

# Using Absorption Refrigerator and Metal Hydrides in Hydrogen Fuel Cell Trains: Draft Design Process and Feasibility

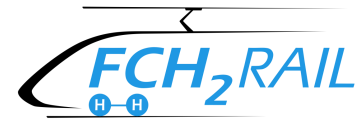
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18/05/2022, Madrid, EHEC 2022

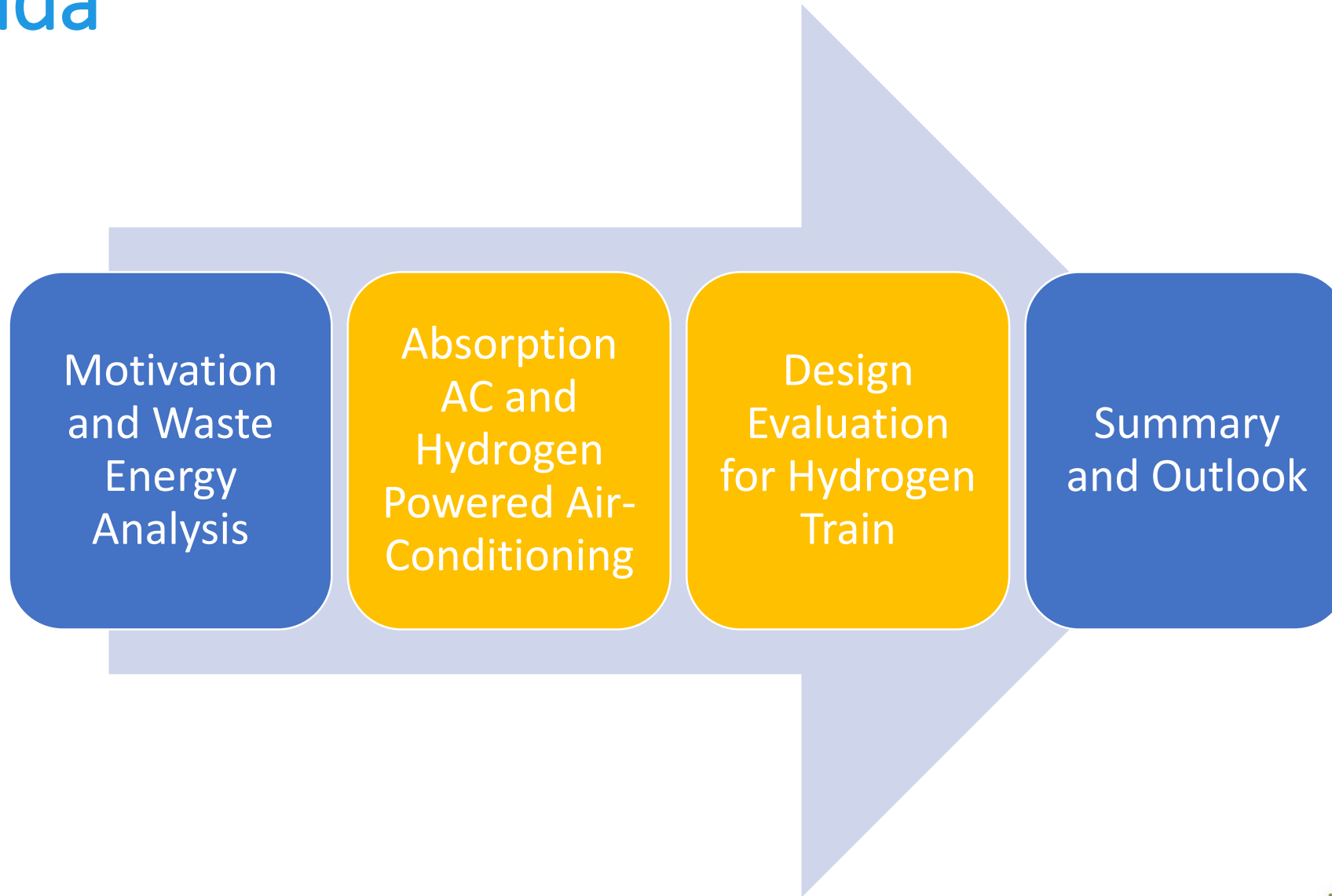
# FCH2RAIL Project in Numbers



- Start date: 01 January 2021
- Duration: 48 Months
- Total budget: **13.3 Mio €**
- H2020 Innovation Action funded by Fuel Cells and Hydrogen 2 Joint Undertaking, now Clean Hydrogen Partnership
- 7 technical Work packages, 29 Milestones, 43 Deliverables
- **2 Demonstrators:** Fuel Cell Hybrid Power Pack and Bi-Mode Train
- 8 Beneficiaries from Belgium, Germany, Spain and Portugal



# Agenda



# Motivation and Objective

## Motivation


- SoA energy demand for cooling ca. 12,300 kWh/a in regional train coach (6,150 kWh electric)
- 370 kgH<sub>2</sub>/a → 3,330 €/a (9 €/kgH<sub>2</sub>)

## Objective

- How to reduce HVAC energy demand in hydrogen trains?
- Use waste energy for this reduction

HVAC: Heating Ventilation and Air-Conditioning

1) N. Schindler (2020) "Deliverable D4.1 State-of-the-art of HVAC Technologies", FINE2



Ref. Ares(2020)7199396 - 30/11/2020

**Furthering Improvements in Integrated Mobility Management, Noise and Vibration, and Energy in Shift2Rail**

**Deliverable D4.1**

**State-of-the-art of HVAC Technologies**

Due date of deliverable: 30/11/2020  
Actual submission date: 30/11/2020

Leader/Responsible of this Deliverable: Niklas Schindler (DB)

WP Approval	TMT Approval	SC Approval
30.09.2020	18.10.2020	13.11.2020

Document status		
Revision	Date	Description
0.1	23.07.2020	Draft
0.2	30.10.2020	Final draft incl. quality check
1.0	30.11.2020	First issue

Project funded from the European Union's Horizon 2020 research and innovation programme – Shift2Rail

Dissemination Level		
PU	Public	X
CO	Confidential, restricted under conditions set out in Model Grant Agreement	
CI	Classified, information as referred to in Commission Decision 2001/844/EC	

[1]

# Waste Energy Analysis

- Hydrogen compression work and waste heat is currently unused in rolling stock

→ FC waste heat and hydrogen compression work can support auxiliaries

➔ What is the amount of energy?  
What is the quality of energy?

