



Nachhaltige Mobilität durch synthetische Kraftstoffe

FINAL MEETING

OME₃₋₅, DMC, MeFo: Techno-economic assessment and conclusion

Ludwigshafen am Rhein, 2 March 2023

Yoga Rahmat, Sandra Adelung, Cornelia Bänsch, Ralph-Uwe Dietrich



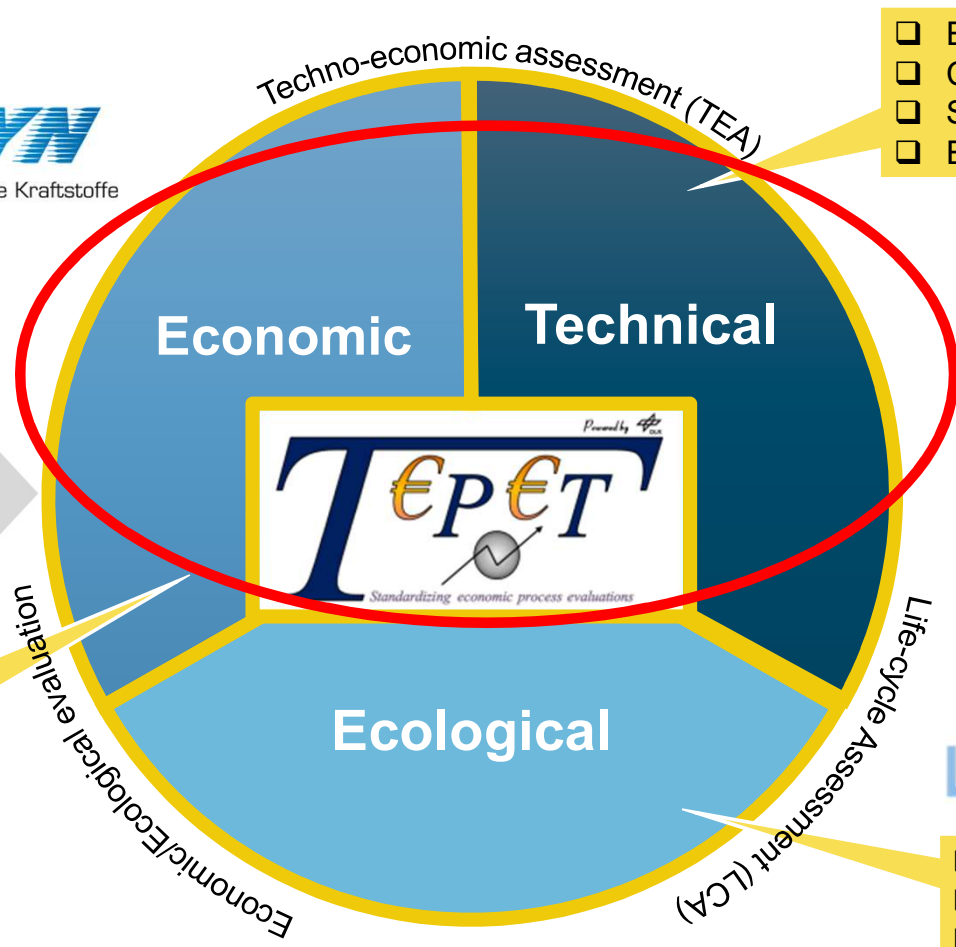
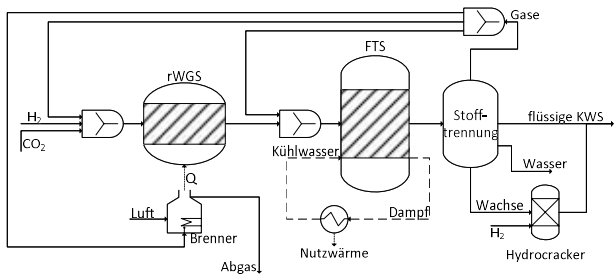
Agenda



- **Techno-Economic and Ecological Assessment @ DLR**
 - TEEA methodology
- Techno-economic assessment of German e-fuels transport options
 - Designer fuels: OME₃₋₅, DMC, MeFo
- Conclusion and discussion
 - Possible e-fuels impact on global transport – Germany as role model?
 - How to make progress from 2023 onwards?

Techno-economic and ecological assessment @ DLR

TEEA methodology



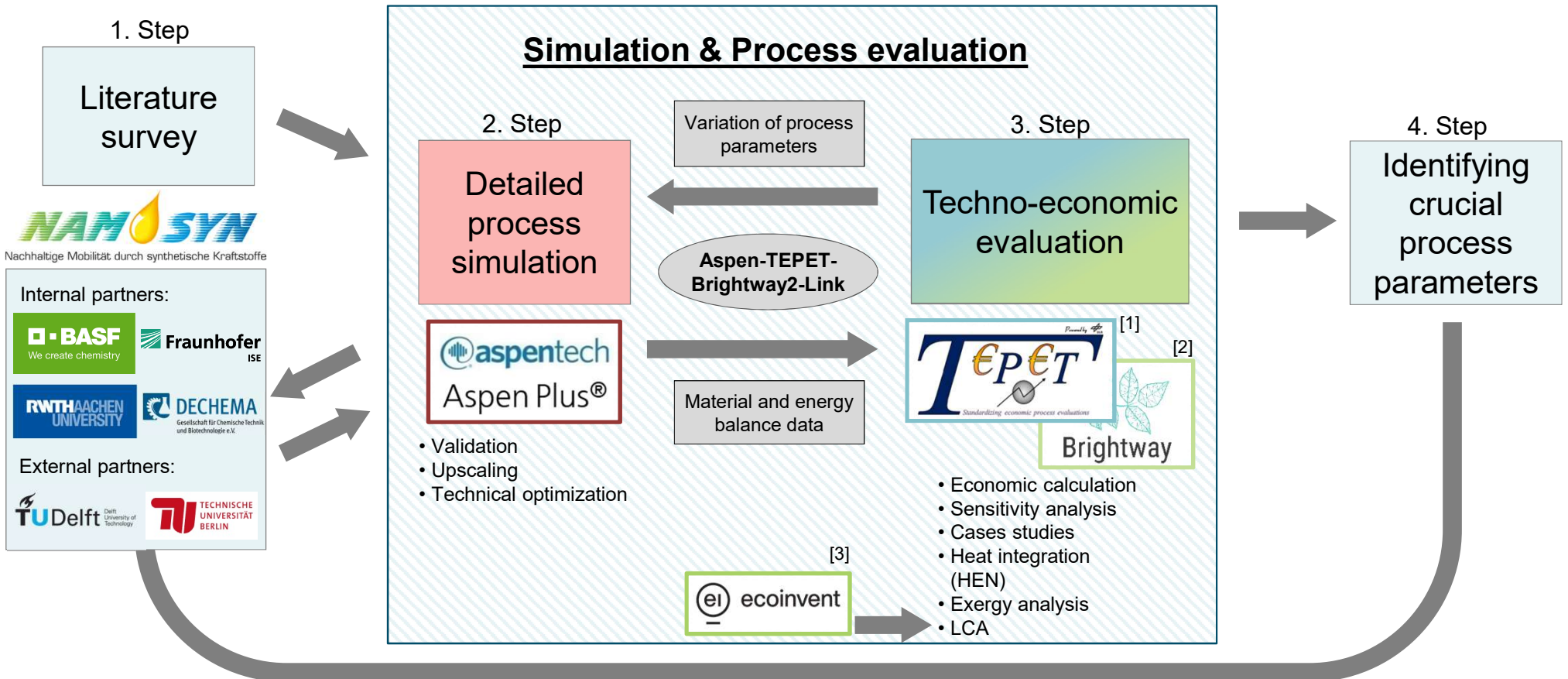
- Efficiencies (X-to-Liquid, Overall)
- Carbon conversion
- Specific feedstock demand
- Exergy analysis

