Redox stability improvement in metal supported cells with strontium titanate based fuel electrodes: *A step towards the next generation solid oxide cells*

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Key performance factors

Catalysis
Sealing
TEC
Reactivity
…

Robustness
Red-ox cycles
Contact
Fuel Utilization
Gas Transport
Balance of Plant
Life Time
Reliability
Start-up time
Poisoning
…

Microstructure / Architecture

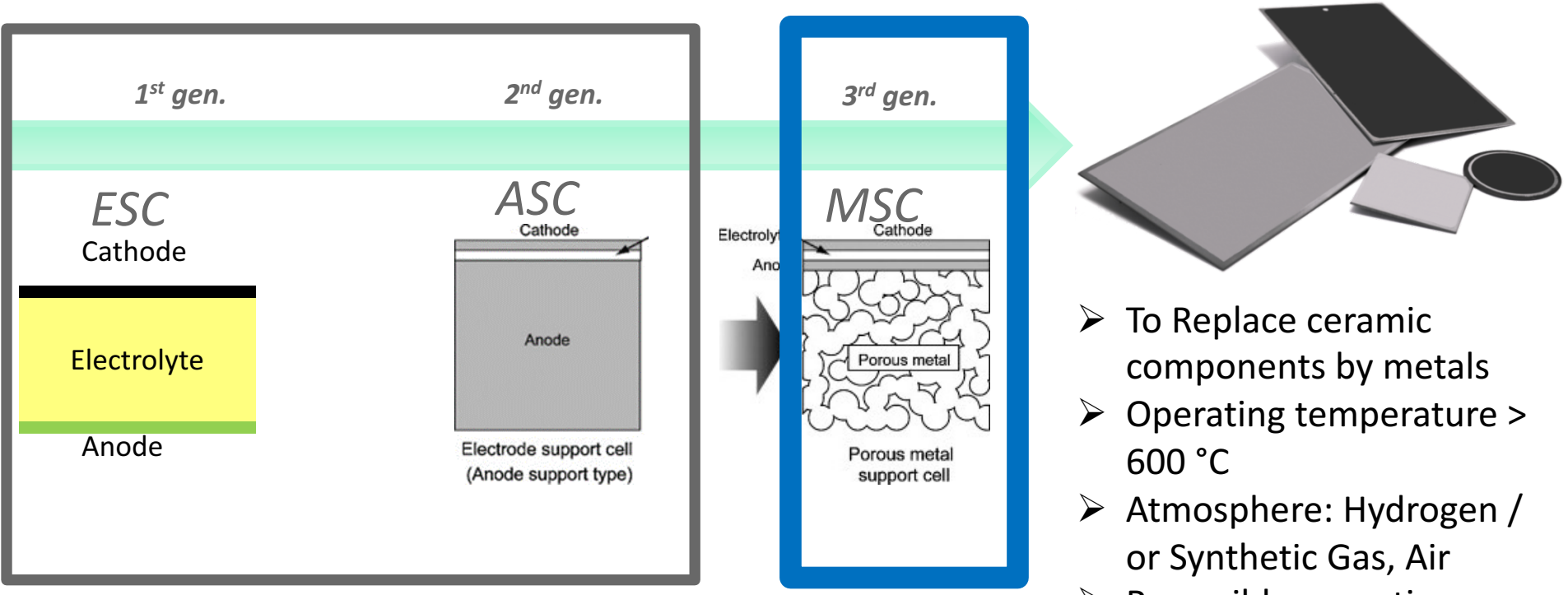
Materials

Manufacturing

➢ To produce kWh

➢ *To store Energy*

Why metal Supported Cells ?



- To Replace ceramic components by metals
- Operating temperature > 600 °C
- Atmosphere: Hydrogen / or Synthetic Gas, Air
- Reversible operation

Table 1
Summary of candidate support metals.

Metal	CTE (ppm K^{-1})	Cost ($/kg 2009)	Relative oxidation resistance
NiCrAlY	15–16	63	Excellent
Hastelloy-X	15.5–16	22	Excellent
Ni	16.5	18	None[a]
Ni–Fe (1:1)	13.7	9	None[a]
300-Series stainless steel	18–20	2	Poor
400-Series stainless steel	10–12	2	Very good

Note that CTE of electrolytes (YSZ, CGO, LSGM) are 10–12 ppm K^{-1}.

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Motivation: towards the next generation SOC

1st gen.	2nd gen.	3rd gen.	4th gen.
ESC	**ASC**	**MSC**	
Limited power density Robustness	High power density Sulfur poisoning Fast thermal cycling Redox Cycling	High power density Sulfur poisoning Fast thermal cycling Redox Cycling	High power density Sulfur resistant Thermal cycling Redox Cycling Low cost
Stationary Transportation	Stationary Transportation	Stationary Transportation	Stationary Transportation

Flexible architecture for multiple applications

Which materials for the next generation of SOCs?

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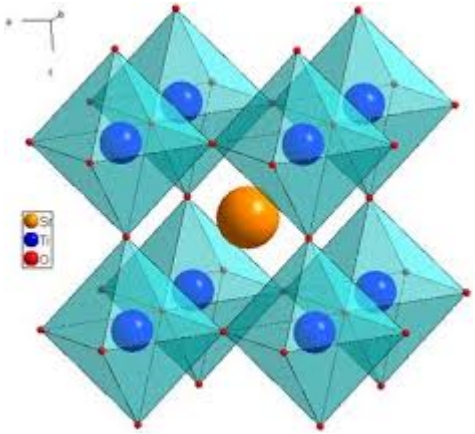
Selection for the next generation with metallic substrates

- *Improving durability of the metallic substrate*
  - ***Implementing alumina forming alloys***

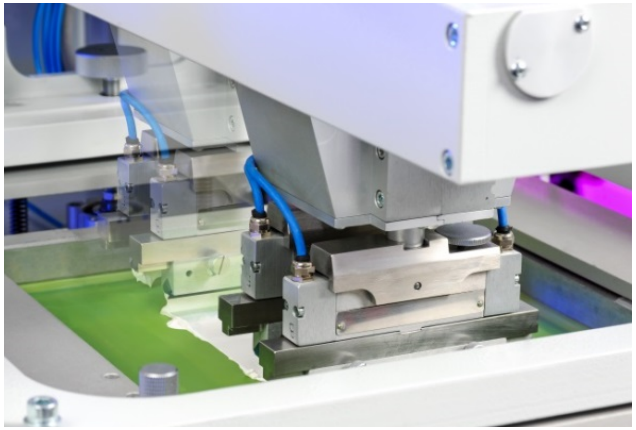
- *Enhancing Sulfur tolerance and redox stability at the anode*
  - ***Perovskite based anode materials***

