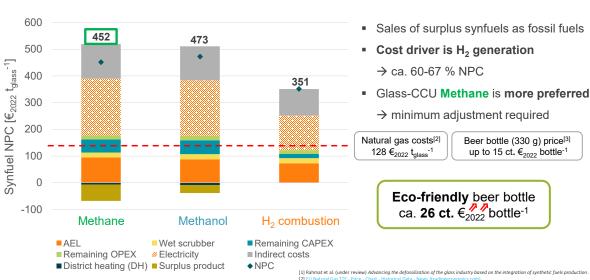


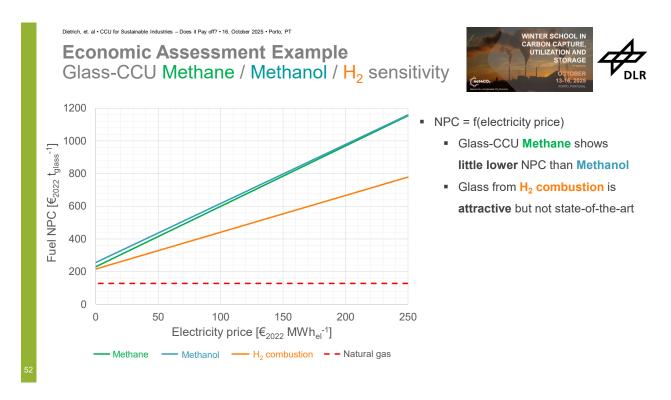


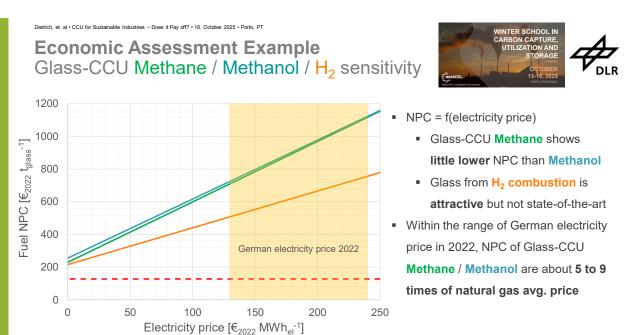
- Sales of surplus synfuels as fossil fuels
- Cost driver is H₂ generation
 - → ca. 60-67 % NPC
- Glass-CCU Methane is more preferred
 - → minimum adjustment required

Detrich, et. al - CCU for Sustainable Industries – Does II Pay off? - 16. October 2025 - Porto, PT **Economic Assessment Example**Glass-CCU Methane / Methanol / H₂ NPC^[1]

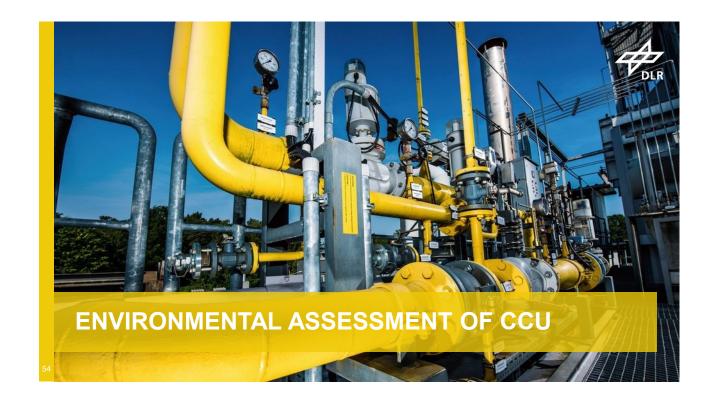


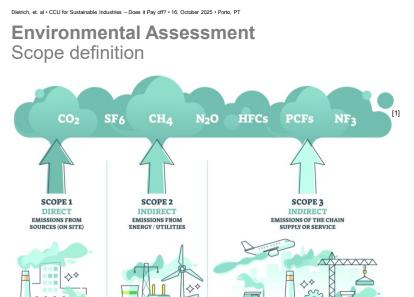






Methanol
 H₂ combustion
 Natural gas









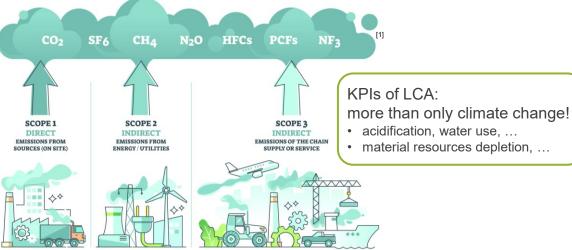
[1] 62d0970d68ea166bcd1c010b_AdobeStock_462557114.jpeg_(4330×3464)

