

Technical and Economical Evaluation of

Biomass-to-Liquid	(BtL)
Power-to- Liquid	(PtL)
Power & Biomass-to-Liquid	(PBtL) Processes

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Open Workshop:
Energy System Integration of Bio-Based Fuels

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A large, curved image of the Earth from space occupies the right half of the slide. It shows a portion of the Arctic region with white ice and surrounding green landmasses and blue oceans. The curvature of the planet is clearly visible.

Knowledge for Tomorrow

Outline

1. Introduction and Motivation

2. Technical evaluation

3. Economical evaluation

4. Results

5. Summary & Outlook



1. Brief introduction: DLR – German Aerospace Center

- 8.200 Employees (Feb. 2018)
- 40 institutes at 20 sites (+ offices in Brussels, Paris, Tokyo, Washington)
- Total budget 925 Mio.€ (2016)
- 6 research areas



Aeronautics

Space

Energy

Transport

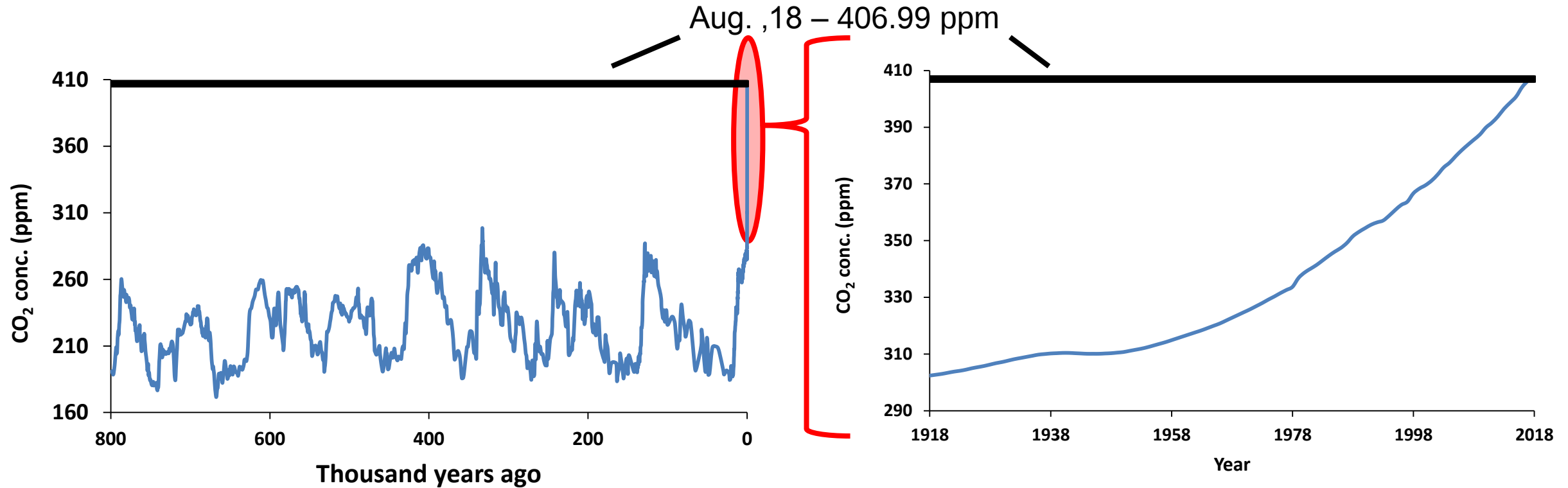
Digitalization

Security

Research Group Alternative Fuels



1. Motivation for alternative fuels – Rising CO₂ levels

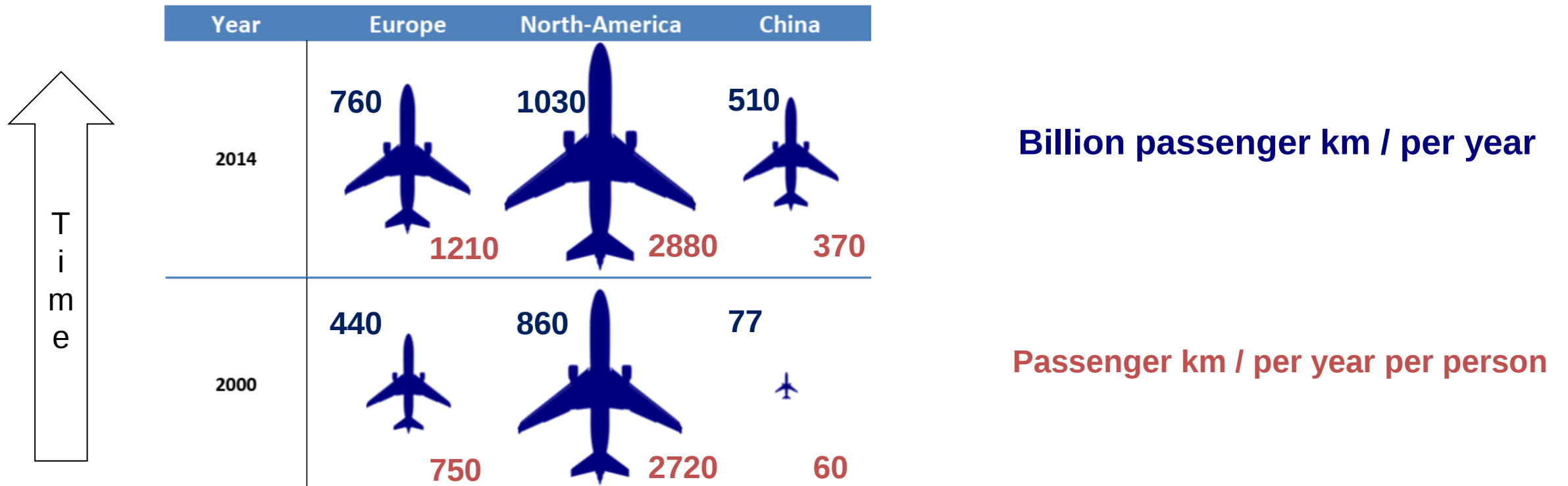


- 1 ppm CO₂ ≈ 8 Gt CO₂
- CO₂ absorbs thermal radiation - rising CO₂ levels → more heat is trapped in atmosphere