- *Improving gas tightness while reducing thickness of electrolyte*
  - ***Thin film multi layer electrolyte***

- *Avoiding High T sintering in reducing atmosphere*
  - ***low T processing in air***



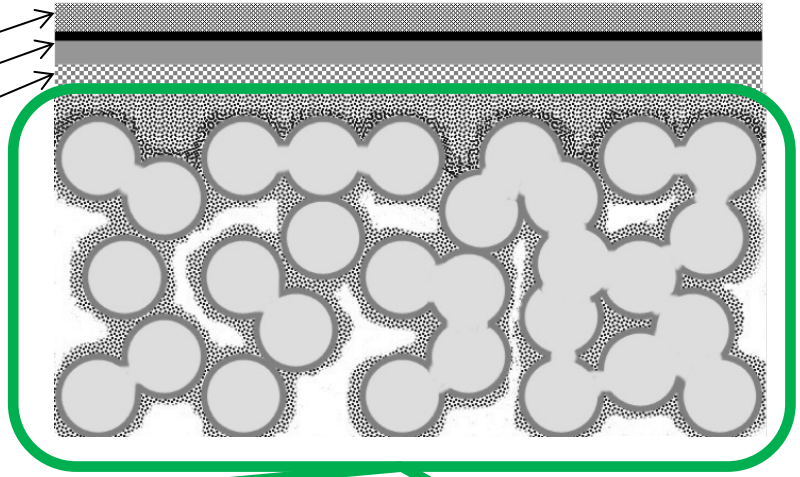
$La_{0,1}Sr_{0,9}TiO_{3-\alpha}$



screen printing

Materials

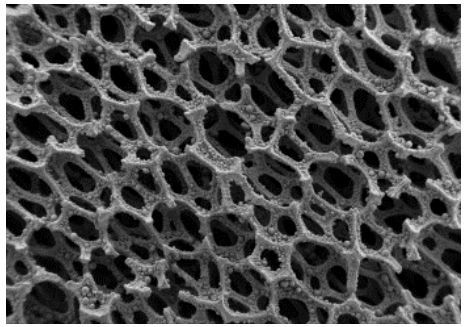
Cathode : $La_{0,4}Sr_{0,6}Co_{0,2}Fe_{0,8}O_{3-\alpha}$
Electrolyte: 8-YSZ / 10-CGO
Anode: CGO-LST (w/o 5-10%Ni)



Metallic substrate at the fuel side

ALANTUM
Innovations in Alloy Foam

CerPoTech
Ceramic Powder Technology



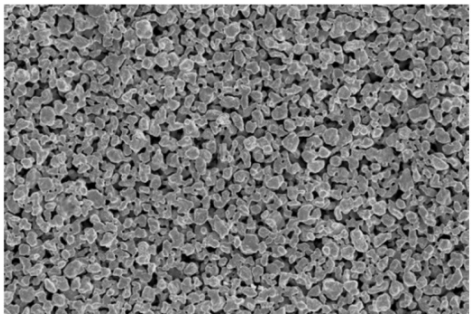
Foam NiCrAl #01
450µm pore size

+

$La_{0,1}Sr_{0,9}TiO_{3-\alpha}$
$NiO + La_{0,1}Sr_{0,9}TiO_{3-\alpha}$ (50:50)

