

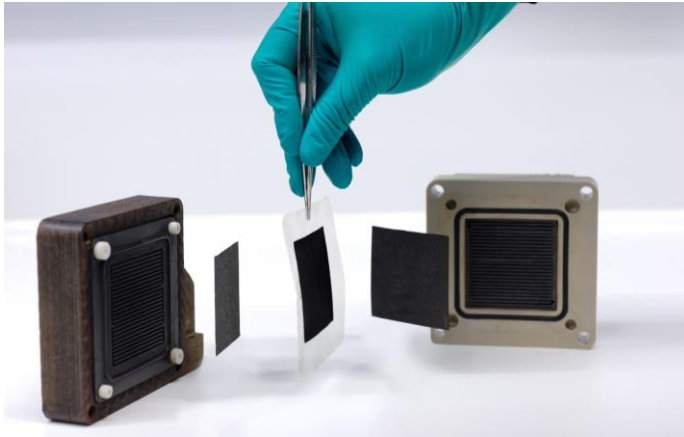
DEVELOPMENT OF MEMBRANE AND ELECTRODES FOR THE HT-PEM FUEL CELL TECHNOLOGY

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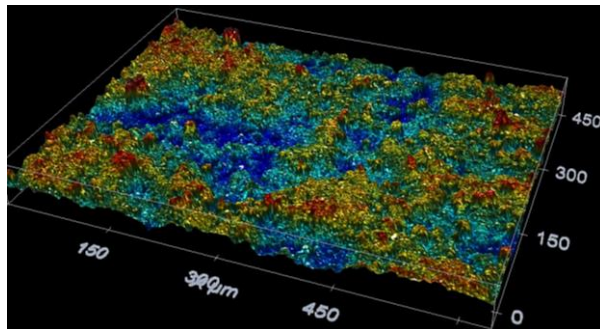




Material Development

Long-term stable, efficient components
for HT-PEM fuel cells

*Catalysts, membranes, electrodes,
membrane-electrode-assemblies*



Analytics and Quality Control

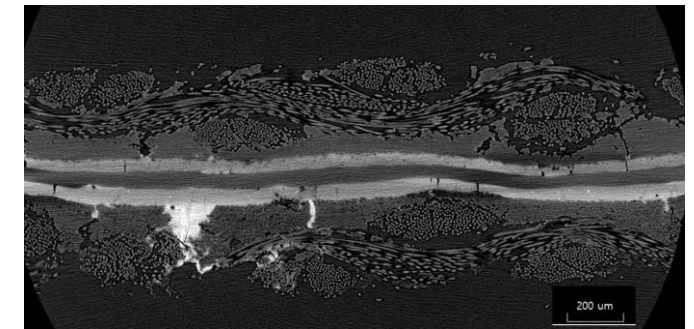
On gas diffusion layers and bipolar
plates after fabrication

Electrochemical, physico-chemical, imaging methods



Performance Studies

From thin-film analysis to PEM fuel cells
*Activity and degradation, contamination effects,
accelerated stress tests*



Cost-efficient Electrodes

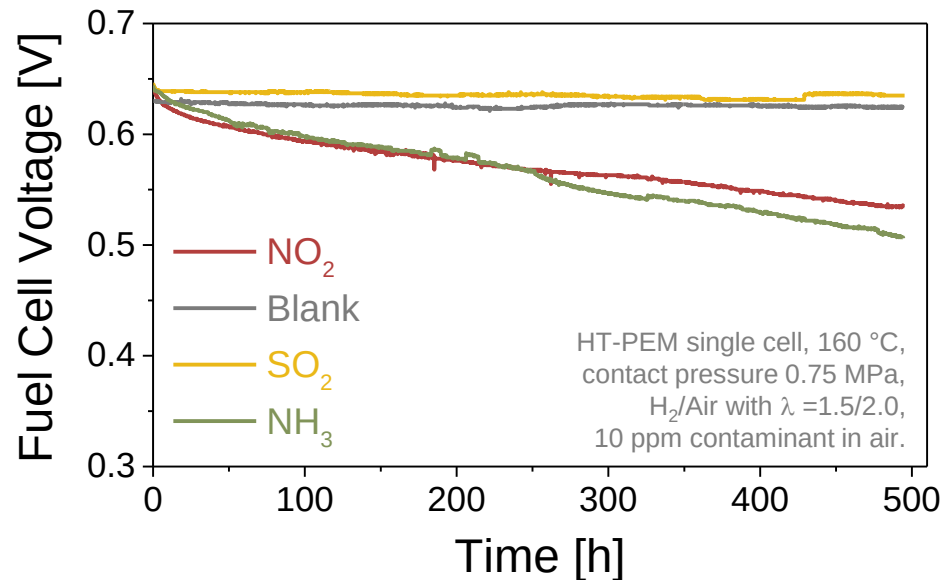
for PEM fuel cells

Reduced PGM-contents, use of M-N-C catalysts

HT-PEM Fuel Cells

Advantages

- Increased tolerance towards contaminants like CO or H₂S due to **160 °C**
- Direct use of industrial quality H₂ or reformates
→ **Application flexibility**



Challenges

- Larger stack sizes compared to LT-PEMFCs
- Limited lifetime due to membrane creeping and corrosion of components
- Phosphate poisoning of catalytic active sites
→ Higher Pt loading of **up to 1 mg_{Pt}cm⁻² per electrode**
- PTFE contents of 10-40 wt.% (CL), 20-40 wt.% (MPL), 0-30 wt.% (GDL)

Increasing membrane stability
Reducing PGM-contents

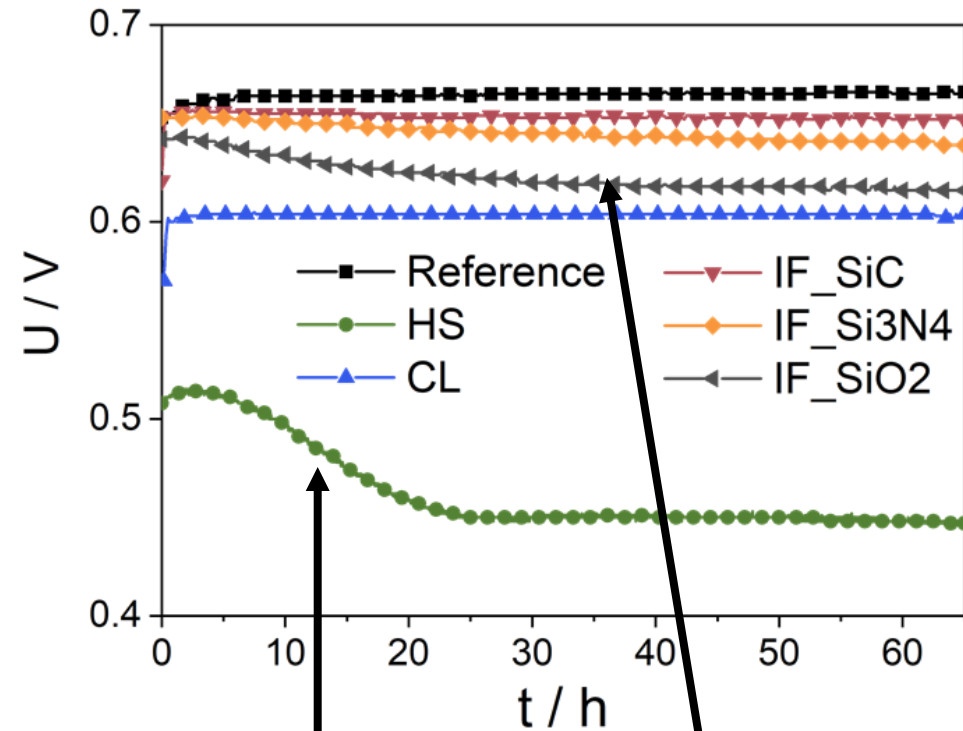
HT-PEM FC – MEMBRANES

Effect of Membrane Modification on Performance

- Collaboration with BASF → Celtec[®]-based study
 - Standard Celtec[®]-P as reference
 - Use of Celtec[®]-based fabrication process
 - Membranes with 2 wt% inorganic filler, crosslinked or increased solid-content

