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# Effects of a Three-Dimensional-Printed Atomizer Component on Fuel-Spray and Flame Characteristics of a Jet-Stabilized Compact Gas Turbine Combustor Fed with Liquid Fuels

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## ABSTRACT

*In this work, the effects of replacing an atomizer component of a confined jet-stabilized gas turbine combustor with a 3D-printed part have been studied. The part is called airblast, and it serves as a wall that collects and flows liquid droplets for a secondary atomization. Therefore, the liquid-surface interaction on the rough surface of the 3D-printed part was of interest. The combustor was operated under various conditions with either a conventionally machined airblast or the 3D-printed airblast. Flames with two liquid fuels were studied for fuel flexibility, and the position of a primary fuel injection was varied to study the influence of the liquid-surface interaction length. Load*

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31 *flexibility was investigated with air jet velocity settings, and flame equivalence ratios of  $\phi=0.8$  and 1.0*  
32 *were tested.*  
33 *Shadowgraphy-based particle tracking analyses presented a reduced atomization performance with the*  
34 *3D-printed airblast, showing large droplet size distributions. However, no significant change in the*  
35 *combustor performance was observed from OH\* chemiluminescence images and emission data, which*  
36 *confirms the versatility of the combustor and assures the compatibility of 3D-printed components with the*  
37 *combustor of this study.*

## 38 **1. INTRODUCTION**

39 Micro gas turbines (MGTs) serve as a promising alternative for decentralized  
40 power generation with high power density, fuel flexibility, and low emissions [1]. Gas  
41 turbines can be operated with either gaseous or liquid fuels [1, 2], and liquid energy  
42 carriers will play an essential role in energy transition systems because they provide  
43 high energy density which can bring advantages in autonomy, transportation, and  
44 storage. MGTs have the potential to operate with a variety of alternative and renewable  
45 liquid fuels produced from various sources (i.e., various compositions and properties),  
46 without major technical modifications. However, when operating MGTs with liquid  
47 fuels, an atomization system is required [2], and it increases the challenges of scalability,  
48 mainly regarding proper mixing of fuel and oxidizer within short time scales.

49 Recently, a canonical single-nozzle confined burner fed by liquid fuels was  
50 developed, employing a high-momentum jet stabilization technology [3]. The burner  
51 was developed with a focus on MGT applications, and it includes a novel in-house dual  
52 pressure swirl atomizer (PSA)/airblast injection concept. The PSA produces a fuel spray,  
53 and the large droplets of the spray are collected and re-atomized by high shear forces

54 on the wall of an airblast. The evaluation of the burner showed that high operational  
55 and thermal load flexibility is achieved with low emissions when using extra light heating  
56 oil (HEL) as fuel [3].

57 One additional challenge with small-scale liquid injection systems lies in the  
58 manufacture of the components. Parts with complex geometries are often required,  
59 which results in long production times and high costs. In this regard, additive  
60 manufacturing of metal components (so-called metal 3D printing), in particular laser  
61 powder bed fusion (LPBF or selective laser melting, SLM), has gained relevance in the  
62 low-cost fast prototyping and production of gas turbine components [4, 5] including  
63 injections systems [6-8]. However, due to the powder-melting and layer-by-layer  
64 building process, the surface quality of 3D-printed metal components is often a matter  
65 of concern in liquid-surface interactions.

66 In recent studies by Cejpek et al. and Jedelský et al. [9, 10], the effects of the  
67 surface roughness on the atomization performance of 3D-printed pressure swirl  
68 atomizers were evaluated. However, the 3D-printed components had to be fabricated  
69 on a large scale due to the size limitation of the available SLM technique. It was  
70 concluded in those studies that large surface roughness and manufacturing  
71 imperfections can worsen the spray quality, e.g., spray distribution uniformity, based on  
72 the evaluation with the up-scaled printed atomizer.

73 Sanchez et al. compared the atomization performance of 3D-printed and  
74 conventionally machined airblast-atomization systems, which resembles typical RQL

75 (Rich-Quench-Lean) aviation combustors (i.e., fuel channels with integrated inner air  
76 swirlers) [7]. It was shown that the functional behavior of the 3D-printed injector  
77 matches the reference part with very little differences. Crayford et al. evaluated a 3D-  
78 printed pre-filming airblast atomization system produced by SLM and electro-polished  
79 afterward to improve the surface quality [11]. A uniform spray was generated, although  
80 the pressure drop of the airflow through the injector was around 30% larger than  
81 predicted. Nevertheless, combustion experiments at atmospheric pressure with Jet A-1  
82 demonstrated flame stability across a wide range of operating conditions.

83 Conclusions from the previous works impose a necessity of studying 3D-printed  
84 parts to further develop burners with desired geometry at lower cost. Therefore, in this  
85 work, the machined airblast of the dual injection system of the confined jet-stabilized  
86 burner in the previous work was replaced by a 3D-printed component to investigate its  
87 impact on the burner's performance [3]. Atomization quality, flame characteristics, and  
88 exhaust gas composition were compared for the 3D-printed and conventionally  
89 machined airblasts installed in the burner. The experiments were performed at  
90 comprehensive operating conditions, using Jet A-1 and HEL as fuel.