1

PLANSEE

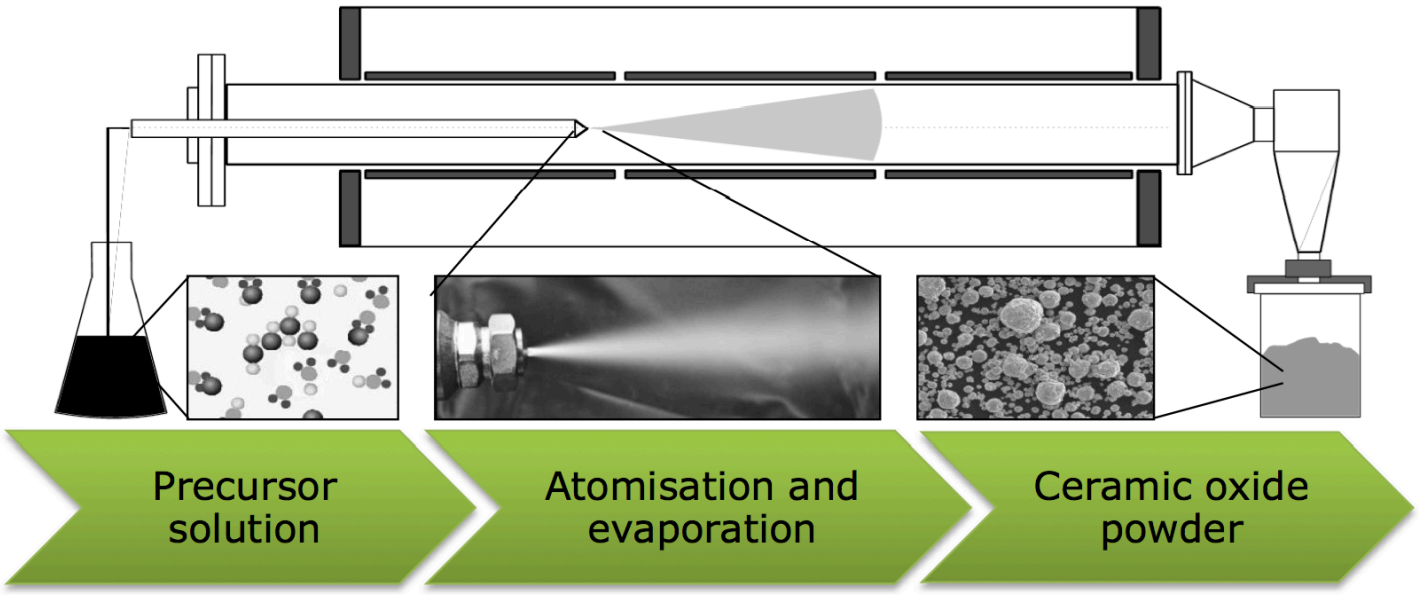


ITM

2

DLR

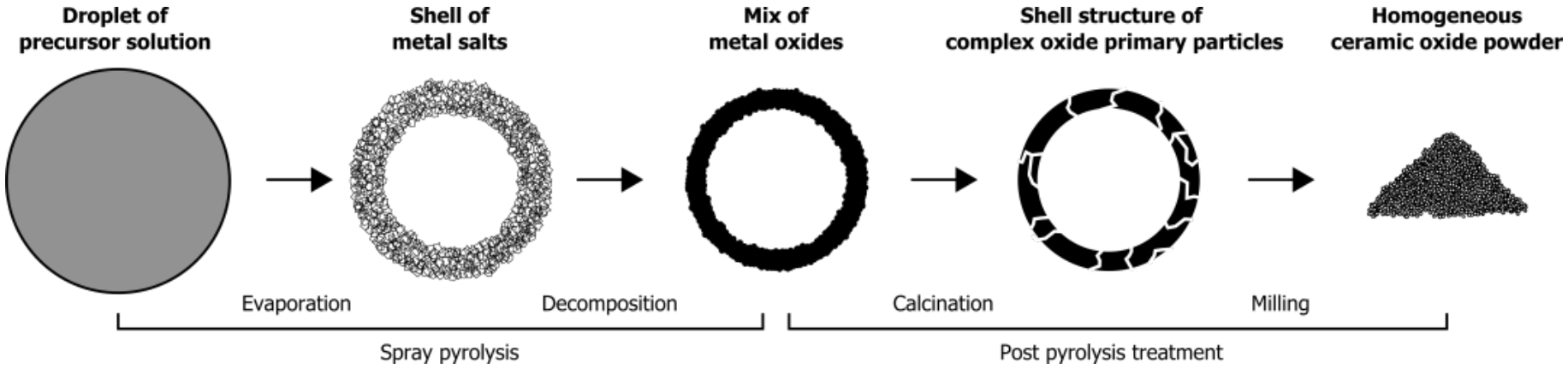
Powder Production Process



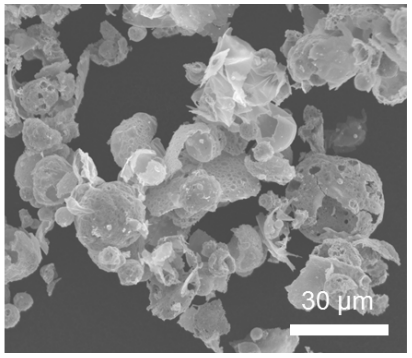
- Spray pyrolysis is CerPoTech's core technology.
- The precursor chemistry, the pyrolysis equipment and know-how make it unique.
- The spray pyrolysis technology allows for a seemless up-scale of the from pilot scale production to industrial size.

CerPoTech
Ceramic Powder Technology

Powder Production Process



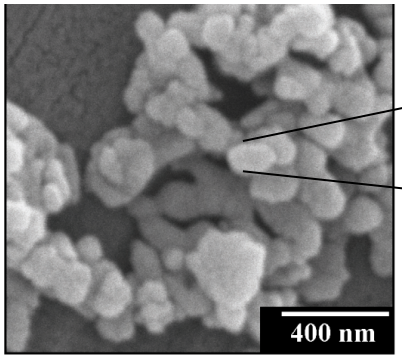
As produced



1-50 µm

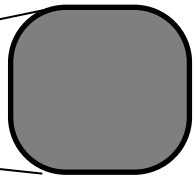
De-agglomeration

Agglomerates



0.1-1 µm

Crystallites



10-500 nm

Specific surface area in the range 1-50 m^2/g

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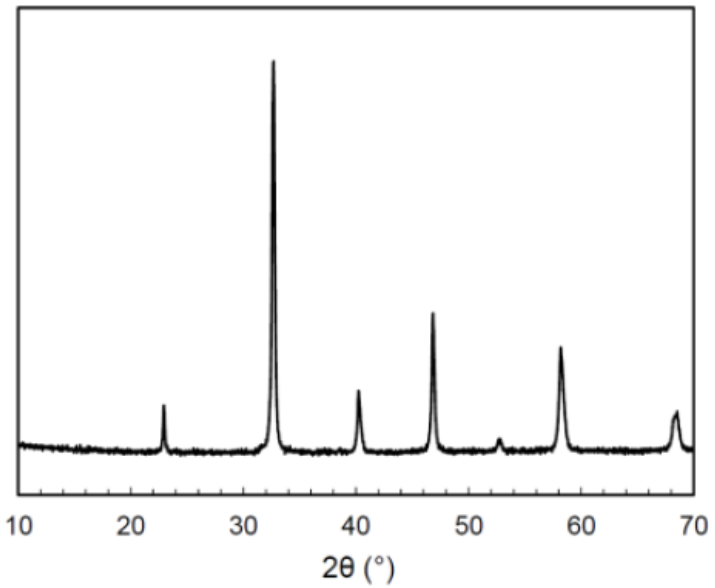
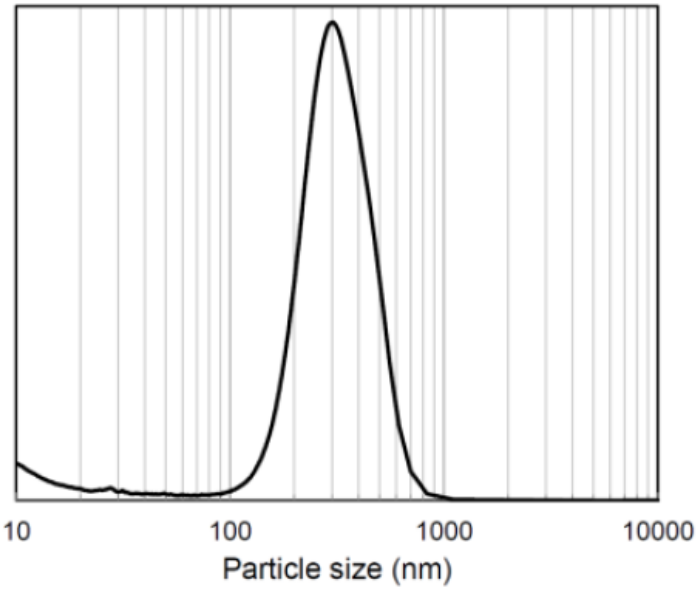
Exact specification depending on material and post treatments

High quality powders





- High phase purity
- Homogeneous powders
- Exact stoichiometry
- Low level of contaminants

- Narrow particle size distribution
- Excellent sinterability / reduced processing temperature