- CAPEX, OPEX, NPC
- Sensitivity analysis
- Identification of most economic feasible process design

- GWP
- Other impact categories
- Identification of impact drivers



TEEA @ DLR



[1] Albrecht et al. (2016) A standardized methodology for the techno-economic evaluation of alternative fuels – A case study, Fuel, 194: 511-526

[2] Mutel (2017) - Brightway: An open source framework for Life Cycle Assessment, Journal of Open Source Software, 2(12): 236

[3] Wernet, G et al. (2016) The ecoinvent database version 3 (part I): overview and methodology. The International Journal of Life Cycle Assessment, 21(9): 1218–1230.



TEA OF DESIGNER FUELS

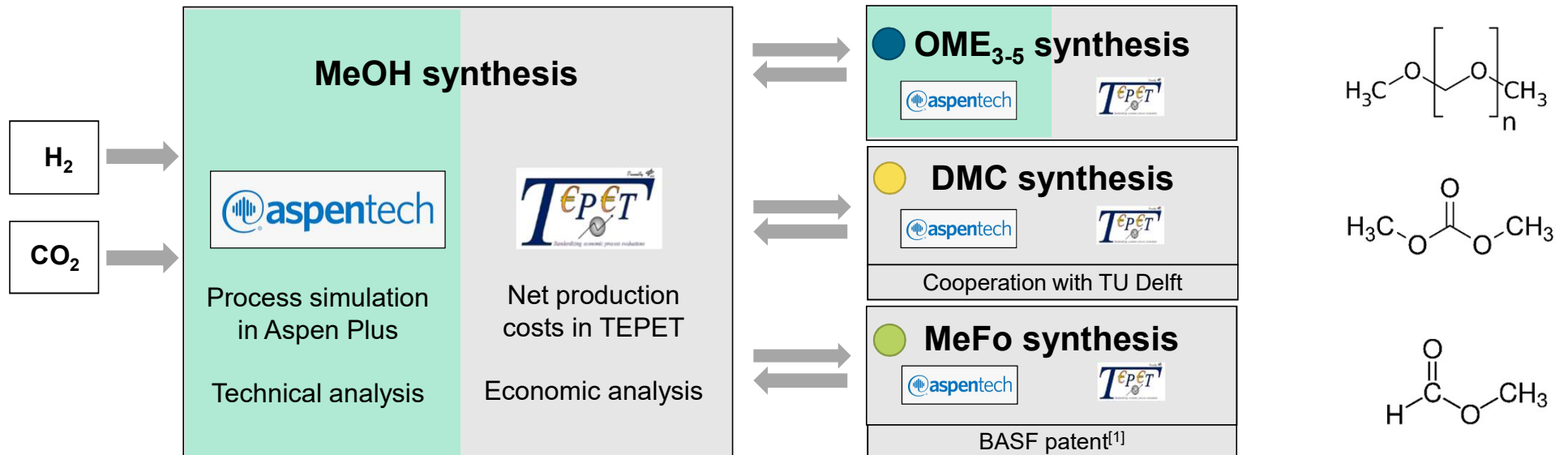
Designer fuels: OME₃₋₅, DMC, MeFo



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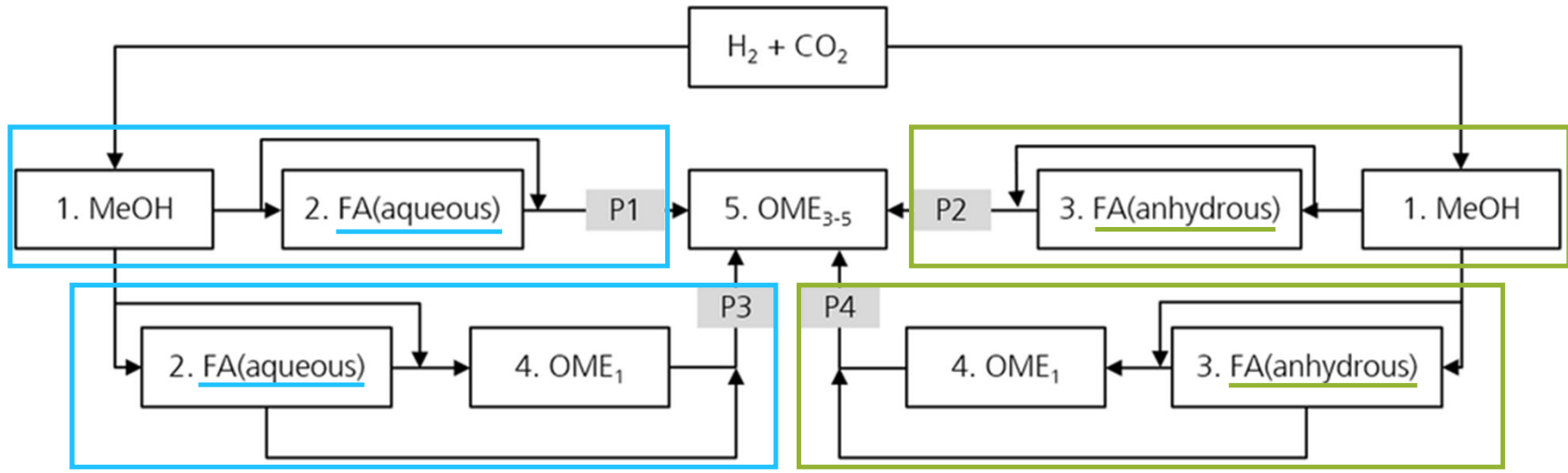
Oxygenates from MeOH