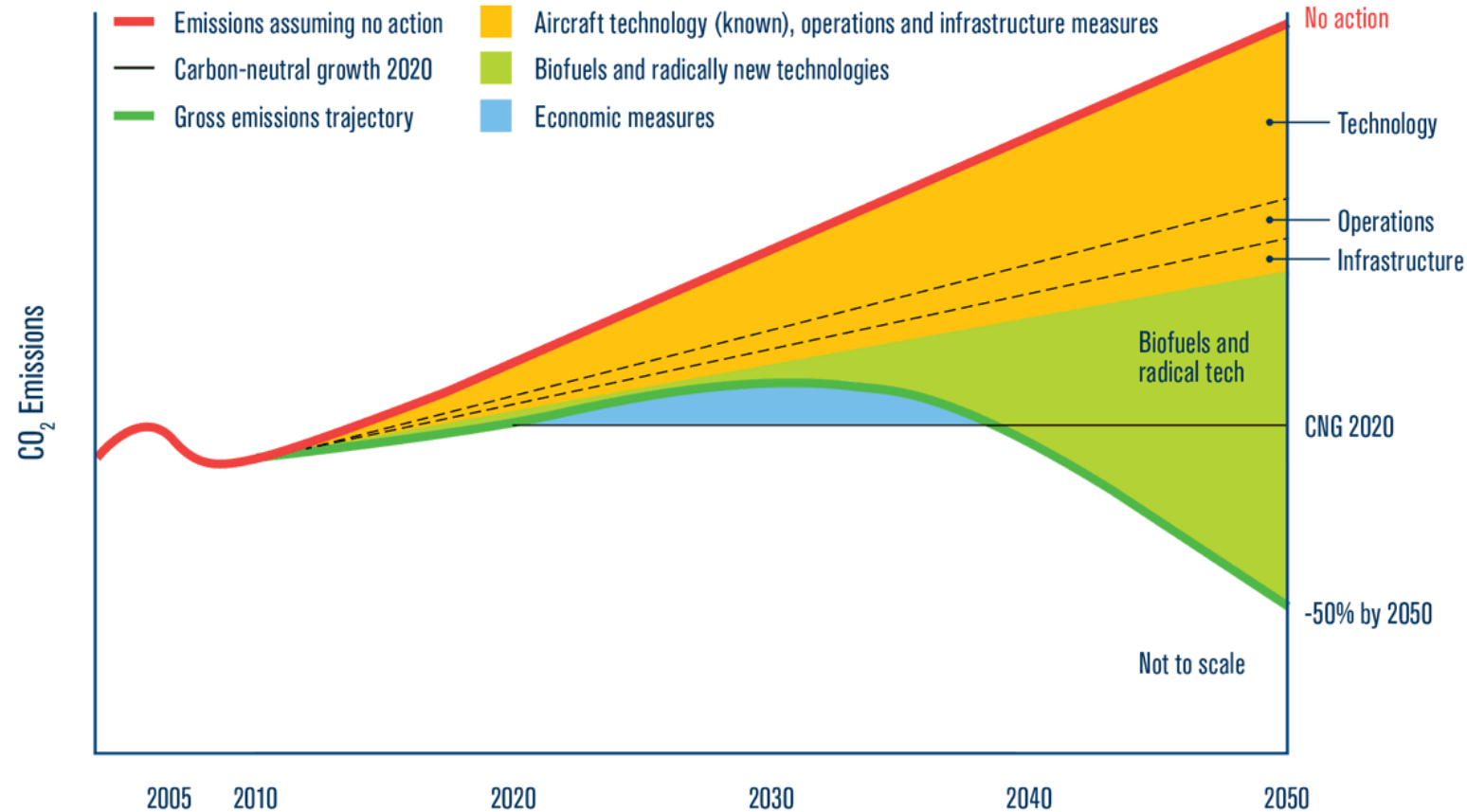
1. Demand for transportation & mobility is rising

- With rising prosperity comes rising demand in mobility and transportation
- Example: Increasing Air traffic



Source: Thess et al., DGLR-Mitgliedermagazin „Luft- und Raumfahrt“ Ausgabe 2/2016, S.20 ff.

1. IATA Technology Roadmap - Reduction of CO₂ emissions in the air traffic sector



- Not every transport sector can be electrified (yet)
- Renewable generated fuels are a solution to decarbonize transport sectors like air traffic