Membrane	
Celtec [®] -P	5 wt%
SiO ₂ Filler	6-8 wt%
Si ₃ N ₄ Filler	
SiC Filler	
Crosslinked	18 wt%
High-solid	

Solid content



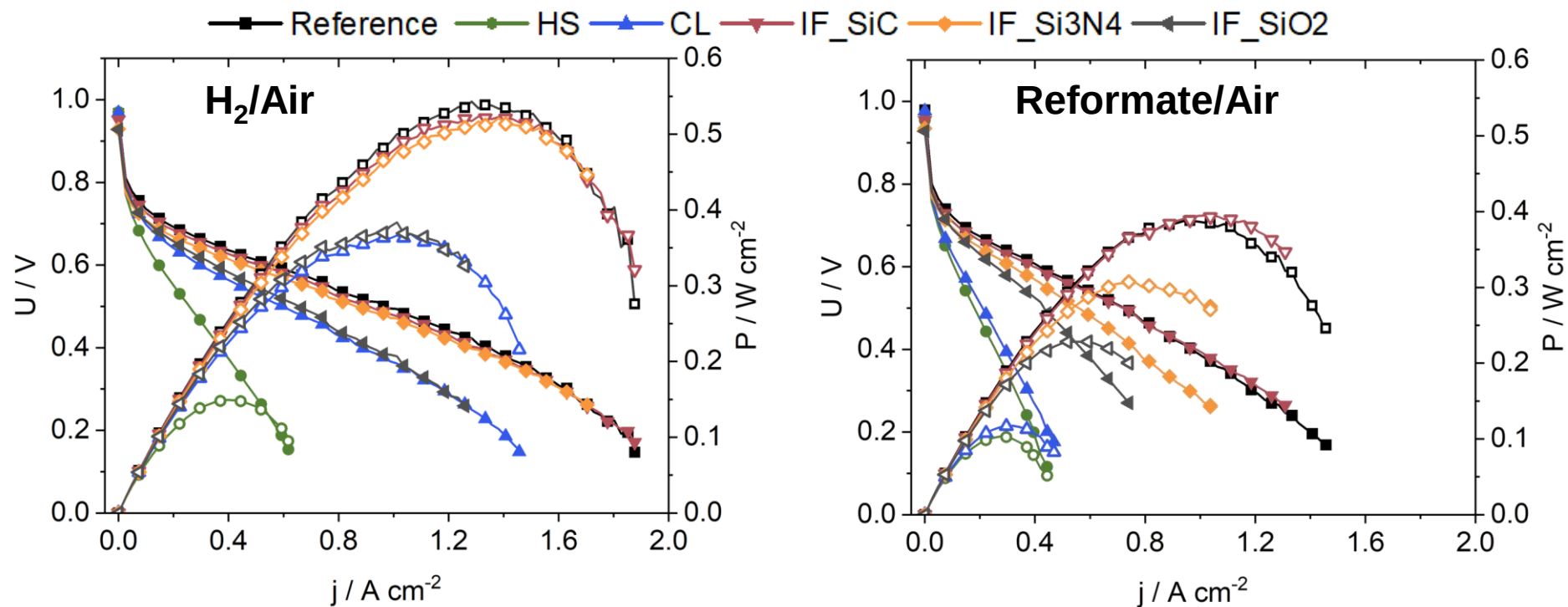
HT-PEM single cell testing: 160 °C, contact pressure 0.75 MPa, dry H₂/Air (1.5/2.0).

Irreversible acid leaching
from membrane

Hydrophilic character
of SiO₂ limits acid
distribution

Effect of Membrane Modification on Performance

- Best performance for silicon carbide as filler in HT-PEM
- Lowest performances for high-solid and crosslinked membranes



HT-PEM single cell testing:
160 °C, contact pressure
0.75 MPa, dry gases.

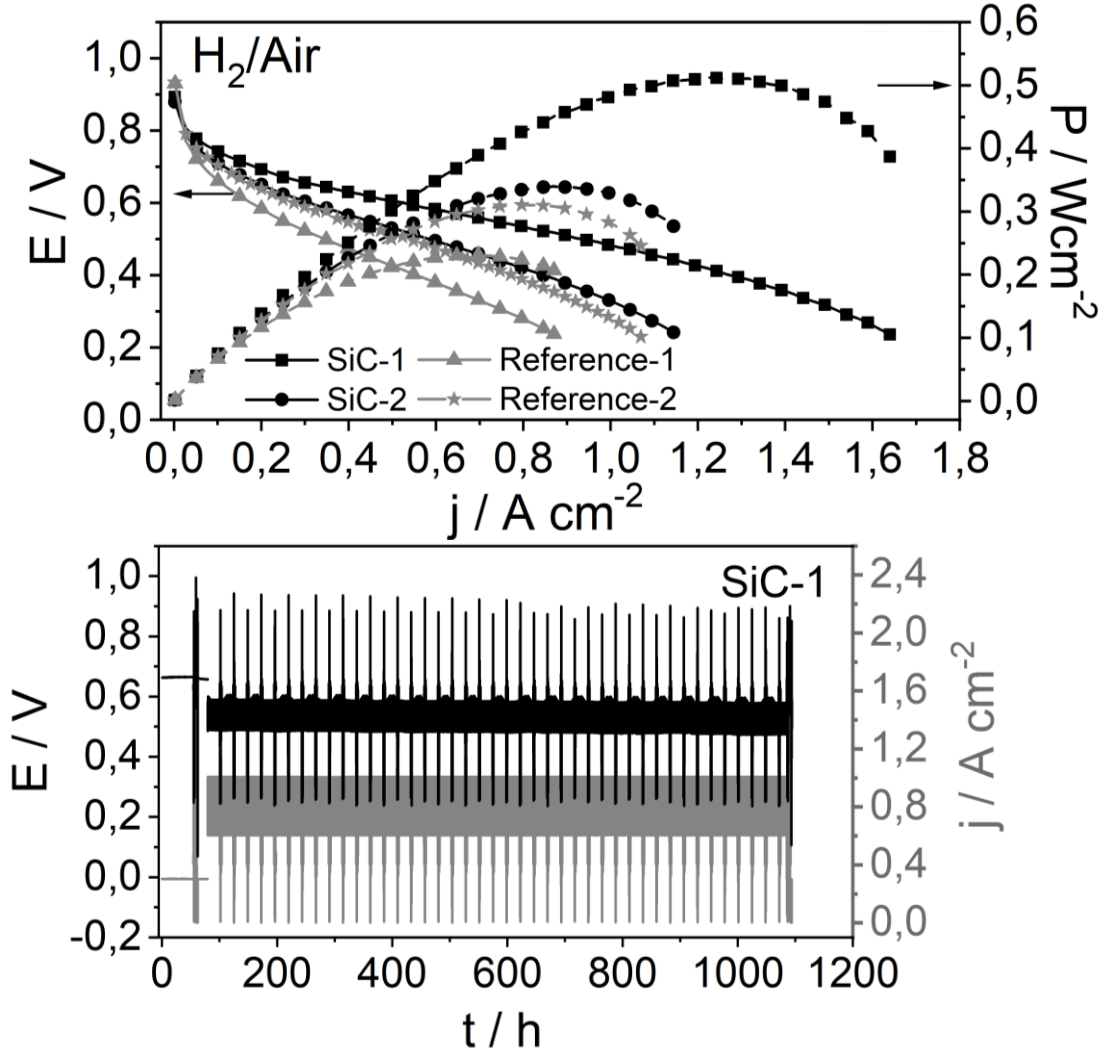
→ Next step: Long-term stability of SiC membrane

