

# Molten Halide Salts for Large-Scale Energy Storage

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# Contents

- Introduction
  - Energy research at DLR
  - Large-scale energy storage for Energy Transition
- Molten halide salts for large-scale energy storage
  - Thermal energy storage (TES)
  - Liquid metal battery (LMB)
- Summary and outlook



# German Aerospace Center (DLR)

- Research Institution (six research areas)
- Space Agency
- Project Management Agency



**Aeronautics**

**Space**

**Transportation**

**Energy**

**Security**

**Digitalization**



# Energy Research Program Themes

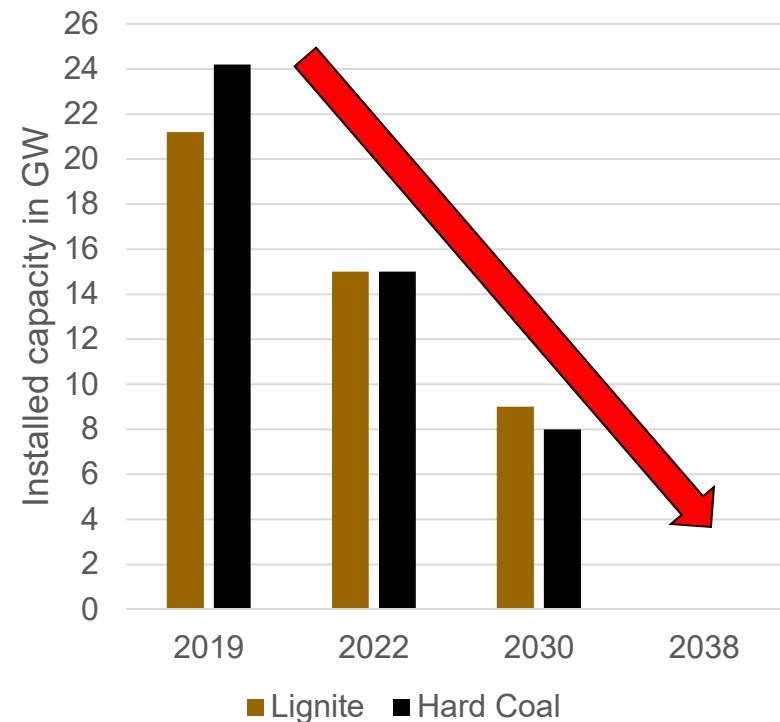
- Efficient fossil-fuel power stations (turbo machines, combustion chambers, heat exchangers)
- Solar thermal power plant technology, solar conversion
- Wind research
- Energy storage (thermal, chemical, electrical)
- High and low temperature fuel cells
- Systems analysis and technology assessment





## Energy Transition in Germany – Increased volatile power from PV/wind

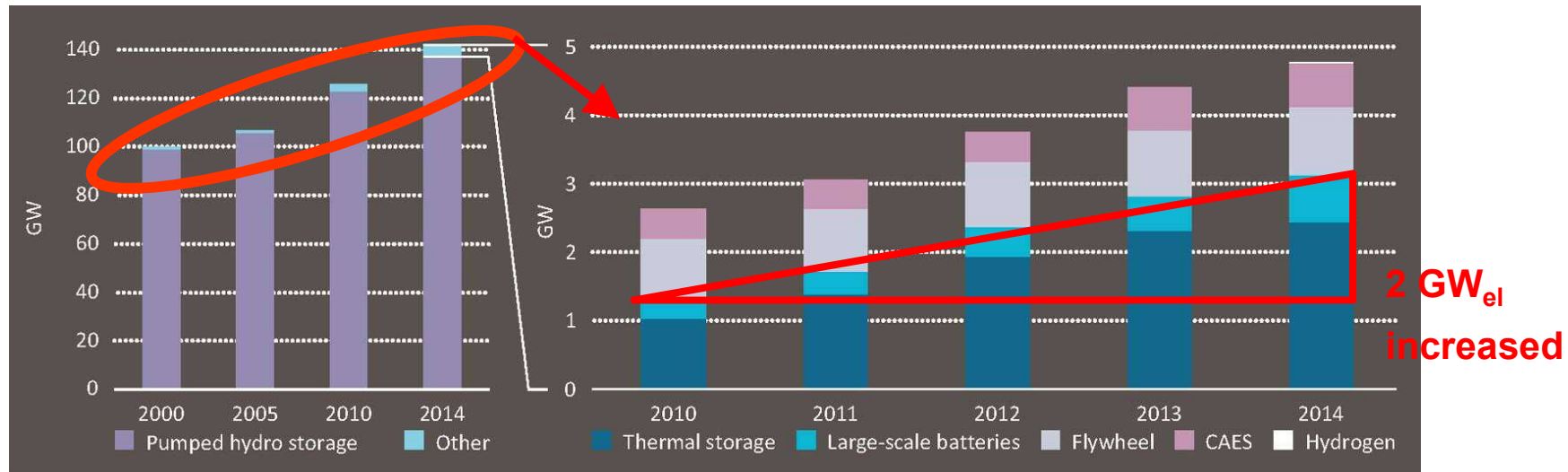
- Currently ~45 GW installed coal power plants in Germany to be shut down stepwise until 2038
- After 2038 no coal power plants in operation anymore
- Additional aspects:
  - The last 9.5 GW of nuclear power plants also to be shut down until 2022
  - **Significant increase of volatile power from PV/wind**
  - **Large-scale energy storage required to stabilize the grid**



Source: Final report of the „Commission on Growth, Structural Change and Employment” 2019



# Installed Global Capacity for Grid-Connected Storage



Sources:

<https://www.iea.org/newsroomandevents/graphics/2015-06-30-installed-global-capacity-for-grid-connected-storage.html>  
[http://www.ren21.net/wp-content/uploads/2018/06/17-8652\\_GSR2018\\_FullReport\\_web\\_final\\_.pdf](http://www.ren21.net/wp-content/uploads/2018/06/17-8652_GSR2018_FullReport_web_final_.pdf)

Grid-connected electrical storage power in 2014:

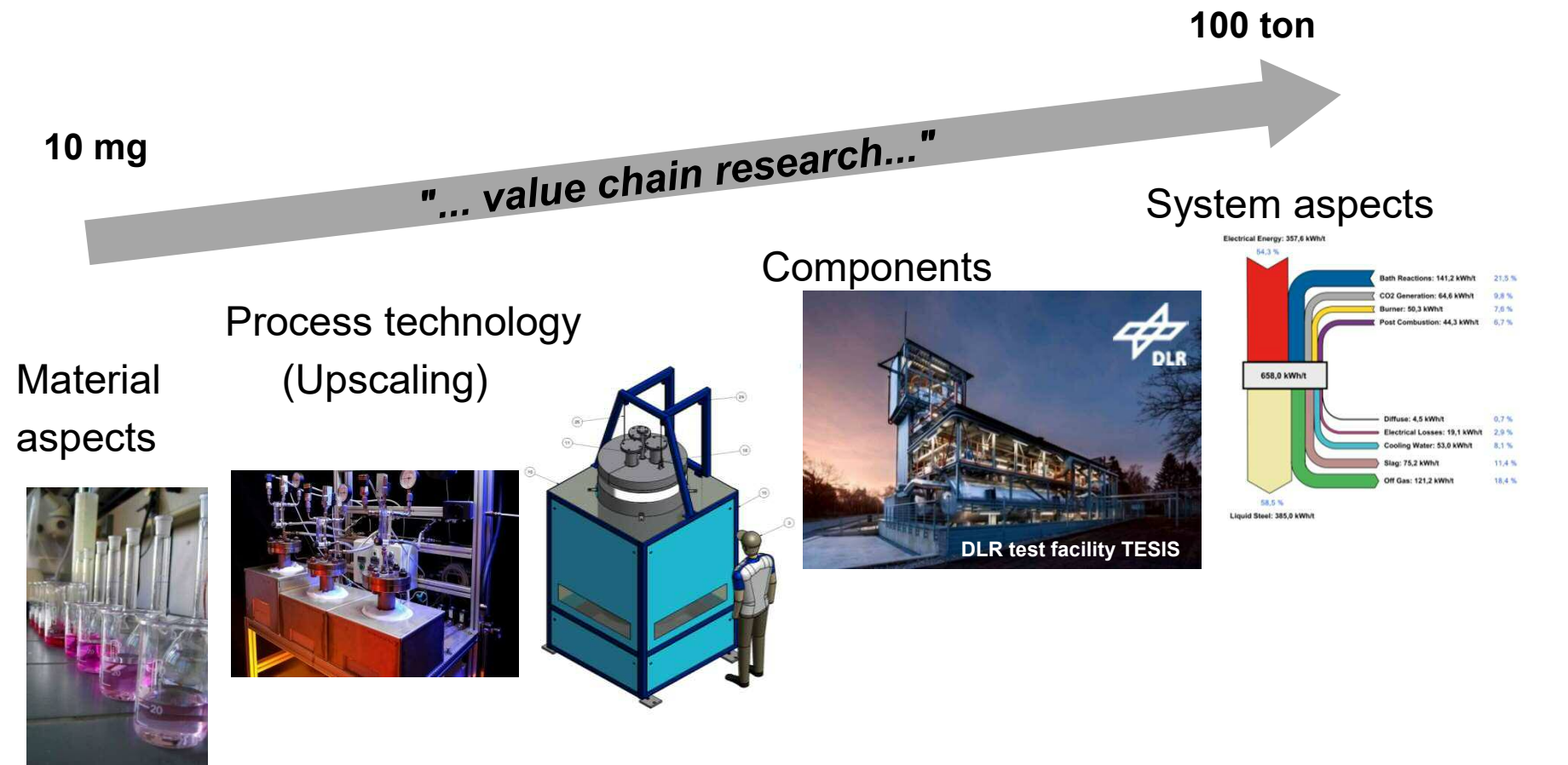
- Pumped hydro ~130 GW<sub>el</sub>
- **Thermal energy storage (TES) ~2.3 GW<sub>el</sub>**
- **Batteries ~0.6 Gw<sub>el</sub>**