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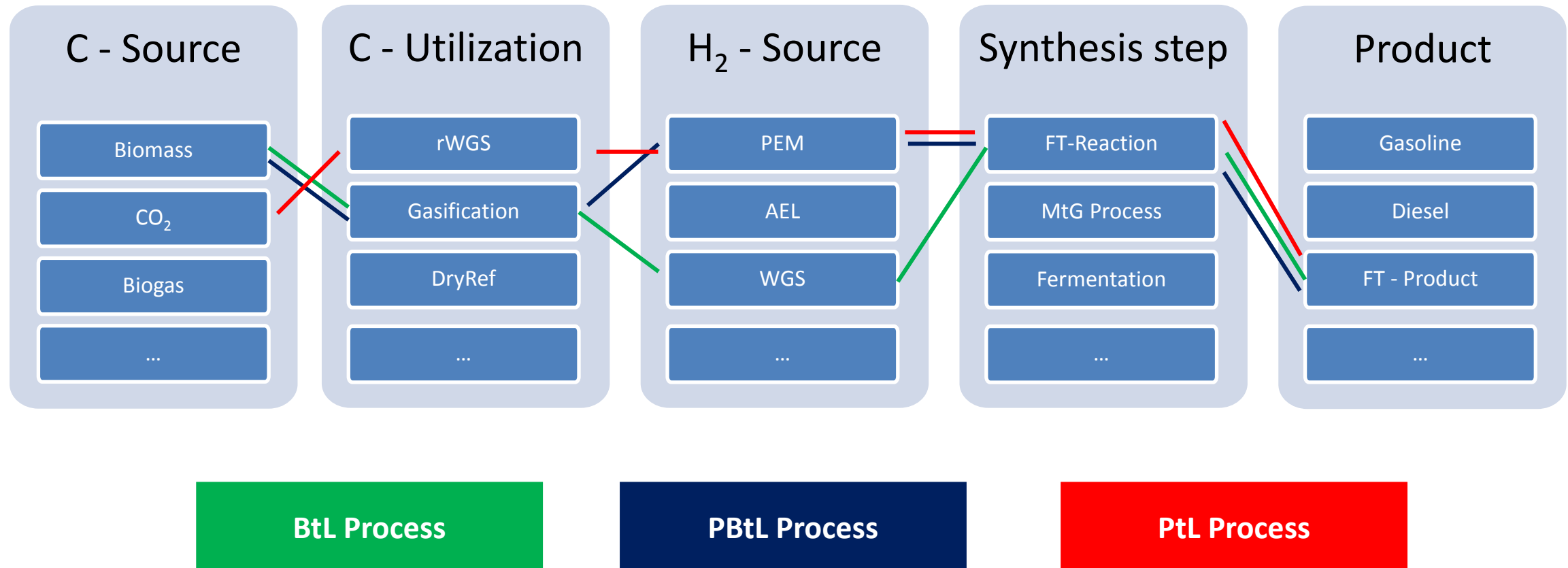
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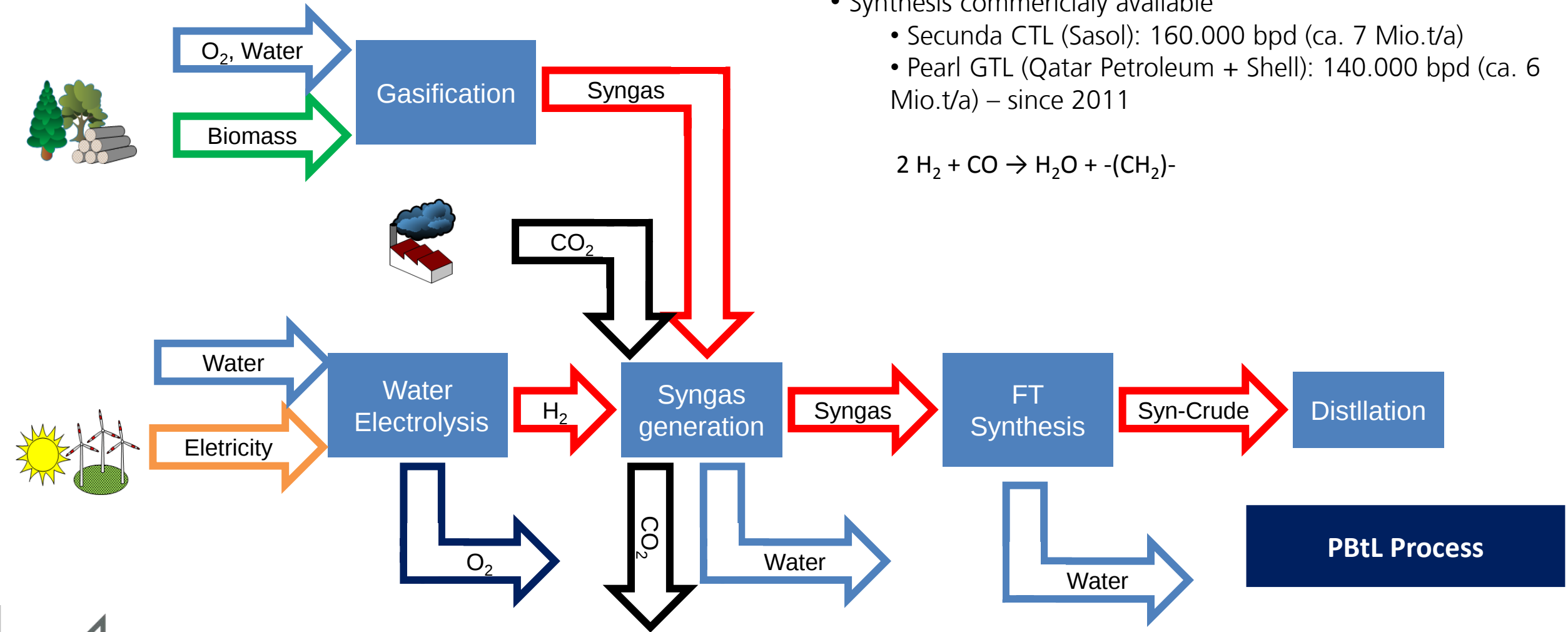


2. Technical evaluation - Production processes

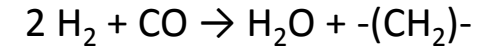
- ASPEN Plus is used for the technical evaluation
- What are the options for alternative fuels



2. The BtL – PBtL – PtL Processes



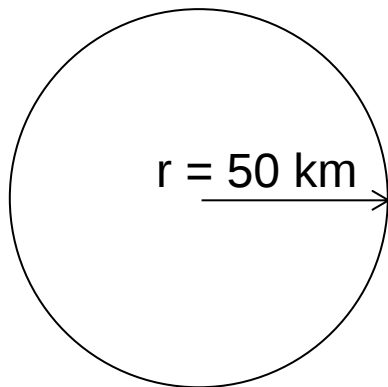
- Synthesis commercially available
 - Secunda CTL (Sasol): 160.000 bpd (ca. 7 Mio.t/a)
 - Pearl GTL (Qatar Petroleum + Shell): 140.000 bpd (ca. 6 Mio.t/a) – since 2011