## 91 **2. MATERIALS AND METHODS**

92  
93

### **2.1. Confined jet-stabilized burner**

94 The design and development of the single-nozzle jet-stabilized burner for liquid  
95 fuels have been described in the previous work [3], so it will be briefly introduced here.  
96 A schematic of the burner assembly on an atmospheric pressure test rig is depicted in  
97 Fig. 1. The combustion chamber has a rectangular cross-section of  $40 \times 50 \text{ mm}^2$  with a

98 total length of 600 mm consisting of three segments providing excellent optical access  
99 (only one of the segments is shown in Fig. 1a). The burner nozzle has an inner diameter  
100 of 12 mm and is placed off-centered along one of the axes to stabilize the flame by  
101 recirculation [12]. Preheated air at a controlled flow rate and temperature is supplied to  
102 the burner. The high-momentum air flow is conditioned through a contoured  
103 contraction nozzle which is coaxial to a fuel lance. The fuel lance supplies fuel, and it is  
104 water-cooled. A pressure swirl atomizer (PSA) is mounted at the tip of the fuel lance.  
105 Throughout this study, a PSA with a flow number of 0.35 was employed. The flow  
106 number is defined according to Lefebvre and McDonell [13], as:

$$107 \quad FN_{US} = \frac{\text{Flow rate, lb/h}}{(\text{Injection pressure differential, psid})^{0.5}} \quad (1)$$

108 The detailed pressure swirl atomizer-airblast injection system is presented in Fig.  
109 1b. When a fuel spray is generated by the PSA, small droplets are transported by high-  
110 momentum air jet directly into the combustion chamber, while large droplets and  
111 ligaments that flow radially are collected by the airblast and re-atomized by shear forces  
112 at the exit. The position and design of the airblast create a geometric split of the entire  
113 air flow into atomization and co-flow air [3]. Depending on how the mixing length ( $l_m$ ) is  
114 set, the fuel and air can continue mixing inside the nozzle or the mixture can directly  
115 enter the combustion chamber.  $l_m$  was kept at 0 in this study. The axial position of the  
116 PSA with respect to the airblast can vary the film length,  $l_f$ , by changing the fixing  
117 position of the fuel lance.

## 118 2.2. 3D-printed airblast

119 Fig. 2 presents a 3D model of the airblast. The airblast was printed as a single  
120 part by SLM using a metal 3D printer (EOS M290) in layers of 40  $\mu\text{m}$  of stainless steel  
121 (316L/1.4404). As illustrated in Fig. 2, some surfaces for sealing were polished after  
122 being printed, to improve their surface roughness ( $R_a = 4\text{-}7\ \mu\text{m}$ ). On the other hand, the  
123 surfaces in contact with the fuel and air flows have kept the surface roughness of the  
124 SLM process ( $R_a = \sim 35\ \mu\text{m}$ ). The surface roughness difference is distinct from the  
125 microscopic images.

### 126 **2.3. Operating conditions**

127 In order to study the effects of the 3D-printed component on the burner system,  
128 multiple parameters were varied for the tests with both the machined airblast and the  
129 3D-printed airblast: liquid fuel, injector (PSA) position, air jet velocity, and equivalence  
130 ratio ( $\phi$ ). Jet A-1 and HEL were chosen as liquid fuels, and injection from the PSA was at  
131 either one diameter (i.e.,  $1d=12\ \text{mm}$ ) or two times the diameter below the nozzle tip.  
132 Air jet velocity (i.e., bulk velocity) was set to 120 or 160 m/s.  $\phi = 0.8$  was set as a  
133 reference value, while  $\phi = 1.0$  was tested for some limited cases. The combinations of  
134 the variable parameters are listed in Table 1, and case numbers are assigned for each  
135 airblast type as a reference. Other parameters, such as mixing length  $l_m=0$  (cf. Fig. 1b)  
136 and the air preheating temperature of 650 K were kept for all cases.

### 137 **2.4. Shadowgraphy, chemiluminescence imaging, and emission measurement**

138 The atomization process was evaluated at different locations downstream in the  
139 burner using double-pulse background-illuminated shadowgraphy. For the double-pulse  
140 illumination, two second-harmonic laser beams from two identical Nd:YAG lasers

141 (Quanta Ray, Spectra Physics) were expanded to a diameter of 150 mm using a spherical  
142 lens ( $f=30$  mm) and utilized to induce light emission from a fluorescence screen  
143 (diffused red-shifted light, decay time  $<50$  ns). The time interval between two pulses  
144 was set to  $2 \mu\text{s}$ . A CMOS camera (LaVision CX12) was employed for the imaging, with a  
145 180 mm macro lens of  $f/2.8$  (Sigma). The field of view was set to  $15 \times 20 \text{ mm}^2$ , and the  
146 size of one pixel in the shadowgraphy image was equivalent to  $5 \mu\text{m}$ . By translating the  
147 burner, six heights in steps of 18 mm in the axial direction were measured, and the  
148 heights were covering from the nozzle exit to the lower part of the flames. At each  
149 height, 300 instantaneous double-frame images were recorded at 10 Hz, with a frame  $\Delta t$   
150 of  $2 \mu\text{s}$ .

151 High-speed  $\text{OH}^*$  chemiluminescence ( $CL$ ) imaging at 14 kHz was simultaneously  
152 employed to study flame behaviors since an  $\text{OH}^*$   $CL$  signal indicates where heat release  
153 zones are located. A high-speed camera (Photron FASTCAM SA5) coupled with high-  
154 speed intensified relay optics (LaVision HS-IRO). A 64 mm  $f/2.0$  UV lens (Halle Nachfl.)  
155 and a 310-320 nm band-pass filter (AHF) were used to collect the  $\text{OH}^*$  signal. The  $CL$   
156 images were taken from the side perpendicular to the shadowgraphy imaging, and  
157 therefore, the off-centered flame and recirculation zone could be visualized in the  
158 images. The field of view was set to  $100 \times 200 \text{ mm}^2$ , which covers one section of the  
159 combustion chamber (cf. Fig. 1).  $CL$  images presented in this study were taken at the  
160 bottom section (i.e., nozzle height) of the burner.



