

# Next steps in the development of bi-functional Gas-Diffusion Electrodes for Zinc-Air-Batteries

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## Introduction

### Motivation

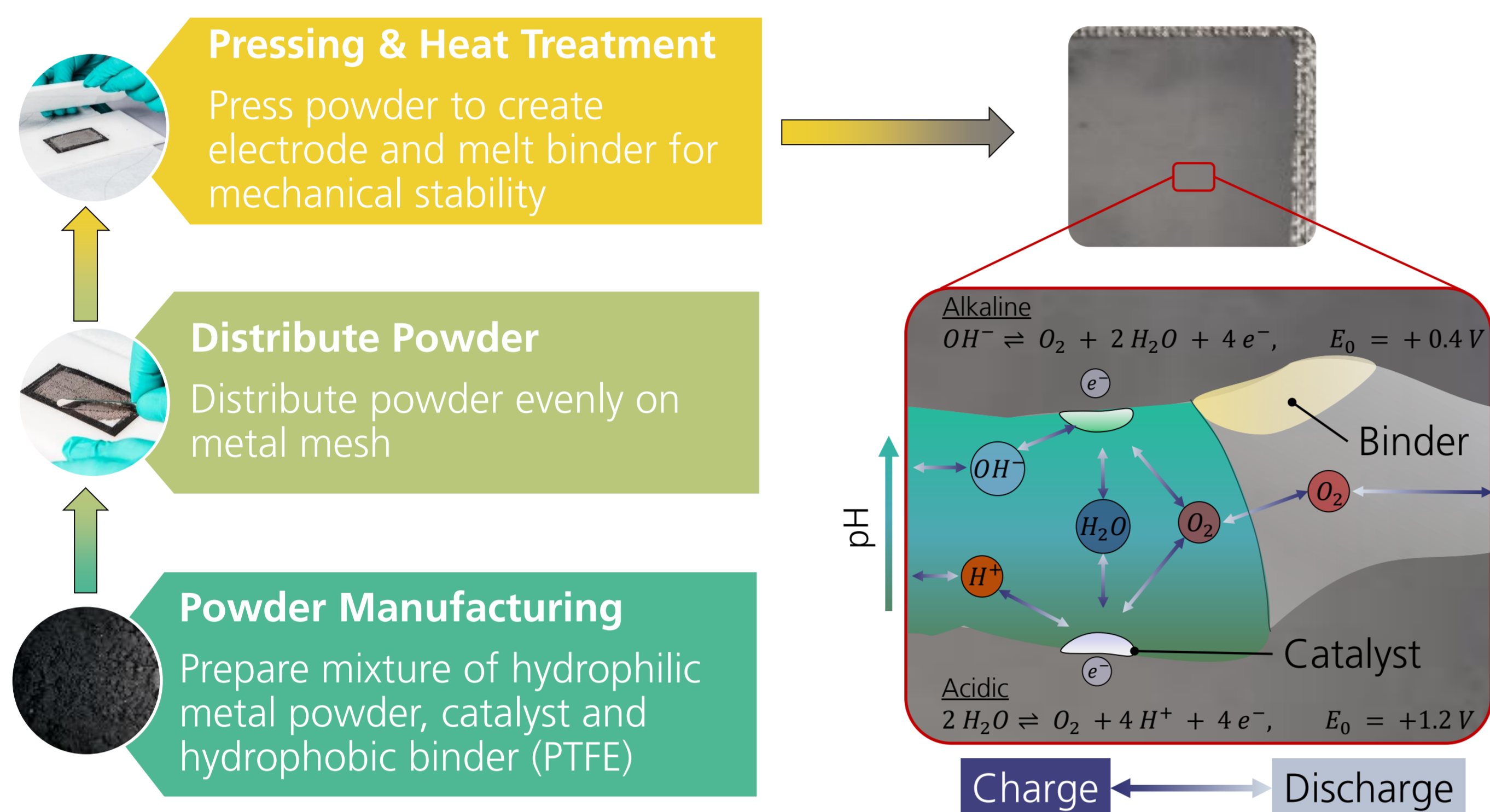
- **Zinc-Air-Batteries (ZAB)** - a solution for **midterm energy storage systems** due to their cost structure, safety and abundance of materials.
- State-of-the-art **gas-diffusion electrodes (GDE)** challenge the economic feasibility due to the sluggish oxygen reactions ( $\eta_{RTE} \approx 60\%$ ) and the use of expensive bi-functional catalysts.
- Additional: **material stability** under oxygen evolution reaction problematic.
- **Existing GDEs need to be optimized for bi-functionality.**