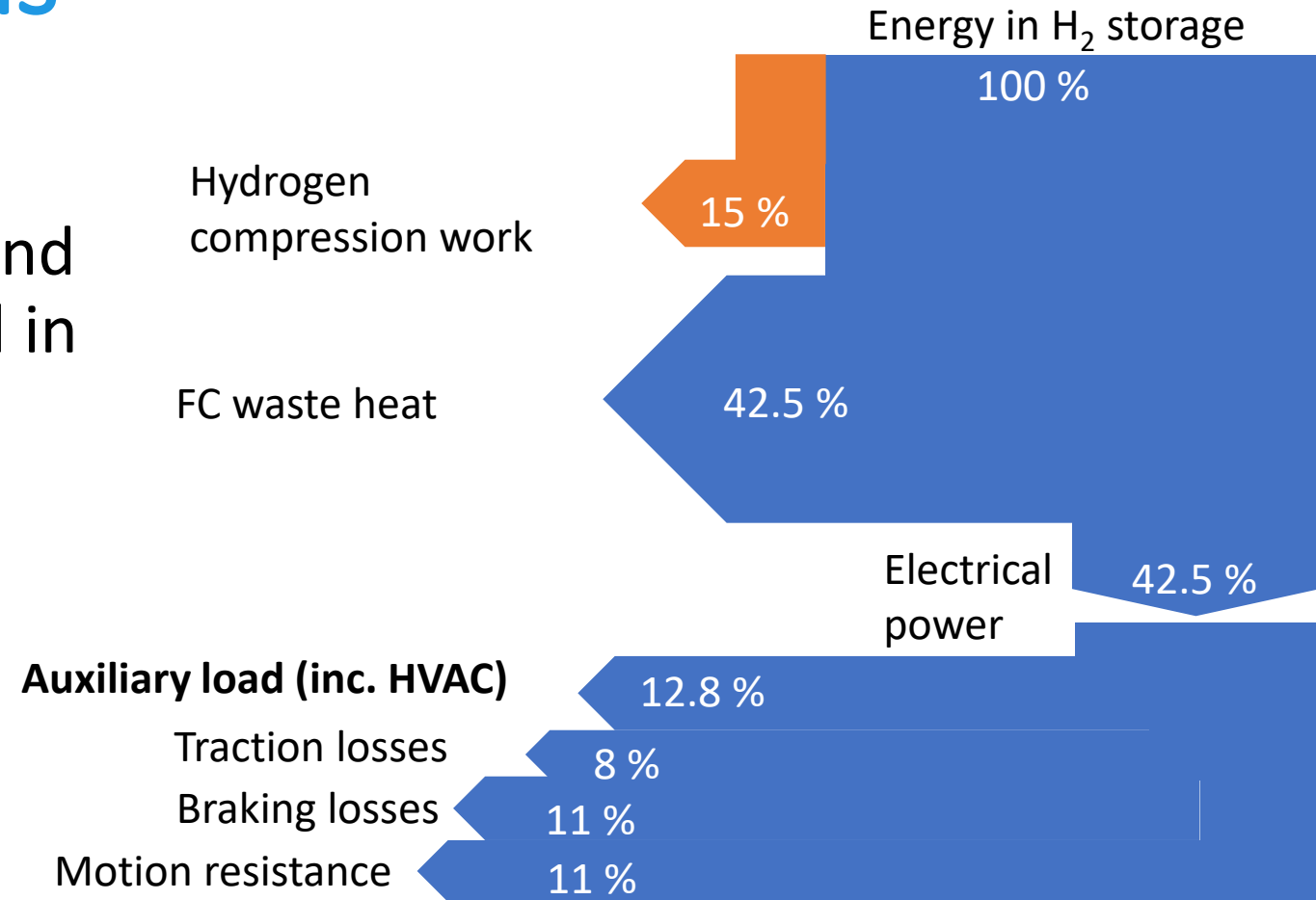


Fig. 2: Energy flow in urban FC rail systems (modified [2, 3])

2) Gonzáles-Gil et. al (2014) "A systems approach to reduce urban rail energy consumption", E. Conversion and Management  
 3) Cummins (2022) "Energy Efficiency of HD30 Systems", Homepage

# Waste Energy - Amount and Quality

## Waste heat flow

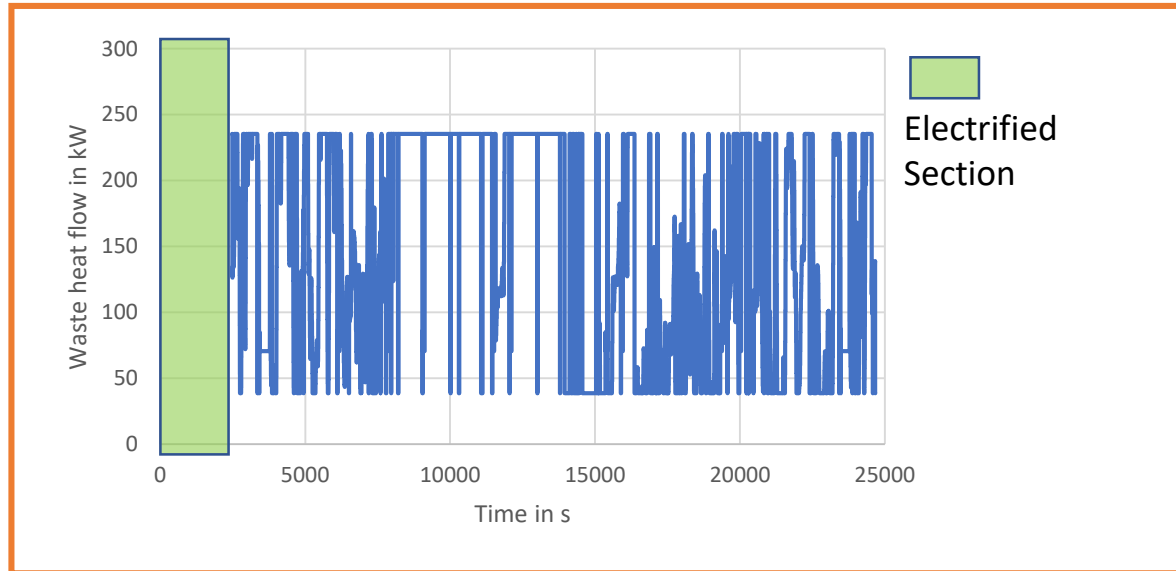


Fig. 3: Simulated fuel cell waste heat for part load use case [4]