Silicon Carbide based HT-PEM Membranes

Degradation over Time



- Test of two particle diameters
 - SiC-1: 0.1–1.0 μm
 - SiC-2: 2.0 μm
- 1,000 h of load cycling
 - 4 min at 0.6 A cm^{-2} & 16 min at 1.0 A cm^{-2}
 - SiC-based lower degradation rates ($<65 \mu\text{V h}^{-1}$ for SiC, $>100 \mu\text{V h}^{-1}$ for Celtec)
 - But: Lower OCVs in case of SiC
- Lower acid losses in case of SiC

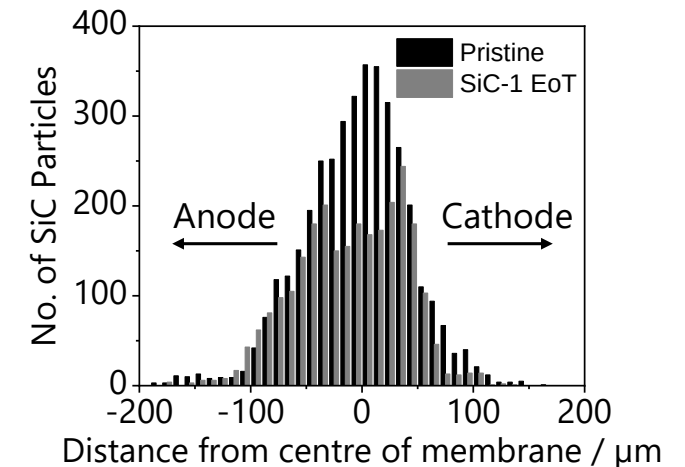
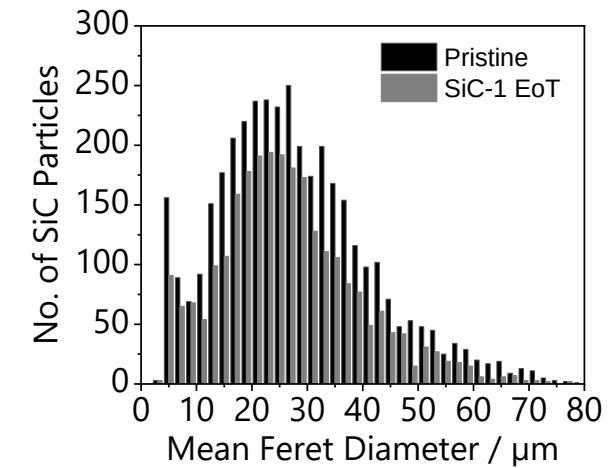
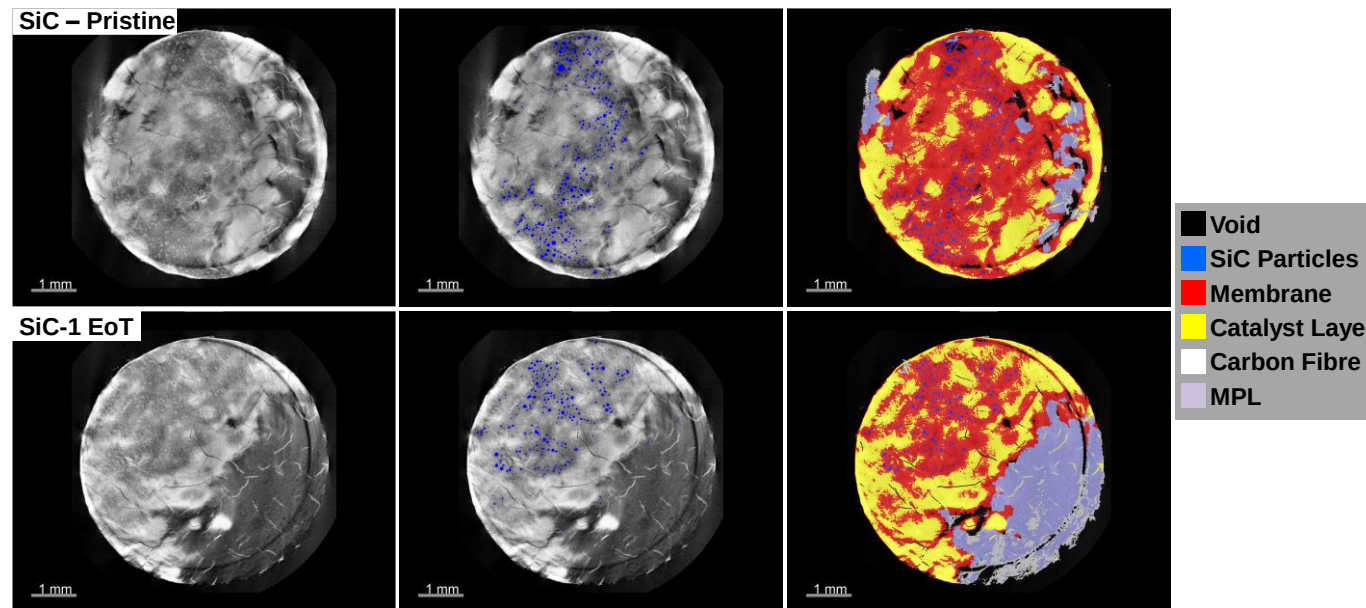


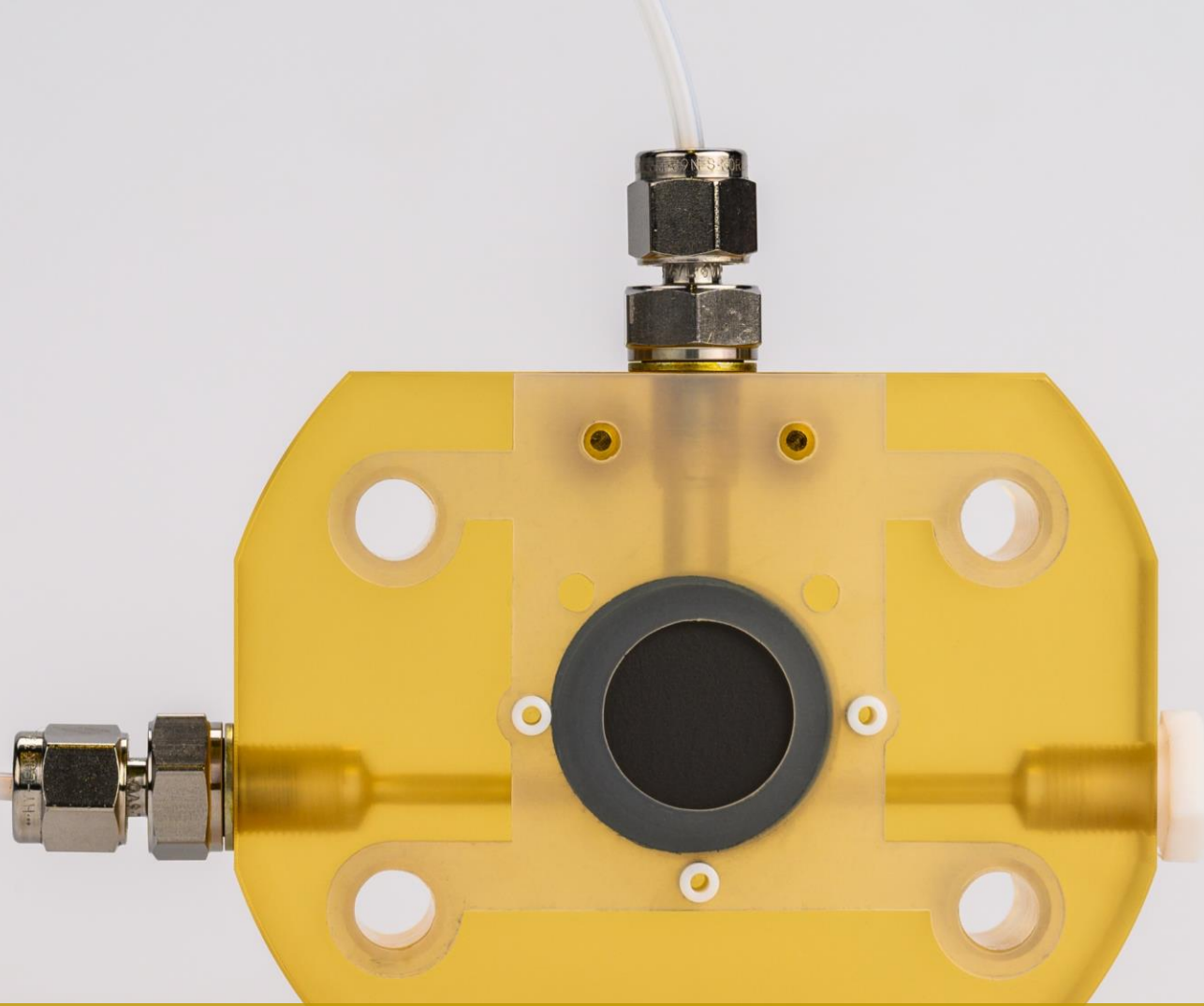
HT-PEM single cell testing: 160 °C, contact pressure 0.75 MPa, dry H₂/Air (1.5/2.0).