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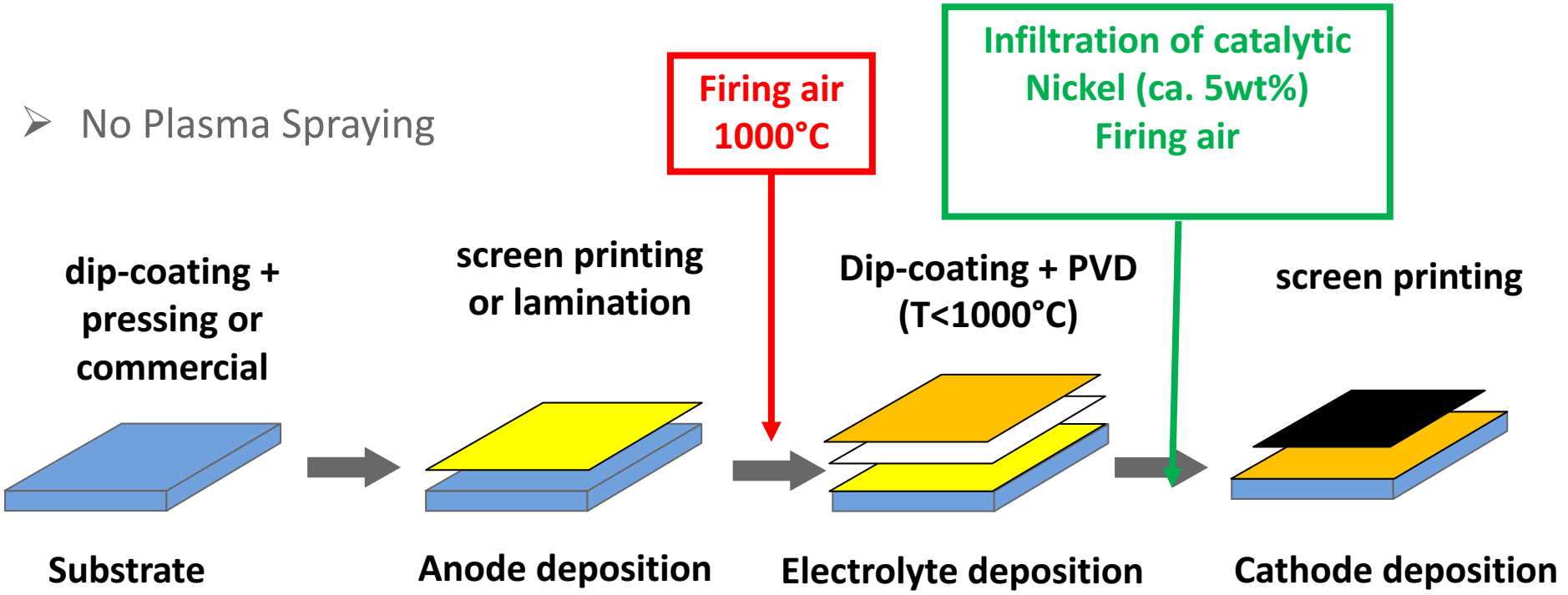
Ceramic Powder Technology

Manufacturing

- No Plasma Spraying



- T_{max} processing: 1000°C
- Atmosphere: air or low P_{o2} for PVD coating
- **No pre-reduction of $La_{0,1}Sr_{0,9}TiO_{3-\alpha}$**
- Conditioning and testing of cell at max. 800°C

Electrochemical Testing

Microstructure:

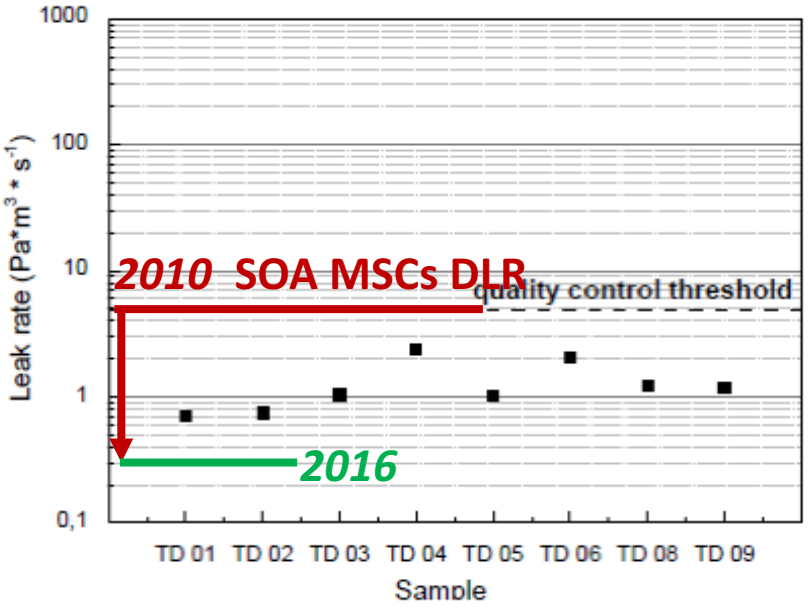
Hermiticity of the electrolyte

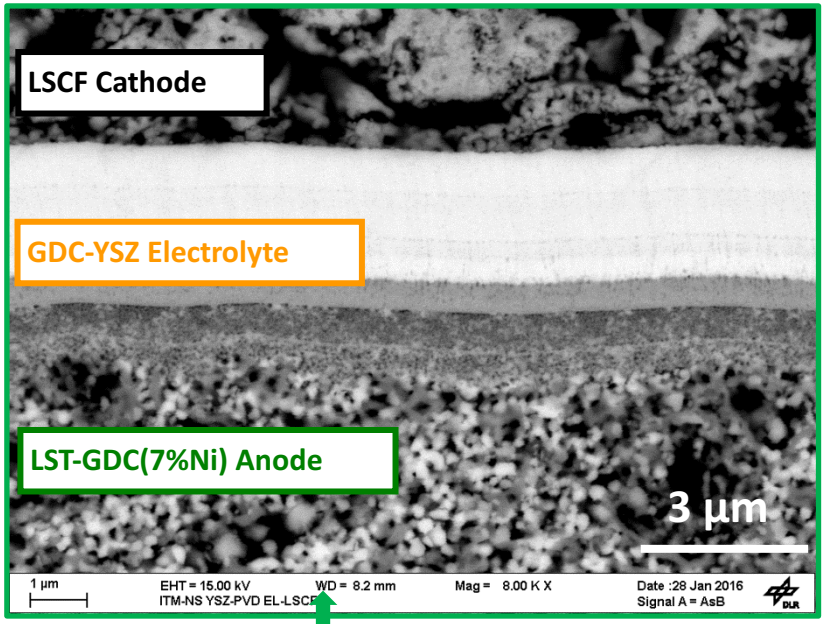
Gas tightness improved by 1 order of magnitude *(compared with PS)*