- ➔ Up to 75 °C fuel cell coolant temperature
- ➔ Waste heat availability is track dependent

## Hydrogen mass flow

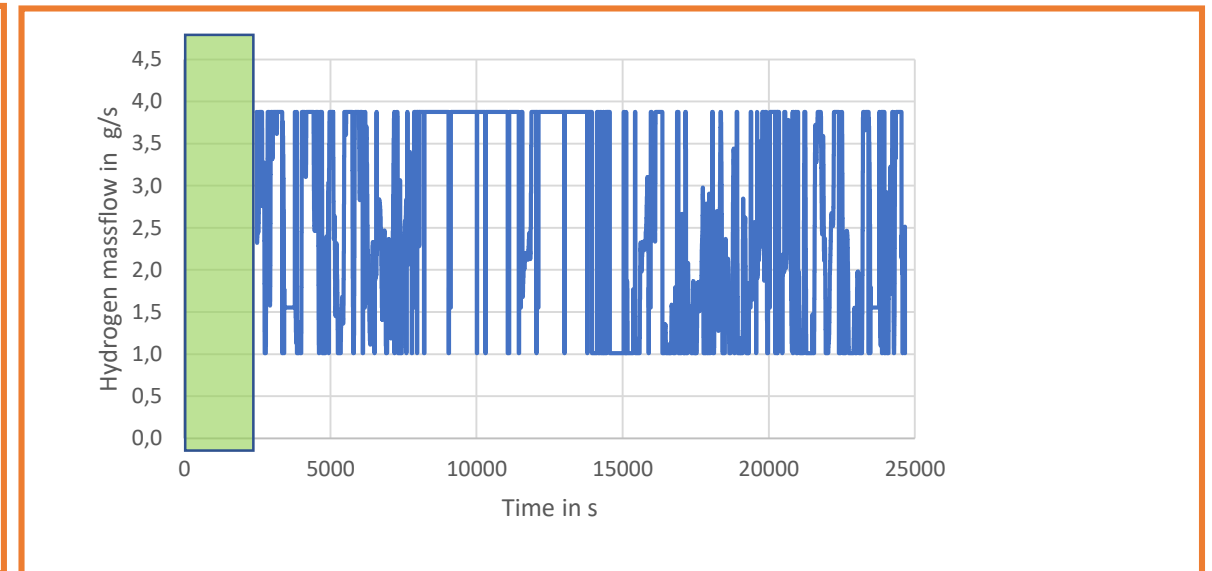
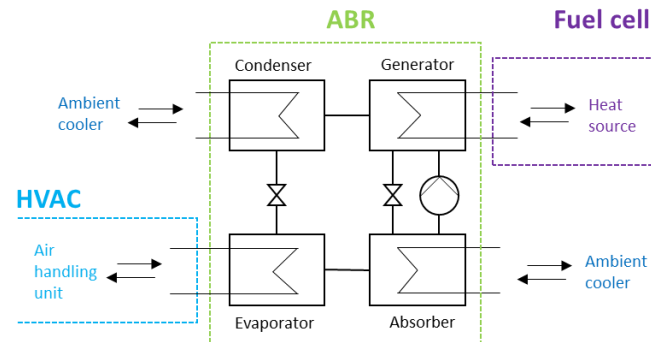


Fig. 4: Simulated hydrogen consumption for part load use case [4]

- ➔ 50 bar is considered as an empty tank and 8.5 bar is the FC inlet pressure (pressure regulator)
- ➔ Compression work is track dependent

# Technologies for Waste Energy Usage

## Absorption refrigerator (Waste heat)

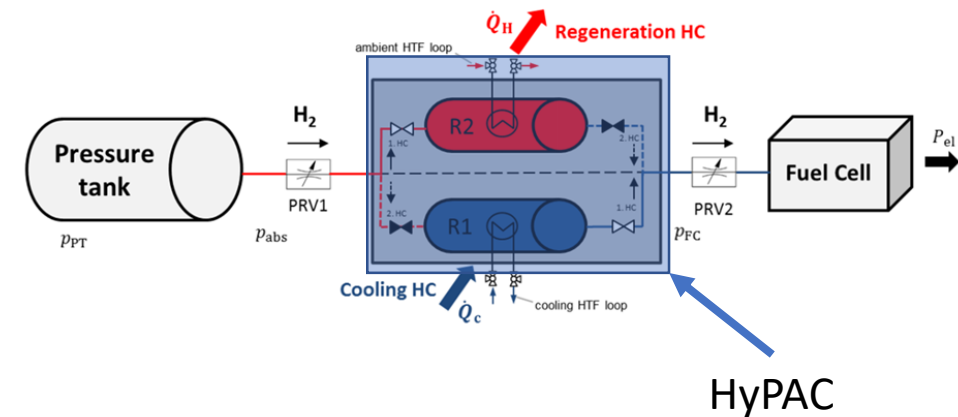


- Pair of refrigerant (water) and absorbent (LiBr) drives refrigerant cycle and thermal compressor
- Thermal compressor uses a heat flow to increase pressure of the refrigerant
- Only liquid pumps and no compressors are needed
- ➔ Fuel Cell's waste heat will be used to provide cooling capacity