**Concentrating Solar Power (CSP) grid-connected molten salt storage in 2015**

- power > 1.5 GW<sub>el</sub>
- capacity > 30 GWh<sub>th</sub> (typically 8 h storage)



# Research Group for TES in MOLTEN SALTS



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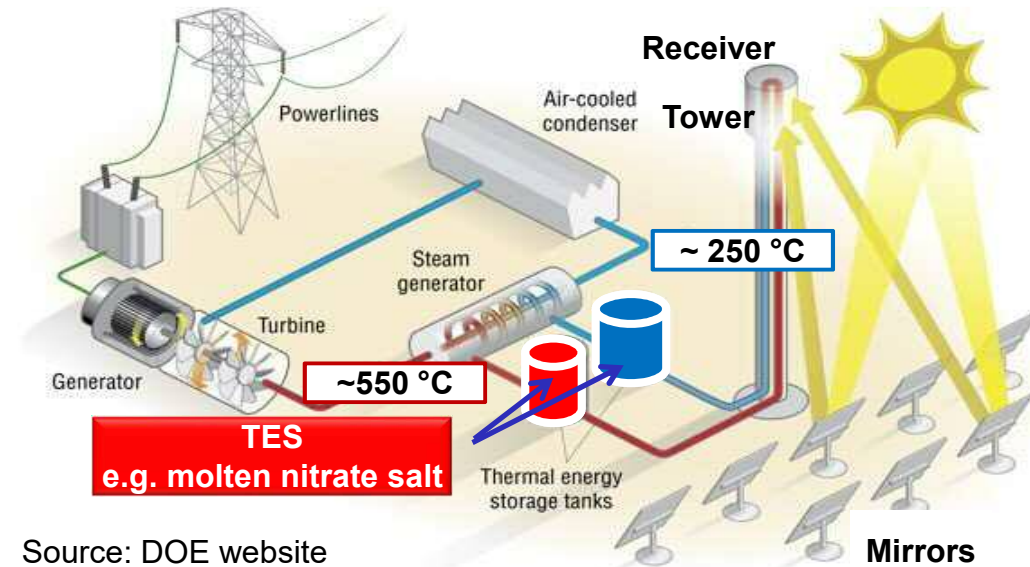




# Molten Salts for Thermal Energy Storage (TES)

- Large-scale hourly storage for **CSP plants** (13 GWh<sub>el</sub>) demonstrated
- **Inexpensive** heat storage capacity from 170 to 560 ° C in molten salts (**nitrate/nitrite**, non-toxic, non-flammable) in large-scale **unpressurized** tanks
- Potential to transfer technology from CSP to **grid-connected storage** → **Carnot battery\***
- **Limitation:** Thermal decomposition of nitrate/nitrite at >560°C

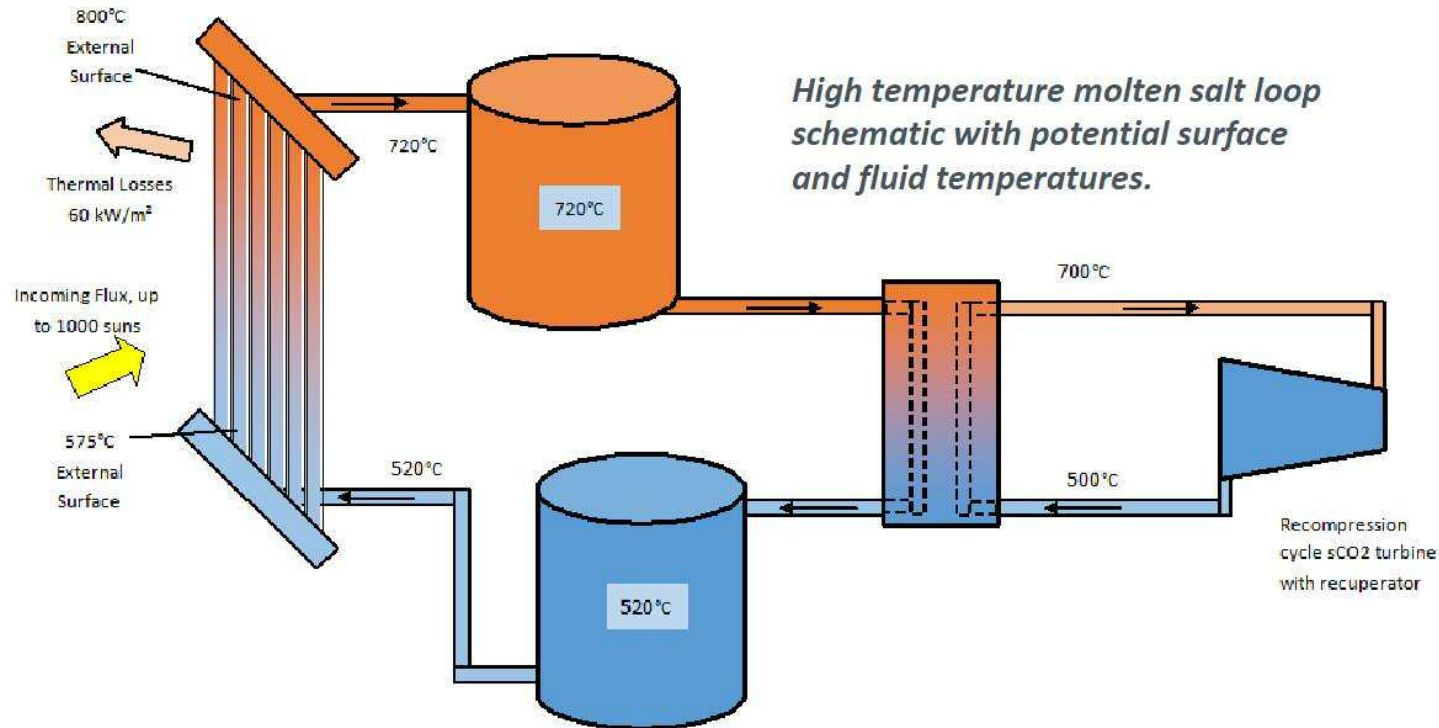
\*<https://www.solarpaces.org/make-carnot-batteries-with-molten-salt-thermal-energy-storage-from-ex-coal-plants/>



Source: DOE website



## Next Generation CSP with Advanced-salt System



### Advanced-salt system + sCO<sub>2</sub> power cycle for higher energy conversion and lower LCOE\*

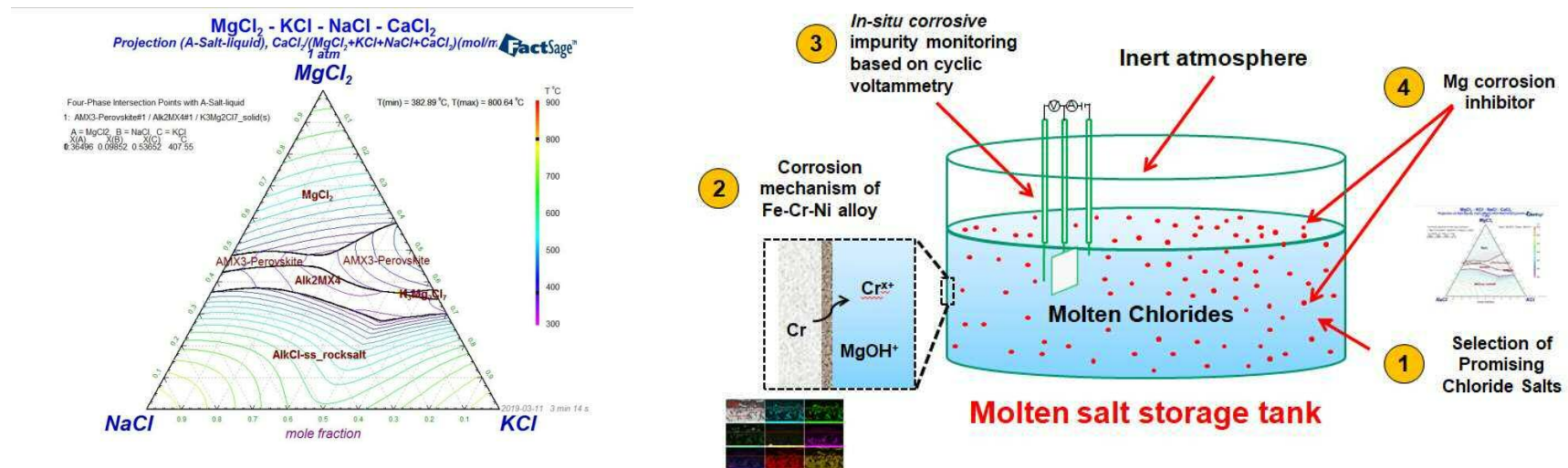
- Advanced-salt system (520-720°C)
- sCO<sub>2</sub> power cycle (500-700°C, efficiency > 50%)

\*M. Mehos et al., Technical Report: NREL/TP-5500-67464, NREL, Golden, CO, 2017.