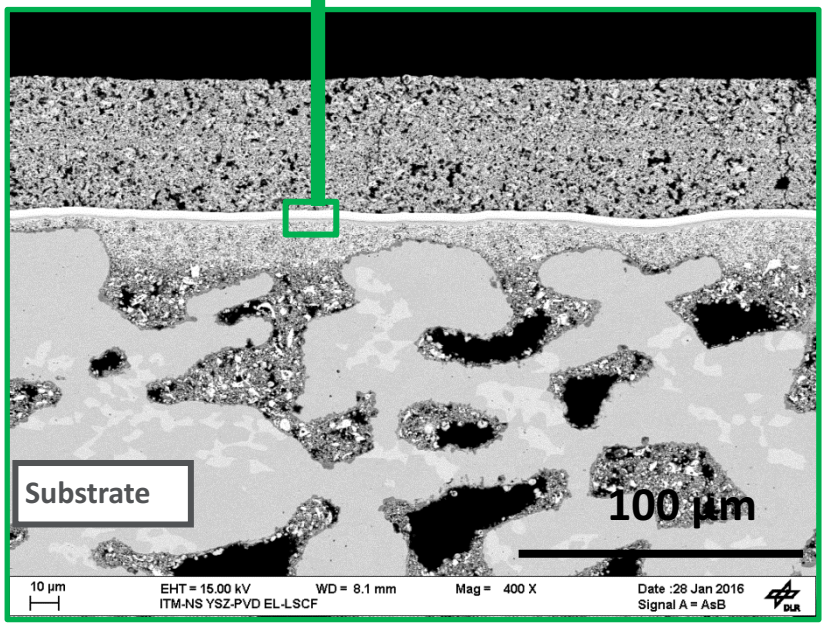
Material consumption reduced by 1 order of magnitude

- PVD: 1,2mg/cm² of YSZ + 1,5mg/cm² of CGO
- PS MSCs: 20mg/cm² of YSZ

!!! Sensitive to Pinholes!!!

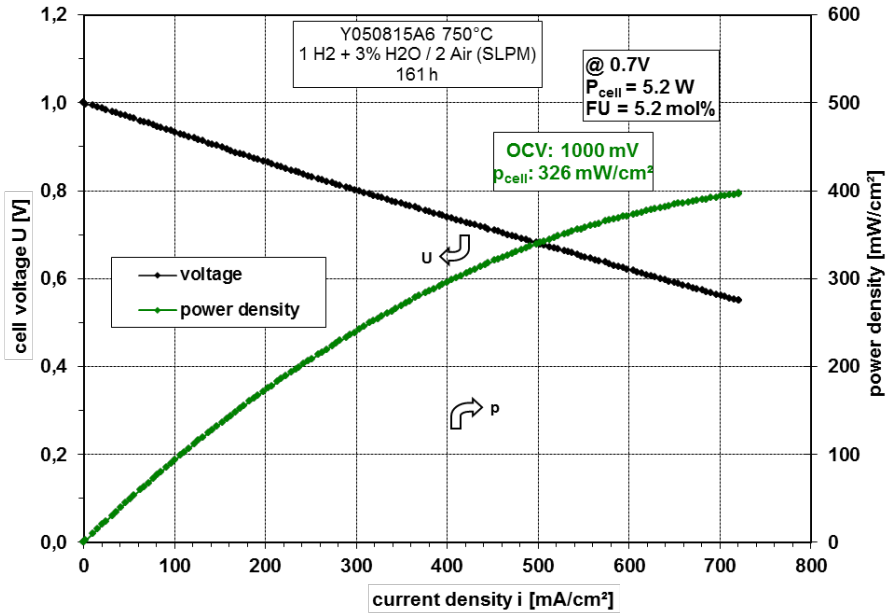




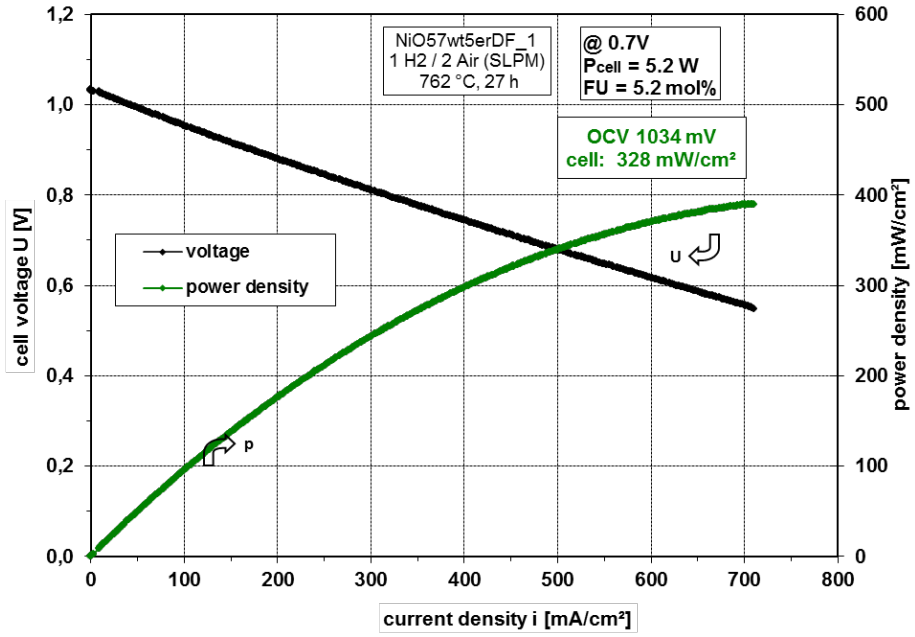


Performance

ITM (ferritic stainless steel) vs NiCrAl (w. LST:NIO)
(Anode Functional Layer: LST:CGO w 5-10wt%Ni) – 16cm²



ITM (ferritic stainless steel)



NiCrAl (w. LST:NIO)

@ 750°C 1slpm H_2 (w. H_2O)/ 2slpm air

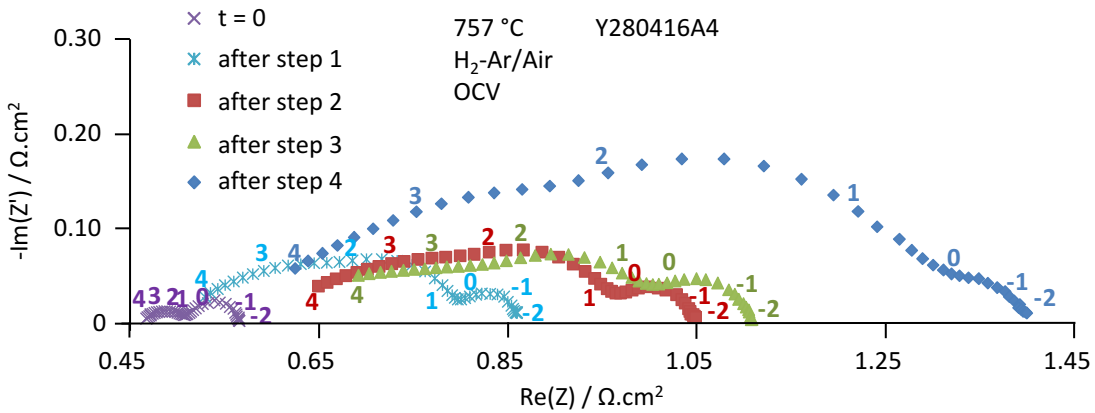
OCV: ca. 1V (!!! Pinhole !!!)