[1] BASF SE – Patent Nr. EP2922815B1

P-t-OME₃₋₅ : The observed routes

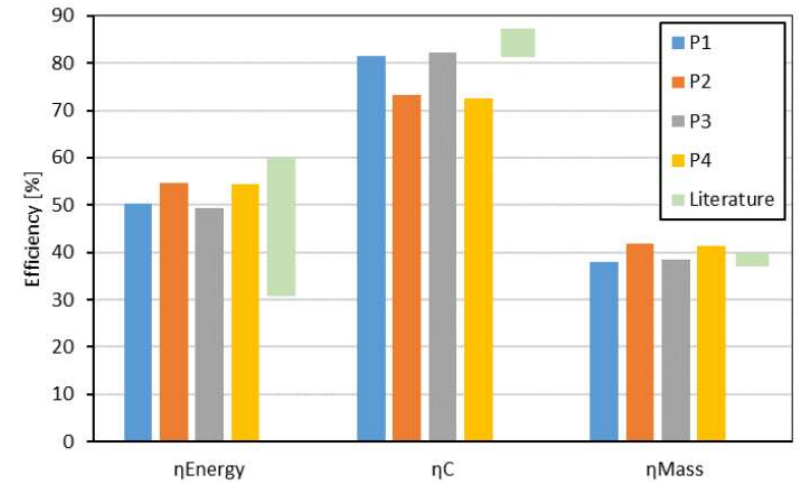
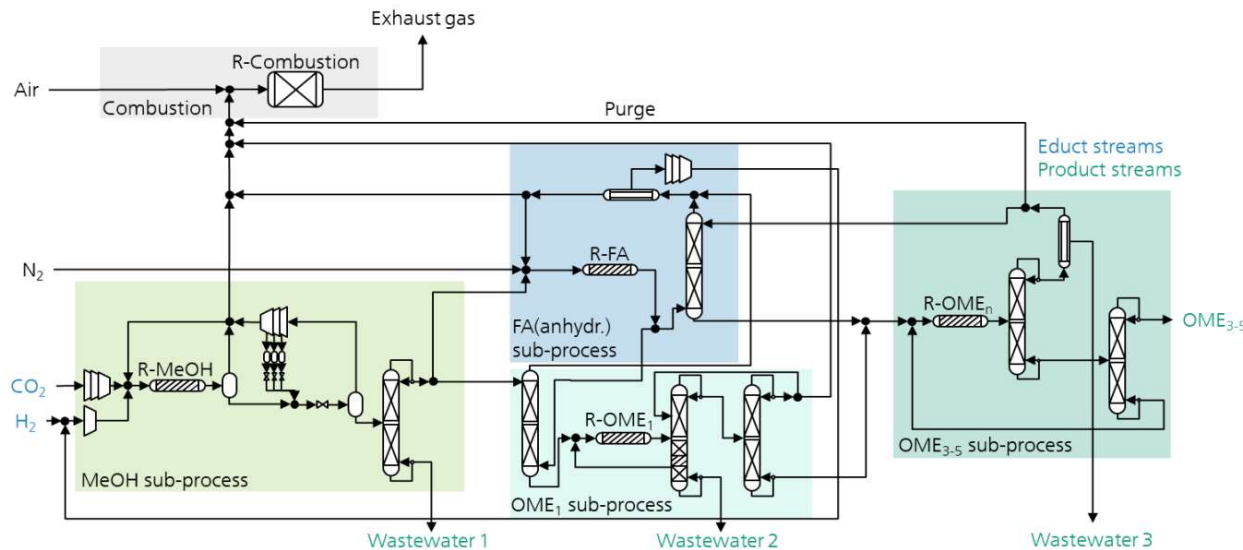
OME₃₋₅ from MeOH



Graph: Mantei et al. (2022): Techno-economic assessment and carbon footprint of processes for the large-scale production of oxymethylene dimethyl ethers from carbon dioxide and hydrogen in Sustainable Energy and Fuels (DOI: 10.1039/D1SE01270C)

P-t-OME₃₋₅ : Technical assessment

Simplified process flow diagram of P4, derived from Fraunhofer ISE factsheet^[1]



$$\eta_{Energy} = \frac{\dot{m}_{OME_{3-5}} \cdot LHV_{OME_{3-5}}}{\sum_k \dot{Q}_k + \sum_l \dot{W}_l + \sum_i \dot{m}_i \cdot LHV_i}$$

$$\eta_C = \frac{C_{OME_{3-5}}}{\sum_i C_i}$$

$$\eta_{Mass} = \frac{\dot{m}_{OME_{3-5}}}{\sum_i \dot{m}_i}$$

	P1	P2	P3	P4
η _{Energy} [%]	50.3	54.6	49.3	54.4
η _C [%]	81.6	73.2	82.1	72.5
η _{Mass} [%]	38.1	41.9	38.5	41.4

[1] Mantei et al. (2022): Techno-economic assessment and carbon footprint of processes for the large-scale production of oxymethylene dimethyl ethers from carbon dioxide and hydrogen in Sustainable Energy and Fuels (DOI: 10.1039/D1SE01270C)

P-t-OME₃₋₅ : Economic assessment

CAPEX: Equipment costs

Equipment type Red: special equipment Green: standard equipment	Characteristics	Literature source (Standard: [1])
Reactors	FA-synthesis (hydrous/anhydrous): fixed bed reactor Remaining type : multi-tubular reactor	[2] (improper capacity range in [1])
Membrane	Water separation: plate membrane, dimensioning [3] H ₂ separation: hollow fiber membrane, dimensioning [4]	[4] (not available in [1])
Film evaporators		[2] (improper capacity range in [1])
Heat exchangers, columns, compressors, pumps, burner, flash drums	Standard equipment according to Peters <i>et al.</i> [1], available in TEPET database	[1]

[1] M. S. Peters, K. D. Timmerhaus, R. E. West, *Plant Design and Economics for Chemical Engineers* 2003, McGraw-Hill Higher Education, New York.