## Example: Selection of Promising Chloride Salts for TES

- Considering thermal and physical properties ( $C_p$ , vapor pressure, melting point), hygroscopicity (corrosiveness) and prices, **MgCl<sub>2</sub>-KCl-NaCl eutectic salt mixture** (<0.35 USD/kg, **thermal stability >800°C**,  $T_m = 385^\circ\text{C}$ ) is selected [1].
- Other research: Corrosion control of structural materials in molten chlorides [2].



FactSage simulation



- 1) W. Ding, et al., *AIP Conference Proceedings*, 2019, 2126: 200014
- 2) W. Ding, et al., *Frontiers of Chemical Science and Engineering*, 2018, 12(3): 564–576





# Contents

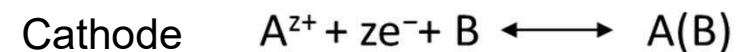
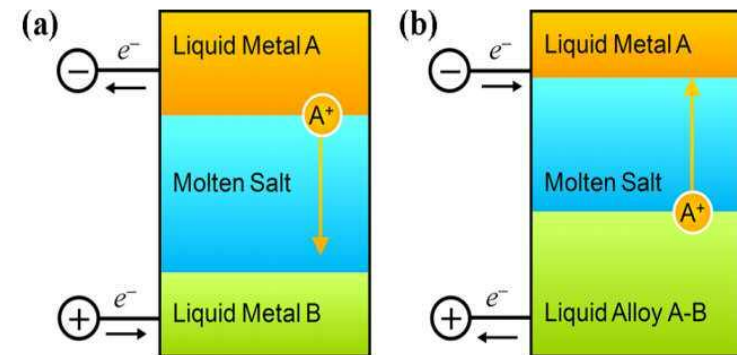
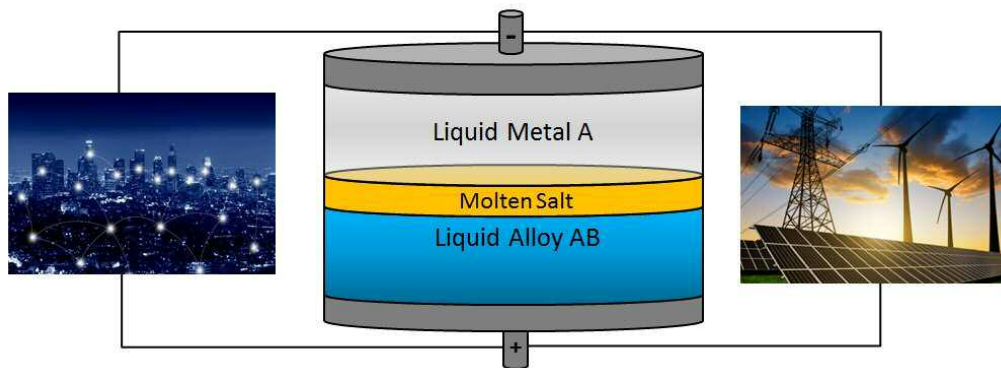
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# Liquid Metal Battery (LMB) for Grid-scale Storage

- **LMBs:**
  - Long life > 10 000 cycles, easy to scale-up → all liquid/liquid interfaces
  - Low storage costs → materials of electrodes and electrolytes
- **Liquid metal electrodes**
  - Low cost metals, high electric conductivity, simple structure of electrodes
- **Molten salt electrolytes**
  - Cheap, high ionic conductivity, low self-discharge, ...



H. Kim, K. Wang, K. Jiang, D. Sadoway, et al., *Chem. Rev.* 113, 2075 (2013).



# State of the Art LMBs

- Li-based LMB with excellent performance in labor-scale achieved
- Na-based LMB with excellent performance in labor-scale still not achieved
  - Low-melting-point  $T_m$  molten salt electrolyte is the key challenge

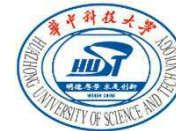
LMBs	Electrode	Electrolyte	$T_m$ [°C]	$T_w$ [°C]	Coulombic efficiency [%]	Energy efficiency [%]	self-discharge rate [mA/cm <sup>2</sup> at full charge]	Capacity loss rate [%/cycle]
<b>Li-LMB (MIT) [1]</b>	Anode: Li; Cathode: Sb-Sn	LiF-LiCl-LiBr	440	500	>98%	70-90	<1	0.006
<b>Na-LMB (ANL) [2]</b>	Anode: Na Cathode: Bi	NaF-NaCl-NaI (single-cation)	530	580	82	59	~20	NA

- 1) K. Wang, K. Jiang, B. Chung, et al., **Nature**, 2014, 514(7522): 348-350.  
 2) H. Kim, K. Wang, K. Jiang, D. Sadoway, et al., **Chem. Rev.** 113, 2075 (2013).

# R&D of Low-temperature Na-based LMB

- **Sino-German project funded by DFG-NSFC:**

- Prof. K. Wang, Dr. H. Li, Huazhong University of Science and Technology (HUST), China
- Dr. A. Weisenburger, Dr. A. Jianu, Karlsruhe Institute of Technology (KIT), Germany



- **Na-based liquid metal batteries with  $T_w < 450^\circ\text{C}$  :**

- Liquid metal electrodes (Na//SbSn and Na//BiSb)
- Na<sup>+</sup>-containing molten salt electrolyte with  $T_m < 400^\circ\text{C}$  and low solubility of Na metal for low self-discharge
- Excellent performance as Li-LMB but lower costs and lower  $T_w$

- **Molten halide salts are promising electrolytes**

- High electrochemical stability ( $>2.5\text{ V}$ )
- High thermal stability ( $>500^\circ\text{C}$ )
- High conductivity
- Low costs
- **But much higher  $T_m$  than electrodes**



# Selection Process of Molten Salt Electrolyte

1. Screening of salt mixtures via phase diagram simulation ( $T_m$ )

2. Experimental measurements of melting temperatures  $T_m$

3. Determination of key molten salt properties as electrolyte

4. Cost pre-analysis of materials

5. Battery pre-tests with selected molten salt electrolytes

Q. Gong, W. Ding, K. Wang, A. Weisenburger, et al. **Molten iodide salt electrolyte for low-temperature low-cost sodium-based liquid metal battery**, *J. Power Sources*, accepted.

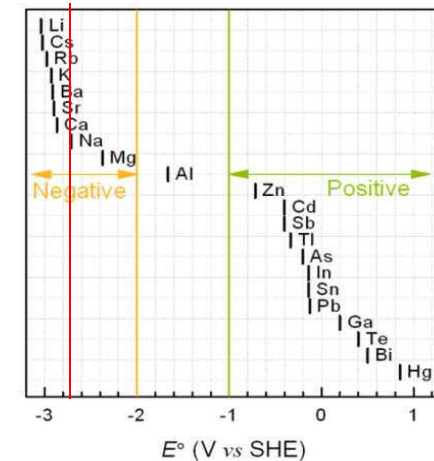




# 1 Screening of Halide Salt Mixtures Regarding $T_m$

- Salt mixture containing:
  - Cation:  $\text{Li}^+$ ,  $\text{K}^+$ ,  $\text{Ba}^{2+}$ ,  $\text{Ca}^{2+}$ ,  $\text{Na}^+$
  - Anion (halide):  $\text{F}^-$  (not selected due to high  $T_m$ ),  $\text{Cl}^-$ ,  $\text{Br}^-$ ,  $\text{I}^-$
- Screening *via* thermodynamic modelling (FactSage) and literature review
- Potential electrolyte salts:
  - $\text{Li}^+$ -containing: Na-Li-K//Cl-Br-I (e.g. Na-Li-K//I:  $T_m = 290^\circ\text{C}$ , Na-Li-K//Cl:  $T_m = 350^\circ\text{C}$ )
  - Not  $\text{Li}^+$ -containing: Na-K-Ba-Ca//Cl-Br-I (e.g. Na-K-Ba-Ca//Cl:  $T_m = 435^\circ\text{C}$ )
- Na-Li-K//I (starting salt system) due to lowest  $T_m$**

Salt system	Example	lowest $T_m$ / $^\circ\text{C}$	mol.%	$T(\text{Na } 30\%)$ / $^\circ\text{C}$	mol.%	$T(\text{Na } 40\%)$ / $^\circ\text{C}$	mol.%	$T(\text{Na } 50\%)$ / $^\circ\text{C}$	mol.%
Binary	Na//Cl, I	573	40.1-59.9						
	Na//Cl, Br	740	25.3-74.7						
	Na//Br, I	645	30.8-69.2						
	Na, Li//Cl	554	27.3-72.7	560	30-70	590	40-60	620	50-50
	Na, Li//Br	509	25.8-74.2	525	30-70	550	40-60	575	50-50
	Na, Li//I	450	20.8-79.2	460	30-70	480	40-60	510	50-50
Ternary	Na, Li//Cl, I	421	43.8(Na/(Na+Li))-53.1					435	50-55
	Na, Li//Cl, Br	417	31.3(Na/(Na+Li))-43.9	425	30-42	465	40-45	530	50-45
		425	32.4(Na/(Na+Li))-42.7						
	Na, Li//Br, I	352	32.5(Na/(Na+Li))-48.9	355	30-50	400	40-40	440	50-30
		351	31.5-48.0						
	Na//Cl, Br, I	573	61.2-0.0-38.8						
	Na, Li, K//Cl			450	30-30-40	525	40-20-40	580	50.0-50.0-0.0
	Na, Li, K//Br			490	30-50-20	540	40-60-0	580	50.0-50.0-0.0
Quaternary	Na, Li, K//I			410	30-40-30	460	40-30-30	505	50.0-16.0-34.0
	Na, K, Ba, Ca//Cl	435	34-7-17-42						