### Objective

1. **Identify electrochemical limits of materials**
2. **Optimize pore network** for changing requirements and conditions of oxygen evolution (2-phase-reaction) and oxygen reduction reaction (3-phase-reaction)
3. **Enhance performance by a multi-layer approach:** addition of specialized reaction and gas-diffusion layer.

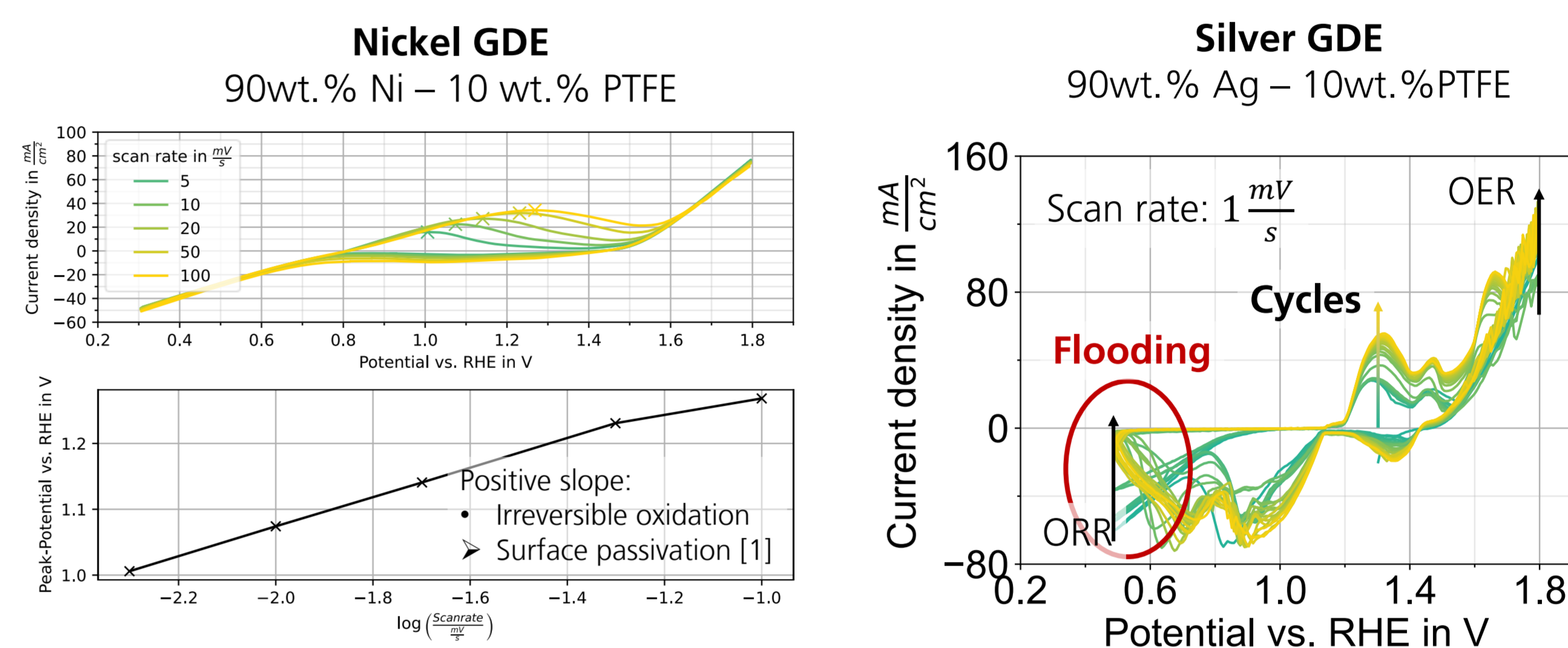
## Bi-functional Gas-Diffusion-Electrodes