[2] D. R. Woods, *Rules of Thumb in Engineering Practice* 2007, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim.

[3] N. Schmitz, *Production of polyoxymethylene dimethyl ethers from formaldehyde and methanol* 2018, Dissertation, TU Kaiserslautern.

[4] R. W. Baker, *Membrane Technology and Applications* 2012, John Wiley and Sons Ltd, Chichester.

P-t-OME₃₋₅ : Economic assessment



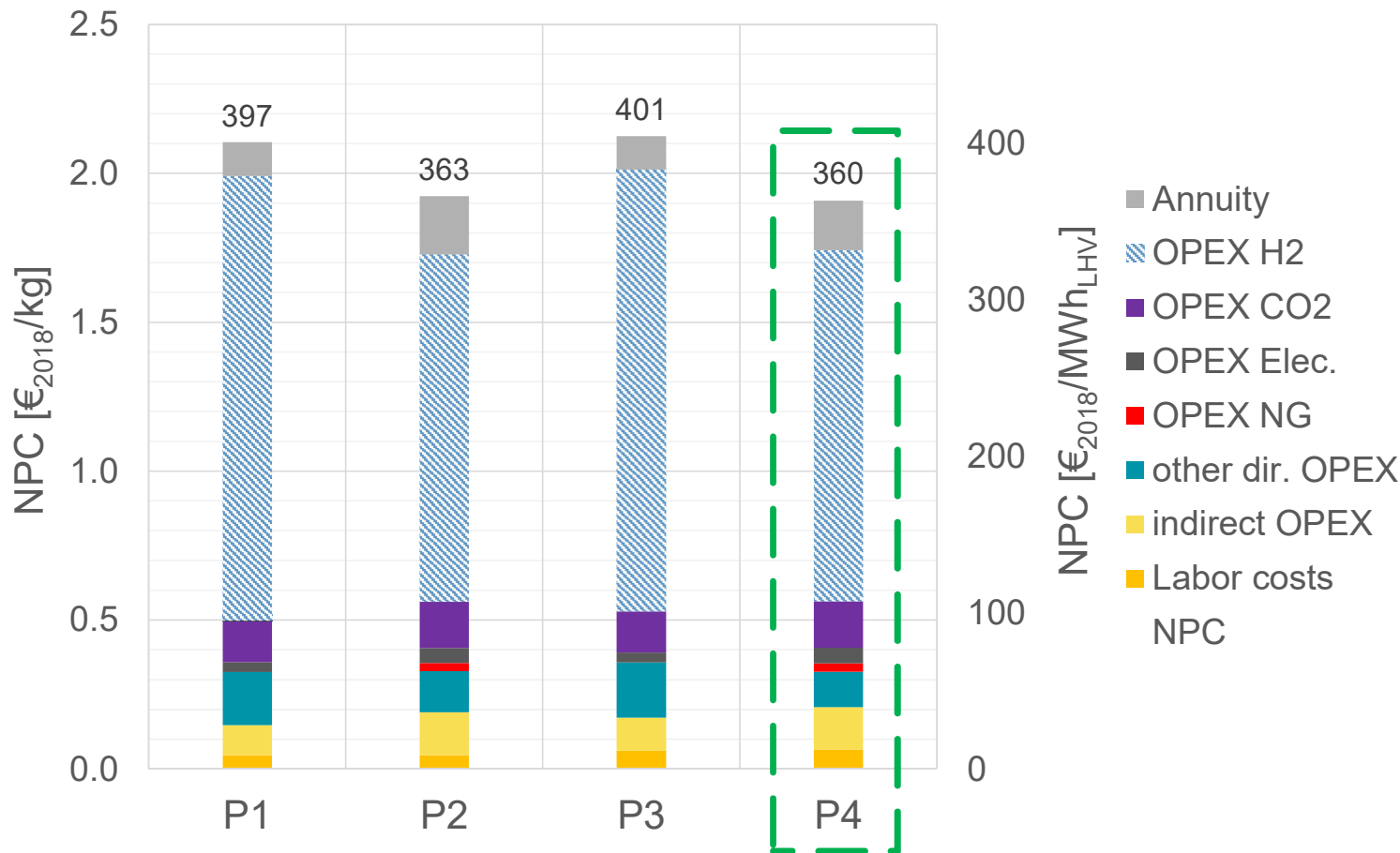
Deutsches Zentrum für Luft- und Raumfahrt
German Aerospace Center