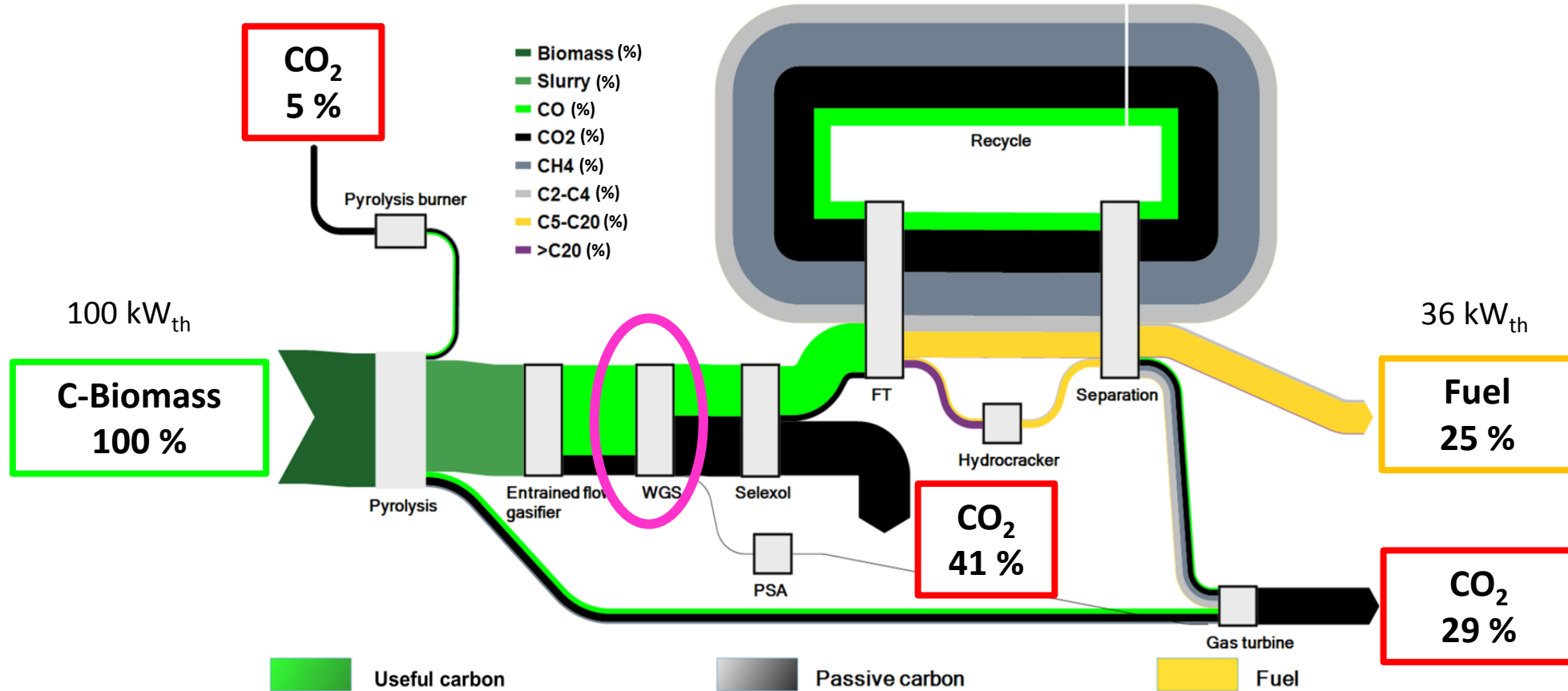
2. Process simulation – Key results for BtL Process

Stream [t/h]	BtL Process
Biomass	22

- H_2/CO ratio for FT-Synthesis ≈ 2
 $2 \text{H}_2 + \text{CO} \rightarrow \text{H}_2\text{O} + \text{-(CH}_2\text{)-}$
- WGS reaction is H_2 source
 $\text{H}_2\text{O} + \text{CO} \rightleftharpoons \text{H}_2 + \text{CO}_2$



2. Carbon flow diagram – BtL Process

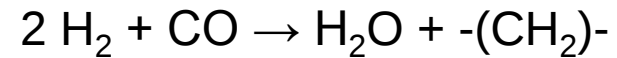


75 % of biomass carbon lost as CO₂

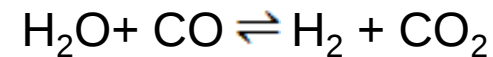
2. Process simulation – Key results for BtL Process

Stream [t/h]	BtL Process
Biomass	22
Liquid product	2.93
C - Conversion	25%

- H_2/CO ratio for FT-Synthesis ≈ 2



- WGS reaction is H_2 source



- Deactivated carbon (CO_2) can't be reutilized
- Lack of H_2 leads to low C-conversion
- PBtL Process with additional H_2 source and rWGS Reactor



2. Process simulation – Key results

Stream [t/h]	BtL Process	PBtL Process
Biomass	22	22
H ₂	-	3.57
Liquid Product	2.93	11.04
C - Conversion	25%	97.7%
XtL Efficiency	36.3%	51.4%

Stream [t/h]	PtL – small	PtL - large
CO ₂	9.05	34.20
H ₂	1.48	5.77
Total	2.93	11.05
C - Conversion	98%	98%
XtL Efficiency	50.6%	50.6%

$$\eta_{XtL} = \frac{\dot{m}_{Prod} \cdot LHV_{Prod}}{\dot{m}_{Biomass} \cdot LHV_{Biomass} + P_{El}}$$



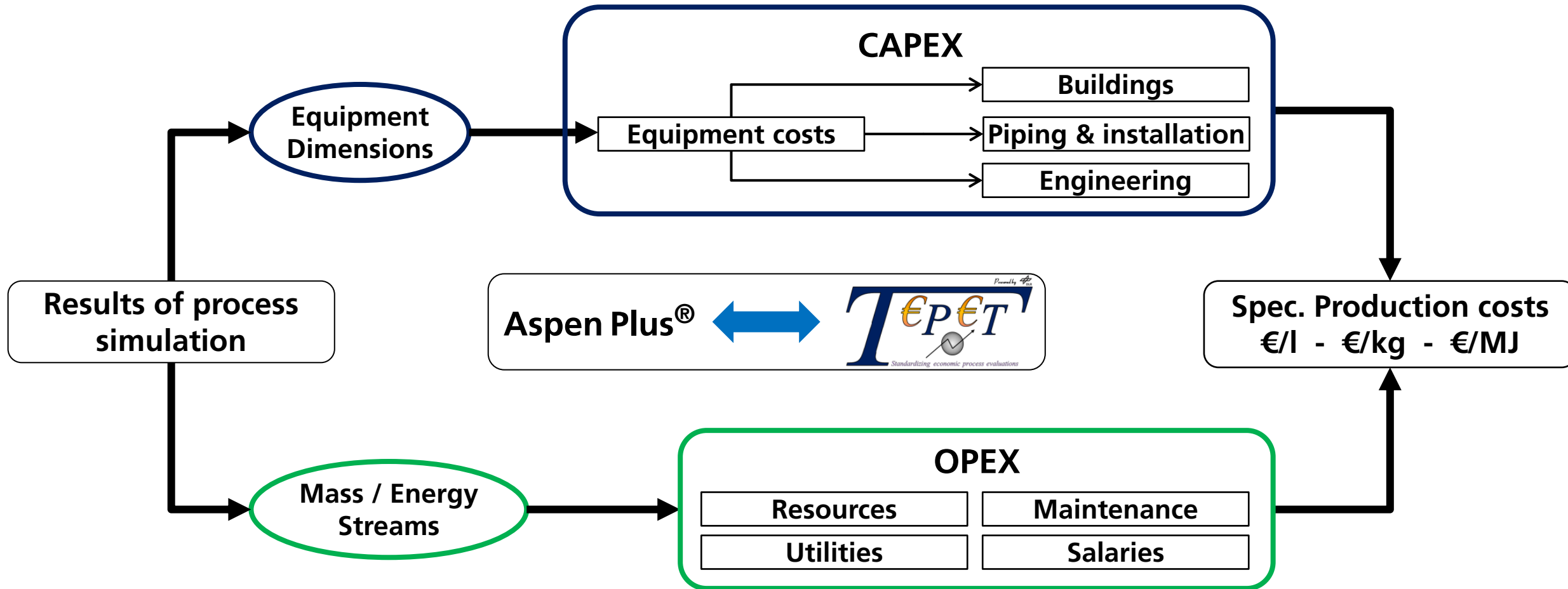
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3. Economical evaluation