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Environmental Assessment Scope definition







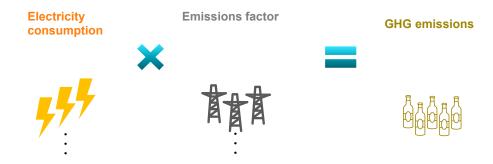
[1] 62d0970d68ea166bcd1c010b_AdobeStock_462557114.jpeg_(4330×3464)

Environmental Assessment Methodology





- ISO 14040/14044 for standard life cycle assessment (LCA) procedure
- Simplified Glass-CCU Methane climate change calculation example:



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Environmental Assessment Methodology



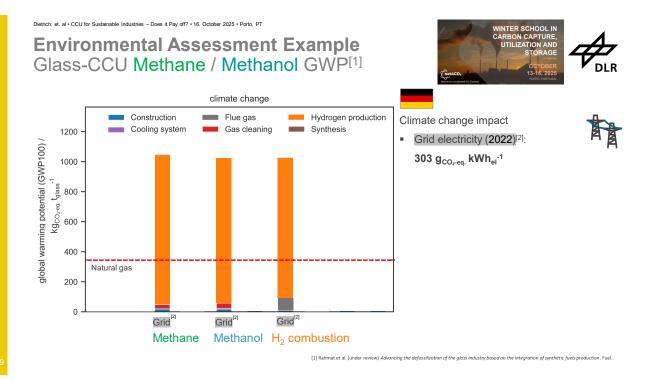


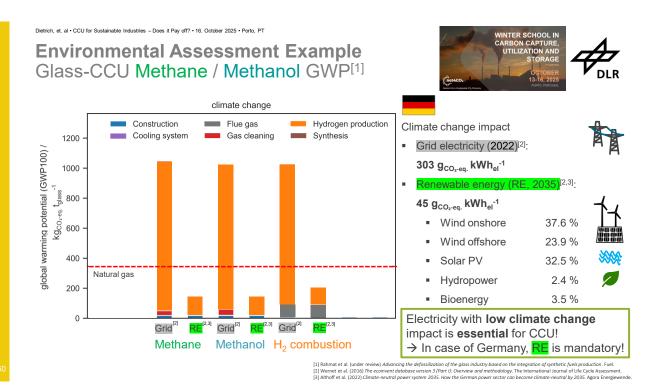
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Fully automated environmental impact estimation using DLR in-house tool





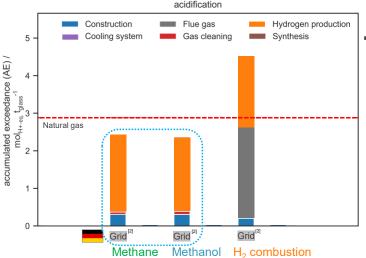


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Environmental Assessment ExampleGlass-CCU Methane / Methanol acidification^[1]







 Glass-CCU Methane / Methanol gives less acidification impact than the use of natural gas

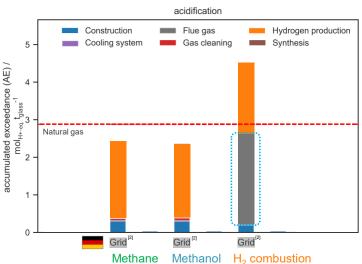
[1] Rahmat et al. (under review) Advancing the defossilization of the glass industry based on the integration of synthetic fuels production. Fuel. [2] Wernet et al. (2016) The ecoinvent database version 3 (Part I): Overview and methodology. The International Journal of Life Cycle Assessment

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Environmental Assessment ExampleGlass-CCU Methane / Methanol acidification^[1]







- Glass-CCU Methane / Methanol gives less acidification impact than the use of natural gas
- Glass industry with H₂ combustion gives more acidification impact than the use of natural gas due to flue gas emission without CCU

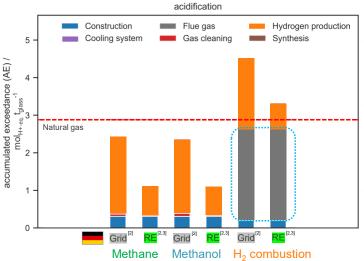
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Environmental Assessment ExampleGlass-CCU Methane / Methanol acidification^[1]