H. Kim, et al., Chem. Rev. 113, 2075 (2013).



# 1 Screening of Halide Salt Mixtures Regarding $T_m$

- **Eutectic Na-Li-K/I:**

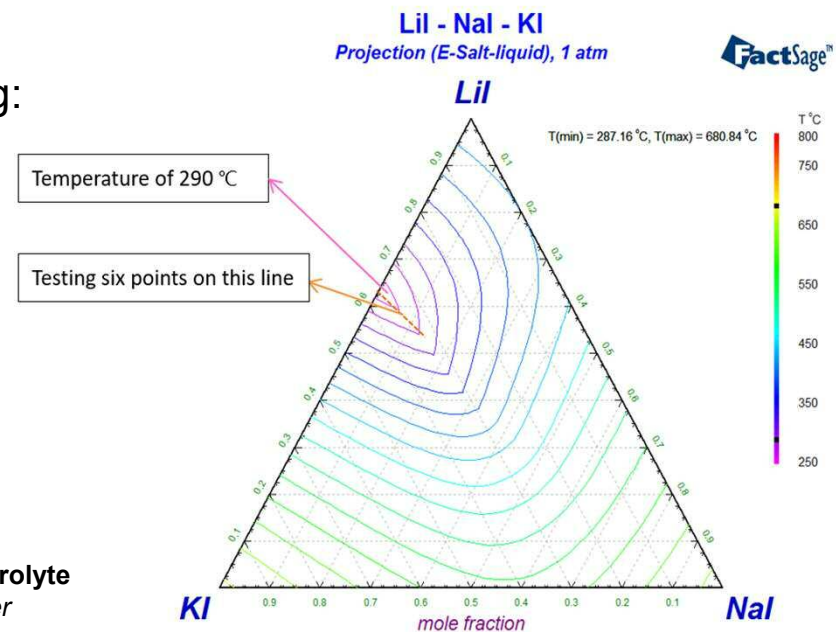
- **Pseudo-binary salt** with  $T_m = \sim 290^\circ\text{C}$
- Eutectic Li-K/I: 63-37 mol%
- Solubility of NaI in the eutectic LiI-KI is  $\sim 12\text{ mol}\%$

- **Na-K-Li/I is promising:**

- Melting temperature  $T_m < 300^\circ\text{C}$
- **But which  $\text{Na}^+$  concentration** regarding:
  - Low Na metal solubility
  - Sufficient  $\text{Na}^+$  conductivity

- Six eutectic salt compositions are selected for further investigation:
  - NaI: 0, 3, 5, 7, 9, 12 mol%

Q. Gong, W. Ding, K. Wang, A. Weisenburger, et al. **Molten iodide salt electrolyte for low-temperature low-cost sodium-based liquid metal battery**, *J. Power Sources*, accepted.



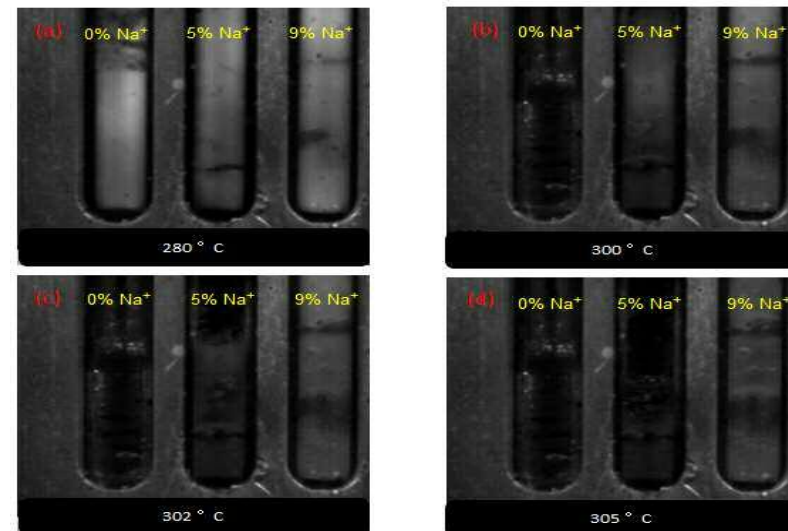
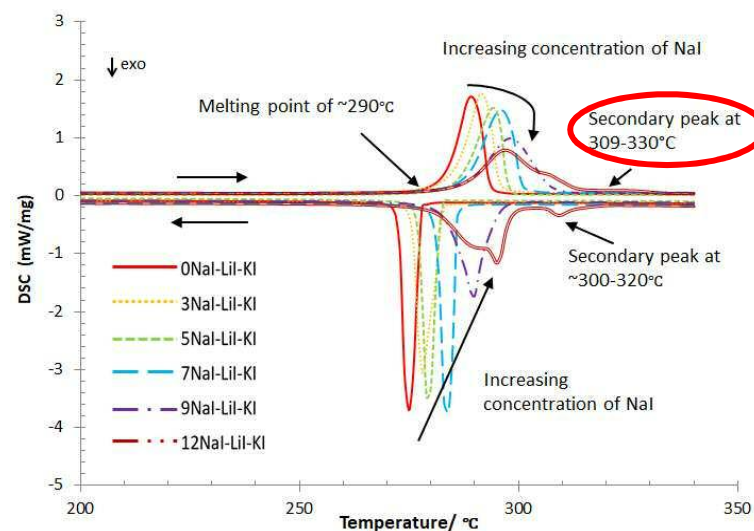
## 2 Experimental measurements of $T_m$

- **Methods:**

- Thermal: Differential scanning calorimetry (DSC)
- Optical: Melting point measurement apparatus (OptiMelt™)

- **Na-K-Li/I:**

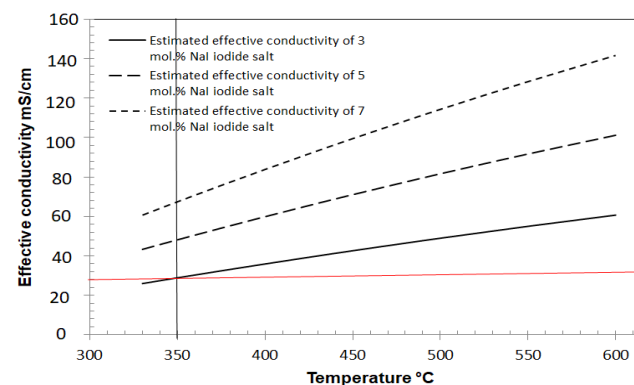
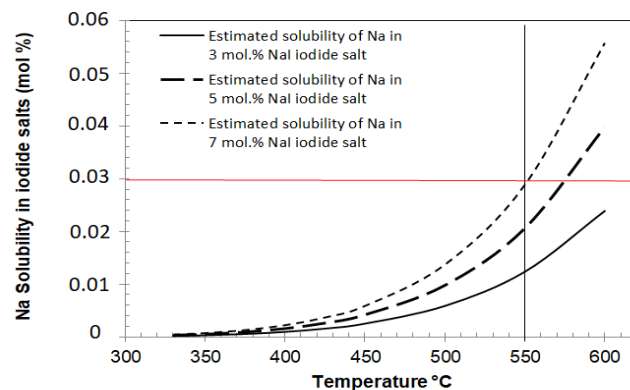
- Solubility of NaI in the eutectic LiI-KI (64-36 mol%) is 7-9 mol%
- 12 mol% NaI: not eutectic, secondary peaks besides main peaks at  $\sim 309-330^\circ\text{C}$



Q. Gong, W. Ding, K. Wang, A. Weisenburger, et al. **Molten iodide salt electrolyte for low-temperature low-cost sodium-based liquid metal battery**, *J. Power Sources*, accepted.

### 3 Determination of Molten Salt Properties as Electrolyte

- **Estimation of Na solubility** in NaI-LiI-KI based on literature data [1]:
  - Dissolution reaction  $Na + Na^+ \rightarrow Na_2^+$
  - < 0.03 mol% at < 550 °C (estimated self-discharge < 1 mA/cm<sup>2</sup>)
  - Underestimated due to dissolution reactions with other cations (i.e., Li<sup>+</sup>, K<sup>+</sup>)
  - Experiments in progress
- **Estimation of Na<sup>+</sup> conductivity** based on [2]:
  - 28 mS/cm for T>350°C for 3-7 mol% NaI
  - Higher than that of electrolyte in conventional Li-ion battery (~10 mS/cm)



- 1) M. Bredig and H. Bronstein, *The Journal of Physical Chemistry*, 64 (1960) 64-67.
- 2) Molten salts: Volume 1. Electrical conductance, density, and viscosity data, 1968.





## 4 Cost Pre-analysis of Materials

- **Salt costs:**
  - NaI-LiI-KI > NaCl-LiCl-KCl > NaF-NaCl-NaI
  - Small effect on battery costs due to thin molten salt electrolyte
- **Salt corrosivity against structural materials:**
  - Not a critical issue due to inert atmosphere of LMB and inhibition effect of Na
  - Conventional stainless steels allowed (KIT: Selection of structural materials)

Salts	Large-scale prices / USD/kg	Sources
NaI	~3	Current price (CP)*
KI	~4	CP
LiI	~40	CP
NaI-LiI-KI eutectic	~20	Calculated with CPs of single salts
NaCl-LiCl-KCl eutectic	~3	Calculated with CPs of single salts
NaF-NaCl-NaI eutectic	~2	Calculated with CPs of single salts

\*CP: current large-scale price of the single salt from [www.alibaba.com](http://www.alibaba.com) [Accessed on May 9th of 2020].

Q. Gong, W. Ding, K. Wang, A. Weisenburger, et al. **Molten iodide salt electrolyte for low-temperature low-cost sodium-based liquid metal battery**, *J. Power Sources*, accepted.