AACE Recommended Practice Class III + IV Accuracy of cost estimation $\pm 30\%$



3. Determination of costs

CAPEX

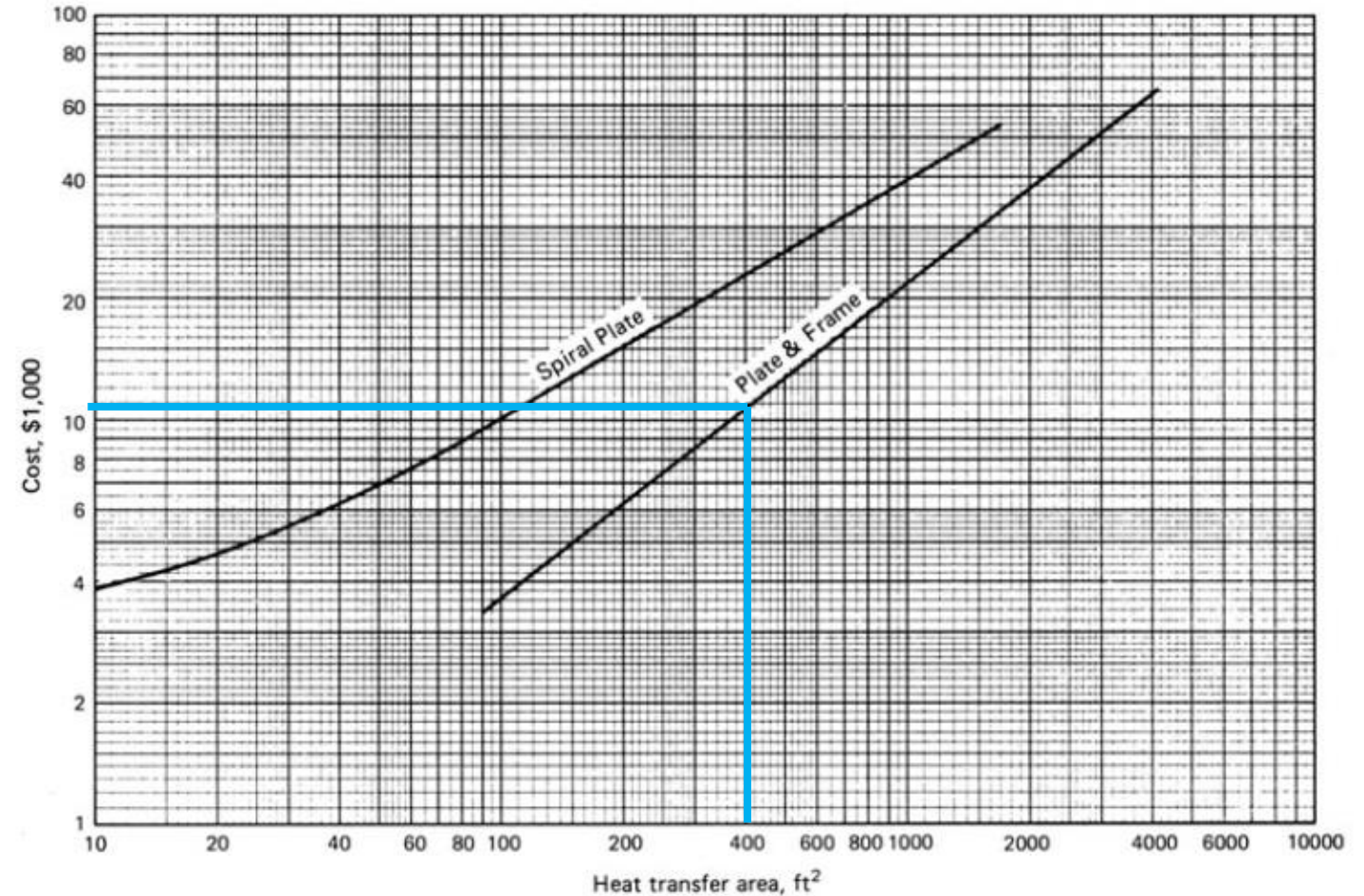
- Standard EQP (Heat exchanger,
- Special EQP has to be obtained
- Remaining costs can be divided into
 - Installation, Buildings...

OPEX

- Available market prices for commercial
- Remaining costs can be divided into
 - Maintenance, Salary,...

$$C_i = C_0 \cdot \left(\frac{S_i}{S_0} \right)^f \cdot \frac{Index_{Jahr_i}}{Index_{Jahr_0}}$$

Heat Exchangers: Spiral, Plate and Frame
304 stainless steel; no insulation



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4. Scenarios the techno economical evaluation

Investment Costs

PEM-Elektrolyseur (stack):	720	€/kW ^[1]	
PEM-Elektrolyseur (system):	1.350	€/kW	(TEPET, incl. cost factors)
Gasifier	103.650	€/(kg _{Slurry} /h) ^[2]	(Scale-factor: 0.7)
Fischer-Tropsch Reactor:	17,44	Mio.€/(kmol _{feed} /s) ^[2]	(Scale-factor: 0.67)

Costs for Resources and by-products

Electricity	99,6	€/MWh ^[3]
Biomass	80,1	€/t ^[4]
Oxygen (export):	24,3	€/t ^[5]
Steam (export):	19,8	€/t ^[6]

Further conditions

<i>Reference year</i>	2017	<i>Operating time of plant</i>	30 years
<i>Annual full load hours</i>	8.260 h/a	<i>Interest rate</i>	7%

[1] G. Saur, Wind-To-Hydrogen Project: Electrolyzer Capital Cost Study, Technical Report NREL, 2008

[2] I. Hannula and E. Kurkela, Liquid transportation fuels via large-scale fluidised-bed gasification of lignocellulosic biomass, Espoo: VTT Technical Research Centre of Finland, 2013.

