

Dual-transition metal and nitrogen co-doped silicon oxycarbide-based catalysts for oxygen reduction at the high temperature PEM fuel cell cathode

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Introduction

- The modern lifestyle and progressive economic growth ever-increasing, global energy consumption, speeding up the climate change.
- The global dependency on fossil fuel has disadvantages (carbon and pollutant emissions), CO₂, NO_x, SO_x, particulate matter.
- Research on clean, efficient, and more sustainable energy technologies. Fuel cells have been
 recognized as possible energy conversion devices for mobile and stationary applications.

DLR (German Aerospace Center)

- More than 9000 employees work in 54 institutes and facilities
- 30 sites across Germany
- DLR Institute of Engineering Thermodynamics Location Oldenburg

High-temperature polymer electrolyte membrane fuel cell (HT-PEM) workgroup

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High temperature PEM fuel cell (HT-PEMFC)



Scheme 1. Schematic representation of the structure of HT-PEMFCs. The relative sizes and distances are not to scale, and the catalyst layer, binder, filler, MPL, and carbon fibers possess significantly different porosities and sizes. <u>DOI: 10.1007/s41918-023-00180-y</u>

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<u>HT-PEMFC</u> is environmentally friendly energy conversion device suitable for heavy-duty transport, stationary, and aviation applications.

Hot HT-PEMFC topic: the development of efficient Pt-group-metal (PGM)-free **oxygen reduction reaction** (**ORR**) catalyst for the fuel cell cathode.

ORR pathways:

4 electrons (e.g. Pt/C)

$$\mathrm{O_2} + 4\mathrm{H^+} + 4\mathrm{e^-} \rightarrow 2\mathrm{H_2O}$$

2 electrons (peroxide production)

$$\mathrm{O_2} + 2\mathrm{H^+} + 2\mathrm{e^-} \rightarrow \mathrm{H_2O_2}$$



M-N-C cathode catalyst materials

- Most promising materials have been developed based on the transition metal and nitrogen co-doped nanocarbon materials (M-N-C).
- Nanocarbon materials: graphene, multi-walled carbon nanotubes (MWCNT), carbide-derived carbons (CDC), polymer-derived carbon (PDC) etc.
 - high surface area, high durability, good electrical conductivity
- Transition metal (TM) and nitrogen co-doping:

a) transition metal (e.g. Fe, Co, Mn) ion coordinated to nitrogen sites (<u>Me-Nx</u>)
b) active N species

- c) transition metal nanoparticles
 - provide active sites for ORR





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Dual metal M-N-C catalysts

The main aim: Preparation of **dual metal** M-N-C materials for HT-PEMFC cathode (M-N-C type)

- Catalyst support/carbon backbone:
 Silicon oxycarbide (SiOC) based materials
- 2. Dual atom metal combinations (supported by literature):
 - 1. Fe/Co
 - 2. Fe/Mn
 - 3. Fe/Cu

Previous collaborations with University of Bremen.

SiOC-based M-N-C were found to be suitable for Fuel cell cathode catalyst application.



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Catalyst preparation



- 1. Polymer-derived carbon (PDC) precursor materials (University of Bremen):
 - 1. Powders of poly(methyl phenyl silsesquioxane), poly(methylsilsesquioxane), graphite, azodicarboxamide, and (3-Aminopropyl)triethoxysilane, imidazole, metal acetylacetonates dispersed in xylene.
 - 2. Pyrolysed, ball-milled, sieved \rightarrow PDC precusor materials:

PDC, MnFe-PDC, CoFe-PDC, CuFe-PDC

- 2. Functionalisation with N-source ZIF-8 (Basolite[®] Z1200) (DLR):
 - 1. Mixed 50/50 wt% of PDC/ZIF-8 in methanol, drying.
 - 2. Pyrolysed at 950 $^\circ C \rightarrow$ N-SiOC catalyst materials:

MnFe-N-SiOC, CoFe-N-SiOC, CuFe-N-SiOC

*3. Acid leaching:

2M sulfuric acid for 16 h at 90 °C followed by second pyrolysis:

MnFe-SiOC-Acid, CoFe-SiOC-Acid, CuFe-SiOC-Acid



Scanning electron microscopy (SEM)



Fig. 1. SEM images of different materials. The FeMn-based material is shown before (-PDC) and after modification with ZIF-8 via pyrolysis at 950 °C (-N-SiOC). The commercial Fe-N-C is also shown for comparison.