### Constraints:

- Waste heat temperature
- Ambient Temperature
- Waste heat amount

## Hydrogen Powered Air-Conditioning (H<sub>2</sub> Compression work)



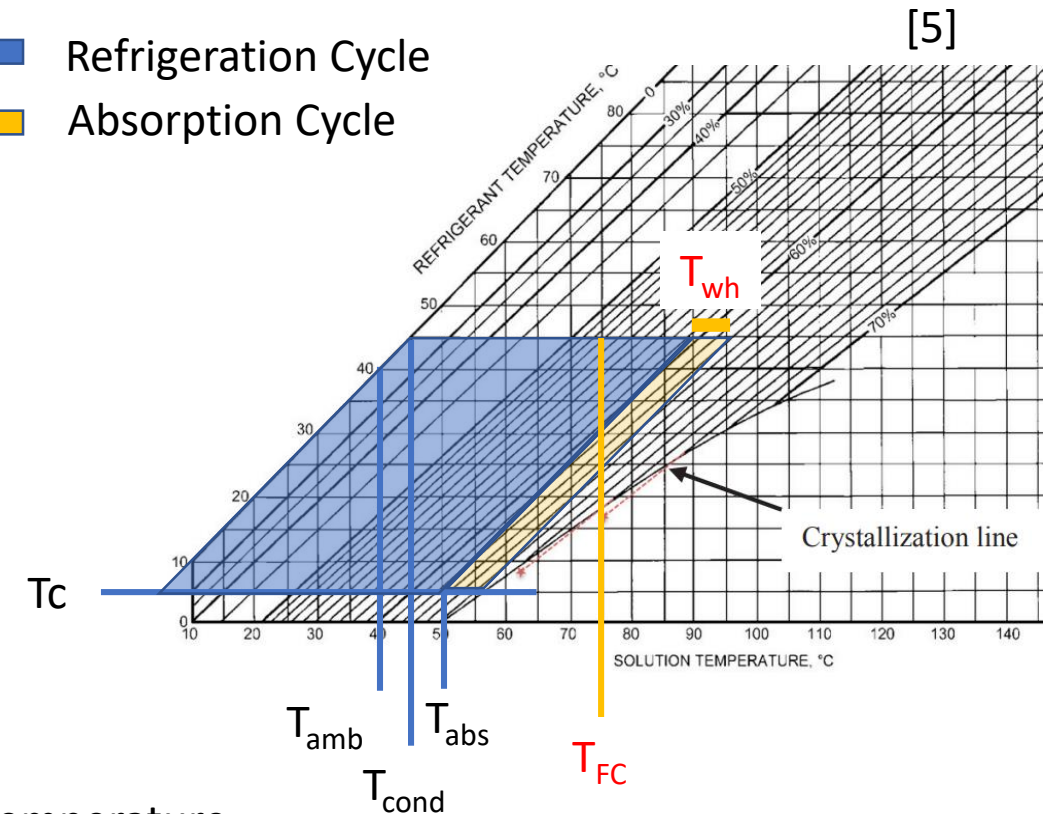


# Absorption Refrigerator

## *standard cycle - LiBr*

Process / Material constraints	
Cooling temperature	$T_c = 5^\circ\text{C}$
Maximum ambient temperature	$T_{\text{amb}} = 40^\circ\text{C}$
Minimum condenser temperature	$T_{\text{cond}} = 45^\circ\text{C}$
Minimum absorber temperature	$T_{\text{abs}} = 50^\circ\text{C}$
Waste heat temperature range	$T_{\text{wh}} = 97^\circ\text{C} - 105^\circ\text{C}$
Fuel cell waste heat temperature	$T_{\text{FC}} = 75^\circ\text{C}$

 Refrigeration Cycle  
 Absorption Cycle



Fuel cell temperature is below minimum waste heat temperature  
Standard cycle is not feasible with fuel cell waste heat temperature



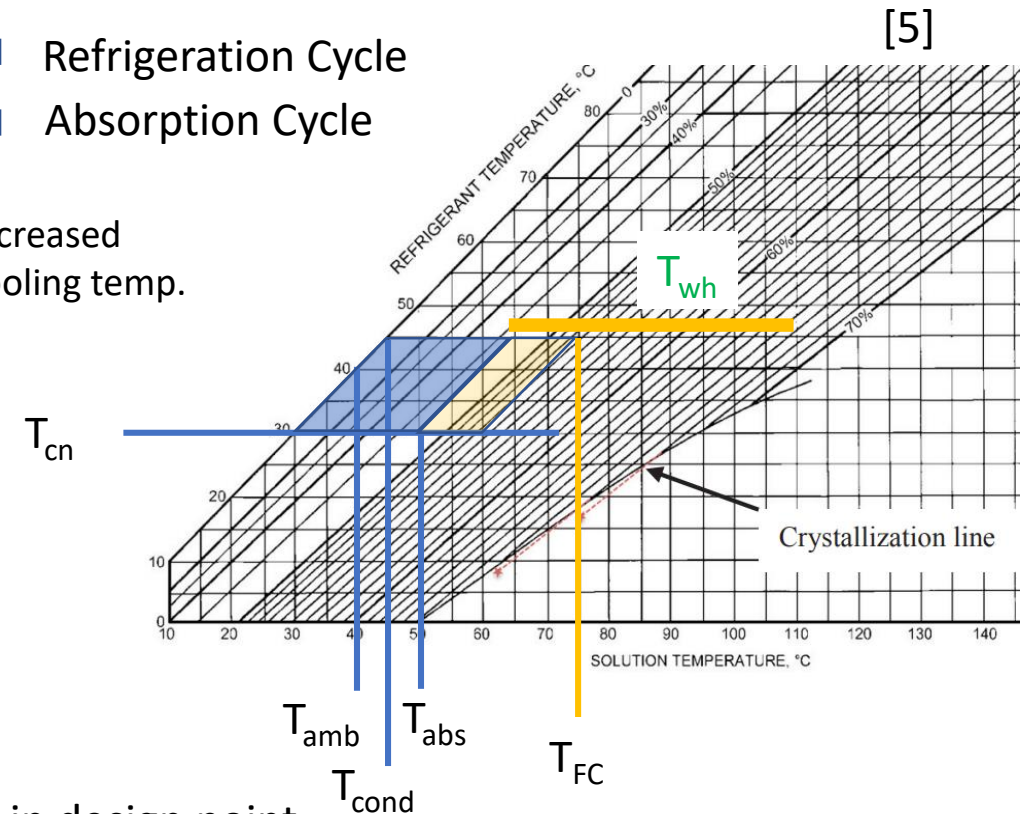
# Absorption Refrigerator

## *improved cycle - LiBr*

Process / Material constraints	
Cooling temperature new	$T_{cn} = 30^{\circ}\text{C}$
Maximum ambient temperature	$T_{amb} = 40^{\circ}\text{C}$
Minimum condenser temperature	$T_{cond} = 45^{\circ}\text{C}$
Minimum absorber temperature	$T_{abs} = 50^{\circ}\text{C}$
Waste heat temperature range	$T_{wh} = 65^{\circ}\text{C} - 105^{\circ}\text{C}$
Fuel cell waste heat temperature	$T_{FC} = 75^{\circ}\text{C}$

Refrigeration Cycle  
Absorption Cycle

Increased cooling temp.