## 5 Battery Pre-tests with Selected Molten Salt Electrolytes

- **Test conditions:**

- ~1 cm thick NaCl(9 mol%)-LiCl-KCl (similar as NaI-LiI-KI) electrolyte,
- $T_w = 450^\circ\text{C}$ , 100 discharge/charge cycles, current up to  $1000 \text{ mA/cm}^2$

- **Results:**

- Higher Coulombic efficiency >95%
- $T_w$  reduced by  $>100^\circ\text{C}$  → low costs for structural and isolation materials
- But unacceptable capacity loss rate → to be improved by battery optimization

LMBs	Electrode	Electrolyte	$T_m$ [ $^\circ\text{C}$ ]	$T_w$ [ $^\circ\text{C}$ ]	Coulombic efficiency [%]	self-discharge rate [ $\text{mA/cm}^2$ at full charge]	Capacity loss rate [%/cycle]
<b>Na-LMB (HUST, KIT, DLR)</b>	Anode: Li; Cathode: Bi-based alloy	NaCl-LiCl-KCl	350	450	>95%	To be measured	0.1
<b>Na-LMB (ANL)</b>	Anode: Na Cathode: Bi	NaF-NaCl-NaI (single-cation)	530	580	82	~20	NA

Q. Gong, W. Ding, K. Wang, A. Weisenburger, et al. **Molten iodide salt electrolyte for low-temperature low-cost sodium-based liquid metal battery**, *J. Power Sources*, accepted.



## Summary and Outlook

- Next generation TES technology based on molten chloride salts is being developed
  - MgCl<sub>2</sub>-NaCl-KCl is selected
  - Focusing on corrosion control of structural materials
- Molten halide salts as electrolyte in LMB:
  - Process for selection of salt mixtures is proposed
  - Li-K-Na halide salt mixtures as promising electrolytes of Na-LMB
  - Battery pre-tests show promising results
  - Other halide salt mixtures will be studied
  - Battery optimization will be performed



# Thank you for your attention!

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## Acknowledgement:





## Locations and employees

Approx. 8700 employees  
with 40 institutes and  
facilities at 20 sites.

Offices in Brussels, Paris,  
Tokyo and Washington.

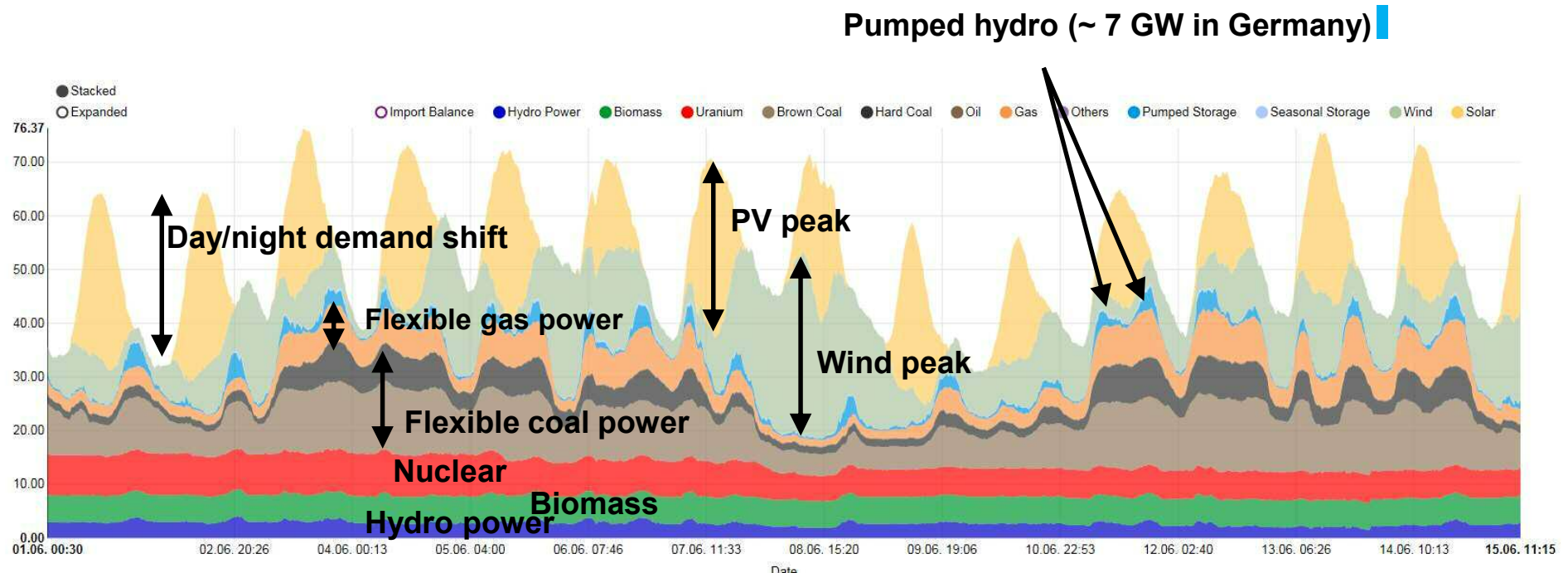
And a research site of  
concentrated solar power  
(CSP) in Almeria/Spain



**Institute of Engineering Thermodynamics**



# Electricity generation in Germany (Example)



In future the situation will be marked by

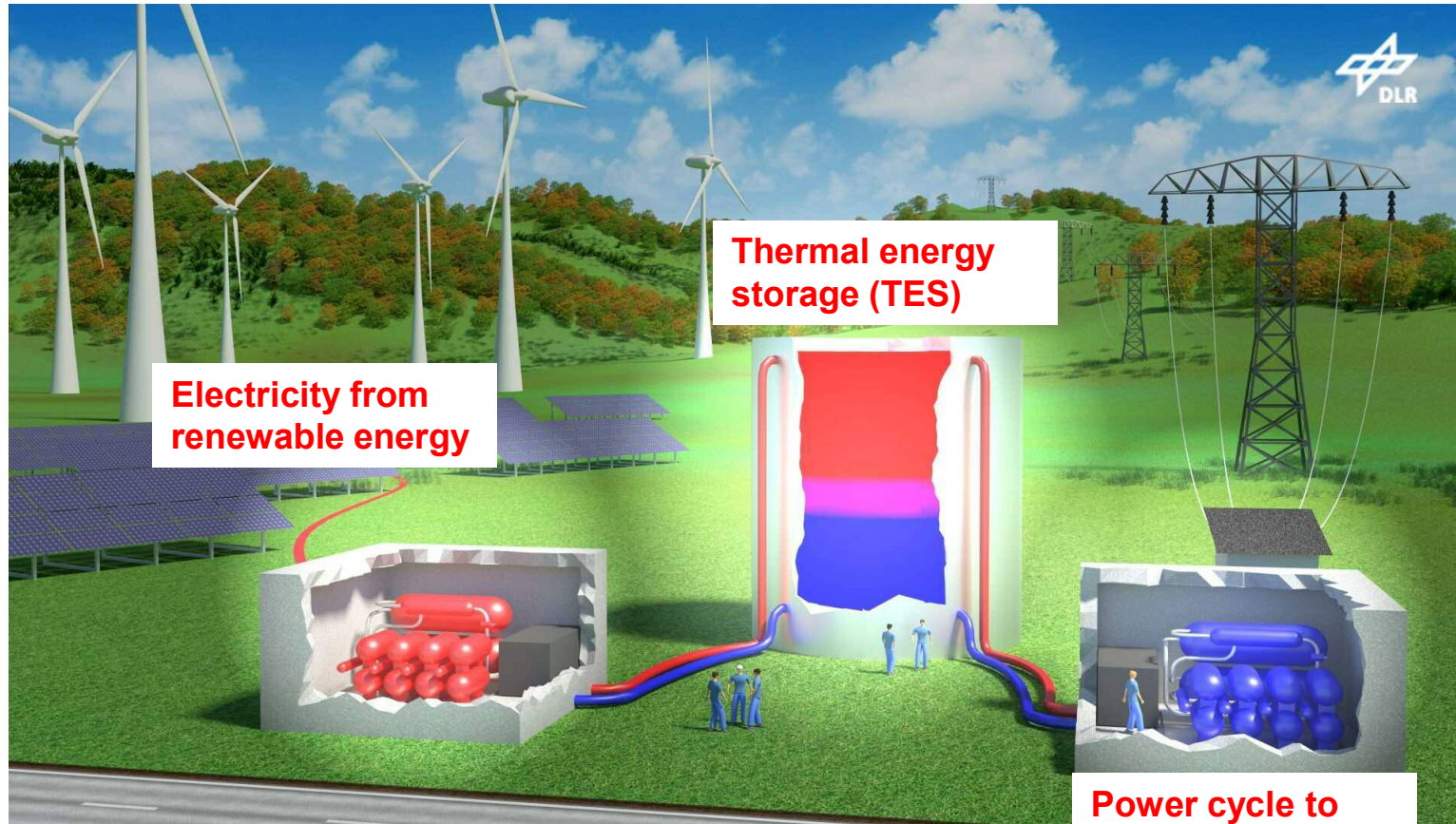
- Large share of volatile PV & wind power with limited operation hours
- Large installed PV & wind power compared to power demand

→ **Flexibility requirement:** Large-scale energy storage, power-to-X, demand side management, hybrid operation,...