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Energy-dispersive X-ray spectroscopy (EDS)

	PDC	CoFe-PDC	CoFe-N-SiOC	MnFe-PDC	MnFe-N-SiOC	CuFe-PDC	CuFe-N-SiOC
С	73.7 ± 1.9	77.1 ± 3.5	75.5 ± 0.9	76.9 ± 1.0	78.4 ± 1.5	74.6 ± 7.4	76.8 ± 2.4
Ν	2.70 ± 0.13	3.38 ± 0.13	6.30 ± 0.42	3.61 ± 0.28	6.71 ± 1.03	2.77 ± 1.26	7.34 ± 0.71
0	18.3 ± 1.5	15.1 ± 2.4	13.3 ± 1.3	13.2 ± 0.7	10.3 ± 0.8	16.5 ± 4.8	12.1 ± 1.2
Si	5.36 ± 0.67	4.04 ± 0.77	4.14 ± 0.62	5.65 ± 0.89	3.85 ± 0.35	4.78 ± 1.19	2.81 ± 1.49
Fe	-	0.21 ± 0.08	0.23 ± 0.05	0.35 ± 0.07	0.26 ± 0.04	0.25 ± 0.06	0.21 ± 0.06
Mn	-	-	-	0.29 ± 0.06	0.20 ± 0.06	-	-
Со	-	0.20 ± 0.06	0.20 ± 0.07	-	-	-	-
Cu	-	-	-	-	-	0.26 ± 0.12	0.38 ± 0.13
Zn	-	-	0.29 ± 0.10	-	0.28 ± 0.15	-	0.28 ± 0.14

Table 1. Elemental composition (at%) of different materials. After the modification of precursor material (-PDC) with ZIF-8 via pyrolysis at 950 °C (-N-SiOC), the introduction of Zn and increase in N amount is observed.



High-resolution transmission electron microscopy (HR-TEM)





Fig. 2. HR-TEM images of different materials after ZIF-8 modification, (a) CuFe-N-SiOC, (b) MnFe-N-SiOC.



X-ray photoelectron spectroscopy (XPS)



Fig. 3. XPS survey spectra of different catalyst materials after the modification with ZIF-8 via pyrolysis at 950 °C (-N-SiOC). The insets show the high-resolution spectrum in the N1s region for the corresponding material.

RRDE half-cell testing (Rotating ring-disk electrode)



WE1: ORR current WE2: Peroxide oxidation current

From WE1/WE2 difference – peroxide yield and electron transfer number per O₂ molecule

https://www.metrohm.com/en/products/a/ut r/aut rrde s.html





DOI: 10.1088/1757-899X/340/1/012017

WE1: M-N-C catalyst on GC WE2: Pt ring RE: MMS (converted to RHE) CE: Pt wire Electrolyte: 0.5 M H₃PO₄, 23 °C







Fig. 4. (a) Disc current density, (b) ring current and electron transfer numbers (*n*) for different catalyst coated GC-disk/Pt-ring electrodes recorded at 1600 rpm in O2-saturated phosphoric acid solution.



RRDE half-cell testing for ORR in 0.5 M H₃PO₄ at 23 °C

Catalyst	E 1/2	MA 0.75V	MA0.80V
CoFe-N-SiOC	770 ± 3	3.41 ± 0.14	1.25 ± 0.10
MnFe-N-SiOC	774 ± 2	3.63 ± 0.08	1.80 ± 0.07
CuFe-N-SiOC	781 ± 6	3.67 ± 0.37	2.20 ± 0.14
Fe-N-C	808 ± 2	11.03 ± 0.14	7.56 ± 0.15
Pt/C (20wt. Pt)	824 ± 3	29.73 ± 2.33	37.35 ± 2.91

Table 2. Half-wave potential (*E*_{1/2}, unit mV vs. RHE) and mass activity (MA, unit A g_{Catalyst}⁻¹) values at 0.75 V and 0.80 V for ORR derived from the disc currents of RRDE measurements performed at 1600 rpm.

Acid leaching (2 M H2SO4) influence on RRDE results



Fig. 5. Acid leaching route is in 2 M sulfuric acid for 16 h at 90 °C + second pyrolysis (Not beneficial for peroxide yield)



Acid leaching (2 M H2SO4) influence on RRDE results

Catalyst	E 1/2	MA 0.75V	MA 0.80V
CoFe-SiOC	770 ± 3	3.41 ± 0.14	1.25 ± 0.10
CoFe-SiOC-Acid	772 ± 2	↑ 3.74 ± 0.18	23% ↓ 0.96 ± 0.09
MnFe-SiOC	774 ± 2	3.63 ± 0.08	1.80 ± 0.07
MnFe-SiOC-Acid	↓ 757 ± 6	↓ 2.99 ± 0.17	30% ↓ 1.26 ± 0.11
CuFe-SiOC	781 ± 6	3.67 ± 0.37	2.20 ± 0.14
CuFe-SiOC-Acid	↓ 726 ± 8	↓ 2.26 ± 0.23	58% ↓ 0.91 ± 0.09

Table 3. Half-wave potential (*E*_{1/2}, unit mV vs. RHE) and mass activity (MA, unit A g_{Catalyst}⁻¹) values at 0.75 V and 0.80 V for ORR derived from the disc currents of RRDE measurements performed at 1600 rpm.