Nachhaltige Mobilität durch synthetische Kraftstoffe

BEniVer

Begleitforschung Energiewende im Verkehr



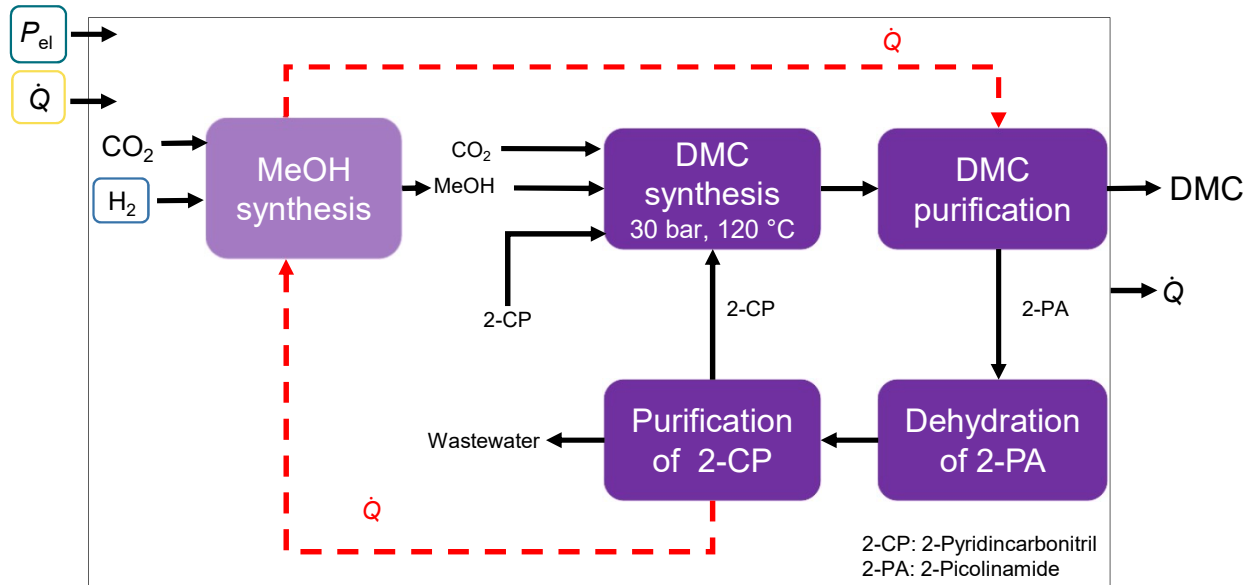
Assumptions	V3.2*
Basis year	2018
Full-load hours	8 000
CO ₂ €/t	71
H ₂ €/t	5 586
Electricity €/MWh	71.5

- *BEniVer general assumptions:
- 300 MW_e power input
 - generic costs - minimum 2018

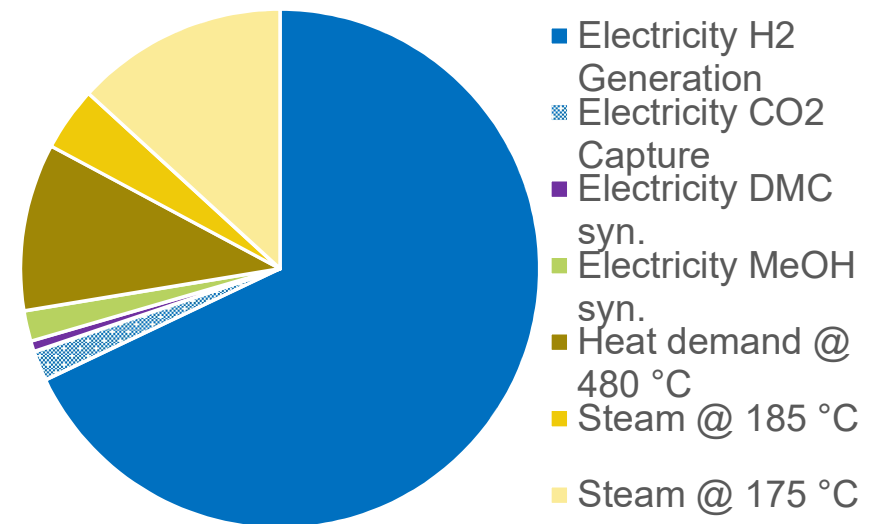
- The anhydrous processes (P2 & P4) form less water out of H₂
- Higher η_{PtL} in P2 & P4
- Lower NPC in P2 & P4
- P4 is the slightly better OME₃₋₅ production option

P-t-DMC : Technical assessment

DMC from MeOH*



Energy demand : 105.8 MW_e + 21.7 MW_{th}
DMC prod. : 50.1 MW_{LHV}



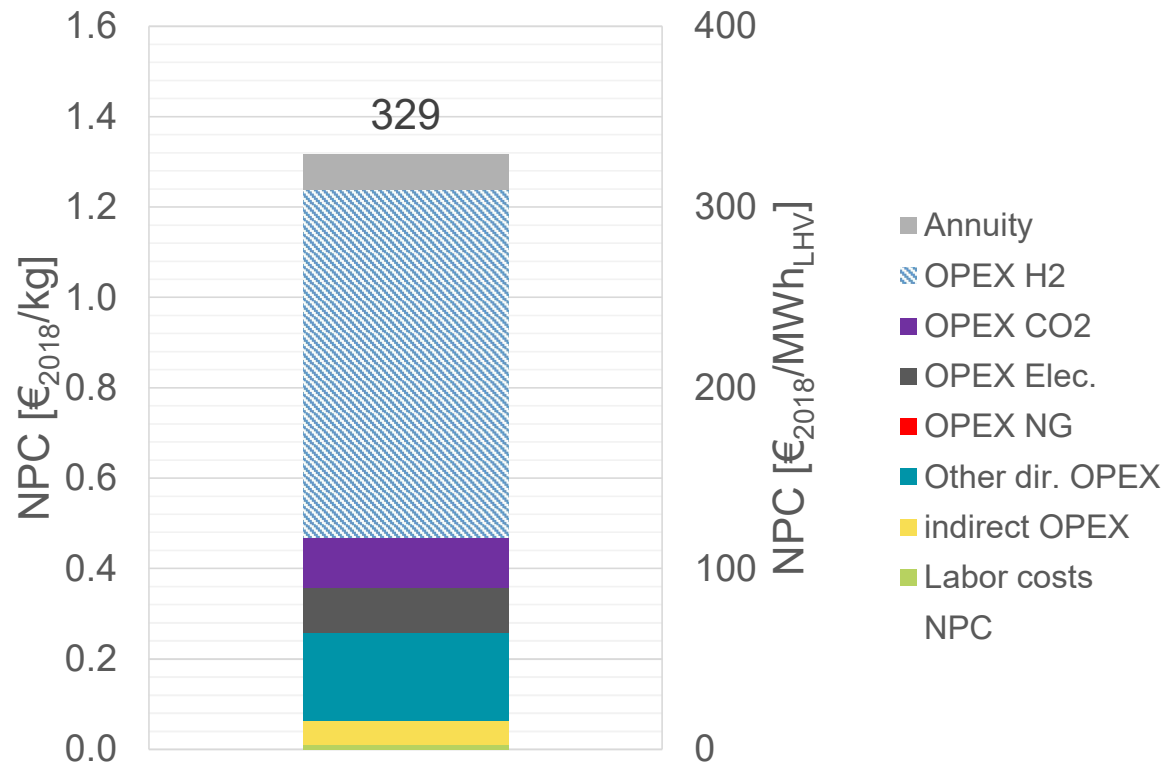
$$\eta_{PtL} = \frac{50.1 \text{ MW}_{LHV}}{105.8 \text{ MW}_e} = 47.3 \% \quad \eta_{EtL} = \frac{50.1 \text{ MW}_{LHV}}{105.8 \text{ MW}_e + 21.7 \text{ MW}_{th}} = 39.3 \%$$