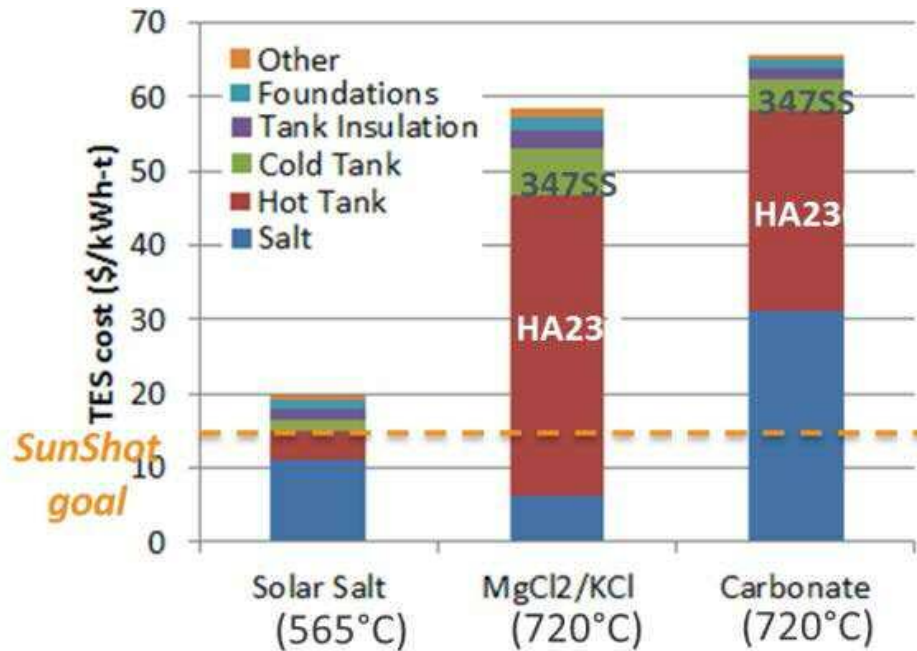
# Carnot Battery



- Electricity- heat (stored) - electricity
- Round-efficiency ~50%
- A conventional coal power plant is being transformed to Carnot battery plant



# Advanced-Salt System – Chlorides or Carbonates



- Chloride/carbonate (>800 °C)
- Salt costs:  
**Chloride** < Nitrate < Carbonate
- Tank costs (corrosion, T):  
Nitrate < Carbonate < **Chloride**

## Estimated costs of various TES systems\*

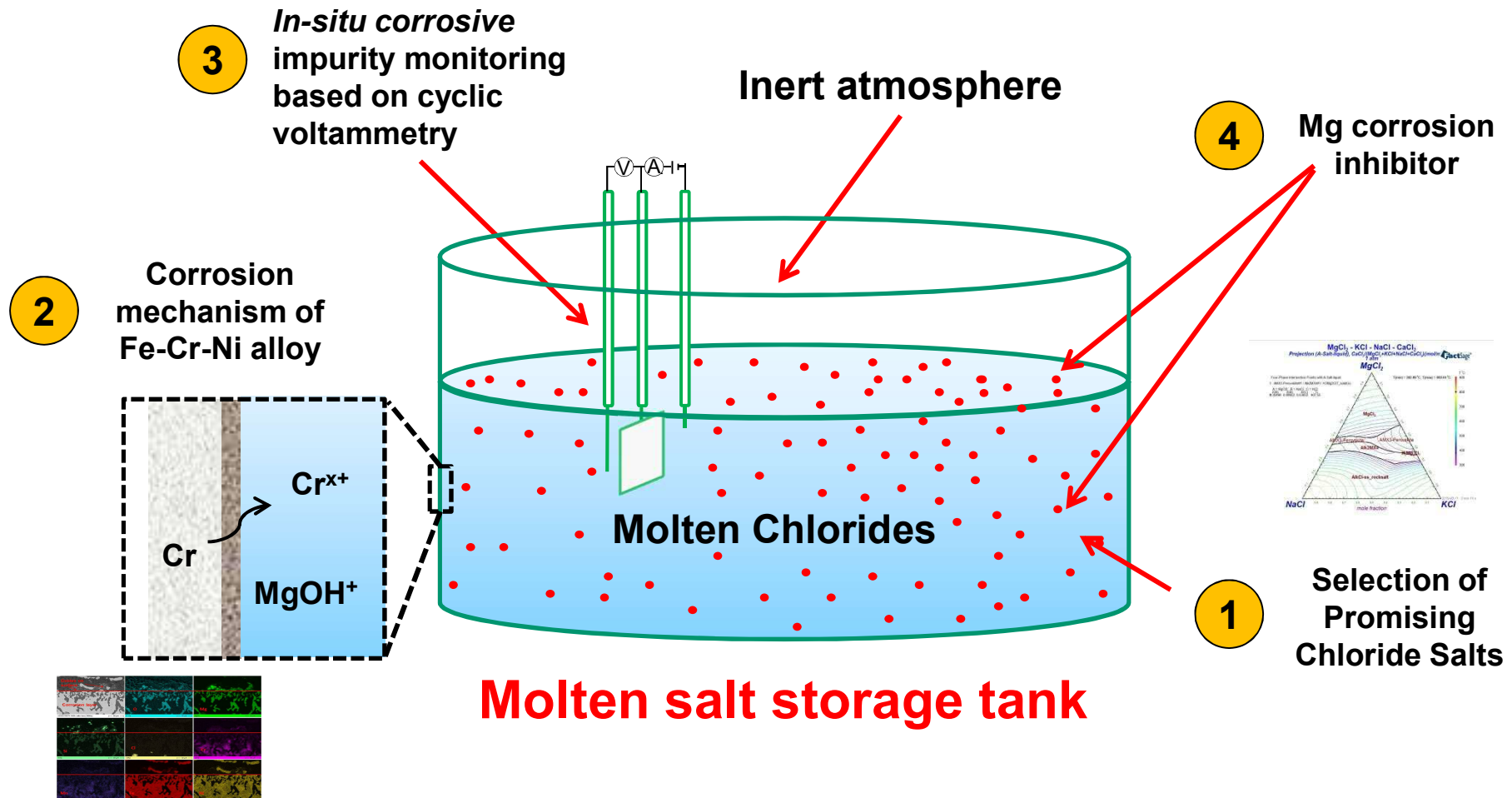
J. Gomez-Vidal, A. Kruizenga, Technology Pathway Molten Salt, Project of CSP Gen 3 Roadmap, 02. 2017  
SunShot Initiative is a federal government program run by DOE.

Reducing corrosiveness of chlorides  
→ Reducing tank (TES) costs by  
using cheaper alloys