161 Exhaust gas composition was measured using a portable reference emission  
162 analyzer (MRU MGA prime), using its probe installed at the top of the combustion  
163 chamber (i.e., 600 mm above the nozzle). The probe was air-cooled to prohibit further  
164 reaction in the tube, and the gas was kept heated up to the gas analyzer to prevent  
165 water condensation during the transportation. The air-cooling amount was adjusted  
166 depending on the flame conditions, and the tube-heating temperature was kept at  
167 120°C.

## 168 **2.5. Particle tracking velocimetry**

169 A sample shadowgraphy image from the lowest height is presented in Fig. 3,  
170 overlaid by detected droplets and computed vectors. Particle detecting, sizing, and  
171 linking between two frames of a shadowgraphy image were done with the help of the  
172 Python toolbox Trackpy (version 0.6.1) [14, 15]. Raw images were pre-processed by flat  
173 background removal and gradient mapping, which provided the best-binarized results.  
174 In the next step, the Trackpy algorithm linked the particles by iteration based on the  
175 initial velocity input (i.e., air jet velocity) and the size similarity. At last, velocity  
176 components were calculated based on the displacement, and the axial velocity  
177 component and size of detected particles were analyzed. The minimum size of detection  
178 was set to 3 pixels, and it is equivalent to a spherical droplet with a diameter of 9.8  $\mu\text{m}$ .

179 For the analysis between different cases, droplet size distributions, instead of  
180 averaged absolute sizes, are compared. This is due to the limitation regarding the depth  
181 of field. The detected particles are accumulated along the lens axis for a certain distance  
182 (i.e., focal depth) and the droplet sizes are overestimated due to the particles slightly

183 out of focus. A depth of field calibration can be useful to compensate this effect, but it  
184 was not possible to obtain reference images with the same temperature gradient as in  
185 an operating burner. Therefore, processing the droplet size information further into a  
186 single representing value and comparing them between cases could lead to a biased  
187 conclusion.

### 188 **3. RESULTS AND DISCUSSION**

189

190 In Fig. 4, as an example, axial velocity-size relations of the detected droplets are  
191 presented for two cases using the machined airblast. All the detected droplets from 300  
192 images of the same height are marked with one color, and six colors are used for the six  
193 heights. An axial velocity component, computed from an apparent displacement on the  
194 images, is used for the analyses due to the lack of three-dimensional information.  
195 Droplet size analysis is based on a sphere-equivalent diameter to compare the droplets  
196 in different shapes. Droplet sizes are discrete due to the conversion from the pixel  
197 counting, and it is more visible for the small values (cf. left part of Fig. 4).

198 Mean curves of the droplets at all heights are added in Fig. 4. Due to the discrete  
199 manner of the droplet sizes, group mean velocities for each size could be easily  
200 computed. On the other hand, velocities had to be grouped arbitrarily with a step of 5  
201 m/s to compute group mean sizes. Using these values, group mean velocity curves were  
202 drawn horizontally, and group mean size curves were drawn vertically in both panels.  
203 When the data points are insufficient in quantity, a fluctuation in the mean curves is

204 observed. Therefore, the large noise level of the mean curves indicates small population  
205 of droplets at the part of the plot (cf. right side of Fig. 4).

206 The entire data set from cases 1 to 20 has been thoroughly investigated using  
207 scatter plots and raw images, and some distinct tendencies were observed. For more  
208 detailed analyses, group mean curves at each measurement height are presented in Fig.  
209 5. For better visibility, individual markers are removed and mean curves for each height  
210 are drawn in Fig. 5, with the same color code used in Fig. 4.

211 In Fig. 5, a clear difference between 120 and 160 m/s air jet velocity cases is  
212 observed. The mean axial velocity is naturally larger for 160 m/s case for all the heights,  
213 and the air jet velocity presents an impact on the droplet size distribution. Looking at  
214 the vertical curves in Fig. 5a, droplets tend to be more populated at certain axial  
215 velocity, and thus some peaks appear. In addition, the peak position shifts to a larger  
216 axial velocity as the height increases. It implies that there is a dominant size group of  
217 droplets that accelerates with the airflow. The grouping is not very pronouncing close to  
218 the nozzle possibly due to the large number of droplets in a wide range of sizes, but the  
219 grouping is trackable from the height 36 mm above the nozzle (cf. the green curve in Fig.  
220 5a) and higher. On the other hand, no dominant droplet size group is observed from the  
221 160 m/s air jet velocity case (cf. Fig. 5b). It shows quite even droplet size distribution,  
222 and it is only noticeable that the overall droplet size is larger for the lowest height than  
223 the other heights.

224 To compare different cases in a straightforward way, the group mean size curves  
225 (i.e., vertical curves in Fig. 5) are drawn together with reduced complexity. A contour of  
226 the full outer join area for each case is introduced, and the detailed process of making a  
227 contour is illustrated in Fig. 6. By using these size contours, the overall size distribution  
228 of each case can be directly compared without losing the height-specific information.

229 The results from all the cases in Table 1 are presented in Fig. 7, where four size  
230 contours are presented in each panel and compared. In each panel, three variable  
231 parameters (cf. Table 1) are shared and noted at the upper right corner. The other two  
232 variables are labeled next to each curve, after their case number and followed by the  
233 total number of droplets detected. In this way, all the cases in Table 1 could be  
234 compared relatively straightforward. For an easier data comparison for the readers,  
235 shades of red or yellow colors are used to present the cases with the 3D-printed  
236 airblast, while the other colors are with the machined airblast. In addition, a few cases  
237 appear again in another panel, and they keep the same colors.