Manufacturing via dry coating, Reaction and Transport



### Material Stability

Cyclic-Voltammetry studies in 6M KOH



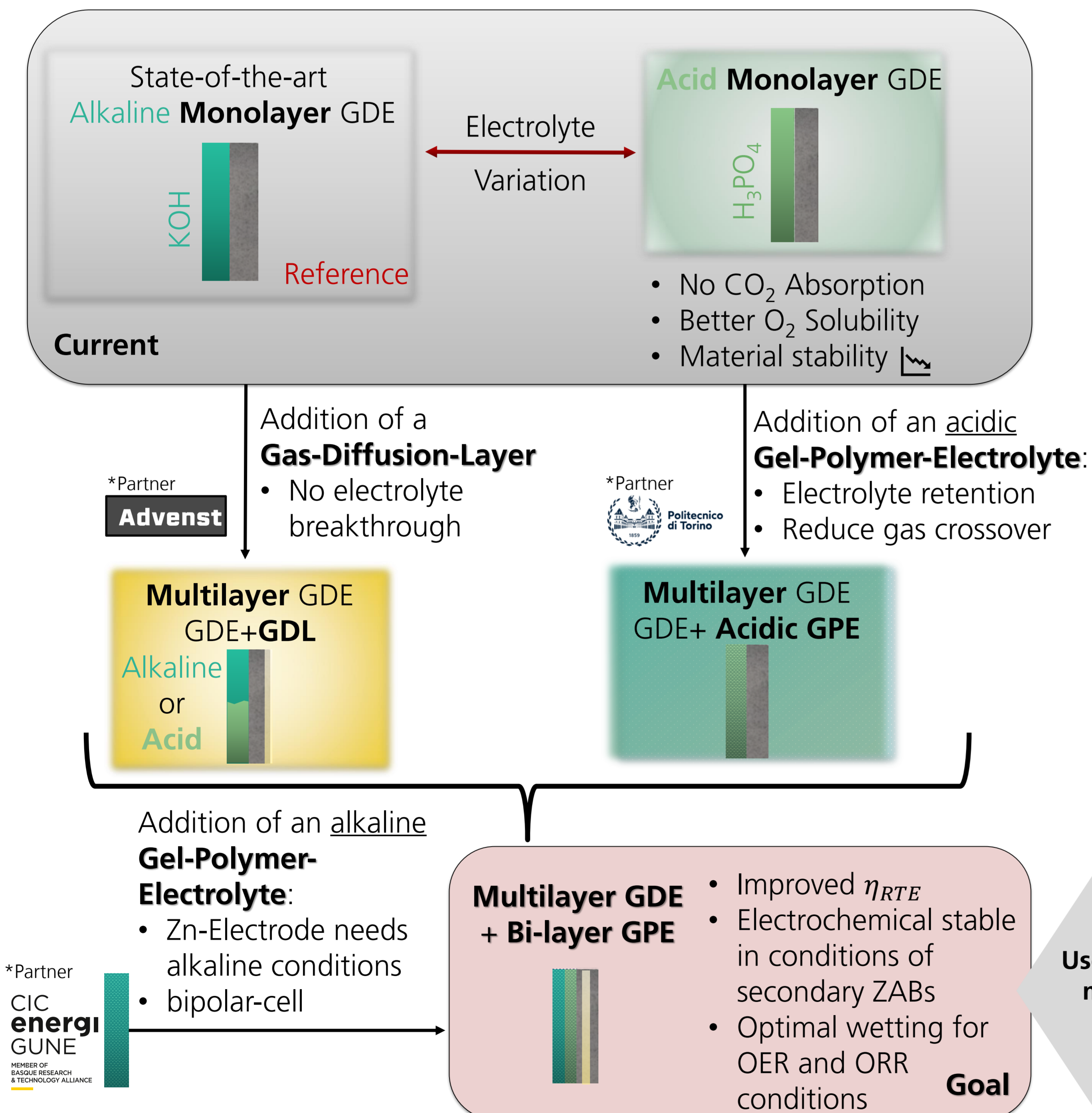
- Potential for OER ( $U > 1V$  vs. RHE) is demanding for used materials
  - e.g. typical used Carbon decomposes @  $U > 1.3 V$  vs. RHE [1]
- Ni and Ag show good performance but degrade quickly