Silicon Carbide based HT-PEM Membranes

Computer Tomography with Machine Learning

- Cooperation with UNSW Sidney
- Lower membrane thinning using SiC
- Evidence of mobility and redistribution of SiC particles

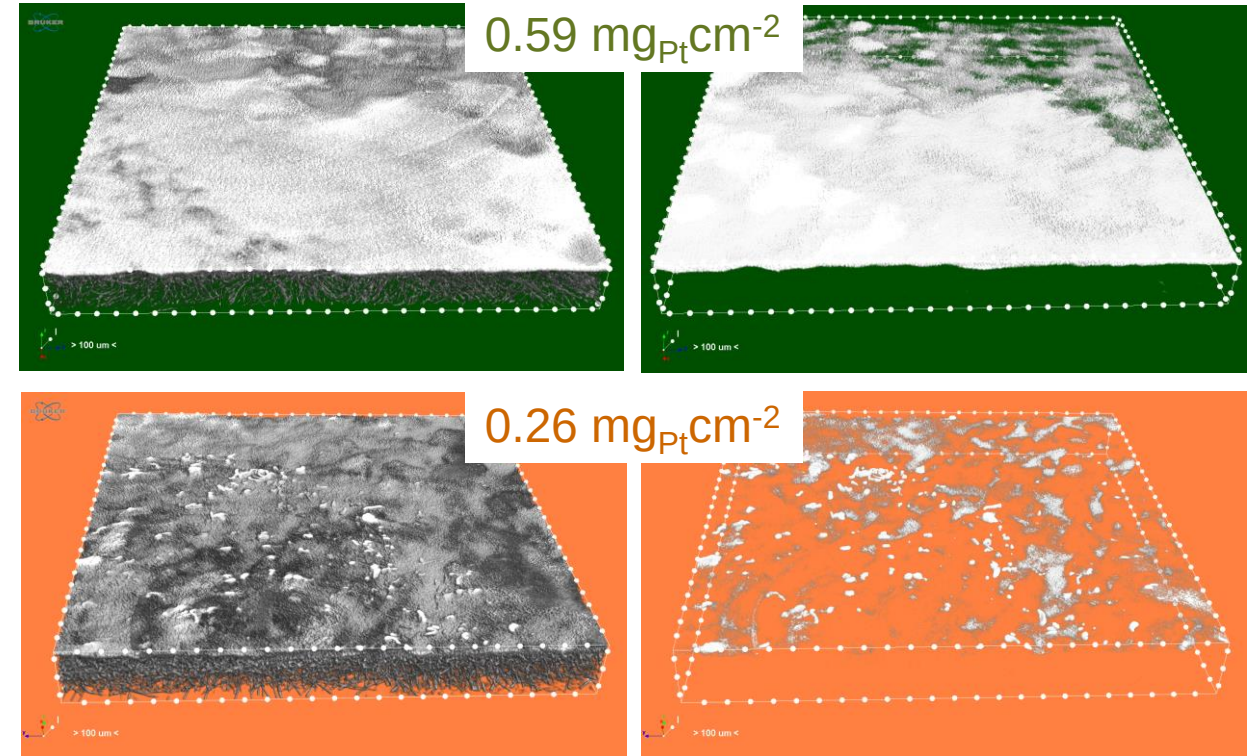
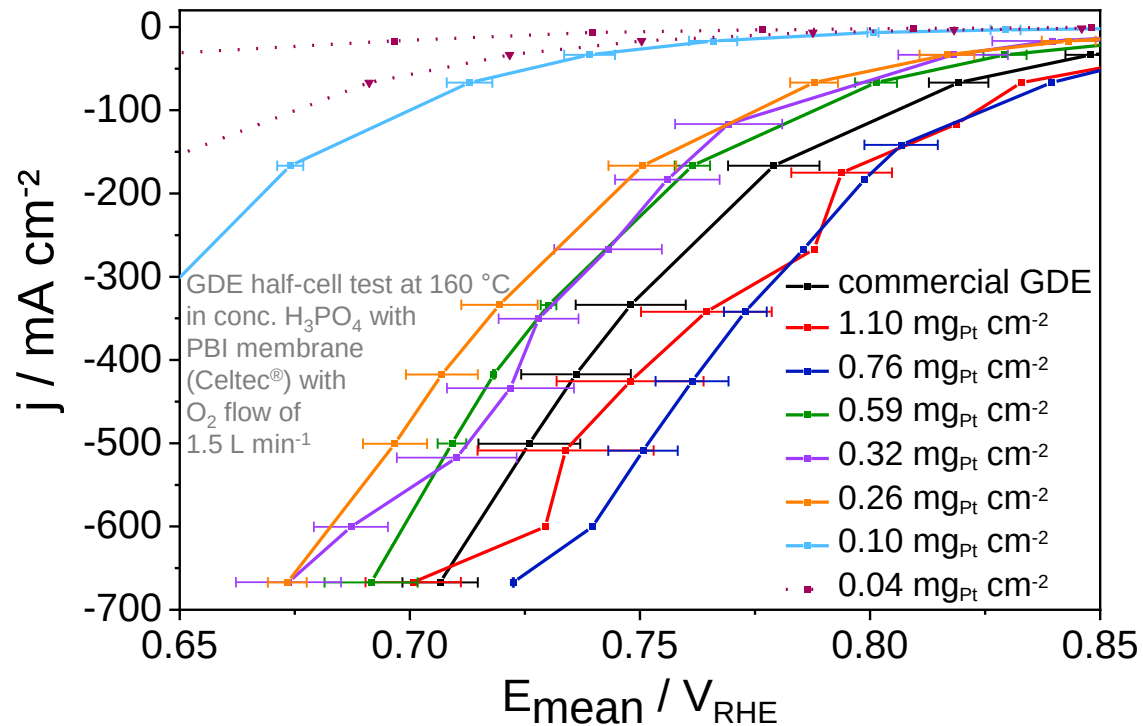




HT-PEM FC – ELECTRODES

HALF-CELL AND SINGLE CELL STUDIES

Reduction of Platinum Contents in HT-PEM Electrodes



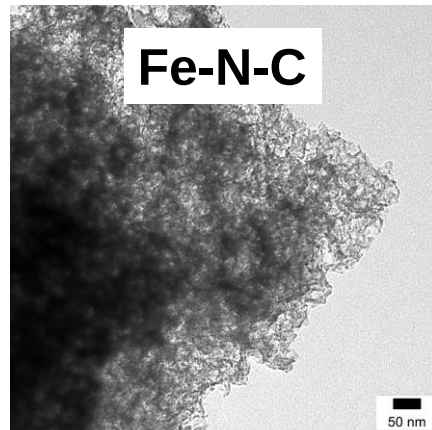
μ -Computed tomographic images of the whole GDEs (left)
and catalyst layers only (right).