238 In Fig. 7, a few general tendencies are found when cases with different airblasts  
239 or air jet velocities are compared. The 3D-printed airblast results in larger numbers of  
240 droplets detected from 30% to 120% more than the machined airblast cases (cf. the  
241 numbers at the end of each label in Fig. 7) for all cases except one pair (i.e., case 5 and  
242 15 in panel a). Regarding the number of droplets detected, efficient atomization and  
243 evaporation of liquid fuel would reduce the number of detectable droplets in the vicinity  
244 of a flame. On the other hand, the larger number of droplets could mean good

245 atomization as well, if the droplet sizes are smaller. Therefore, the number of droplets  
246 has to be interpreted together with the mean droplet size for each case. In general,  
247 most of the cases in Fig. 7 present pronounced droplet number increase accompanied  
248 by mean size increase, which supports that the 3D-printed airblast produces larger  
249 droplets as a result of a less efficient atomization performance.

250 As discussed earlier in Fig. 5, the flatness of a group mean velocity curve is  
251 correlated to the air jet velocity, and the trend is shown in Fig. 7a, 7b, and 7e. 120 m/s  
252 setting tends to present distinct peak sizes at certain velocities, but peaks are less  
253 pronounced for 160 m/s cases. There are two cases that do not follow this general  
254 trend, namely, cases 15 and 20 in Fig. 7a and 7b, respectively. Both cases are with the  
255 3D-printed airblast and the injector positioned at 2d. Therefore, it implies that the  
256 presence of the dominant size group is related to the interaction between the surface of  
257 the airblast and the liquid fuel. From the observation, a rougher surface of the wall and  
258 a longer interaction between the wall and the liquid are represented by the peaks in the  
259 velocity-size plot. However, further investigation is necessary to understand the detailed  
260 physics of the phenomenon.

261 The effect of different airblast types can be studied using Fig. 7a and 7b as well.  
262 On average, 3D-printed airblast forms larger droplets than the machined airblast. When  
263 the machined airblast is employed, Jet A-1 results in a smaller mean droplet size than  
264 HEL. However, with the 3D-printed airblast, smaller mean droplet sizes are measured

265 from the HEL cases than the Jet A-1 cases. Therefore, the largest differences in the mean  
266 droplet sizes are observed from the pair of cases 3-13 (cf. in Fig. 7a).

267           When the PSA is moved downstream (from 2d to 1d position) the deviation  
268 between different airblasts becomes smaller. They are compared in Fig. 7c and 7d with  
269 the previous pairs of cases 3-13 and 8-18, respectively. If we look at the individual  
270 contours in panels c and d closely, two contours on the left side of each panel show  
271 similar mean droplet size values, but the other two on the right are deviated. In other  
272 words, whether the injector is located at 1d or 2d is not critical for the machined  
273 airblast, but for the 3D-printed airblast, it results in a poorer atomization when the  
274 contact length between liquid fuels and the airblast gets longer. The decreasing number  
275 of droplets detected for the 2d cases (cf. cases 13 and 18 in Fig. 7c and 7d, respectively)  
276 also supports the less efficient atomization of the 3D-printed airblast combined with the  
277 injector at the 2d position.

278           Each of four contours in Fig. 7e and 7f were generated from data of three  
279 heights, instead of four heights like the other conditions (cf. Fig. 6), due to occasional  
280 strong signal intensities that saturated some images at upper heights. This might have  
281 been attributed to the larger thermal power for 160 m/s air jet velocity cases combined  
282 with good atomization performance for the injector position of 1d (e.g., Fig. 7e). On the  
283 other hand, the rich flame condition was the reason for the strong signal for Fig. 7f  
284 cases.

285           According to the results and evaluations presented, the 3D-printed part has a  
286 clear impact on the atomization quality of the injection system. Therefore, its further  
287 effects on flame characteristics and burner performances are investigated by analyzing  
288 averaged OH\* *CL* images. Since an extensive parameter study for the injection concept  
289 with a machined airblast has been done and presented by Hampp et al. [3], the current  
290 study focuses more on the comparison between the different airblasts.

291           From all pairs of the *CL* images (i.e., with the machined and the 3D-printed  
292 airblast), three pairs are presented in Fig. 8. A minor structural difference in the flame  
293 shape was observed from all pairs. As presented in the previous work [3], flames on this  
294 burner tend to have an elongated leading edge at the center of the burner tapering  
295 toward the nozzle. This phenomenon is well observed in the current study as well.  
296 However, with the 3D-printed airblast, the intensity of the leading edge gets weaker, so  
297 the flame shape becomes slightly broader and more symmetric. Less efficient  
298 atomization leading to a compactor flame shape is counter-intuitive, but the shortened  
299 leading edge with the 3D-printed airblast was observed from all the sets of 10 pairs and  
300 well presented in Fig. 8.

301           Apart from the general trend of the shortened leading edge, no significant  
302 change in the flame shape due to the larger droplet size was observed. For example, the  
303 averaged *CL* images presented in Fig. 8a are from the pair that shows the largest  
304 difference in the mean droplet size of the Jet A-1 liquid fuel (i.e., cases 3 and 13 in Fig.  
305 7a). Even though the mean droplet size is about 25% (10  $\mu\text{m}$ ) larger with the 3D-printed

306 airblast than with the machined airblast (cf. Fig. 7a), the corresponding *CL* images show  
307 similar intensity and spatial distribution of the OH radicals to each other. The similar *CL*  
308 images suggest no major influence in the flame shape and heat release zone attributed  
309 to the atomization performance change.

310 The other examples presented in Fig. 8b and 8c show the similar trend. Cases 8  
311 and 18 have the largest droplet size difference for HEL (cf. Fig. 7b), and cases 9 and 19  
312 are from the flames at the stoichiometric condition. The global structure of the flame  
313 does not present distinct dependencies on the type of airblast or spray characteristics.