### Multilayer

### Pore Network

## Architecture Design

## Optimize Pore Network



### Model development

Simple models for an informed GDE Design

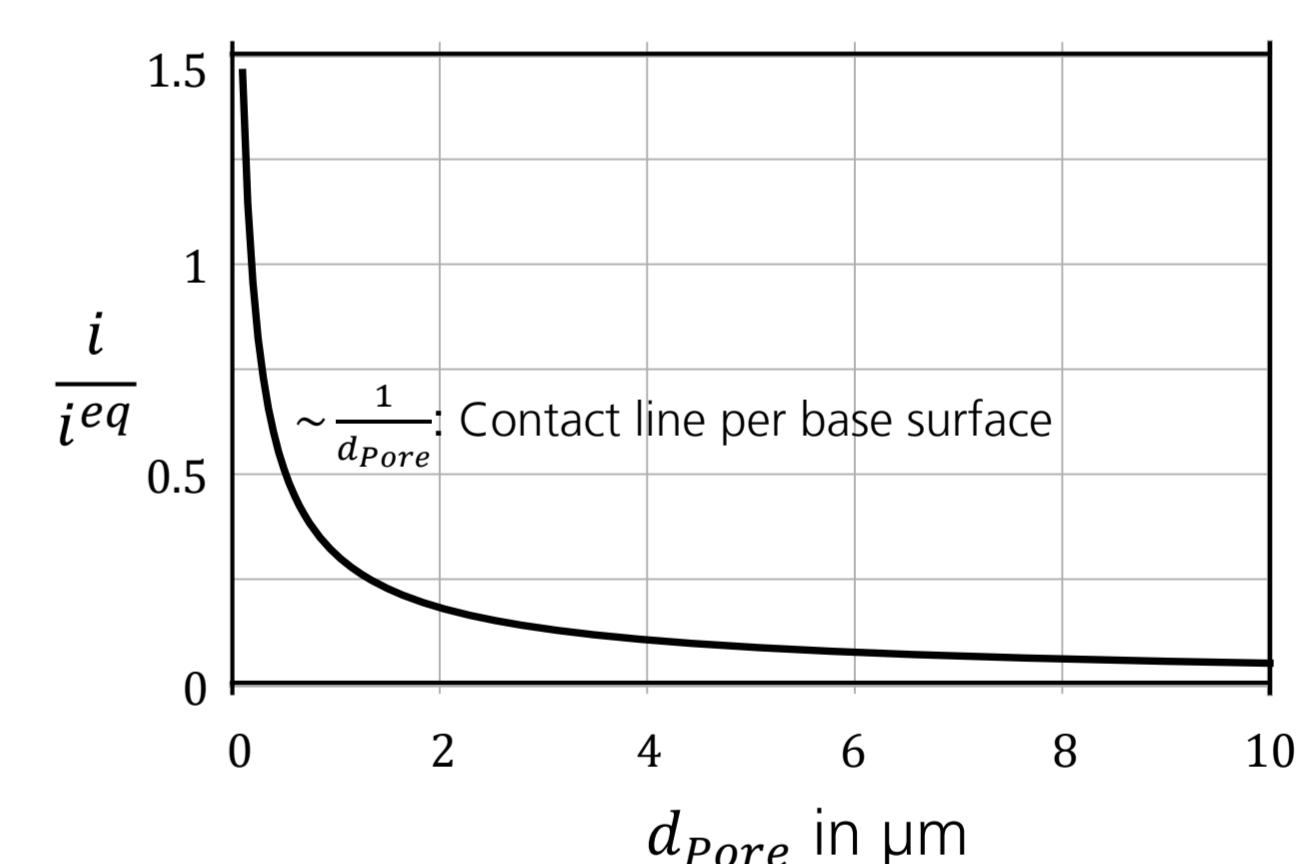
1. Oxygen Transport and Reduction Reaction in a cylindrical pore (2D)

$$r(\rho_p) = k_0 a_W^2 a_{O_2} \exp\left[-\frac{(1-\alpha)F}{RT}\eta\right] \quad (3)$$