→ Simple reduction of Pt-loading limited
→ Next step: Hybrid HT-PEM electrodes

Reduction of Platinum Contents in HT-PEM Electrodes

Hybrid HT-PEM Electrodes

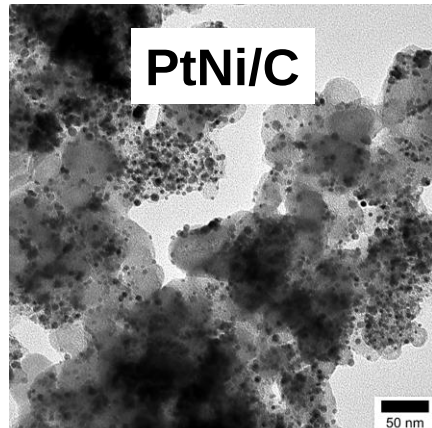
- Pt content reduction through incorporation of catalytic active filler
→ Studying the effect of Fe-N-Cs in Pt-alloy cathodes



Fe-N-C

10 wt%

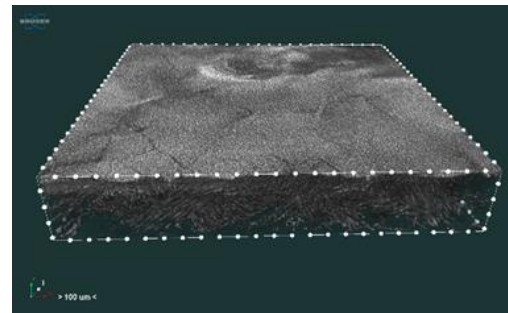
+ 40 wt% PTFE



PtNi/C

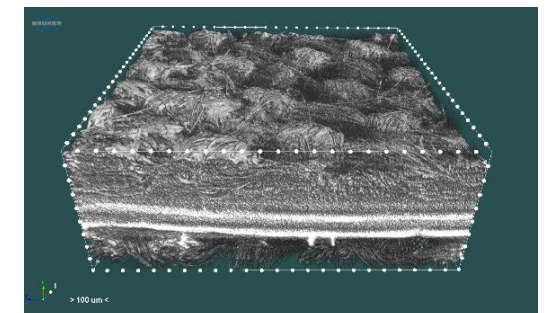
50 wt%

Hybrid Gas Diffusion Electrode (GDE)



Ultrasonic spray coating of cathode on woven Celtec®-based gas diffusion layers followed by sintering at 350 °C for 10 minutes in N₂ atmosphere

Membrane-Electrode-Assembly (MEA)



MEA-assembling analogous to Celtec®-technology with active area of 20.25 cm² and reduced Pt-content on cathode site

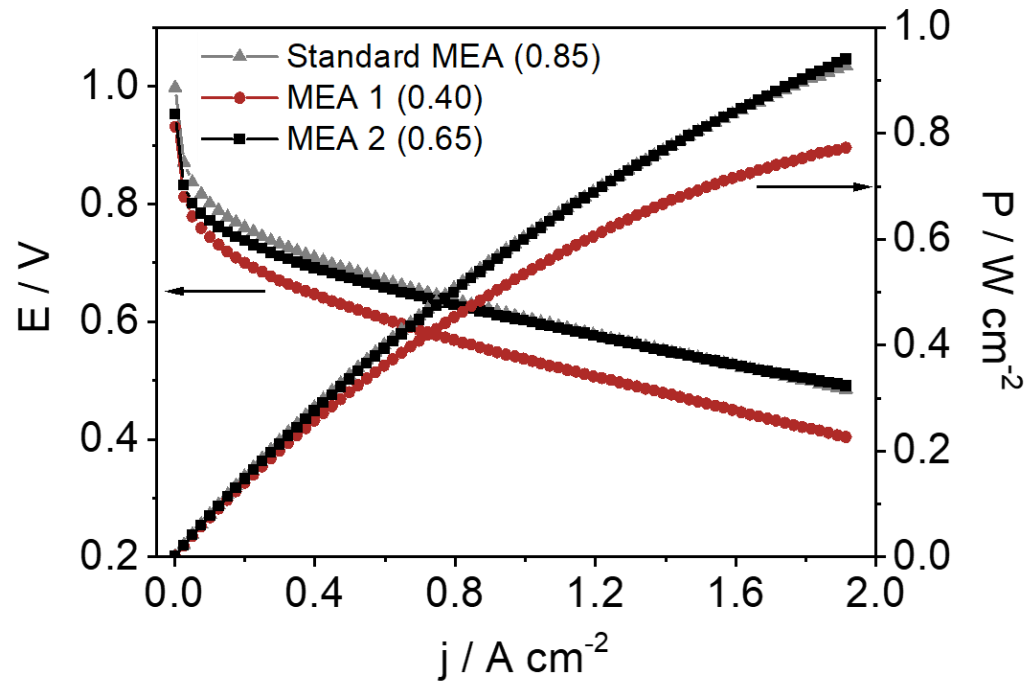
Standard: 0.85 mg_{Pt} cm⁻²

GDE 1: 0.40 mg_{Pt} cm⁻²

GDE 2: 0.65 mg_{Pt} cm⁻²

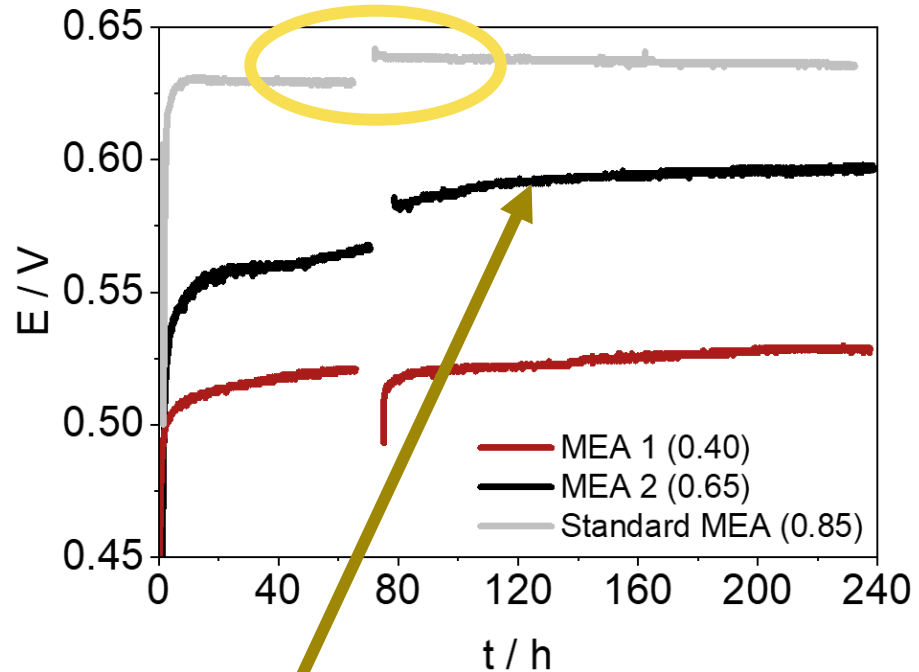
Reduction of Platinum Contents in HT-PEM Electrodes