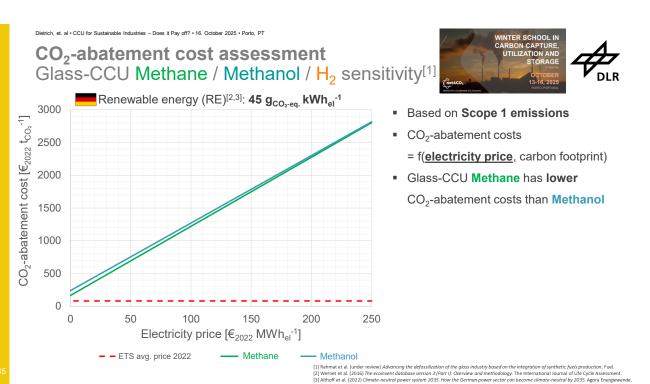


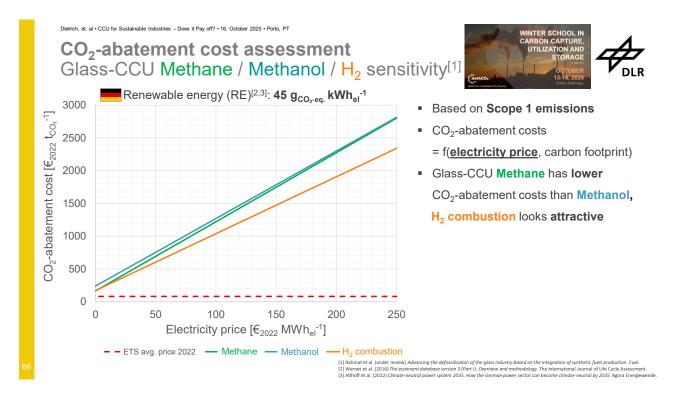


- Glass-CCU Methane / Methanol gives less acidification impact than the use of natural gas
- Glass industry with H₂ combustion gives more acidification impact than the use of natural gas due to flue gas emission without CCU
- The use of RE for CCU decreases the acidification impact even further

[1] Bahmat et al. (under review) Advancing the defossilication of the glass industry based on the integration of synthetic fuels production. Fuel.
[2] Wernet et al. (2016) The cocinvent database version 3 (Part I): Overview and methodology. The International Journal of Life Cycle Assessment.
[3] Althoff et al. (2022) Climate-neutral power system 2035. How the German power sector on become climate neutral by 2035. Again stengeneended.







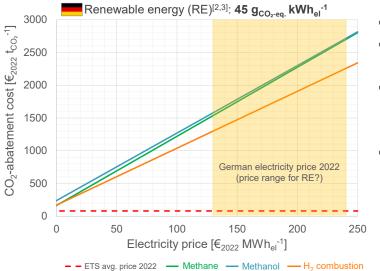
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- Does it pay off? -

CO₂-abatement cost assessment Glass-CCU Methane / Methanol / H₂ sensitivity^[1]







- Based on Scope 1 emissions
- CO₂-abatement costs
 = f(electricity price, carbon footprint)
- Glass-CCU Methane has lower
 CO₂-abatement costs than Methanol,
 H₂ combustion looks attractive
- Within the range of German electricity price in 2022, CO₂-abatement costs of Glass-CCU Methane / Methanol are about 19 to 34 times of ETS avg. price

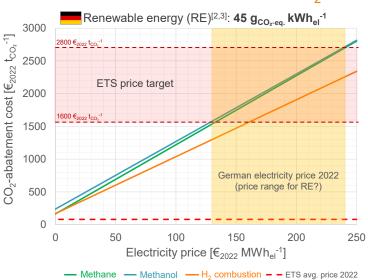
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CO₂ abatement cost assessment Glass-CCU Methane / Methanol / H₂ sensitivity

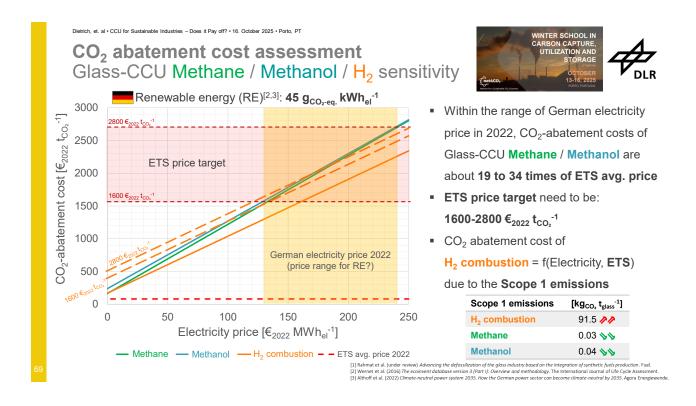






- Within the range of German electricity price in 2022, CO₂-abatement costs of Glass-CCU **Methane / Methanol** are about **19 to 34 times of ETS avg. price**
- ETS price target need to be: 1600-2800 €₂₀₂₂ t_{CO₂}-1