$$\frac{\partial x_{O_2}}{\partial t} = \nabla(D_{O_2}\nabla x_{O_2}) + r$$

$$\mu_{O_2}^{(l)} = \mu_{O_2}^{(g)}$$

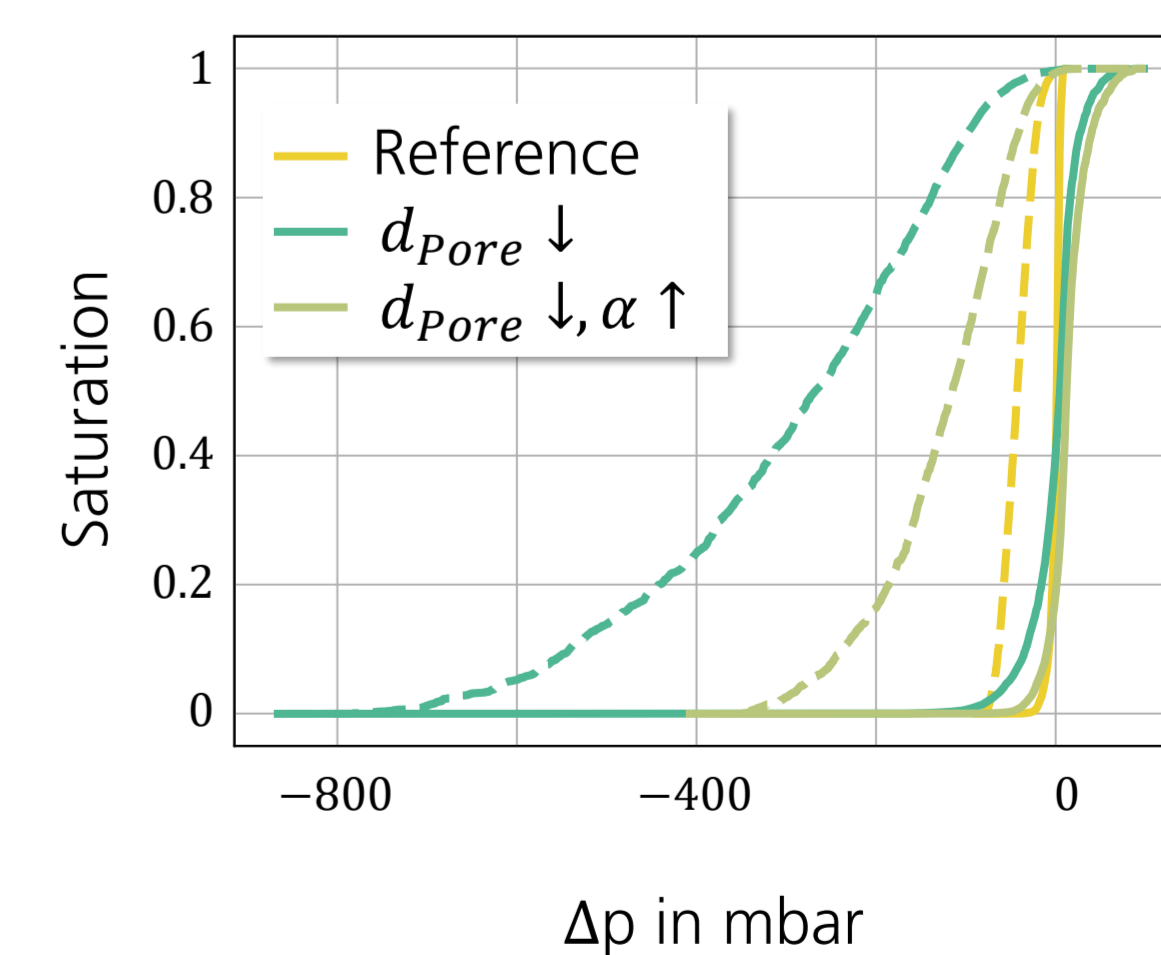
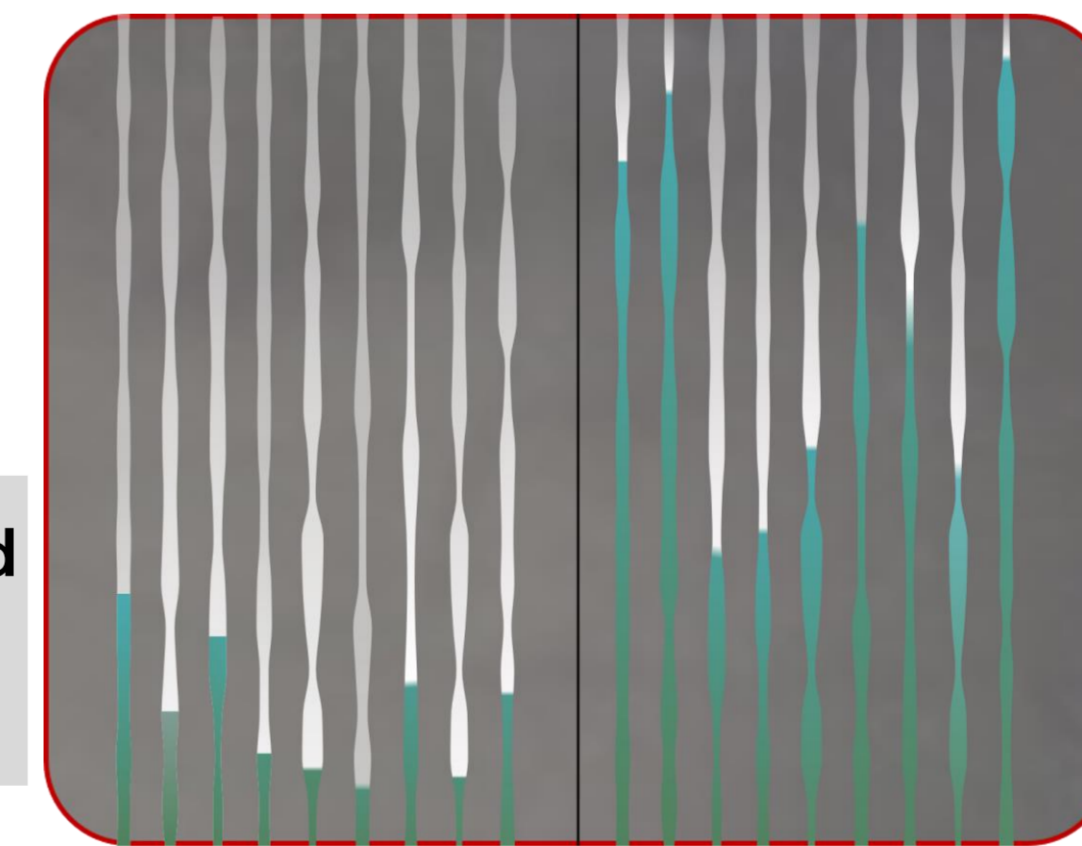
$$x_{O_2}/x_{O_2}^{eq} = 1$$