Power density at 0,7 V ca. 320 mW/cm² (improved up to 450 mw/cm²)

Performance nearly independant in tested condition from the substrate (Manufacturability)

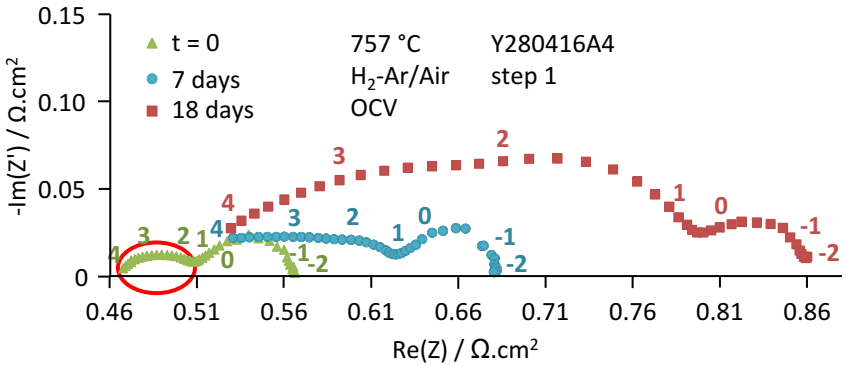
Interfaces and Electrodes aged during operation

Metal foam substrate - operation 1500 hours



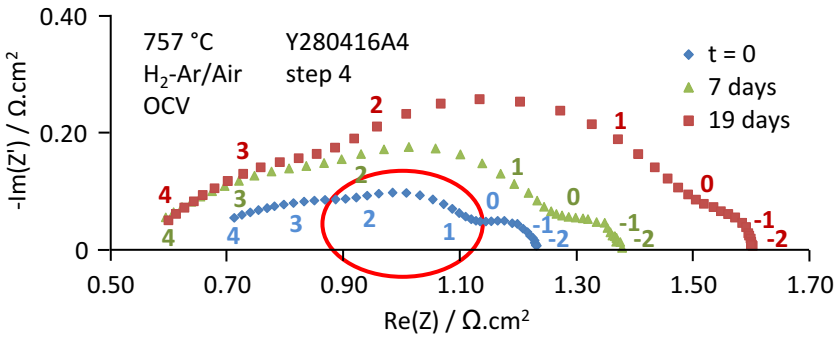
Assignment of degradation based electrokinetic modeling