314 Emission data from the burner has been analyzed and compared to find any  
315 possible indications of different flame behaviors. Nitrogen oxides (NO<sub>x</sub>) are especially of  
316 interest since they could indicate a flame temperature difference. For each flame  
317 condition, 60 data points (sampling rate of 1 Hz) of NO<sub>x</sub> and CO quantity, which were  
318 saved during the *CL* imaging, were averaged. The averaged values were corrected to  
319 15% oxygen and plotted in Fig. 9 with their standard deviations.

320 From the NO<sub>x</sub> emission data in Fig. 9a, flames with the 3D-printed airblast tend  
321 to have slightly larger values for most of the cases than with the machined airblast. The  
322 difference is larger for the HEL flames, but not significantly. In addition, a relation  
323 between the NO<sub>x</sub> emission and the droplet size difference (cf. Fig. 5) is hard to establish.  
324 For example, large droplet size differences observed in Fig. 5 are pairs of cases 3-13, 5-  
325 15, and 10-20. On the other hand, large NO<sub>x</sub> emission differences in Fig. 9 are pairs of  
326 cases 6-16, 7-17, and 10-20.



327 CO emission data in Fig. 9 presents similar trend as the NO<sub>x</sub> emission data. For  
328 the cases with Jet A-1, no significant correlation between emission values and the airblast  
329 type is observed. HEL flames show more deviated values between the machined and the  
330 3D-printed airblast cases. However, the difference is relatively small as less than 25 ppm  
331 for the  $\phi=0.8$  cases and 55 ppm for the  $\phi=1$  case. Despite the increased emission with  
332 the 3D-printed airblast, CO levels at all  $\phi=0.8$  conditions in this study are within the  
333 range of the reported typical CO emission level of gas turbines, which is between 5 and  
334 330 ppm [16].

335 The large difference of CO emission levels is observed from the same pairs of the  
336 cases as the NO<sub>x</sub> emission result (i.e., 6-16, 7-17, and 10-20) with an addition of 9-19.  
337 Therefore, it is not correlated with the droplet size difference results, either. The NO<sub>x</sub>  
338 and CO emission levels are responding more sensitively to the flame conditions (air jet  
339 velocity and  $\phi$ ) than the type of airblast.

#### 340 4. CONCLUSION

341 The series of tests with the machined and the 3D-printed airblast presents that the  
342 impact of the 3D-printed part on the atomization quality is not negligible. Droplet size  
343 distribution clearly changes toward a larger value with the 3D-printed airblast, and a  
344 larger number of droplets are detected as well. Therefore, it is concluded that the  
345 atomization with the 3D-printed airblast is less efficient than the conventionally  
346 machined airblast, due to the interaction between the liquid and the rough surface.

347 On the other hand, the less efficient atomization does not affect much negatively on the  
348 flame behavior in this burner. No significant change in the flame position and intensity  
349 has been observed, and the emission profile stayed stable as well. This can be attributed  
350 to the robust burner system that can stabilize flames under a wide operation range.  
351 Therefore, it was concluded that employing the 3D printed components to the burner  
352 system would provide comparable combustion characteristics while giving significant  
353 benefits by realizing challenging geometry, reducing time for manufacturing, and saving  
354 cost.

355 Nevertheless, multiple trends and phenomena are observed during this study and  
356 require further investigation. An example is the interaction between a liquid fuel and a  
357 3D-printed surface and how it affects the atomization performance of an injection  
358 system. Fundamental studies to answer the questions will help find the boundary of the  
359 operational range of the current burner system with 3D-printed components, which  
360 would further serve to optimize the combustor.

361

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363

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366 secondary electron imaging of the airblast surfaces.

367

368

369 **NOMENCLATURE**

370

<i>CL</i>	Chemiluminescence
<i>FN</i>	Flow Number (US)
HEL	Extra Light Heating Oil
MGT	Micro Gas Turbine
$\phi$	Equivalence Ratio
PSA	Pressure Swirl Atomizer
SLM	Selective Laser Melting

371

372

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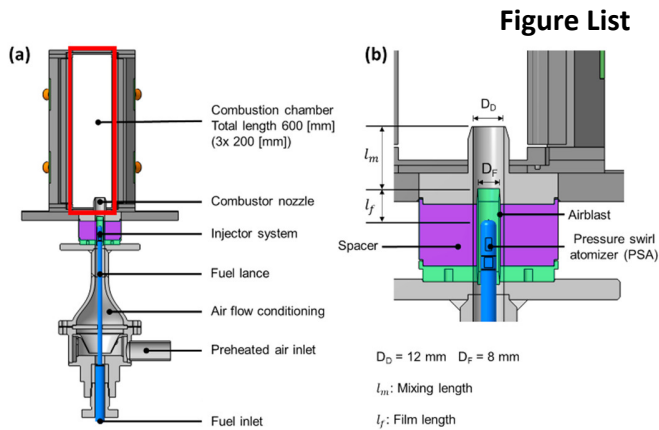