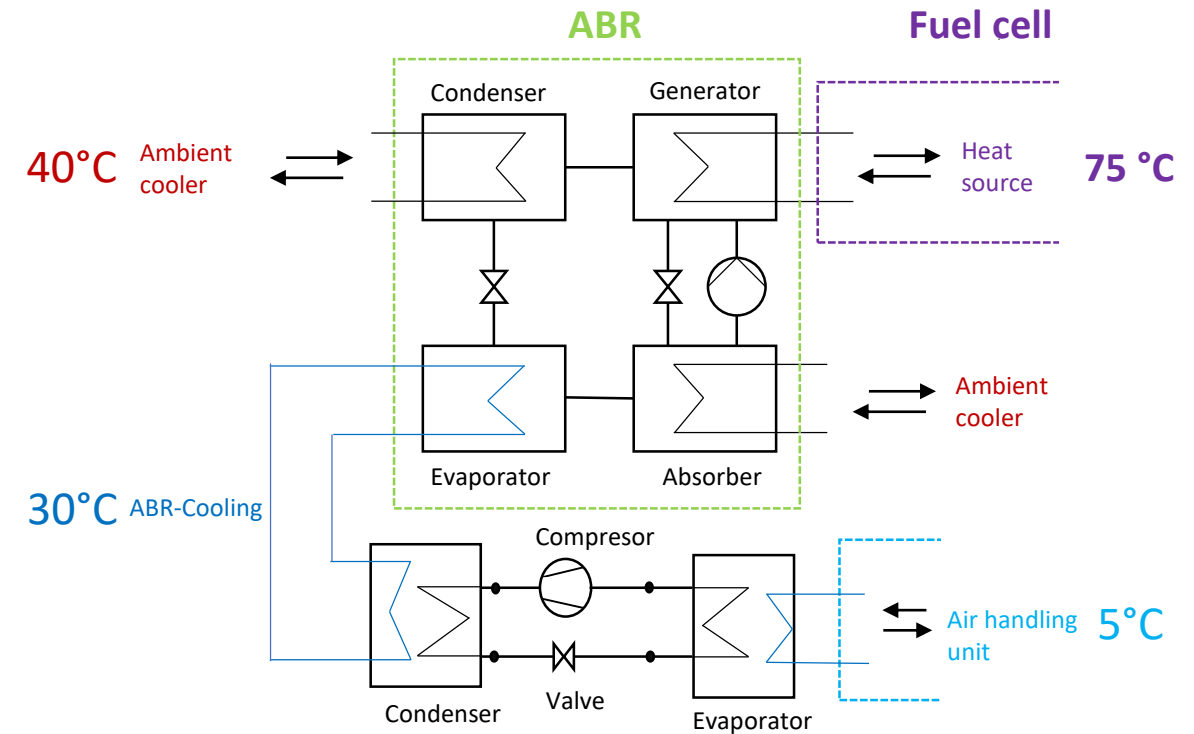
Improved absorption AC cycle provide cooling capacity in design point  
Combination with Vapor Compression Refrigerator System is necessary

4) M. Kordel (2022) „D1.6 - Report on concept, draft design and preliminary simulation requirements”, FCH2Rail

# Absorption Refrigerator

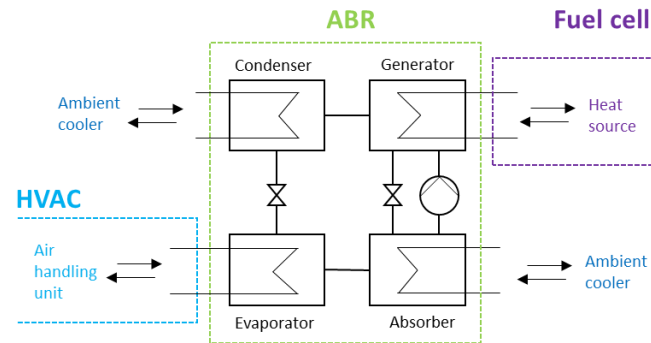
## *new concept*

- With this fuel cell system, the absorption refrigerator can operate in a cascade with a VCRS
- 77 % of the time, the waste heat is above 58 kW and the absorption refrigerator can provide the cooling capacity in design point
- Concept in design point is defined
- Next Steps: Annual energy savings in different climate zones

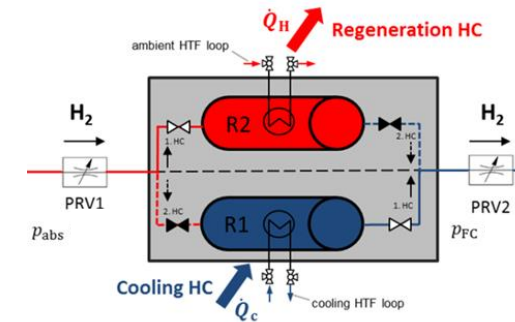


# Technologies for Waste Energy Usage

## Absorption Refrigerator



## HyPAC (H2 Compression work)



- 2 Metal-Hydride reactors
  - Absorption of high pressure H2 from hydrogen tank → Heat
  - Desorption at low pressure towards fuel cell → Cold
  - Switching between absorption and desorption when desorption pressure is below threshold (8.5 bar)
- Pressure difference between tank and fuel cell will be used to provide cooling capacity

### Constraints:

- Tank pressure and fuel cell pressure
- Ambient temperature
- Hydrogen mass flow and dynamics