increase of R_s and R_{pol}



degradation of interfaces

contact between ionic conductors



degradation of electrodes

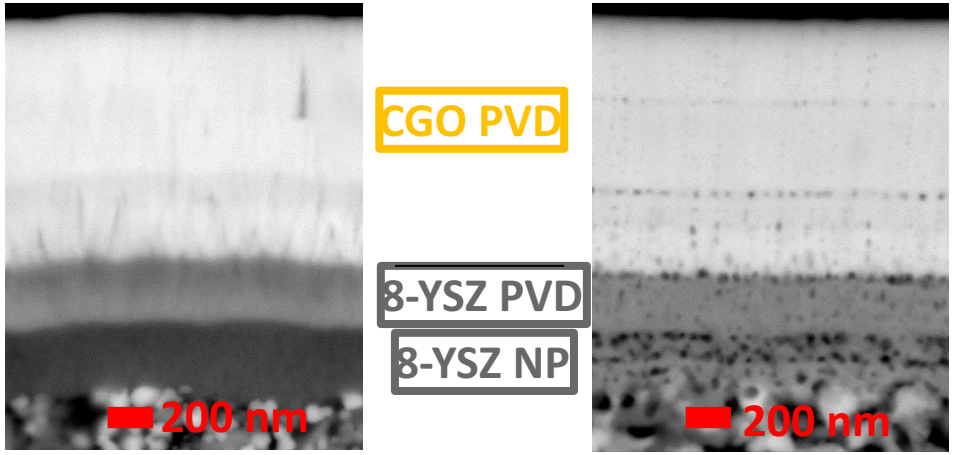
anode & cathode

V. Yurkiv et al., Journal of Power Sources, 287 (2015) 58 - 67

Degradation of interfaces

multi-layer electrolyte

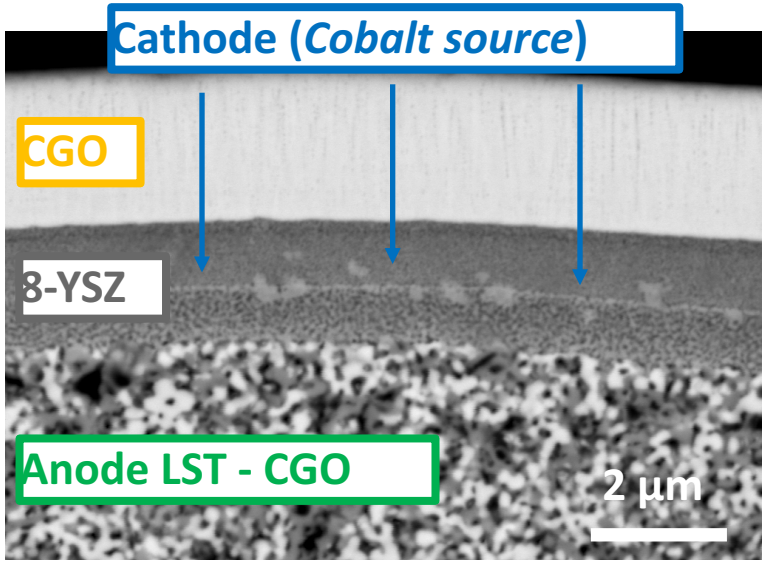
interfaces in Electrolyte

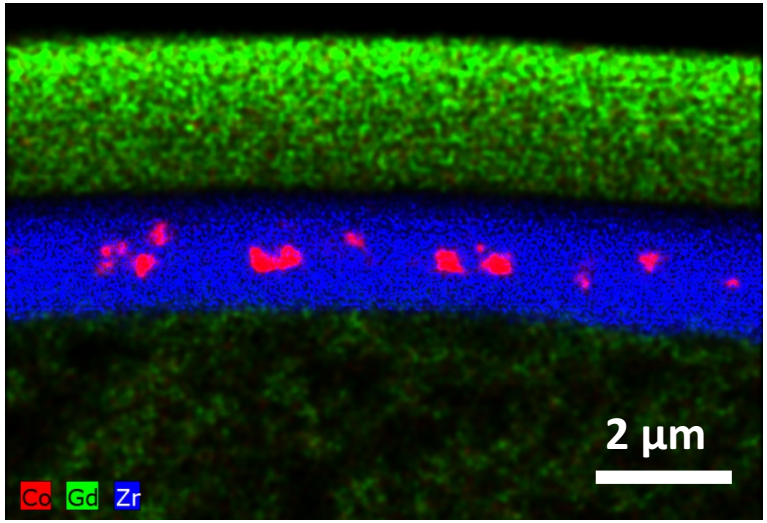


Fine pores in the PVD layer
Sintering of the nano-porous Layer

No measured influence on leak rate
Impact on apparent resistivity of the layer an ionic transfer (?)

Cation diffusion





Increase of electronic transport?

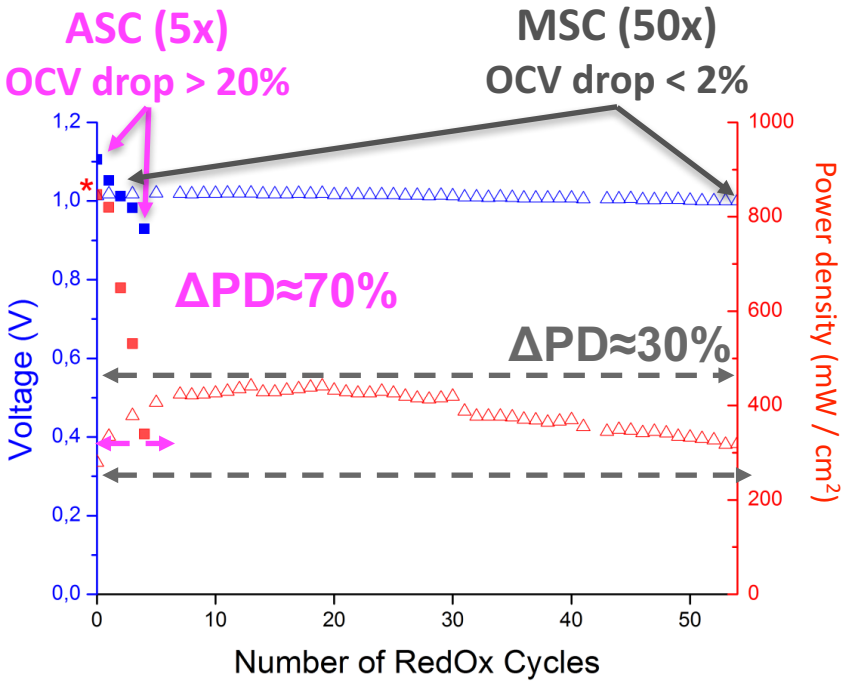
Degradation of interfaces

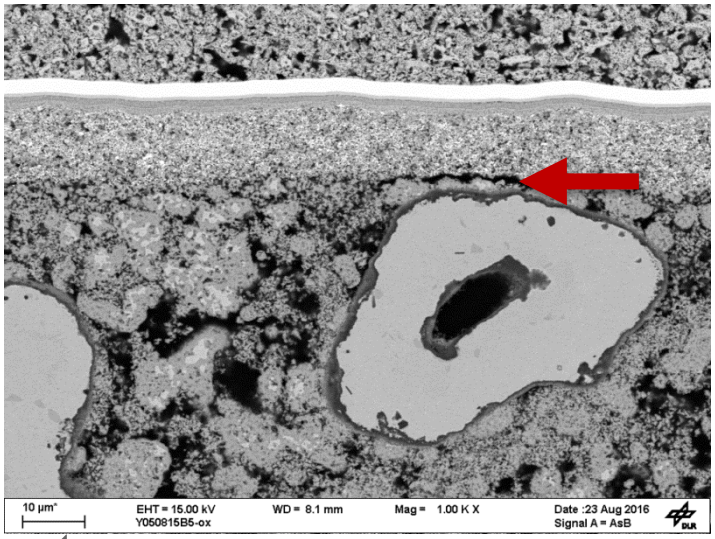
Redox cycles (30 min in O_2 @750°C)

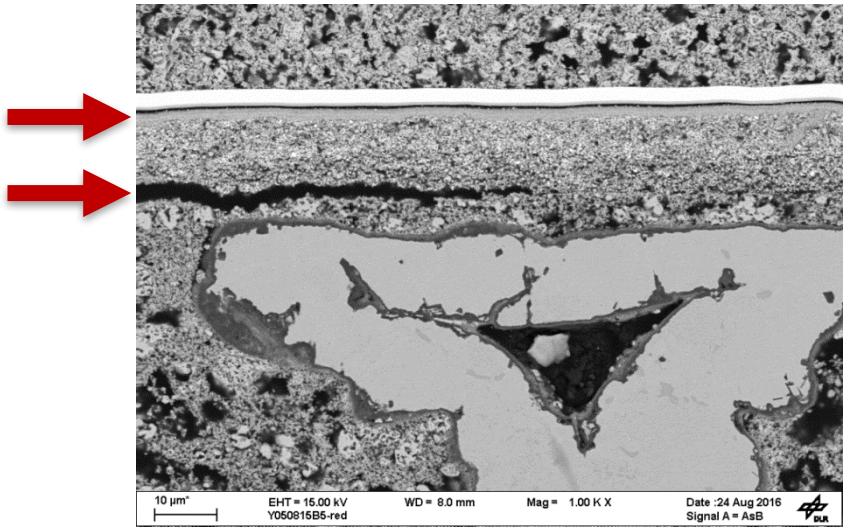
No fatal failure of the electrolyte
➢ NiCrAl « armored » substrate?

Performance still affected
Cracks due to repeated volume expansion of nickel during oxidation

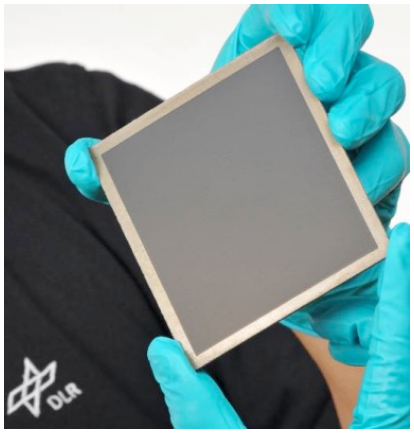
Ni rearrangement?