Hybrid HT-PEM Electrodes



HT-PEM single cell testing: 160 °C, contact pressure 0.75 MPa, Dry H₂/Air (1.5/2.0); polarization curves: H₂/O₂ (1.5/9.5)

Voltage increase in case of conventional Pt-based MEA immediately after electrochemical measurements



Slow voltage increase caused by electrolyte redistribution in presence of Fe-N-C

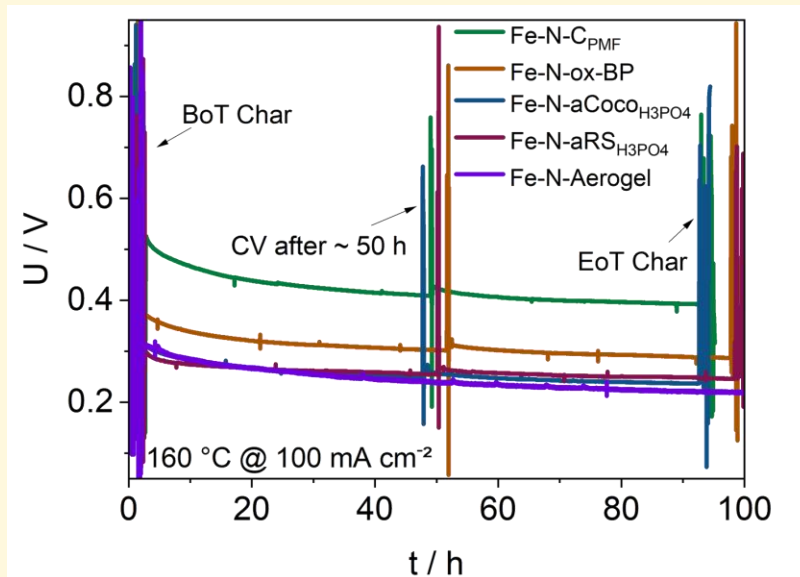
→ Improvement of catalyst layer needed

PGM-Free Electrodes

Metal-Nitrogen-Carbon Catalysts (M-N-C)

Fe-N-C-based electrodes first studies

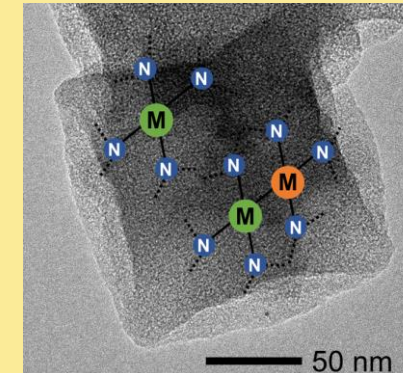
- Investigation of C-supports for Fe-N_x^[1-4, 5]



- Performance limitations of support-based Fe-N-Cs in HT-PEMFC
- Insufficient stability in HT-PEMFC
- Inhomogeneous catalyst layer

Fe-N-C-based electrodes current studies

- Catalyst optimization
 - Bimetallic FeCo^[6] and FeSn-N-Cs^[7]



- Analysis of CL fabrication
 - Binder content^[8]
 - Additives^[9]
 - Drying method^[10]

[1] J. Hülstede et al., Materials 2021,14, 1, 45.

[3] J. Müller-Hülstede et al., J. Power Sources 2022, 537, 231529.

[5] T. Zierdt et al., ChemSusChem 2025, 18, e202401843.

[7] J. G. Buschermöhle et al., ACS Catal. 2025, 15, 6, 4477–4488.

[9] T. Zierdt et al., ECS Trans. 2024, 114, 325.

[2] J. Müller-Hülstede et al., ACS Appl. Energy Mater. 2021, 4, 7, 6912.

[4] J. Müller-Hülstede et al., Int. Journal Hydrogen Energy 2024, 50, 921-930.

[6] M. Mooste et al., Electrochimica Acta 2025, 514, 145620.

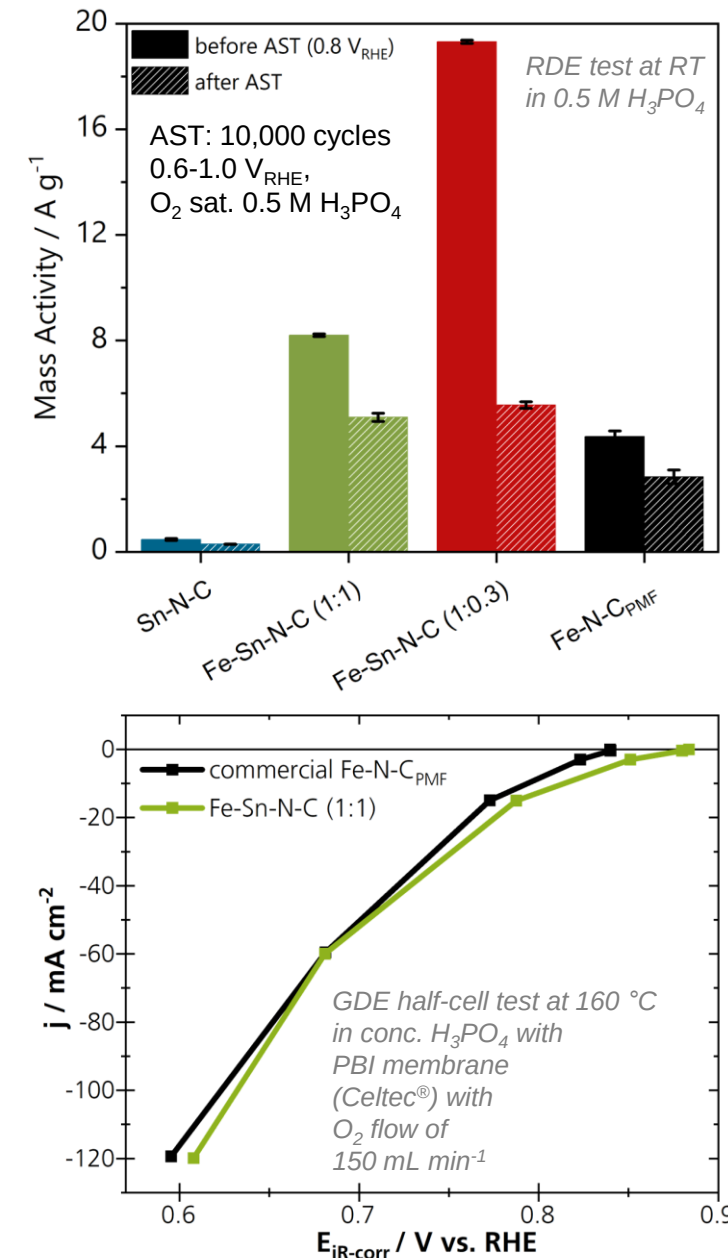
[8] T. Zierdt et al., ChemElectroChem 2024, 11, e202300583.

[10] T. Zierdt et al., ChemSusChem. 2025, 18, e202500905.