* Innovative lab scale process of TU Delft, publication pending, project results corrected with MeOH production assessment of Rahmat et al.
R-U. Dietrich, Y. Rahmat, DLR-TT, 2 March 2023

P-t-DMC : Economic assessment



DMC from MeOH*



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Begleitforschung Energiewende im Verkehr

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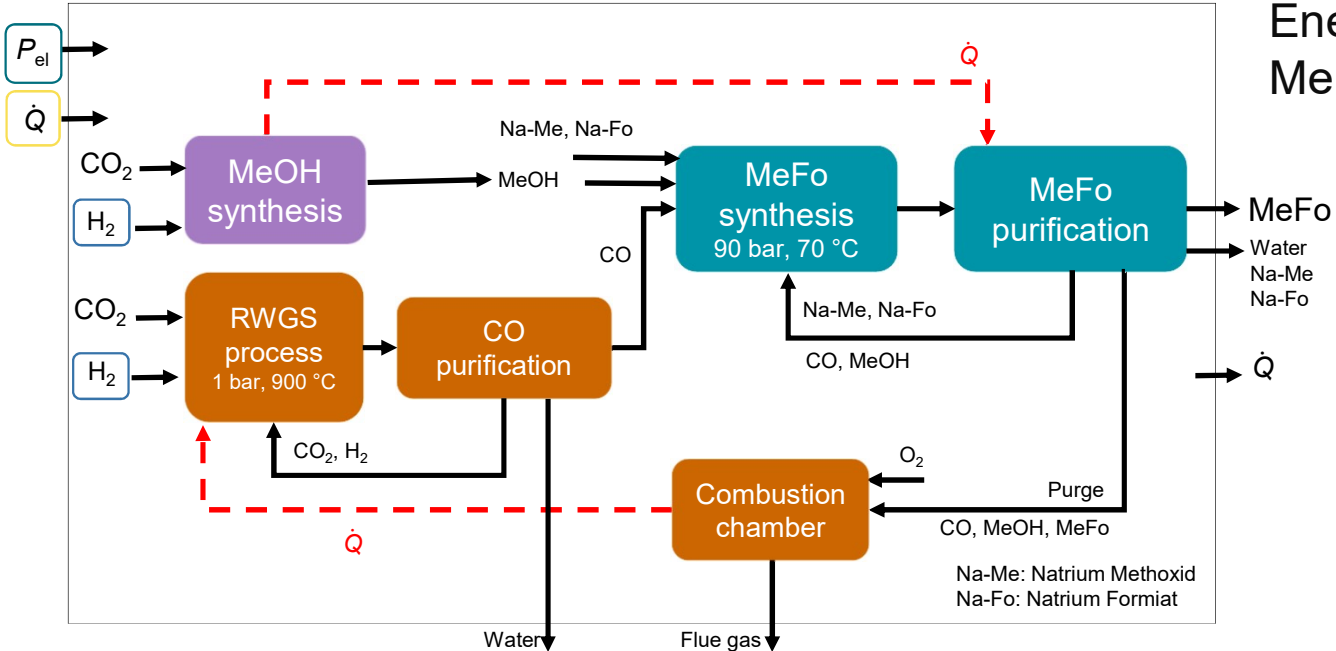
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- H₂ is the cost driver
- CAPEX annuity does not play significant role
- Techno-economic comparison on the slide 15

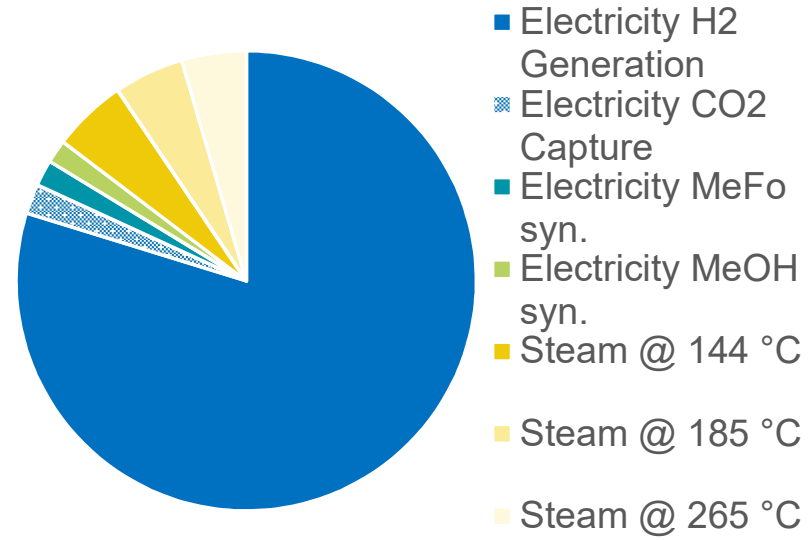
* Innovative lab scale process of TU Delft, publication pending, project results corrected with MeOH production assessment of Rahmat et al.
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P-t-MeFo : Technical assessment