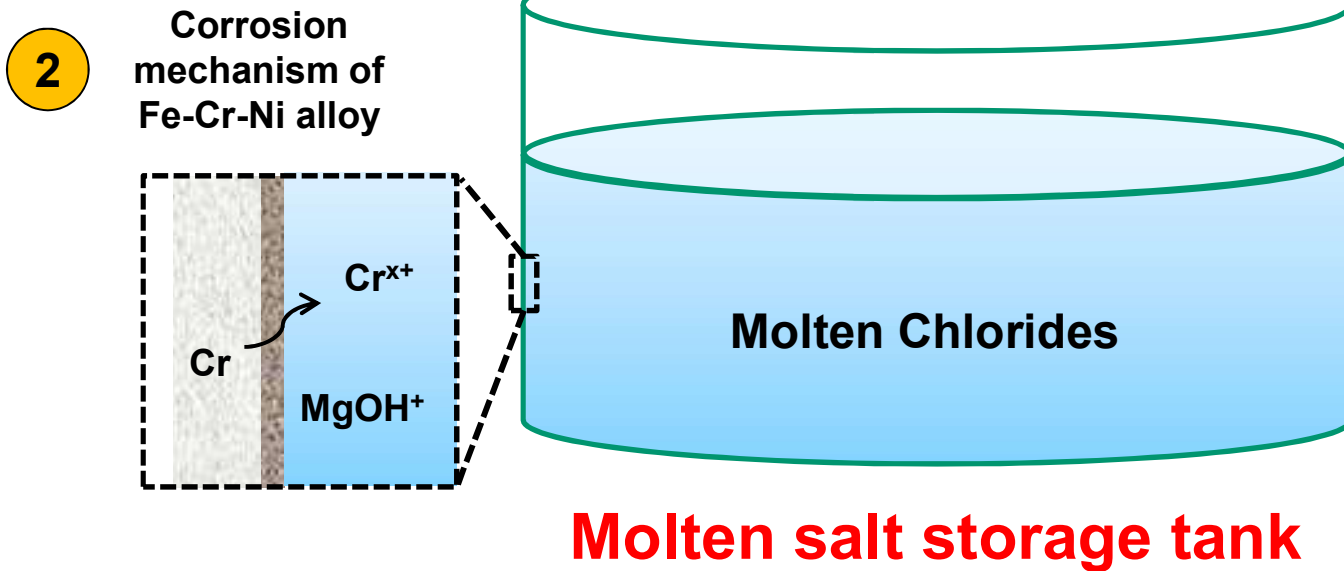




# R&D of Molten Chlorides for Thermal Energy Storage



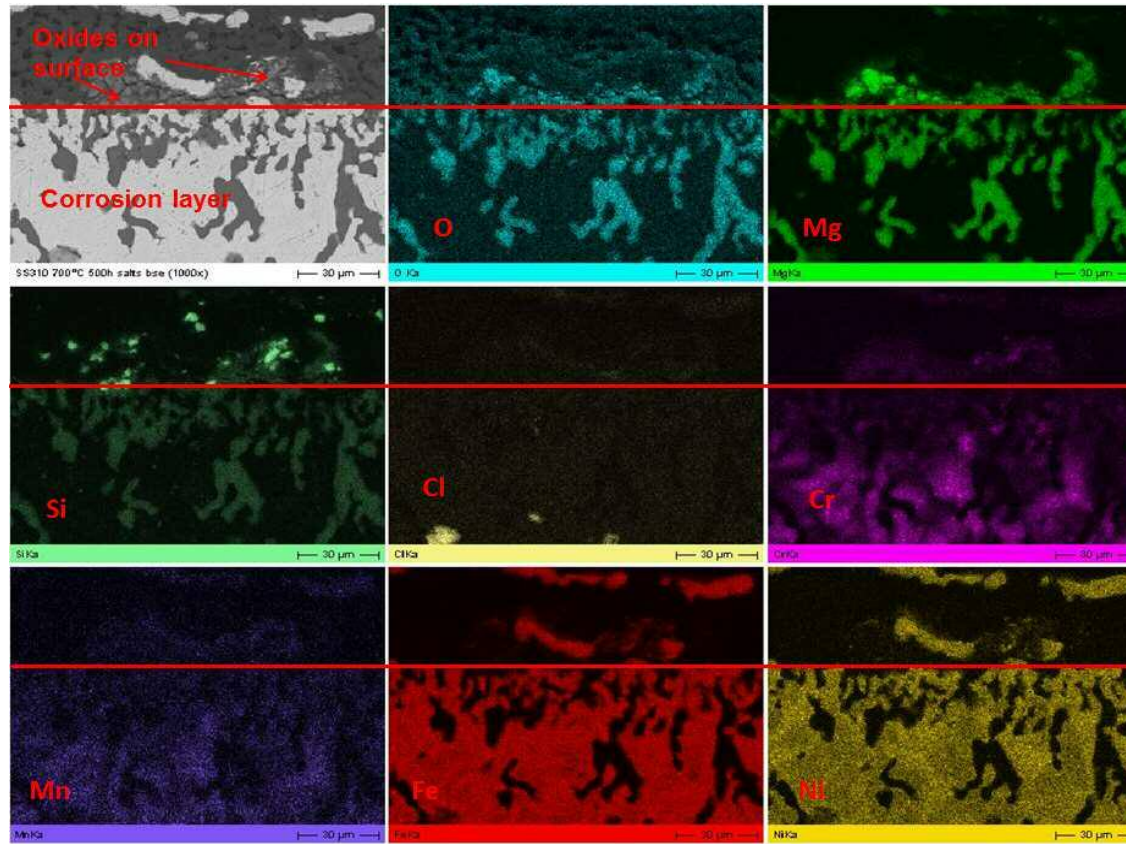
## 2 Corrosion Mechanism of Commercial Fe-Cr-Ni Alloys



\*W. Ding, et al., *Solar Energy Materials & Solar Cells*, 2018, 184: 22–30.



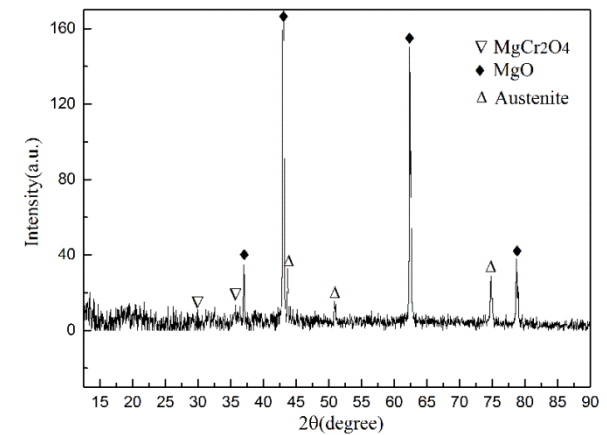
## 2 Proposed Corrosion Mechanisms



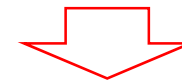
SS 310 in MgNaK chloride (700°C, 500 h)

\*W. Ding, et al., *Solar Energy Materials & Solar Cells*, 2018, 184: 22–30.

XRD for oxides on surface



- Large amount of Mg and O detected in holes in corrosion layer
- $\text{MgCr}_2\text{O}_4$  and MgO detected in oxides on surface

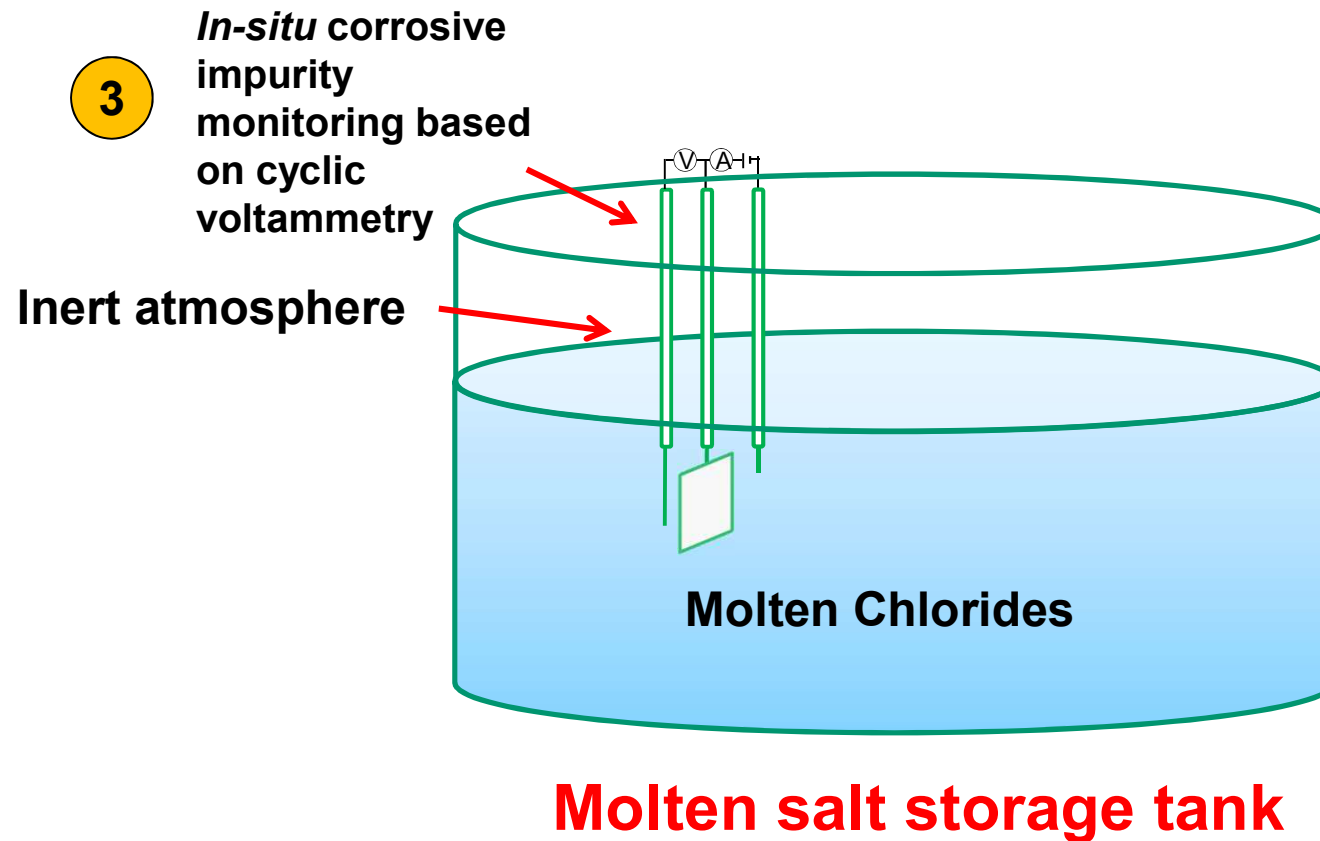


Corrosion mechanisms:

- Cr dissolved preferentially
- Corrosion is driven by impurities like  $\text{MgOHCl}$



### 3 In-situ Monitoring of Corrosive Impurities

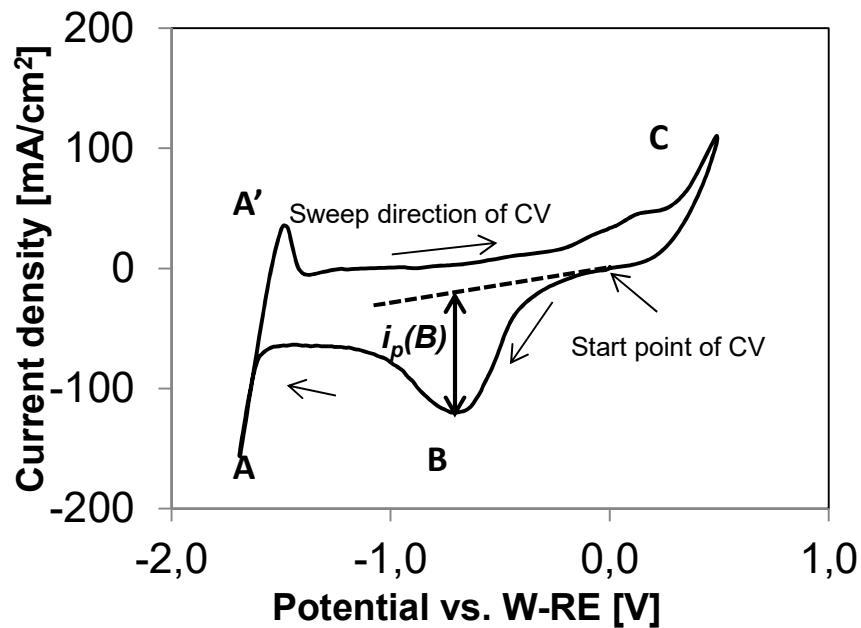


W. Ding, et al., *J. Energy Storage*, 2018, 15: 408–414.



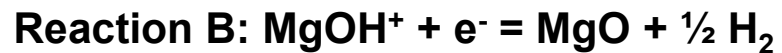


### 3 Cyclic Voltammetry (循环伏安法)



MgCl<sub>2</sub>/KCl/NaCl (60/20/20 mole%) at 500 °C,  
Tungsten as working, counter and reference electrode

