Simulating a Pneumatics Network using the DLR ThermoFluidStream Library

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Content

- Introduction
- Using the DLR ThermoFluidStream Library
- Modeling Tee Branches
- Testing Tee Branches
- Modeling Pneumatic Networks
- Conclusions



Introduction

Pneumatic system:

- turbulent flow of a compressible medium
- large pipe network
- highly non-linear components (eg actuators, valves)

Modeling approaches for components:

- PDE-based (CFD)
- 1d/2d coarse grained finite volume (special Modelica libraries)
- 0d = simple ODE or algebraic equation (standard Modelica library MFL)

Modeling of large networks:

- using MFL is cumbersome (Drente, Junglas 2015)
 - large system of nonlinear equations
 - initialisation problem is still unsolved (here)
 - tee branches particularly difficult
 - models only run after drastic simplifications
- DLR ThermoFluidStream Library TFS (Zimmer et al. 2022)
 - generally assumes fixed flow direction
 - adds inertial pressure of fluid → mass flows become state variables
 - clever approximation scheme decouples components
 - leads to linear or small non-linear equations \rightarrow initialisation often works
 - suitable approach for pneumatic pipe networks?

Using the DLR ThermoFluidStream Library

Basic ideas of the TFS library:

• incorporate pressure difference due to fluid inertia

$$\Delta r = -L \frac{d\dot{m}}{dt}$$

- often neglected in quasi-static processes (MFL)
- inertance L independent of thermodynamical state
- in TFS generally defined as small global constant
- steady mass flow pressure \hat{p} given by

 $p=\hat{p}+r$

approximate its change in a component

 $\Delta \hat{p} = f(p, \dot{m}) \approx f(\hat{p}, \dot{m})$

- leads to decoupling of components
- makes initialization problem feasible
- connectors



Specialized library PneuBibTFS:

- mainly wrappers around TFS components
 - define medium as SimpleAir
 - reduce number of parameters
- examples
 - Pipe, Bend
 - Tank (with inflow and outflow)
 - PressureSource, PressureSink
- MassFlowSource, MassFlowSink
 - mass flow is state variable in TFS!
 - implemented with control valve using PT1 dynamic
 - simpler with linear valve
 - actuator = linear MassFlowSink
- tee branches need special care

Modeling Tee Branches (1)

Tee branches:

• split or join mass flows



- simplification: 90° angle and identical cross sections A
- complex behaviour
 - changed total cross sections → dynamic pressure changes
 - internal friction \rightarrow pressure drops
- nonlinear coupling across the complete model
 - MFL: drastic simplifications necessary (substitutional pipe length)
 - TFS: no nonlinear coupling of components (mass flow is state variable!)

Equations of basic splitter TeeBranchS:

- simplifications
 - constant temperature
 - constant density, coming from input state
 - in applications usually ok
- loss functions ζ_{cs} , ζ_{cb}
 - describe friction and part of dynamical pressure
 - here: simple fit polynomials
- basic equations

$$\begin{array}{rcl} 0 &=& \dot{m}_{i} + \dot{m}_{s} + \dot{m}_{b} \\ \rho &=& \rho(\hat{p}_{i}, h_{i}) \\ \Delta p_{s} &=& -\frac{1}{2\rho A^{2}} \zeta_{cs} \left(\frac{\dot{m}_{b}}{\dot{m}_{i}}\right) \dot{m}_{i}^{2} \\ \Delta p_{b} &=& -\frac{1}{2\rho A^{2}} \zeta_{cb} \left(\frac{\dot{m}_{b}}{\dot{m}_{i}}\right) \dot{m}_{i}^{2} \\ \Delta p_{dyn,s} &=& \frac{1}{2\rho A^{2}} (\dot{m}_{i}^{2} - \dot{m}_{s}^{2}) \\ \Delta p_{dyn,b} &=& \frac{1}{2\rho A^{2}} (\dot{m}_{i}^{2} - \dot{m}_{b}^{2}) \\ \hat{p}_{s} &=& \hat{p}_{i} + \Delta p_{dyn,s} + \Delta p_{s} \\ \hat{p}_{b} &=& \hat{p}_{i} + \Delta p_{dyn,b} + \Delta p_{b} \\ h_{s} &=& h_{i} \\ h_{b} &=& h_{i} \end{array}$$

• in TFS additional equations for r variable (Zimmer 2020)

Modeling Tee Branches (2)