[3] Eurostat, Preise Elektrizität für Industrieabnehmer in Deutschland, 2017

[4] C.A.R.M.E.N. – Preisentwicklung bei Waldhackschnitzel (Energieholz-Index)

[5] NREL, "Appendix B: Carbon Dioxide Capture Technology Sheets - Oxygen Production," US Department of Energy, 2013

[6] Eigene Berechnung basierend auf dem Gaspreis der Eurostat Datenbank

4. Result: Cost comparison of BtL / PBtL / PtL - process

 Elektrolysis

 Pyrolysis

 Gasifier

 Selexol

 Fischer-Tropsch

 Rest (CAPEX)

 Electricity

 Biomass

 Rest(Ressources/Utilities)

 Maintenance

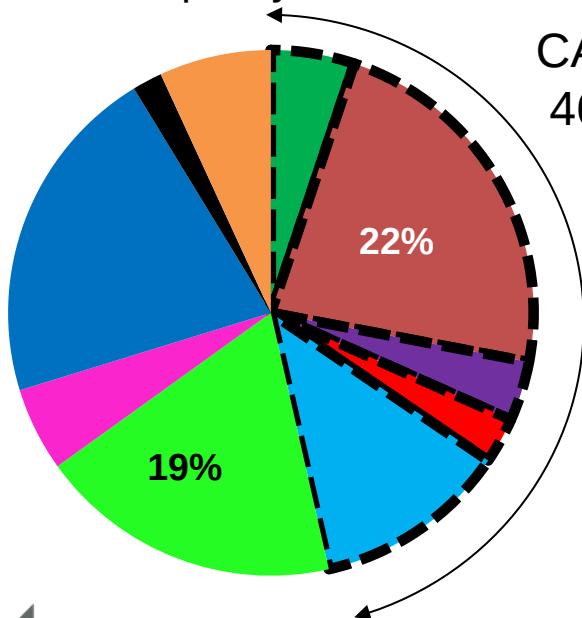
 Salary

 Rest (OPEX)

Biomass-to-Liquid (BtL)

FCI: ca. 411 Mio. €
 Production costs: ca. **2.36 €/l**
 Production capacity: ca. **24.2 kt/a**

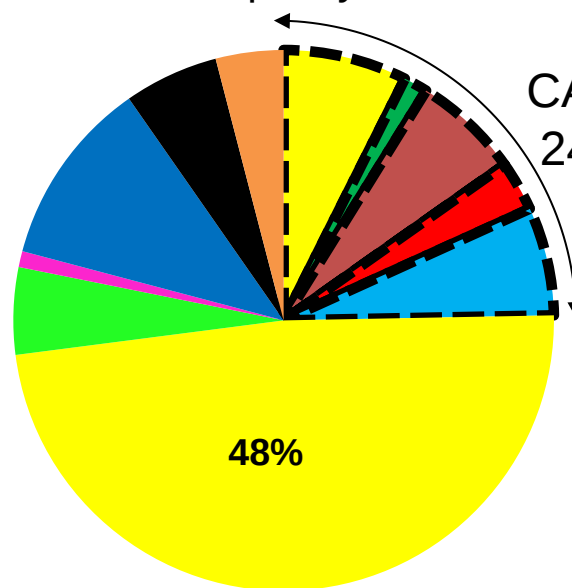
CAPEX:
46.5 %



Power&Biomass-to-Liquid (PBtL)

FCI: ca. 781 Mio. €
 Production costs: ca. **2.23 €/l**
 Production capacity: ca. **91.2 kt/a**

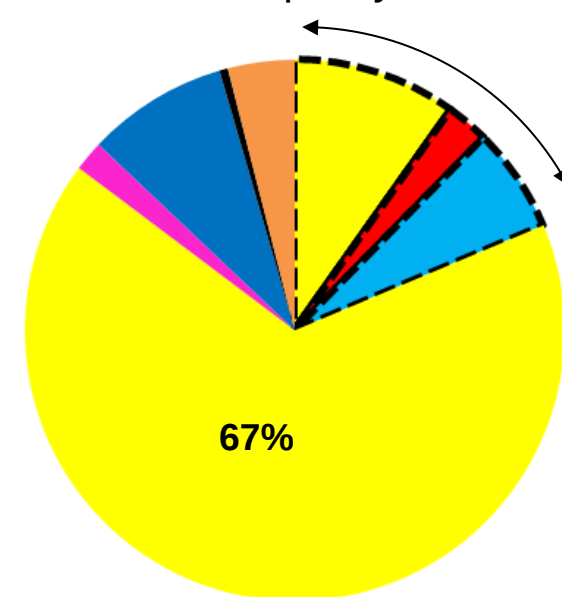
CAPEX:
24.7 %



Power-to-Liquid (PtL) - Large

FCI: ca. 696 Mio. €
 Production costs: ca. **2.64 €/l**
 Production capacity: ca. **91.2 kt/a**