Bimetallic Fe-Sn-N-C Catalysts

- MOF-based synthesis with one pyrolysis step
 - Two metal ratios Fe:Sn (1:1 and 1:0.3)
 - Fe-loadings between 0.7 and 1.0 wt. %
- Activity and stability
 - In diluted H_3PO_4 enhanced mass activity for Fe-Sn-N-Cs
 - Beneficial effect of small amounts of Sn
 - In HT-PEM GDE half-cell higher OCV and comparable performance to commercial Fe-N-C
 - Catalyst layer fabrication has strong impact on performance

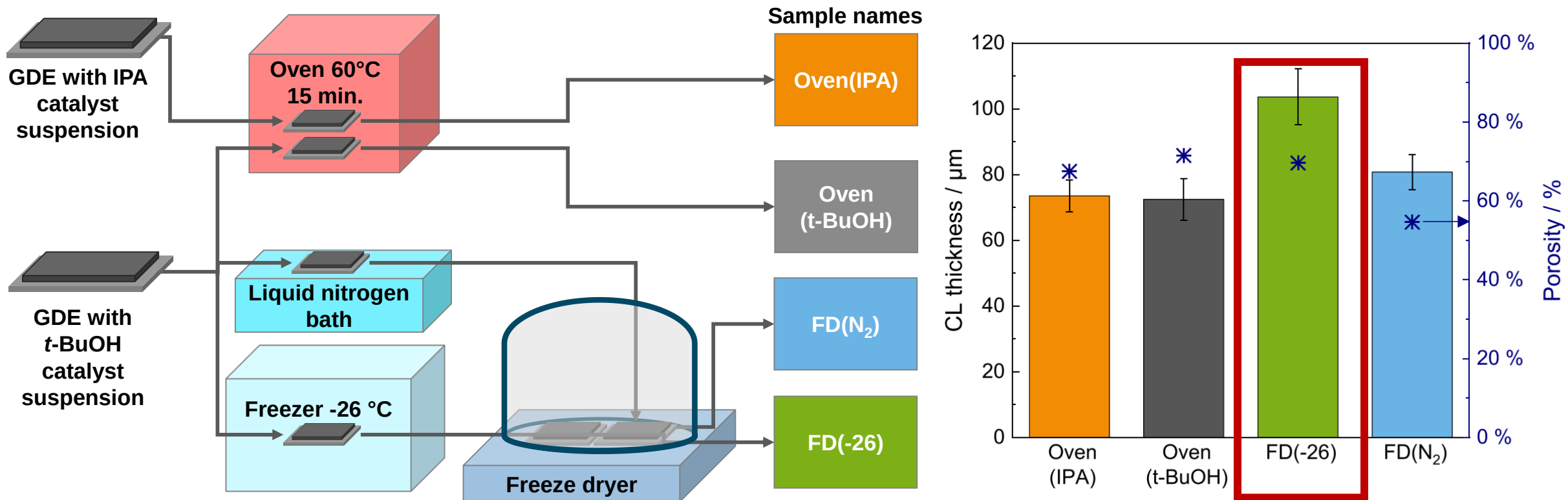
→ Further structural analysis of catalyst (*in-situ*) needed
→ Optimization of catalyst layer fabrication required



Optimization of Fe-N-C-based Catalyst Layers

Freeze-Drying vs. Oven-Drying

- Beneficial effect of freeze-drying on Pt-based CLs in CCMs for LT-PEMFC^[1]
- Transferable to Fe-N-C-based CLs using commercial PMF-011904?^[2]

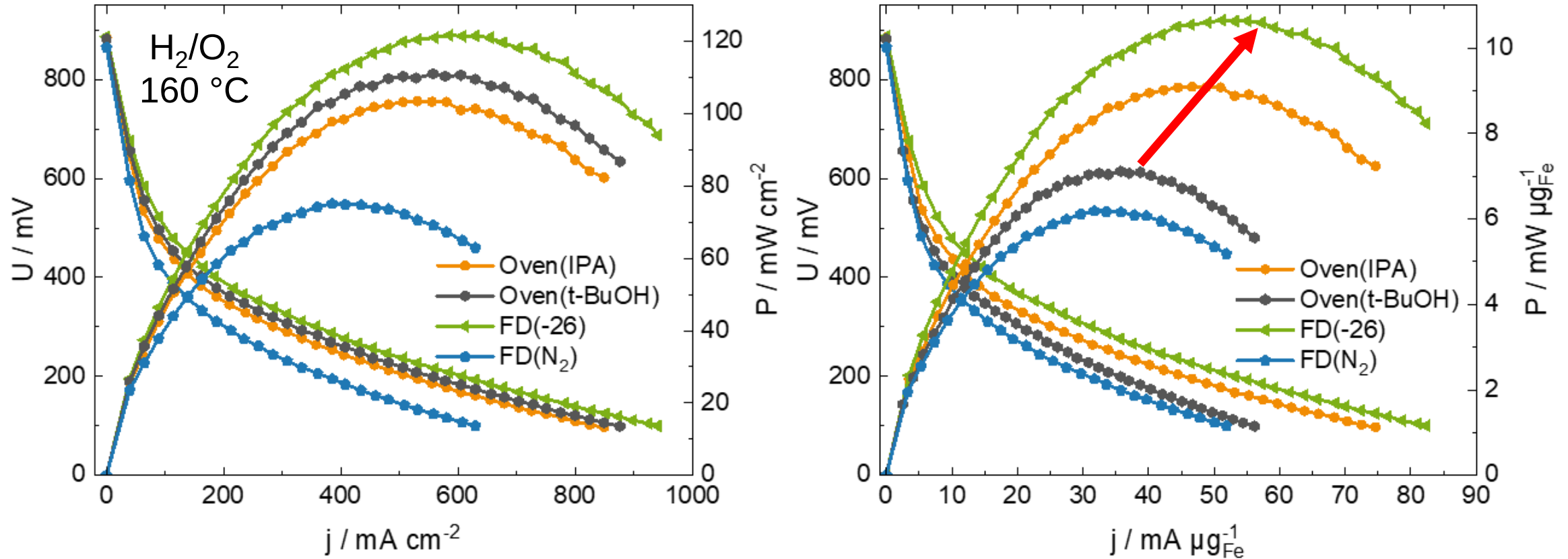


[1] K. Talukdar, S. Delgado, T. Lagarteira, P. Gazdzicki, K. A. Friedrich, J. Power Sources 2019, 427, 309.

[2] T. Zierdt, et al., ChemSusChem. 2025, 18, e202500905.