MeFo from MeOH*



Energy demand : 102.5 MW_e + 13.8 MW_{th}
 MeFo prod. : 55 MW_{LHV}



$$\eta_{PtL} = \frac{55 \text{ MW}_{LHV}}{102.5 \text{ MW}_e} = 52.5 \%$$

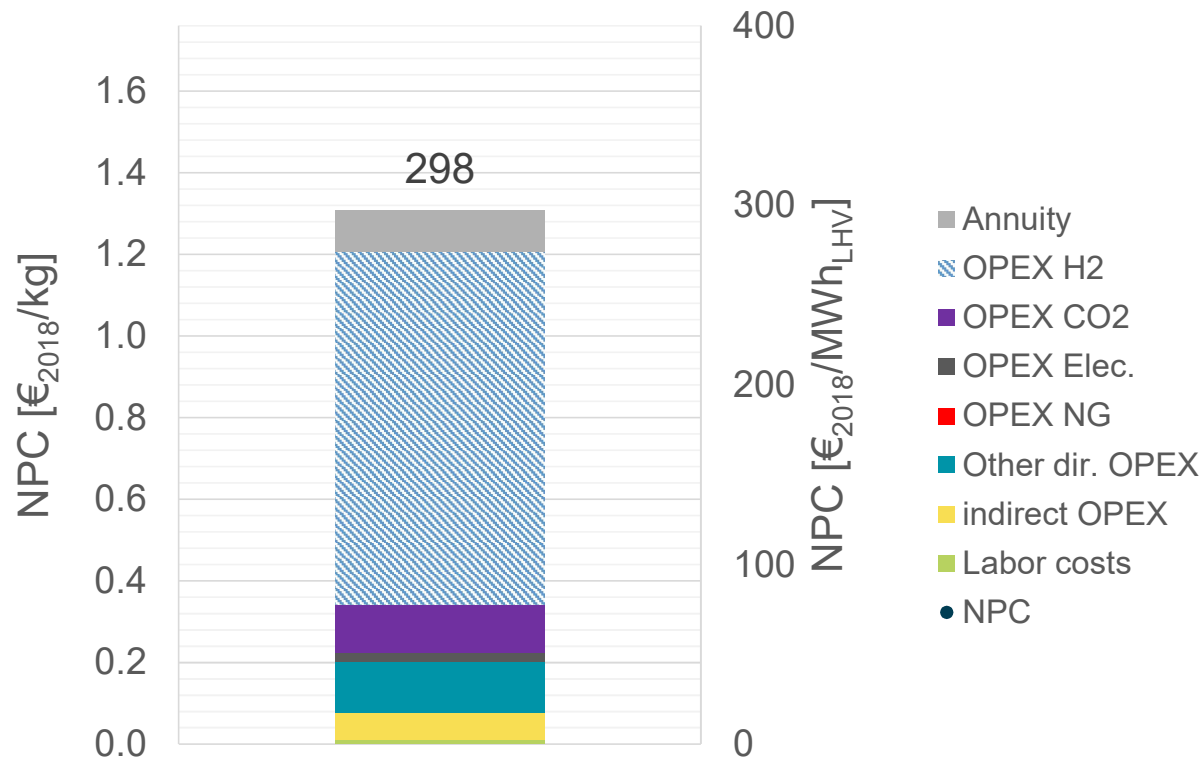
$$\eta_{EtL} = \frac{55 \text{ MW}_{LHV}}{102.5 \text{ MW}_e + 13.8 \text{ MW}_{th}} = 46.4 \%$$

* state-of-the-art BASF process, taken from patent Nr. EP2922815B1, project results corrected with MeOH production assessment of Rahmat et al.
 R-U. Dietrich, Y. Rahmat, DLR-TT, 2 March 2023

P-t-MeFo : Economic assessment



MeFo from MeOH*



BEniVer

Begleitforschung Energiewende im Verkehr

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 • 300 MW_e power input
 • generic costs - minimum 2018

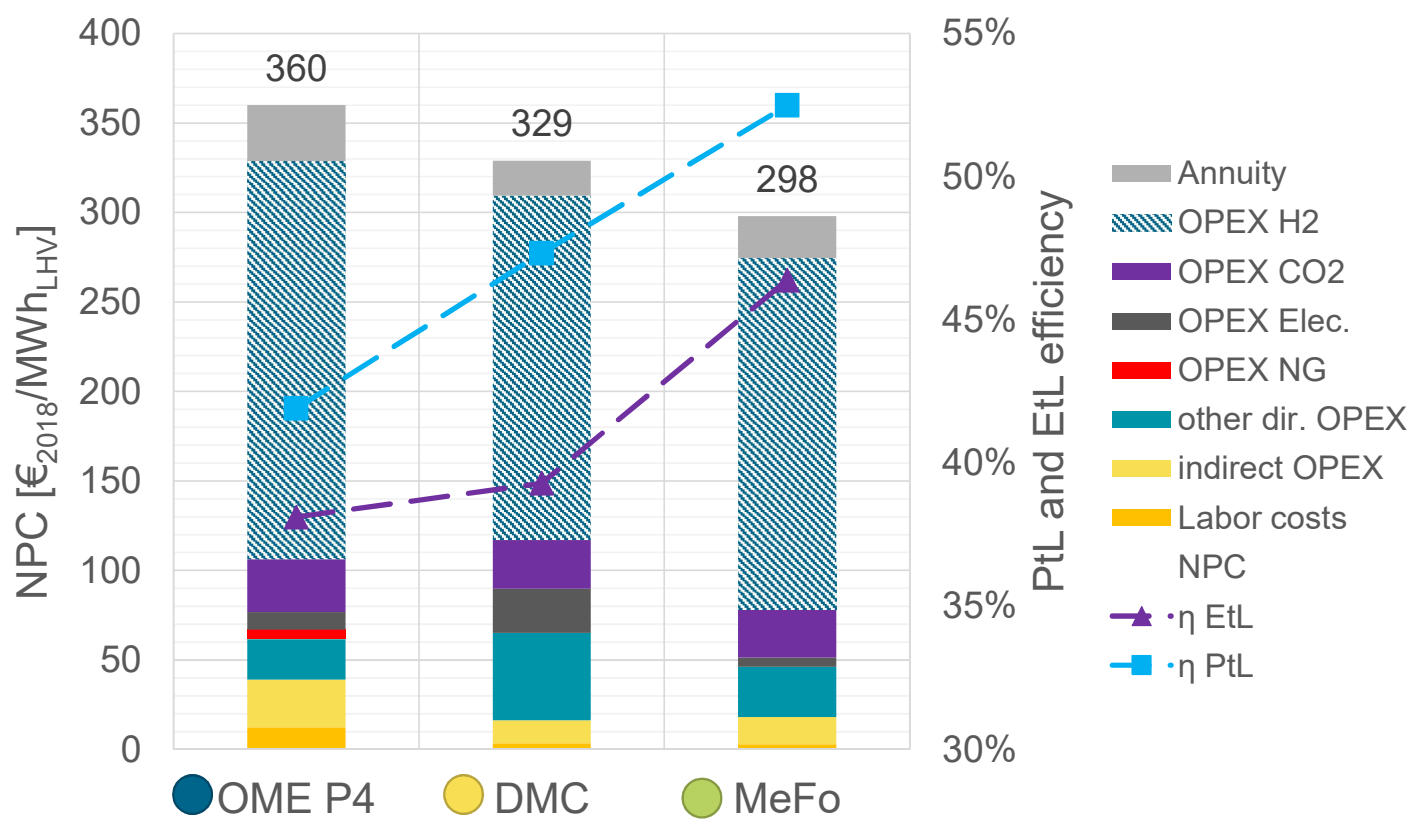
- H₂ is the cost driver
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* state-of-the-art BASF process, taken from patent Nr. EP2922815B1, project results corrected with MeOH production assessment of Rahmat et al.
 R-U. Dietrich, Y. Rahmat, DLR-TT, 2 March 2023