CAPEX:
18.6 %

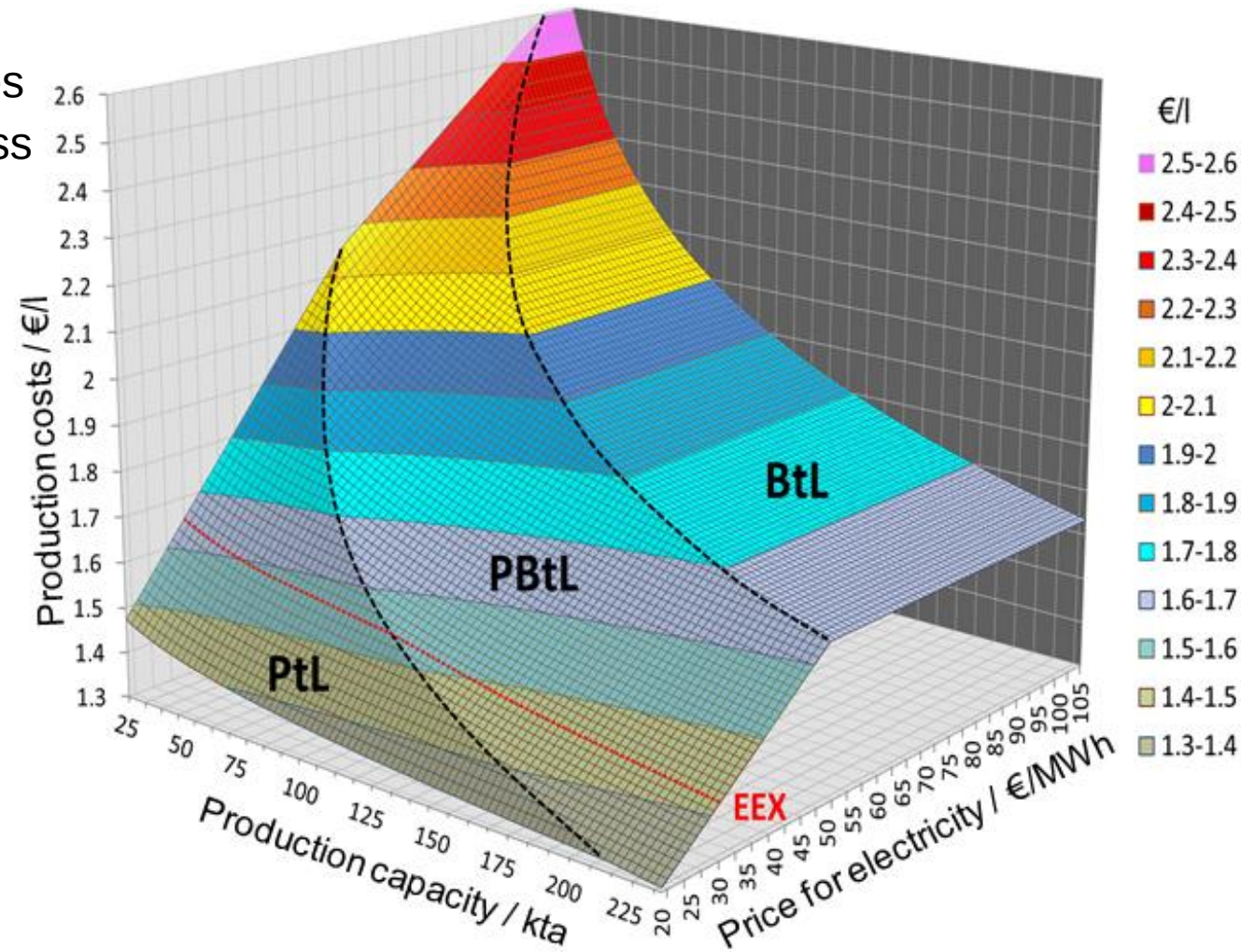
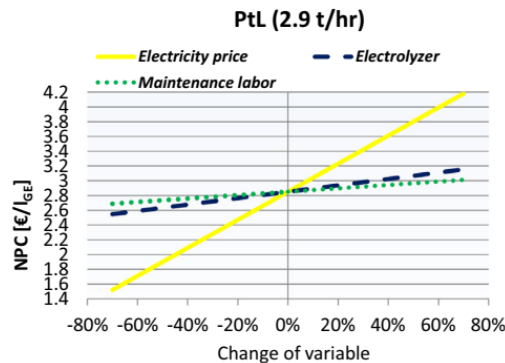


4. Sensitivity analysis

- TEPET is capable of performing sensitivity analyzes
- Specific production cost for different varying process parameters.

Example

- Influence of electricity price
- Influence of production capacity
„economy of scale“



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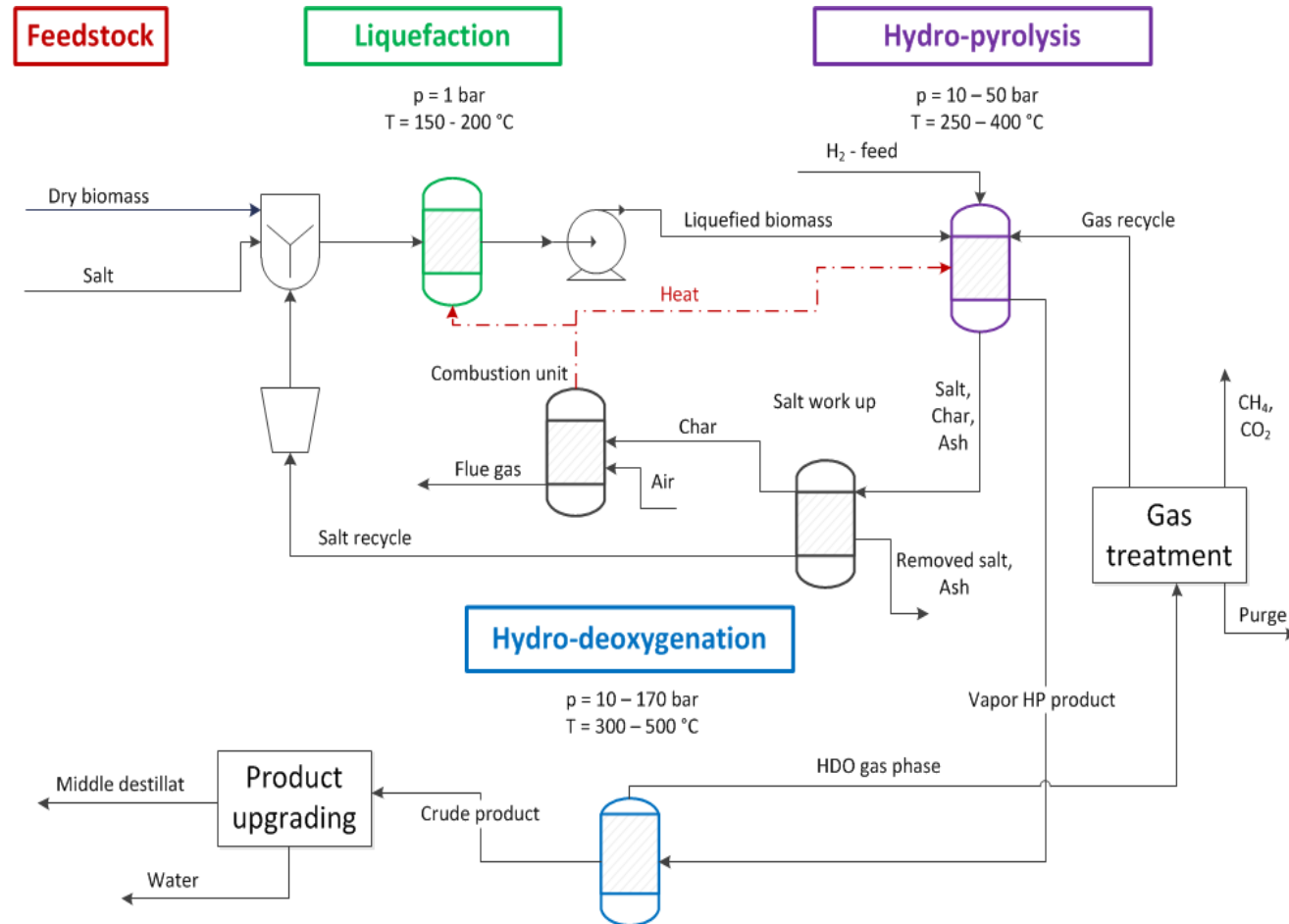
- Tool for the technical and economical evaluations are available
- Open and transparent cost estimation method
- Opportunities for development can be shown and outlined
 - Technological perspective: e.g.: Yield curves, efficiencies etc.
 - Economical perspective: e.g.: Influence of electricity price, economy of scale etc.
- “Bottlenecks” and their influence can be identified and → e.g. carbon flow-diagram