Variant TeeBranchS1:

• uses DynamicSplitter from TFS



- computes dynamic pressure differences using cross section areas
- adds SplitterPressureLoss component for ζ functions



- differences to TeeBranchS
 - DynamicSplitter is adiabatic, not isothermal
 - SplitterPressureLoss uses density after DynamicSplitter, not at Inlet
 - 147 equations instead of 28

Variant TeeBranchS2:

- basically like TeeBranchS1
- DynamicSplitter uses densities at input and output streams
- adds two nonlinear equations inside the component

Joining components:

- TeeBranchJ, TeeBranchJ1 and TeeBranchJ2, similar to splitters
- different handling of r variables

Testing Tee Branches (1)

Basic test models:

• join case, mass flows given at inlets, pressure at outlet



- results for basic components in MFL and TFS almost identical
- deviations in straight branch for density aware components

• results for MFL and several TFS components



pressure straight



Testing Tee Branches (2)

Stability of models:

- possible behaviour
 - runs with standard initial conditions
 - runs with special initial conditions
 - doesn't run
- tests with different boundary conditions
 - pressure at inflow, mass flow at outflow
 - mass flow at inflow, pressure at outflow
 - pressure at inflow and outflow
- results
 - MFL model works always
 - all TFS models work for simple cases (two mass flows given)
 - basic TFS component works in most non-simple cases
 - other TFS components work never in non-simple-cases
- problem
 - initialization works always
 - pressure soon rises exponentially
 - differential equations are highly unstable!
 - thorough mathematical investigation needed

Adding a pipe at straight inflow or outflow:

- simple cases
 - all TFS work (as before)
 - some MFL models don't work!
- non-simple cases
 - non-conclusive
 - some MFL models get unstable (don't run)
 - some TFS become stable
- preliminary conclusion
 - adding pipes destabilizes MFL (larger nonlinear system)
 - adding pipes stabilizes TFS

Modeling Pneumatic Networks (1)

Example model:

• network 1



- difference to MFL version
 - tank has dedicated inflow and outflow
 - connected via a loop with splitter and joiner
- stability
 - MFL: only runs with simplistic tee branch models
 - TFS: all three versions run with standard initial conditions
 - ${\scriptstyle \bullet \ } \rightarrow$ preliminary conclusion from tests verified



- differences between tee branch versions below plot accuracy
- negligible temperature and density changes

Modeling Pneumatic Networks (2)

Extended example model:

• adds auxiliary tank betwen two consumers



- stability
 - base model stops at 80 s (consumer at tank 1 is switched on)
 - simple remedy: add small pipe in tank loop



- significant deviations due to drastic simplifications in MFL version
- smaller pressure variation at consumer2

Modeling Pneumatic Networks (3)

Real-world model:

- medium-sized model from industrial partner
 - implemented in PneuBib + MFL
 - 60 components (3 pumps, 1 tank, 12 consumers, 17 simple tee branches)
 - ≈ 4500 equations
- porting to PneuBibTFS
 - specify flow directions
 - include tank via a small loop
 - initial pressure of tank = pump pressure (all equal)
 - ≈ 1750 equations
- simulation stops after 1 s
 - several flows have wrong direction
 - due to identical pump pressures
- remedy
 - increase pressure of one pump marginally
 - ${\scriptstyle \bullet \ } \rightarrow$ all flow directions fixed
 - \blacksquare \rightarrow model runs, reproduces results of MFL version qualitatively

Conclusions

TFS-based pneumatics library:

- usually works directly
 - in case of instability add auxiliary pipes
- more accurate results
 - dynamic pressure changes missing in crude MFL version
- more detailed tee branch components
 - change results only marginally
 - generally reduce stability

Using OpenModelica:

- introduced additional problems with MFL version
- with PneuBibTFS no differences to Dymola
 - enhanced OpenModelica simulator
 - TFS models much simpler for simulator

Enhancement of tank model:

- more realistic: use one tank port in both flow directions
- possible due to TFS enhancement for bidirectional flows
- open questions
 - significantly better results?
 - stability?

Problem of stability:

- cause
 - MFL: nonlinear equations
 - TFS: unstable differential equations
- probably related
- open questions
 - mathematical analysis of instability
 - mechanism of stabilization through pipes

Initialization problem:

- in MFL still open (Drente, Junglas 2015)
- in TFS solved (at least for pneumatics networks)