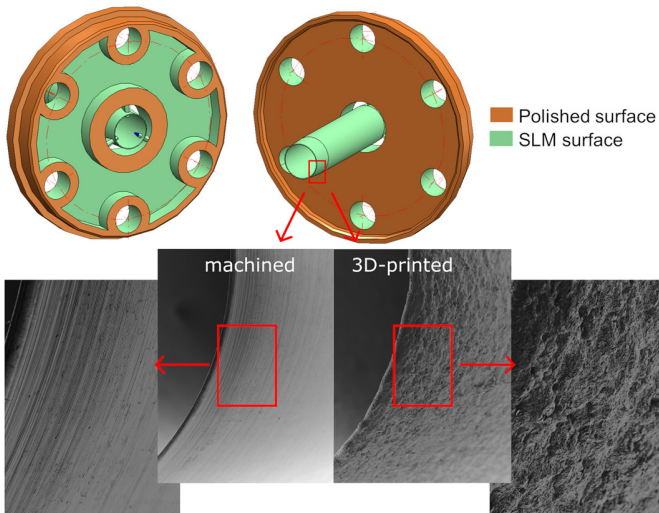
Figure List

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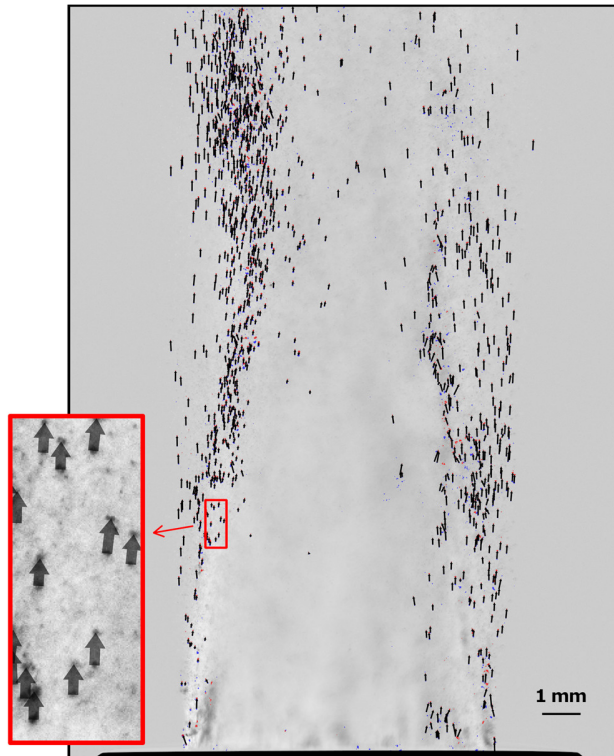
Fig. 1 SCHEMATIC of a confined jet-stabilized burner and details of a pressure swirl-airblast liquid fuel injection system [3]. The region in the red box (a) is utilized for the legends in Fig. 4, 5, and 6.



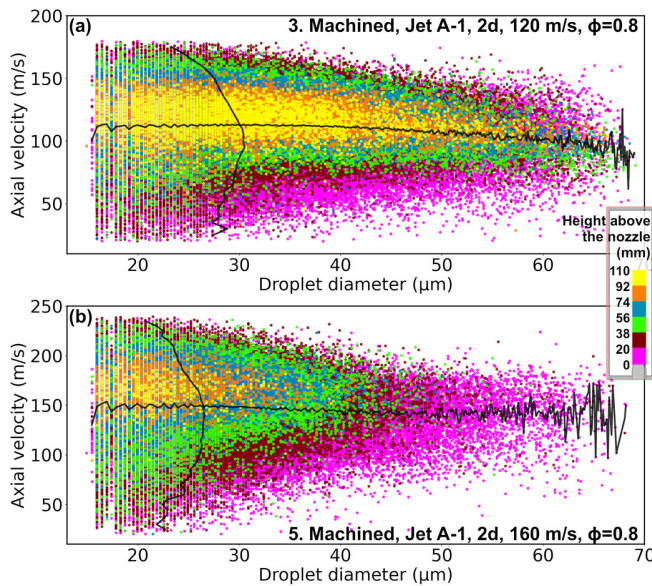
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Fig. 2 3D model and microscopic images of the machined and 3d-printed airblast

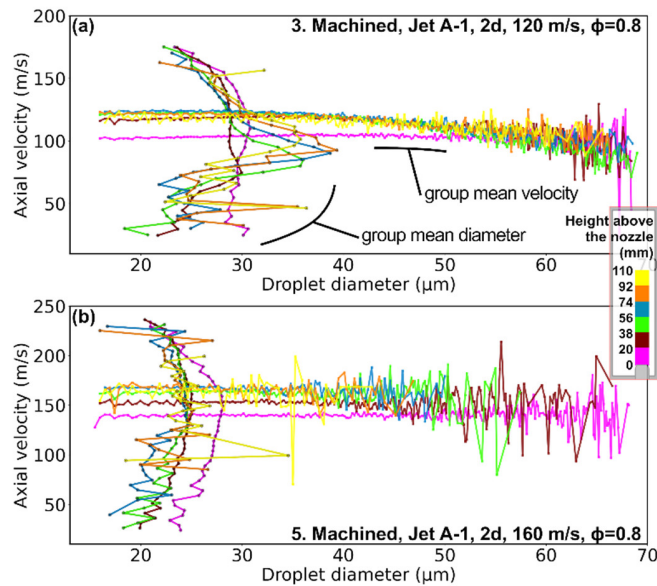


432 Fig. 3 SAMPLE shadowgraphy image  
 433 overlaid by a particle tracking result. Two frames are taken with a time interval of  $2 \mu\text{s}$   
 434 at the height close to the nozzle for case nr. 6 (cf. Table 1) condition. Vectors indicate  
 435 the displacement of detected particles.