Designer fuels : Techno-economic assessment



Oxygenates from MeOH : **OME₃₋₅**, **DMC**, **MeFo**



BEniVer

Begleitforschung Energiewende im Verkehr

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*BEniVer general assumptions:
generic costs - average 2018

- OME₃₋₅ through the route P4 is not the winner
- MeFo has the lowest NPC due to its relatively high efficiency
- **Application as drop-in fuels?**

A futuristic concept car with a white upper body and a dark blue lower body. It has a sleek, aerodynamic design with a large, curved windshield and a low profile. The car is parked on a paved surface with greenery and a lake in the background.

CONCLUSION: PTX FOR TRANSPORT?

Global e-fuel assessment – initial contribution



Comparing generic / designer fuels

	SNG	MeOH	FT	OME ₃₋₅	DMC	MeFo
Production: technical						
η_{PtX} [%]	59	53	40	42	47	52
η_{EtX} [%]	exotherm.	51	41	38	39	46

$$\eta_{PtX} = \frac{\dot{m}_{fuel} \cdot LHV_{fuel}}{\sum \dot{P}_{el}}$$

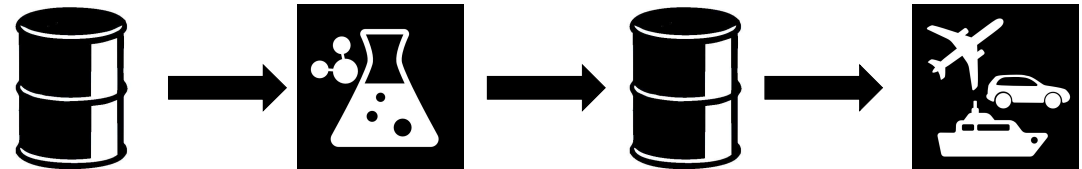
$$\eta_{EtX} = \frac{\dot{m}_{fuel} \cdot LHV_{fuel}}{\sum \dot{P}_{el} + \sum \dot{Q}}$$

Conclusion for e-fuels options in global transport

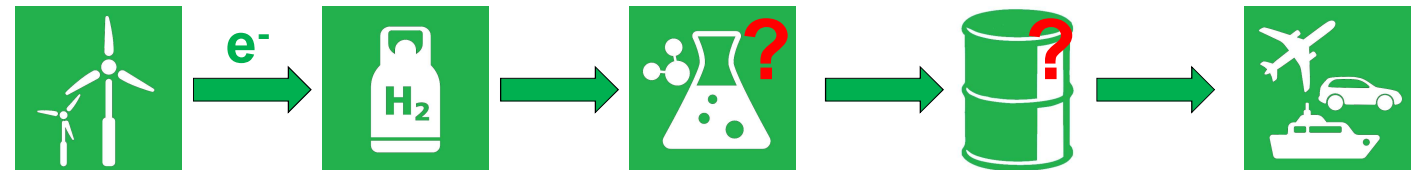
Simple pictograms



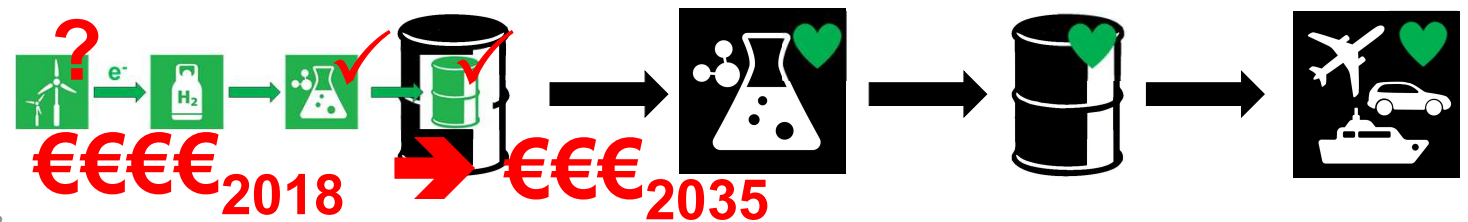
- Present (2018 → 2023)



- Future Dream (2018)
E&V Questions

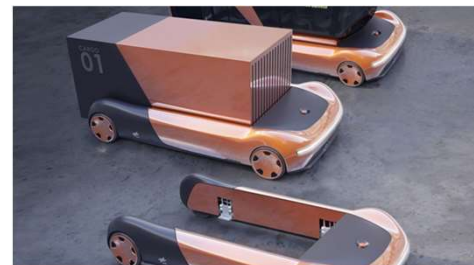


- Reality Check 2023
Q&A



Outlook: Transport beyond 2023

- Maximize mileage from green electrons
 - Favor public over private transport
 - Favor rail over road / air transport
 - Favor electric over hydrogen over ICE
- Invent new / better electric locomotion
 - Efficient public transport
 - New e-bikes, -cars, -trucks, -planes, -ships
 - Smart connection between transport options
- Don't ignore the legacy fleet (short-term response?)
 - Instant drop-in fuels blending mandate
 - Little electrification in marine and aviation
 - Maximize GHG abatement at minimal cost





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**THANK YOU FOR YOUR ATTENTION
ANY QUESTIONS?**

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Ludwigshafen am Rhein, 2 March 2023

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