1 - EU – ABC-Salt Project

www.abc-salt.eu – EU No. 764089

- Liquefaction of biomass in a molten salt environment with subsequent middle distillate production by the process steps:
 - Biomass liquefaction
 - Hydro-pyrolysis
 - Hydro-deoxygenation
- Process development from **TRL 2** up to **4**
- Prototype manufacture with a biomass feed of 100 g/h and a hydrocarbon yield of 35 wt. %
- Diesel net production costs < 0.80 €/l



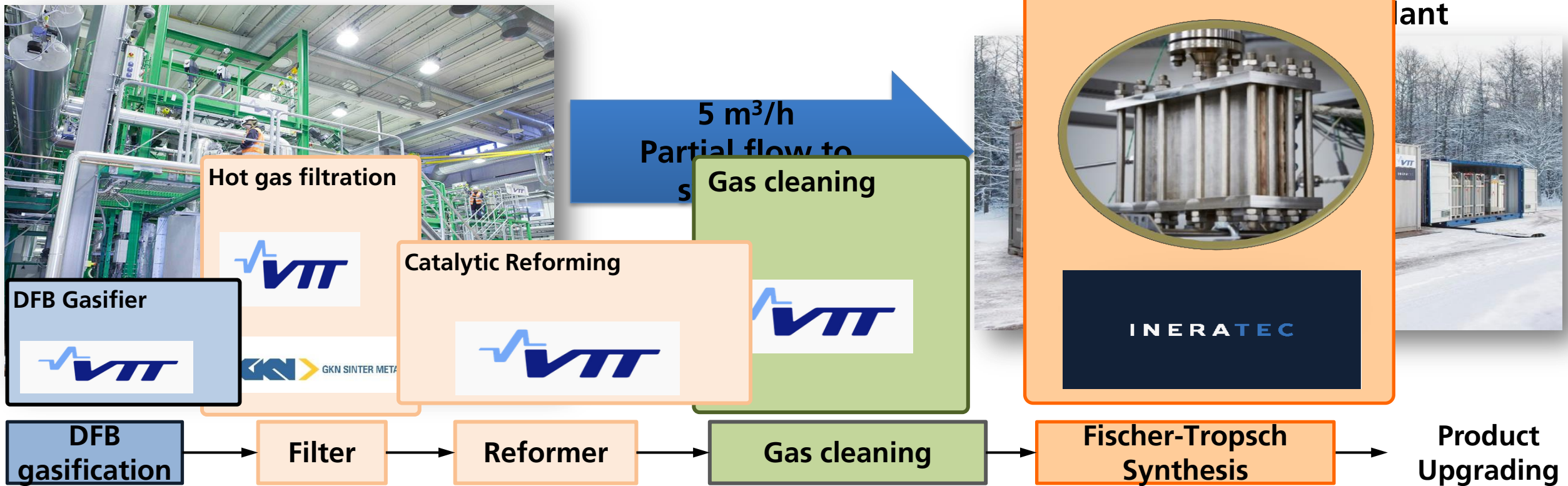
2 - EU – ComSyn Project

www.comsynproject.eu – EU No. 727476

- Compact Gasification and Synthesis process for Transport Fuels

DFB PILOT @ VTT

COMSYN
NEXT GENERATION
BIO-FUEL TECHNOLOGY



3 - EU – FlexCHx Project

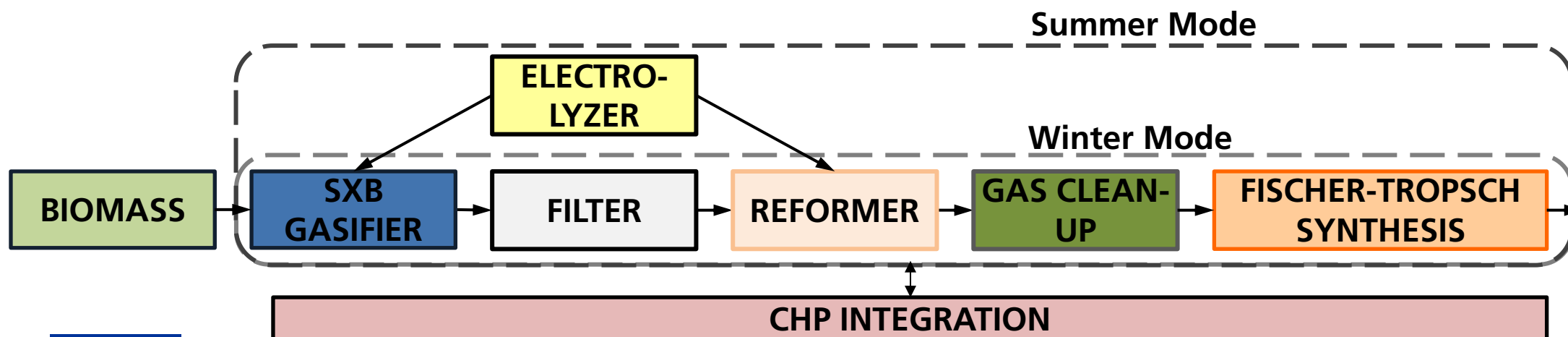
www.flexchx.eu – EU No. 763919



- Flexible generation of heat, power and transport fuels

Catalytic Tar Reforming

- New and robust catalyst, developed by Johnson Matthey results in cheap operating expenditures with low investment costs
- CO content can be increased via CO₂ recycling



Thank you for your attention

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Knowledge for Tomorrow



Energy system integration

- What does the energy system of the future look like?
- Sector coupling → Breaking the boundaries of heat, electricity and fuel market
- Taking the influence of production process into account? Rising demand increases the price?
- Estimating the available amount of a given resource? e.g.: Biomass, CO₂, Electricity
 - Minimum energy required for gas purification
 - CO₂ with DAC: 1.08 GJ_e/t_[1] → 0.3 MW / t_{CO2}/h

[1] APS Physics in 2011 Report about “Direct Air Capture of CO₂ with Chemicals”