RDE half-cell stability testing for ORR in 0.5 M H₃PO₄ at 23 °C



Fig. 6. RDE voltammetry curves recorded at 1600 rpm before and after stability testing for 10 000 cyclic voltammetry (CV) cycles in O₂- saturated 0.5 M H₃PO₄ solution. Commercial Fe-N-C (PMF-0011904, Pajarito Powder) is included for comparison.

(26 h CV test in 400 mV potential window)

GDE half-cell testing

(Gas diffusion electrode)



https://gaskatel.de/en/test-cells-for-the-electrochemistry/





Test Cell FlexCell

Voltammetric Test Cell PTFE / PP



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GDE half-cell testing for ORR (conc. H₃PO₄ at 160 °C)





Fig. 7. Measurement consists of chronopotentiometry followed by impedance spectroscopy at certain current value steps (e.g. -0.3 mA, -2.35 mA, -11.8 mA... ...-280 mA). Resistance value is used for iR-drop compensation at certain current.

GDE half-cell testing for ORR (conc. H₃PO₄ at 160 °C) (Single measurement with each catalyst material)



Fig. 8. GDE half-cell polarisation curves. Shown data points have been obtained via chronopotentiometry measurements corrected for iR-drop value using the impedance spectroscopy at corresponding current value.

GDE testing (acid leaching influence) (Averaged measurement results with each catalyst material)



Fig. 9. GDE half-cell polarisation curves. Acid leaching route is in 2 M sulfuric acid for 16 h at 90 °C + second pyrolysis.

GDE testing (acid leaching influence)



Fig. 10. Investigation of low current density region (ca. 0.9 - 0.6 V) using the logarithmic scale for current density.

GDE testing and acid leaching influence



Catalyst	OCP	E 187	
CoFe-N-SiOC	752 ± 15	219 ± 12	
CoFe-SiOC-Acid	17 mV ↑ 769 ± 14	64% ↑ 360 ± 27	
MnFe-N-SiOC	775 ± 38	218 ± 21	
MnFe-SiOC-Acid	39 mV ↑ 814 ± 12	~3% ↑ 224 ± 25	
CuFe-N-SiOC	788 ± 15	201 ± 50	
CuFe-SiOC-Acid	38 mV ↓ 750 ± 13	~6% ↑ 214 ± 28	
Fe-N-C	865 ± 24	421 ± 27	

Table 4. Open circuit potential (OCP, unit mV vs. RHE) and potential value at 187 mA cm⁻² (*E*₁₈₇, unit mV vs. RHE) for ORR derived from the GDE polarisation curves with different cathode catalyst materials.

Conclusions



Dual transition metal containing SiOC materials

Functionalised with N using ZIF-8 and pyrolysis method

RRDE half-cell testing for ORR in 0.5 M H₃PO₄, 23 °C:

- CuFe and MnFe-containing materials more promising at RT (*E*1/2, *n* value)
- CoFe material showed an increase in ORR activity and long-term stability after acid treatment
- Acid treatment not beneficial for CuFe and MnFe-containing materials

GDE half-cell testing for ORR with conc. H₃PO₄ at 160 °C:

- Acid treated and non-treated CuFe and MnFe-containing materials similar
 - *MnFe material showed considerable increase in OCP value after acid treatment*
- CoFe material showed a considerable increase in ORR activity after acid treatment

(Manuscript under preparation)

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Thank you for your kind attention!

Questions?

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Extra no. 1



PBI membranes for HT-PEMFCs

HT-PEFCs run at an operating temperature of about 160 °C with membrane electrode assemblies (MEAs), based on a polybenzimidazole-type polymer loaded with phosphoric acid (H₃PO₄) – e.g. *m*-PBI or *ab*-PBI (see Fig. 1). In the temperature range between 160 °C and 180 °C, the polymers loaded with H₃PO₄ display very high proton conductivity, relatively low gas permeability, and good mechanical stability.

The high operating temperature above 100 °C has several advantages over low-temperature polymer membrane fuel cells (LT-PEMFCs), which are limited to operating temperatures below 80 °C. m-PBI, Poly[2,2'-(m-phenylen)- 5,5' bibenzimidazol]



ab-PBI, Poly[2,5-benzimidazol]



Fig. 1: Repeating units of two polybenzimidazole-type polymers

https://www.fz-juelich.de/en/iek/iek-14/research/pcl/spectroscopy/pbi-membranes





Fig. E1. (a) Disc current, (b) ring current and electron transfer numbers (*n*) for different catalyst coated GCdisk/Pt-ring electrodes recorded at 1600 rpm in O2-saturated 0.5 M phosphoric acid solution.

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Extra no. 3





Fig. E2. RDE voltammetry curves for ORR recorded at 1600 rpm in O₂-saturated 0.5 M phosphoric acid solution with different loadings of commercial Fe-N-C catalyst (mg cm⁻²) and Pt/C (20 μg_{Pt} cm⁻²). Catalyst loading of 0.4 mg cm⁻² (PMF-0011904, Pajarito Powder) was chosen for comparison in this work.