1] Rahmat et al. (under review) Advancing the defossilitation of the giass industry based on the integration of synthetic fuels production. Fuel.
2) Wernet et al. (2016) The ecoinvent database version 3 (Part 1): Overview and methodology. The International Journal of Life Cycle Assessment.
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Technology Readiness Level (TRL) Example of Glass-CCU





Needs of further experimental researches

- Each equipment, as a stand-alone technology, has TRL 8-9
- Typical SoA glass manufacturing plant has a desulphurization and nitrogen removal unit, while CO₂ is emitted to the air

7

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Technology Readiness Level (TRL) Example of Glass-CCU





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- Typical SoA glass manufacturing plant has a desulphurization and nitrogen removal unit, while CO₂ is emitted to the air
- To get commercial: search for optimization potential
 - Better electrolyzer, carbon capture, system (heat) integration, ...

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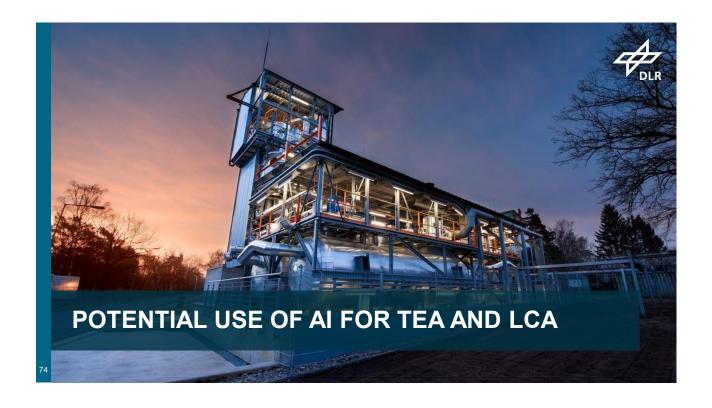
Technology Readiness Level (TRL) Example of Glass-CCU





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- Each equipment, as a stand-alone technology, has TRL 8-9
- Typical SoA glass manufacturing plant has a desulphurization and nitrogen removal unit, while CO₂ is emitted to the air
- To get commercial: search for optimization potential
 - Better electrolyzer, carbon capture, system (heat) integration, ...
- Glass-CCU technical challenge:
 CO₂ capture unit and the integration to the glass furnace
 - → the process concept has TRL 5
- Demonstration plant is needed to proof viability and CO₂ abatement cost



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Promises of Al in TEA & LCA

It does it for you, does it?





Data and Inventory collection

Methods and Modelling creation

Uncertainty, Sensitivity analysis

Dynamics, Scenarios Governance, Auditability Increase Data Security

Will AI save you more time for your problem solution compared to your individual time expenditure for AI training and application?

Dietrich, et. al • CCU for Sustainable Industries - Does it Pay off? • 16. October 2025 • Porto, PT Think twice when using AI in TEA & LCA Garbage in - Glossy Garbage out Hallucination Uncalibrated points Data misclassification Weak audit trails Explainability gaps Unclear validity and sources Ethical concerns (accountability) Correlation blindness Look for peer-reviewed data Methods Uncertainty, Data and Dynamics, Governance, and Increase Inventory Sensitivity Modelling **Scenarios** Auditability **Data Security** collection analysis creation Drifting away from compliances and norms Scenario generation without Data leakage risks Overfitting and underfitting of trends clear decision and relevance privacy concerns Far from engineering practice

net4co2 Winterschool 2025, Porto, Portugal

Don't undermine the energy consumption of AI

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Can Al help in TEA & LCA, carefully used?





Data wrangling & QA-flags Draft preparation and model outline

Document mining and number verification

77

Can Al help in TEA & LCA, carefully used?