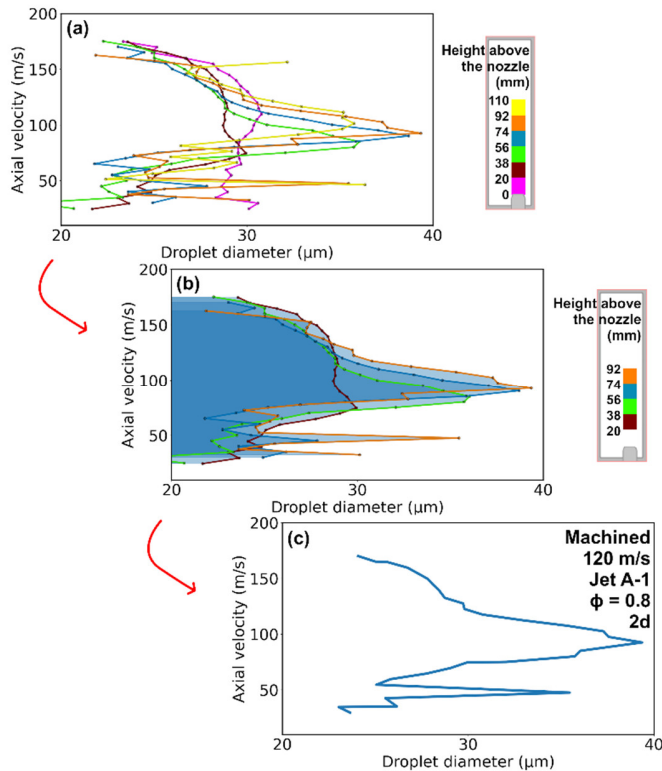


436 Fig. 4 VELOCITY-SIZE scatter plots of  
 437 detected Jet A-1 droplets. Air jet velocities of 120 m/s (case nr. 3) and 160 m/s (case nr.  
 438 5) are compared, with the machined airblast and PSA located at 2d below the nozzle tip.  
 439 Mean group velocities (horizontal) and mean group sizes (vertical) of all detected

440 droplets are drawn with the black lines. The mean curves of each height are presented  
 441 in Fig. 5.



442 Fig. 5 GROUP mean velocity and  
 443 group mean size plots of detected Jet A-1 droplets. Air jet velocities of 120 m/s (case nr.  
 444 3) and 160 m/s (case nr. 5) are compared, with the machined airblast and PSA located at  
 445 2d below the nozzle tip. Data points of individual droplets are presented in Fig. 4.



446 Fig. 6 ILLUSTRATION of drawing  
 447 contours using grouped mean droplet size curves. Vertical lines of a sample case (case



448 nr. 3) in Fig. 5 are presented (a), four central heights are selected, and the area under  
449 the curves is filled with blue (b). A contour of the filled area is drawn with blue (c). The  
450 blue contour can be found in Fig. 7a and 7c.

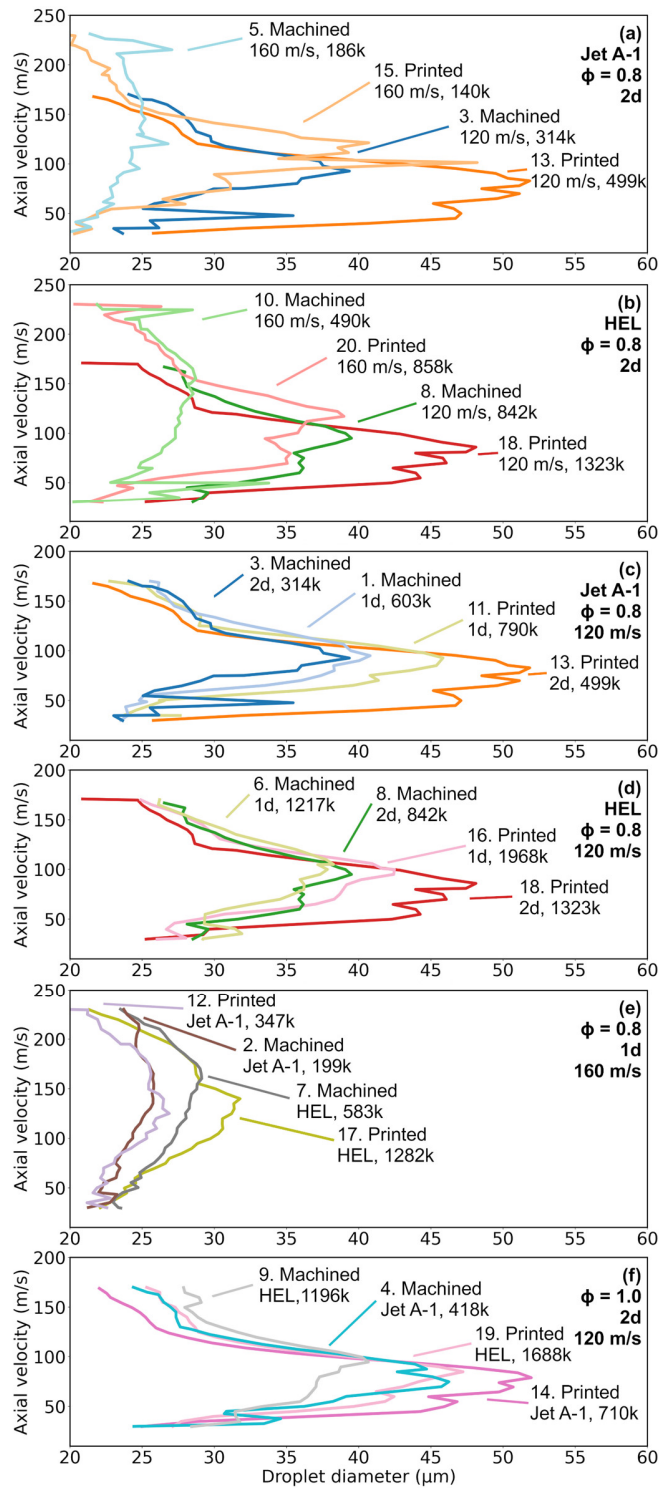


Fig. 7 ATOMIZATION performance

451 analysis at various conditions using droplet size contours. Droplet size contours of  
 452 various cases are compared (cf. Fig. 6). Shared parameters within one panel are noted at  
 453 the upper right corners, and individual parameters are noted with the case numbers  
 454

455 from Table 1, and the total number of droplets detected from each set of 300 images  
 456 (e.g., 710k=710000 droplets).