Optimization of Fe-N-C-based Catalyst Layers

HT-PEMFC Performance

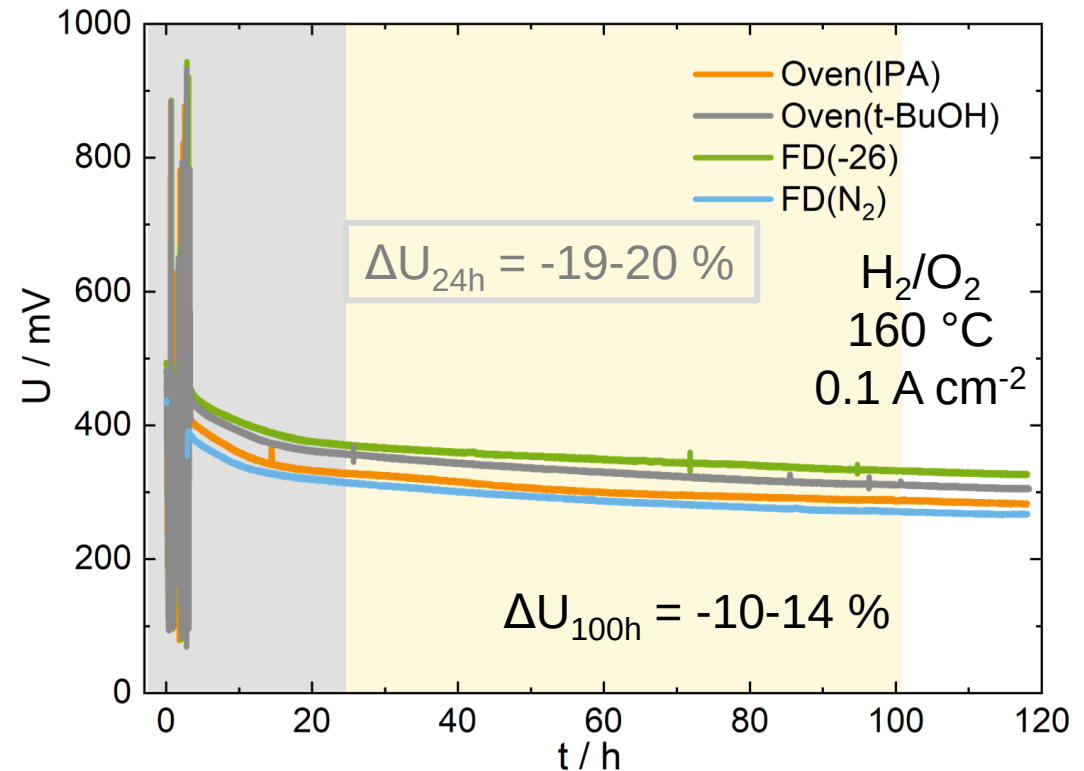


- Increase of peak power density by up to 45 % through freeze-drying of CL
 - Possibility of improved accessibility of active sites

Optimization of Fe-N-C-based Catalyst Layers

Stability over 100 h

- Stability for 100 h at 0.1 A cm^{-2}
 - Similar voltage losses independent of CL fabrication method
 - Voltage losses assumed due to formation of reactive oxygen species typically for Fe-N-Cs



→ Catalyst layer fabrication negligible effect on stability

→ Stabilisation of active Fe-N_x sites required

Outlook

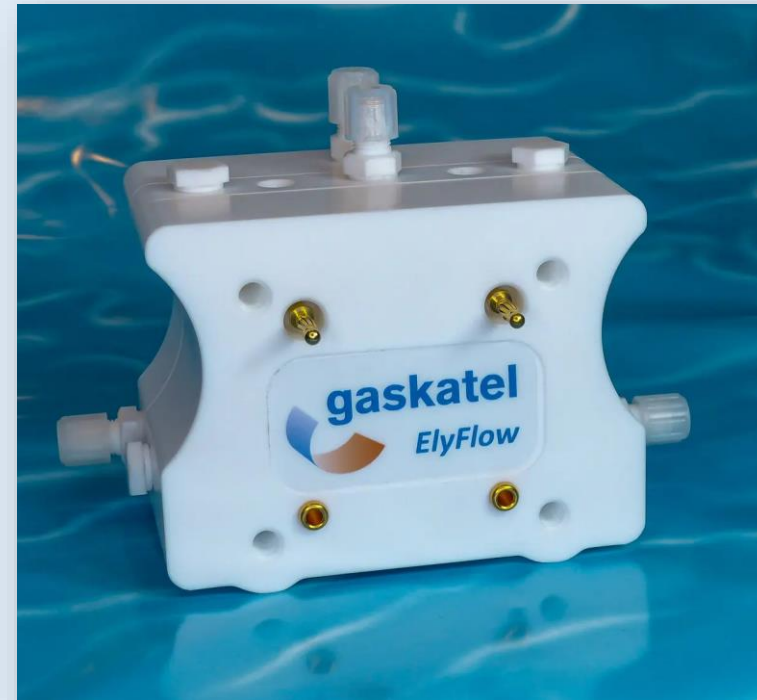
Next to material development...

- **Quality control of gas diffusion electrodes using realistic operation conditions**
 - Broad range (HOR, HER, OER, ORR, CO₂RR, NRR)
 - RT-160 °C and 1-6 bara
 - Testing of advanced measuring setup at DLR

TheMes



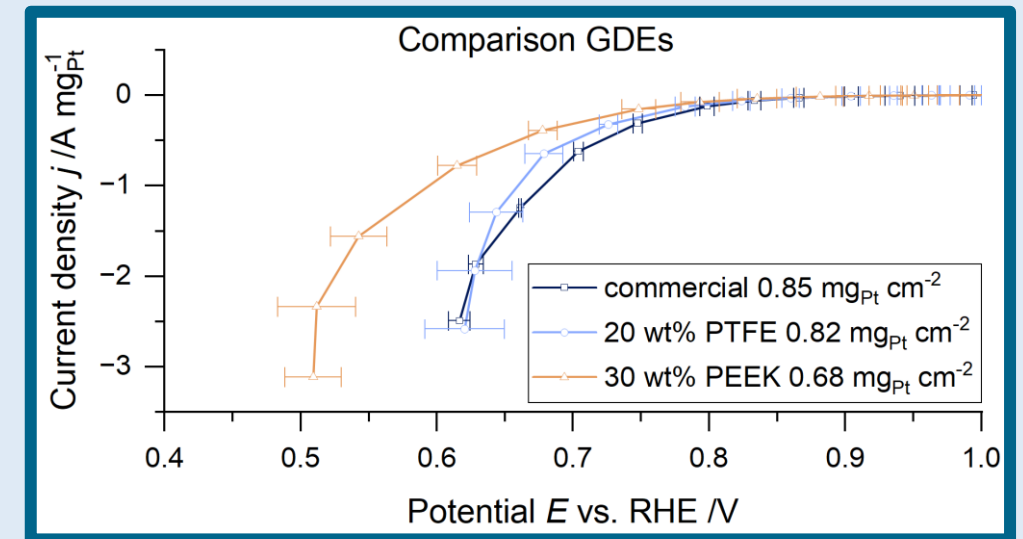
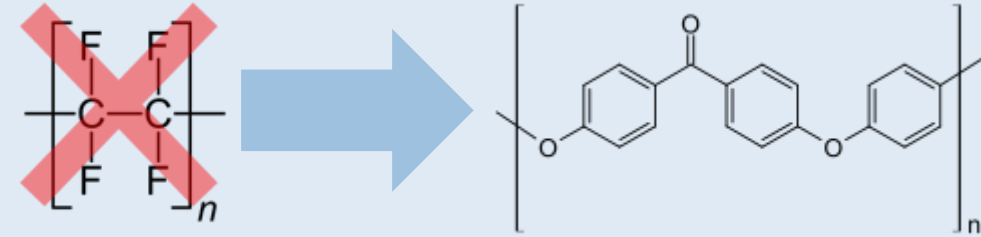
Federal Ministry
for Economic Affairs
and Energy



Outlook

Next to material development...

- Quality control of gas diffusion electrodes using realistic operation conditions
- **Replacement of PFAS in HT-PEMFC**
 - Implementation of PFAS-free polymers
 - Potential for fast up-scaling



GDE half-cell test at 160 °C in conc. H_3PO_4 O_2 flow of $150\ mL\ min^{-1}$

Outlook

Next to material development...

- Quality control of gas diffusion electrodes using realistic operation conditions
- Replacement of PFAS in HT-PEMFC
- **HT-PEM fuel flexibility for case of disasters and civil protection**
 - Containerized fuel cell system – capable of running on both methanol and hydrogen
 - Coordination and multi-fuel switching and testing



HiPEM-TECH2026

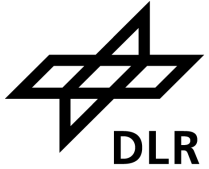
June 24th-26th, 2026

Oldenburg, Germany



HiPEM TECH

Thank you for your attention!



Acknowledgments



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