# HyPAC

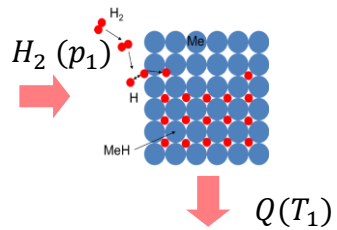
## state of the art

### Material Characteristics

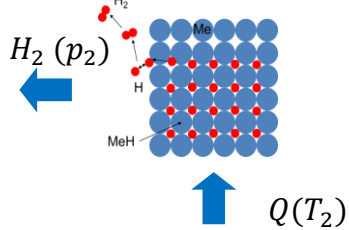
$$\ln\left(\frac{p_{eq}}{p_0}\right) = \frac{\Delta H_{abs/des}}{R \cdot T_{EQ}} + \frac{\Delta S_{abs/des}}{R}$$

$$\dot{Q}_{abs/des} = \frac{\dot{m}_{H_2}}{M_{H_2}} \cdot \Delta H_{abs/des}$$

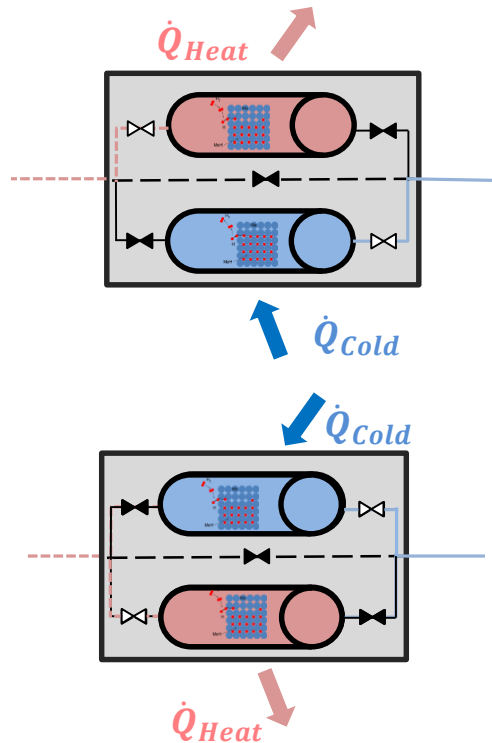
#### Absorption:



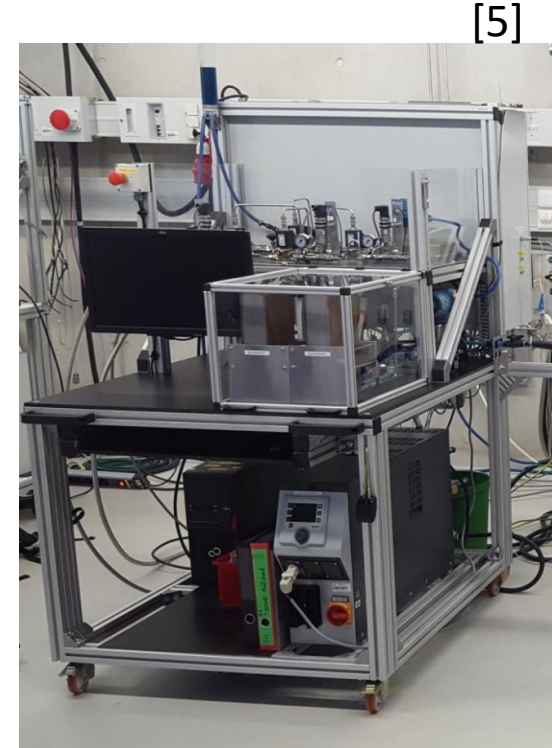
#### Desorption:



### Operating Principle

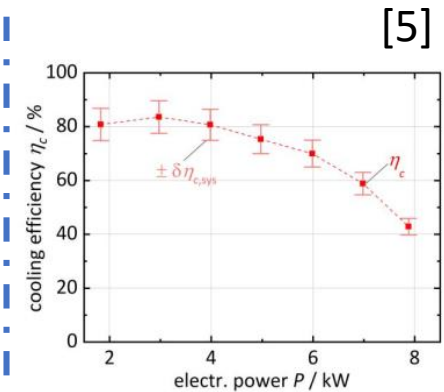


### Test Bench



5) C. Weckerle (2020) "A metal hydride air-conditioning system for fuel cell vehicles."

### Test Bench – Efficiency



Capability is temperature and pressure dependent  
An established material was selected for FCH2Rail

# HyPAC

standard cycle

Process / Material constraints	
Cooling Temperature requirement	$T_c = 5^\circ\text{C}$
Optimal Fuel Cell Inlet Pressure	$p_{FC0} = 6 \text{ bar}$
Maximum ambient temperature	$T_{\text{amb}} = 40^\circ\text{C}$
Minimum recool temperature	$T_{\text{rec}} = 45^\circ\text{C}$
Minimum tank pressure	$p_{\text{abs}} = 50 \text{ bar}$
Actual Fuel Cell Inlet Pressure in FCH2RAIL	$p_{FC} = 8.5 \text{ bar}$