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- Spots duplicates, incorrect units, and missing information
- Can help in pulling out numbers from documentsCan help in selecting key parameters

Data wrangling & QA-flags Draft preparation and model outline Document mining and number verification

- Suggests rough estimation for a fuel plant Assists in cost assessment
 - (e.g. more recent data than standard literature)





EU Energy-intensive industries





Opportunities for CCU towards Sustainability*

- Steel and basic metals (irons, aluminum, copper, ...)
- Chemicals (ammonia, fertilizers, plastics, ...)
- Cement and non-metallic minerals (glass, ceramics) → 100 Mt_{CO}, p.a.
- Petrochemicals (oil refining, ...)
- Pulp and paper (forest-based products)

- → 160 Mt_{CO}, p.a.
- \rightarrow 130 Mt_{CO₂} p.a.
- → 80 Mt_{CO₂} p.a.
- → 50 Mt_{CO₂} p.a.

* see: Fig. 1: Share of CO₂ emissions in the total industrial CO₂ emissions in the EU

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EU Energy-intensive industries





Opportunities for CCU towards Sustainability*

- Steel and basic metals (irons, aluminum, copper, ...) → 160 Mt_{CO₂} p.a. | fossil fuel 2 2 2
- Chemicals (ammonia, fertilizers, plastics, ...)
- Cement and non-metallic minerals (glass, ceramics)
- Petrochemicals (oil refining, ...)
- Pulp and paper (forest-based products)



- → 130 Mt_{CO}, p.a. | fossil feedstock ¬¬¬
- → 100 Mt_{CO₂} p.a. high temperature
- \rightarrow 80 Mt_{CO₃} p.a.
- → 50 Mt_{CO}, p.a.

^{*} see: Fig. 1: Share of CO₂ emissions in the total industrial CO₂ emissions in the EU

EU Energy-intensive industries





Opportunities for CCU towards Sustainability*



- Steel and basic metals (irons, aluminum, copper, ...)
- Chemicals (ammonia, fertilizers, plastics, ...)
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- → 160 Mt_{CO₂} p.a. | fossil fuel 777
- → 130 Mt_{CO}, p.a. fossil feedstock 777
- → 100 Mt_{CO}, p.a. j high temperature ¬
- → 80 Mt_{CO₂} p.a.
- → 50 Mt_{CO₂} p.a.

Glass-CCU is adaptable to other energy-intense industries with other scale, GHG concentration, temp., pressure, ...

* see: Fig. 1: Share of CO₂ emissions in the total industrial CO₂ emissions in the EU

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EU Energy-intensive industries





Opportunities for CCU towards Sustainability*



- Steel and basic metals (irons, aluminum, copper, ...) → 160 Mt_{CO₂} p.a. | fossil fuel → → →

- Chemicals (ammonia, fertilizers, plastics, ...)
- → 130 Mt_{CO₂} p.a. | fossil feedstock ¬¬¬
- Cement and non-metallic minerals (glass, ceramics)
- → 100 Mt_{CO₂} p.a. high temperature
- Petrochemicals (oil refining, ...) Pulp and paper (forest-based products)
- \rightarrow 80 Mt_{CO₃} p.a. 50 Mt_{CO2} p.a.

Glass-CCU is adaptable to other energy-intense industries with other scale, GHG concentration, temp., pressure, ... each application unique -> chemical engineering homework

^{*} see: Fig. 1: Share of CO₂ emissions in the total industrial CO₂ emissions in the EU

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Conclusion



- CCU in energy-intensive industry requires:
 - Deep understanding on the technical processes and process simulation skills
 - Standardized economic assessment
 - Environmental impact assessment beyond CO₂
- Findings of Glass-CCU:
 - Methane is the low-hanging fruit for the decarbonization of glass industry
 - Greenflation of beer bottle is expected with about 70 % higher price (15 ct€ → 26 ct€)
- CCU technology transfer from glass industry to other energy-intense industries is feasible but not straightforward
- Al is a fast assistant, but not your guide!
- DLR provides standardized assessment for any CCU technology, feed gas, scale, location, regulation, ...!



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Outlook





- Standardized techno-economic and environmental assessment is based on basic engineering design
 - AACE class III/IV (FCI accuracy of ±30 % assumed)
 - Detailed design will proof if you were right
- Demonstration plant will experimentally validate the findings

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- CCU regulation should reflect the real benefits
 - EU ETS price target should be fulfilled to make CCU economically attractive
 - Binding environmental policies are essential for the deployment of CCU
- The greener the electricity source, the more attractive becomes CCU technology!
 - CCU applications will evolve or the plants will shut down*
- See EU Net-Zero Industry Act: https://single-market-economy.ec.europa.eu/publications/net-zero-industry-act en

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Dedicate your career to a sustainable industry?

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