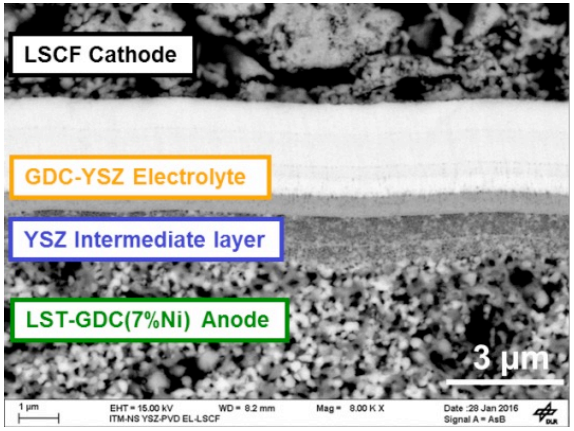




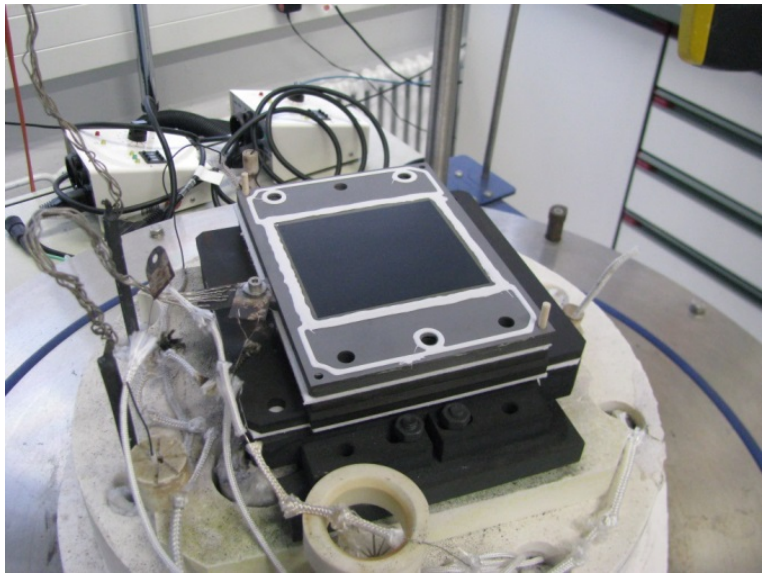


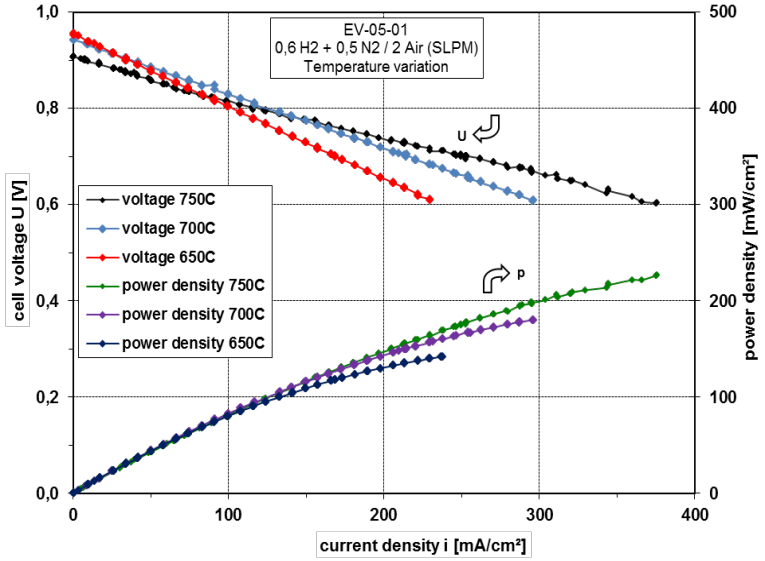
Up-scaling





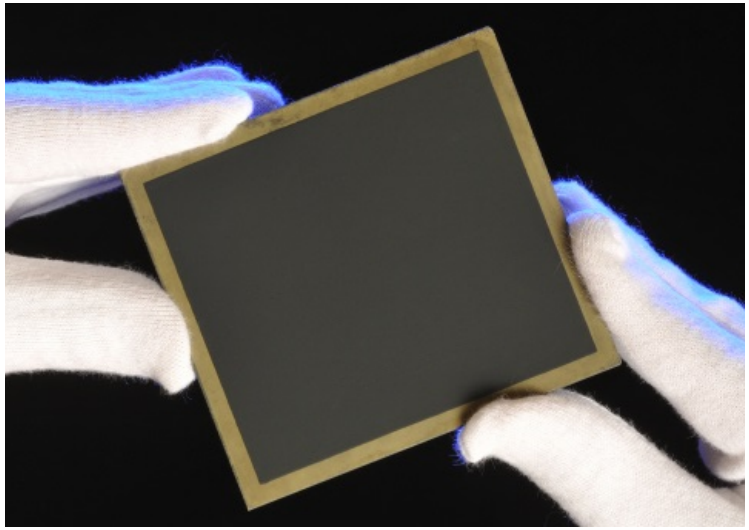
- size up to 90 mm x 100 mm
- Adapted sealing
- Power density for 1 level stack at 166 mW/cm² @ 750 °C and at 0,7 V





Conclusion & Perspectives

- ***metal supported cell with LST were produced. Processing route has been designed to tackle requirements for manufacturing.***
- ***Thin film electrolyte technology developed and demonstrated.***
- ***Power Density > 400 mW / cm² at 750°C*** *and 0,7V is obtained. Addition of nickel was necessary to enhance kinetic at the fuel electrode.*



- ***OCV drop of less than 2% for 50 forced redox cycles at 750°C***
- ***Integrity of the electrolyte is maintained***

- ***Cell-Architecture can be up-scaled at stack size and is economically realistic***

- ***Degradation of the interfaces in the multi-layer electrolyte (Lower operating T)***
- ***Both fuel electrode are subject to degradation (new set of materials)***
- ***Investigation in electrolysis operation***

DLR

Acknowledgements

This work was funded by the European Union's Seventh Framework Programme (FP7/2007-2013) for the Fuel Cells and Hydrogen Joint Technology Initiative under grant agreement n°303429.

Thank you for your attention!
And please visit us in the Exhibition, Booth 210

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