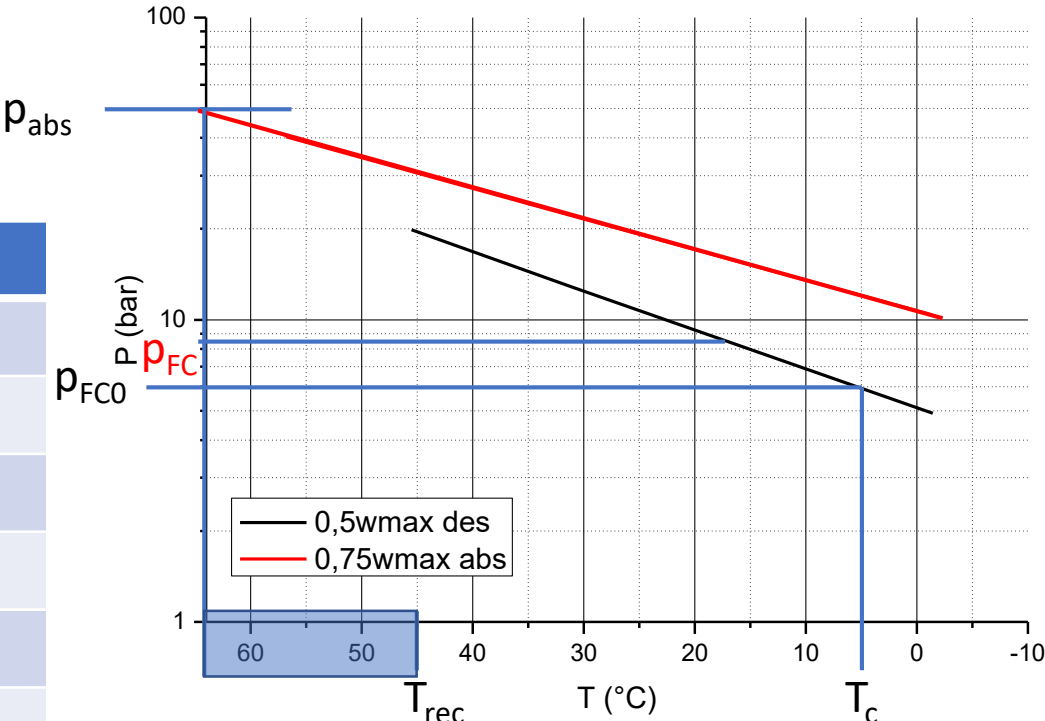


Fig. 5: Van't hoff plot of C2-Hydralloy metal hydride [5]



Fuel cell pressure is above optimal fuel cell inlet pressure  
Standard cycle is not feasible with fuel cell pressure

$$\ln\left(\frac{p_{GG}}{p_0}\right) = \frac{\Delta H_{abs/des}}{R \cdot T_{GG}} + \frac{\Delta S_{abs/des}}{R}$$

5) C. Weckerle (2020) "A metal hydride air-conditioning system for fuel cell vehicles."

# HyPAC

## *improved cycle*

Process / Material constraints	
Cooling Temperature new	$T_{cn} = 18.5^{\circ}\text{C}$
New Fuel Cell Inlet Pressure	$p_{FC} = 8.5 \text{ bar}$
Maximum ambient temperature	$T_{amb} = 40^{\circ}\text{C}$
Minimum recool temperature	$T_{rec} = 45^{\circ}\text{C}$
Minimum tank pressure	$p_{abs} = 50 \text{ bar}$
Actual Fuel Cell Inlet Pressure in FCH2RAIL	$p_{FC} = 8.5 \text{ bar}$

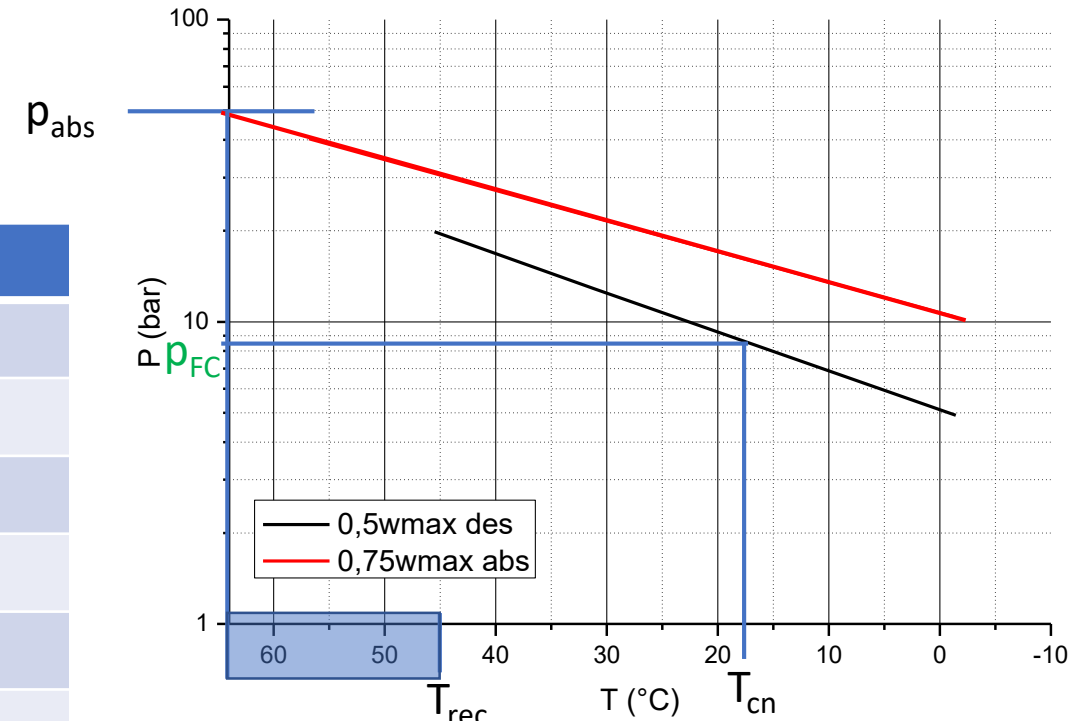


Fig. 5: Van't Hoff plot of C2-Hydralloy metal hydride [5]

➔ Improved HyPAC cycle can provide cooling capacity in design point  
Combination with VCRS is necessary