Most stable corrosive impurity **MgOH<sup>+</sup>**

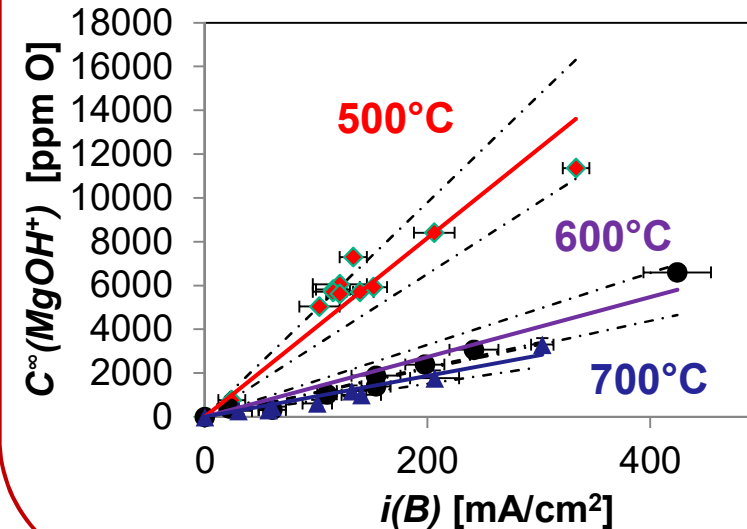


W. Ding, et al., *J. Energy Storage*, 2018, 15: 408–414.

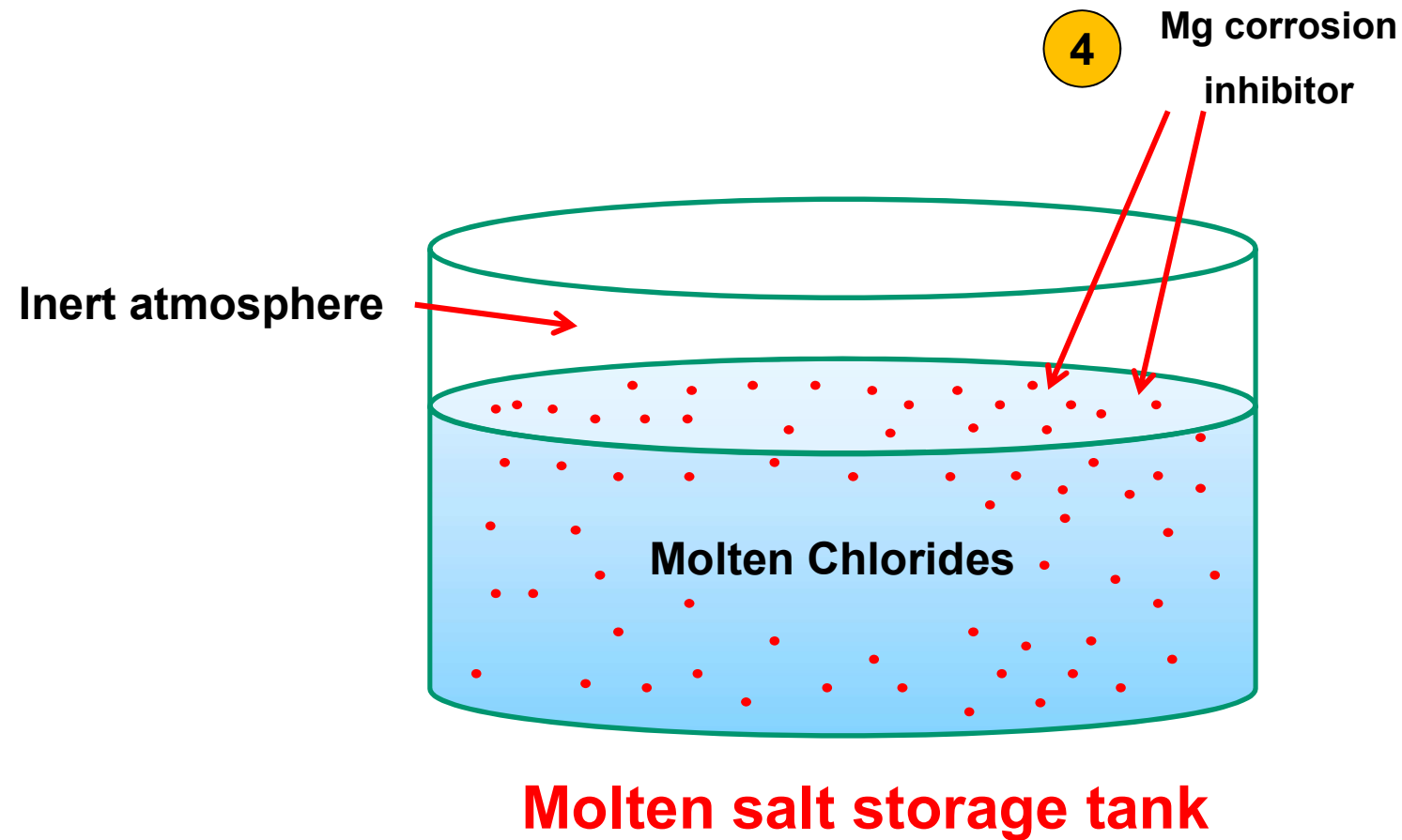


Peak current density of the peak B ( $i_p(B)$ )  
**proportional** to bulk concentration of MgOH<sup>+</sup>  
in molten chloride, i.e.,

$$C^\infty(\text{MgOH}^+) = k(T, v)(B) * i_p(B)$$



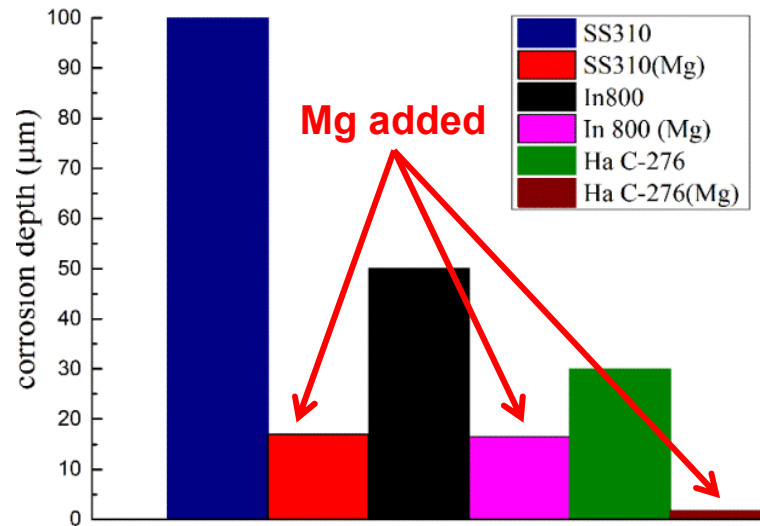
## 4 Mg Corrosion Inhibitor (腐蚀抑制剂)



\*W. Ding, et al, *Solar Energy Materials & Solar Cells*, 2019, 193:298-313.



## 4 Reduced Corrosion Rates by Mg



Measured corrosion depth of alloys after exposure to molten  $\text{MgCl}_2\text{-KCl-NaCl}$  at 700 °C for 500 h without and with Mg addition

\*W. Ding, et al, *Solar Energy Materials & Solar Cells*, 2019, 193:298-313.

Calculated redox potential of  $\text{MgCl}_2\text{-KCl-NaCl}$  (60–20–20 mol%) with Mg addition at 800 °C, and calculated equilibrium molar fractions of  $\text{CrCl}_2$ ,  $\text{FeCl}_2$  and  $\text{NiCl}_2$  in the melt.

	Redox potential $\Delta G_{\text{Cl}_2}$	$\text{Mg}^{2+}$	$\text{MgOH}^+ \text{Cl}^-$	$\text{Cr}^{2+}$	$\text{Fe}^{2+}$	$\text{Ni}^{2+}$
EMF at 800 °C (V)		2.46	1.46	1.35	1.12	0.875
$\Delta G_f^\circ$ at 800 °C (kJ/mol)		– 475	– 141	– 261	– 216	– 170
$C_{\text{eq}}$ (mol%)	without Mg	– 360 kJ/mol (0.1 bar $\text{H}_2$ )	$4 \times 10^{-3}$	$1.5 \times 10^{-5}$	$9.8 \times 10^{-8}$	$5.6 \times 10^{-10}$
		– 298 kJ/mol (0.1 mbar $\text{H}_2$ )	$4 \times 10^{-3}$	$1.5 \times 10^{-2}$	$9.7 \times 10^{-5}$	$5.6 \times 10^{-7}$
	with Mg	– 500 kJ/mol	0.6	$4 \times 10^{-9}$ (0.1 mbar $\text{H}_2$ )	$2.3 \times 10^{-12}$	$1.5 \times 10^{-14}$
					$1.5 \times 10^{-14}$	$8.5 \times 10^{-17}$

- Adding Mg as corrosion inhibitor can significantly reduce the corrosion rate in case of Fe-Cr-Ni based alloys, to ~10% compared with the case without Mg addition.
- Inhibition mechanism: Adding Mg reduces redox potential of molten chloride salts.