⇒ Small pores perform better because reaction only happens close to the contact line

2. Modelling of wetting degree: Randomly generated parallel pores  $p_c$  curves with mixed wettability

$$p_c = -2\sigma r_p^{-1} \cos[\alpha \cdot \theta_{NW} + (1-\alpha)\theta_W] \Rightarrow \text{Adjust wettability with PTFE content } \alpha$$



## References

- (1) Yi, Y., et al. (2017). "Electrochemical corrosion of a glassy carbon electrode."
- (2) Rohe, M., et al. (2019). "Processes and Their Limitations in Oxygen Depolarized Cathodes: A Dynamic Model-Based Analysis."
- (3) Wiesner, F., et al. (2024). "Unveiling the Role of PTFE Surface Coverage on Controlling Gas Diffusion Layer Water Content."

## Summary

- To achieve a economical viable ZAB for midterm storage state-of-the-art electrodes need to be improved to overcome their shortcomings: low  $\eta_{RTE}$  & material stability.
- In the **HIPERZAB** project first steps are done to follow two approaches:
  1. Use model based insides to improve the monolayer GDE
  2. Extend the monolayer architecture



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This work is done in cooperation with the partners in the **HIPERZAB** project and with help of the Institute of Chemical Process Engineering, Uni. Stuttgart.

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