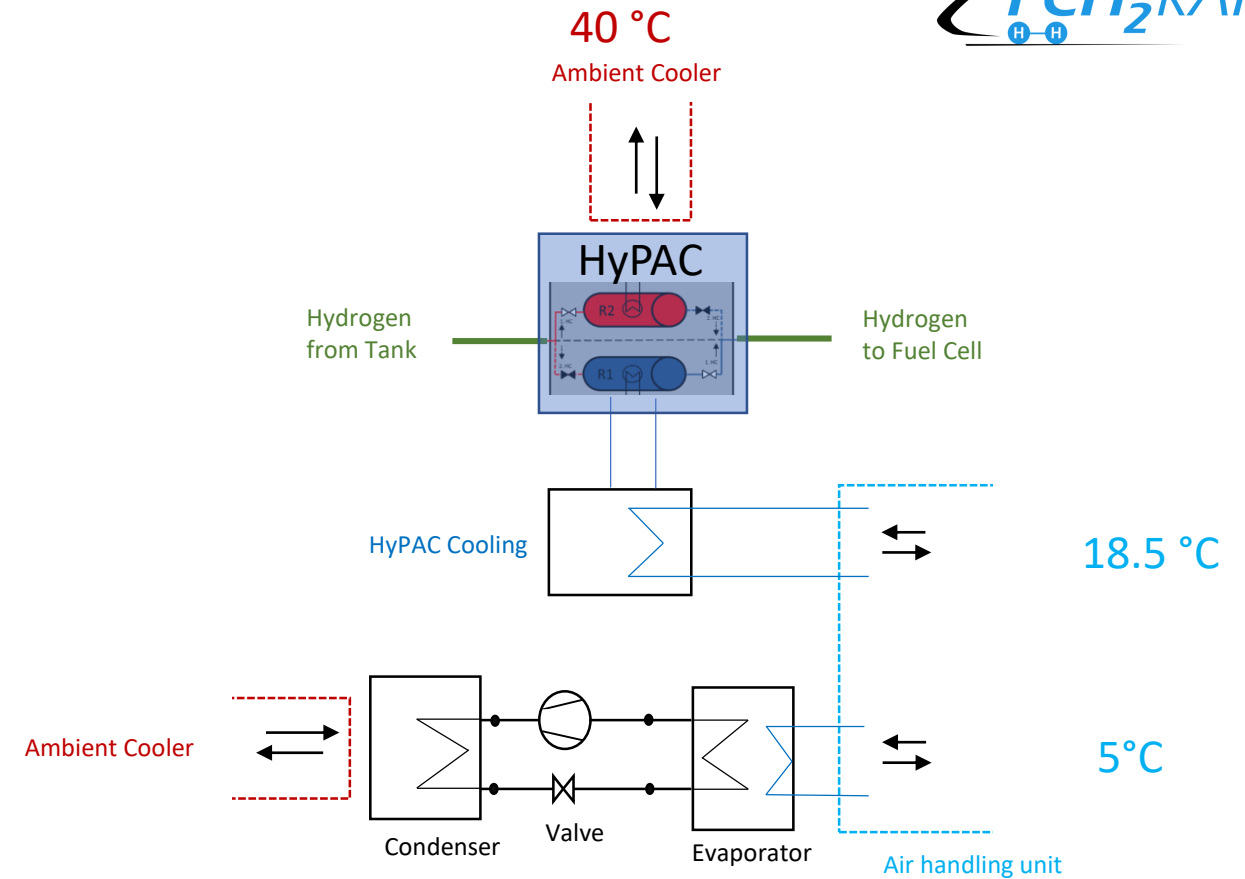
5) C. Weckerle (2020) "A metal hydride air-conditioning system for fuel cell vehicles."



# HyPAC

## *new concept*

- Combination with VCRS is necessary to cover all operating points
- With 3.9 g/s ( $H_2$ ) 32 kW cooling capacity can be provided
- 32 % of the time the Hydrogen massflow is above 3.9 g/s
- Concept in design point is defined
- Next Steps: Annual energy savings in different climate zones and for part load operating



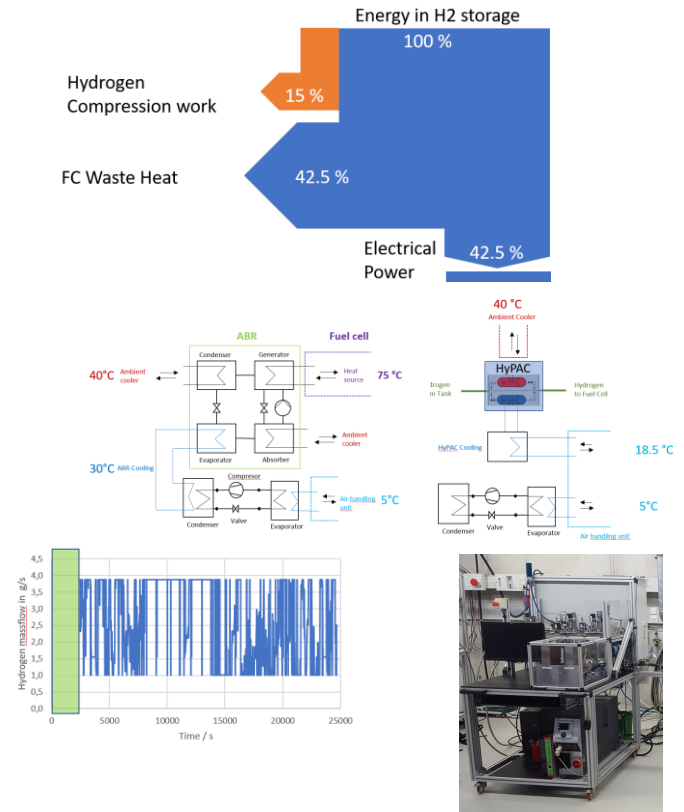
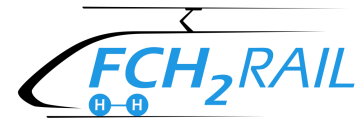
32 % of the time, cooling capacity can be reduced by up to 32 kW  
For the FCH2Rail scenario, 70.7 kWh cooling energy can be saved (35.6 kWh electrical)

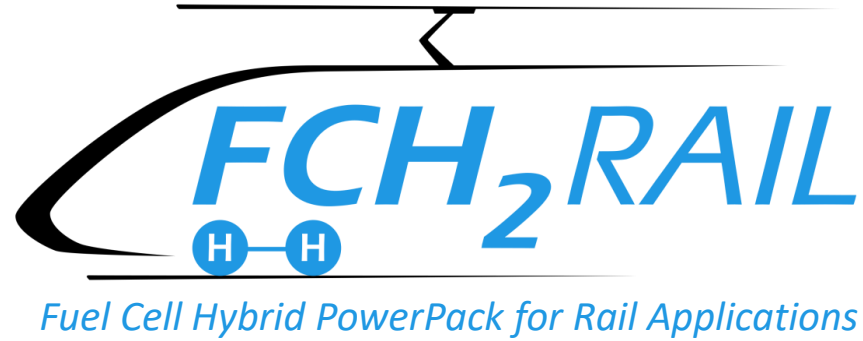
# Summary and Outlook

- Waste heat and pressure energy is currently unused on rolling stock
- Design concept for Absorption AC and HyPAC in FCH2Rail FC train has been developed
- Absorption AC (LiBr) can support VCRS 77 % of the time in selected use case
- HyPAC can reduce up to 32 % cooling capacity in design point

## Outlook

- Detailed simulations in different climate zones
- Calculation of potential annual energy reduction for both technologies  
→ Part load





Thank you for your attention



[www.fch2rail.eu](http://www.fch2rail.eu)