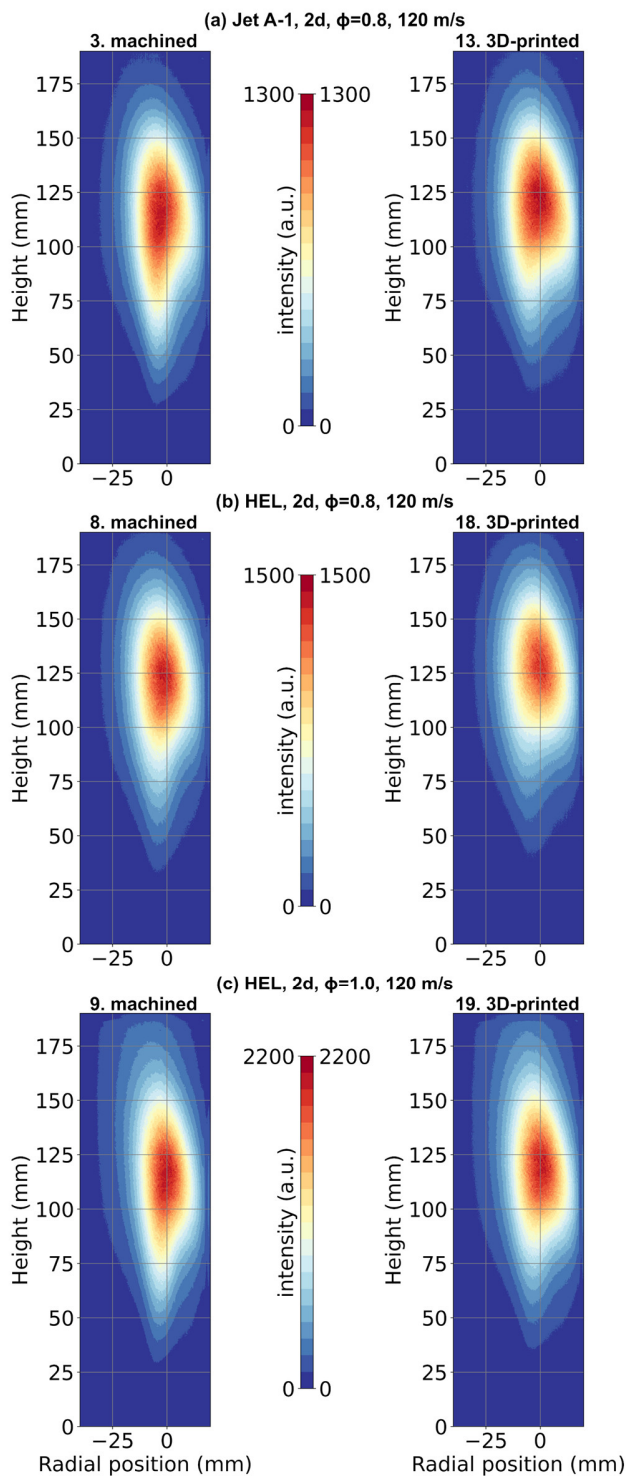
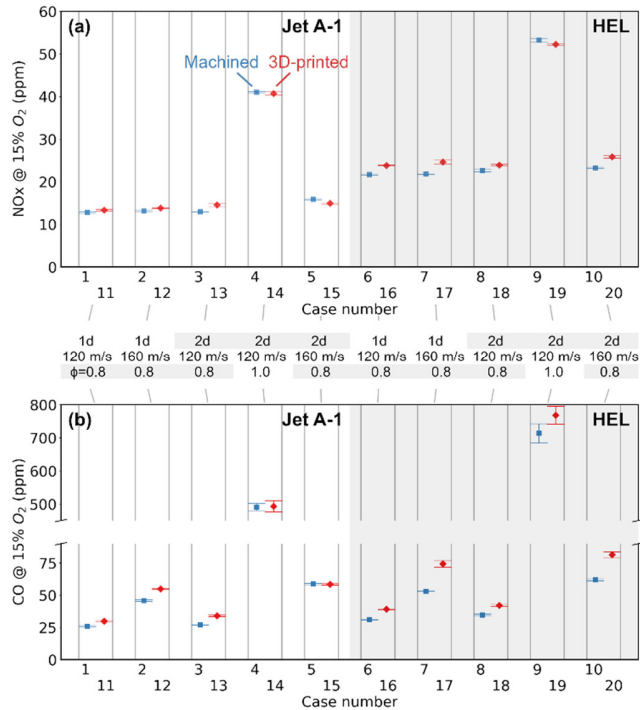


Fig. 8 AVERAGED OH\*

457  
 458 chemiluminescence images with the machined airblast and the 3D-printed airblast. Jet

459 A-1 flames are presented in panel a, and HEL flames are presented in panels b and c.  
 460 Detailed parameters are noted in each panel. A discrete color scale with a 5% interval is  
 461 used.



462 Fig. 9 EMISSION data of nitrogen  
 463 oxides (NOx) and carbon monoxide (CO). Data points with the machined airblast (blue)  
 464 and the 3D-printed airblast (red) are plotted together for comparison. Cases 1 to 5 on  
 465 the left are the results of Jet A-1 flames, and cases 6 to 10 on the right are with HEL as a  
 466 liquid fuel. Standard deviation of each data point is represented by error bars.  
 467

468

**Table Caption List**

469

Table 1      EXPERIMENTAL conditions of the study

470

471

**TABLE 1:** EXPERIMENTAL conditions of the study

472

Fuel	Injector position	Air jet vel. (m/s)	$\phi$	Case nr. 473 (Airblast type)	
				Machined	Printed
<b>Jet A-1</b>	1d	120	0.8	1	11
		160	0.8	2	12
	2d	120	0.8	3	13
			1.0	4	14
		160	0.8	5	15
<b>HEL</b>	1d	120	0.8	6	16
		160	0.8	7	17
	2d	120	0.8	8	18
			1.0	9	19
		160	0.8	10	20