

Cavitation and multi-phase phenomena in liquid rocket engine systems

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5th Cavitation Workshop, Chania, 27-28 June 2017



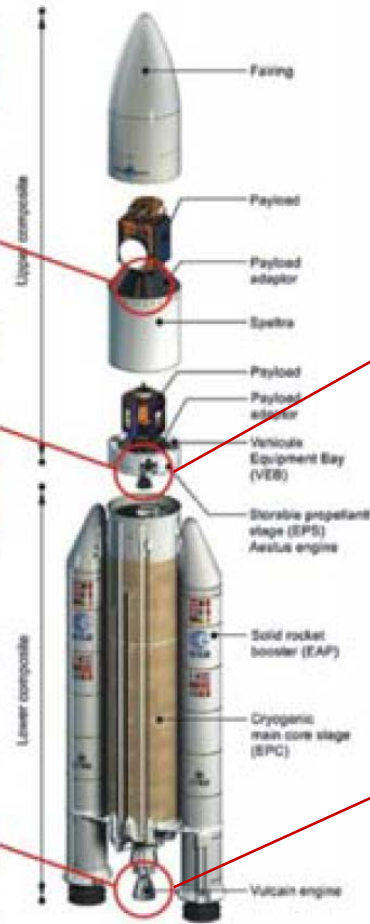
Knowledge for Tomorrow



German Space Center (DLR) Institute of Space Propulsion - Lampoldshausen



Institute of Space Propulsion – Lampoldshausen: supporting the European Space Program



Aestus Engine, 30 kN
storable hypergolic propellants,
N₂O₄/MMH



Vulcain Engine, 1360 kN
cryogenic propellants,
LOX/LH₂



Outline

- Overview of cavitation events in LRE
 - Turbopumps
 - Flash injection
 - Valves operation

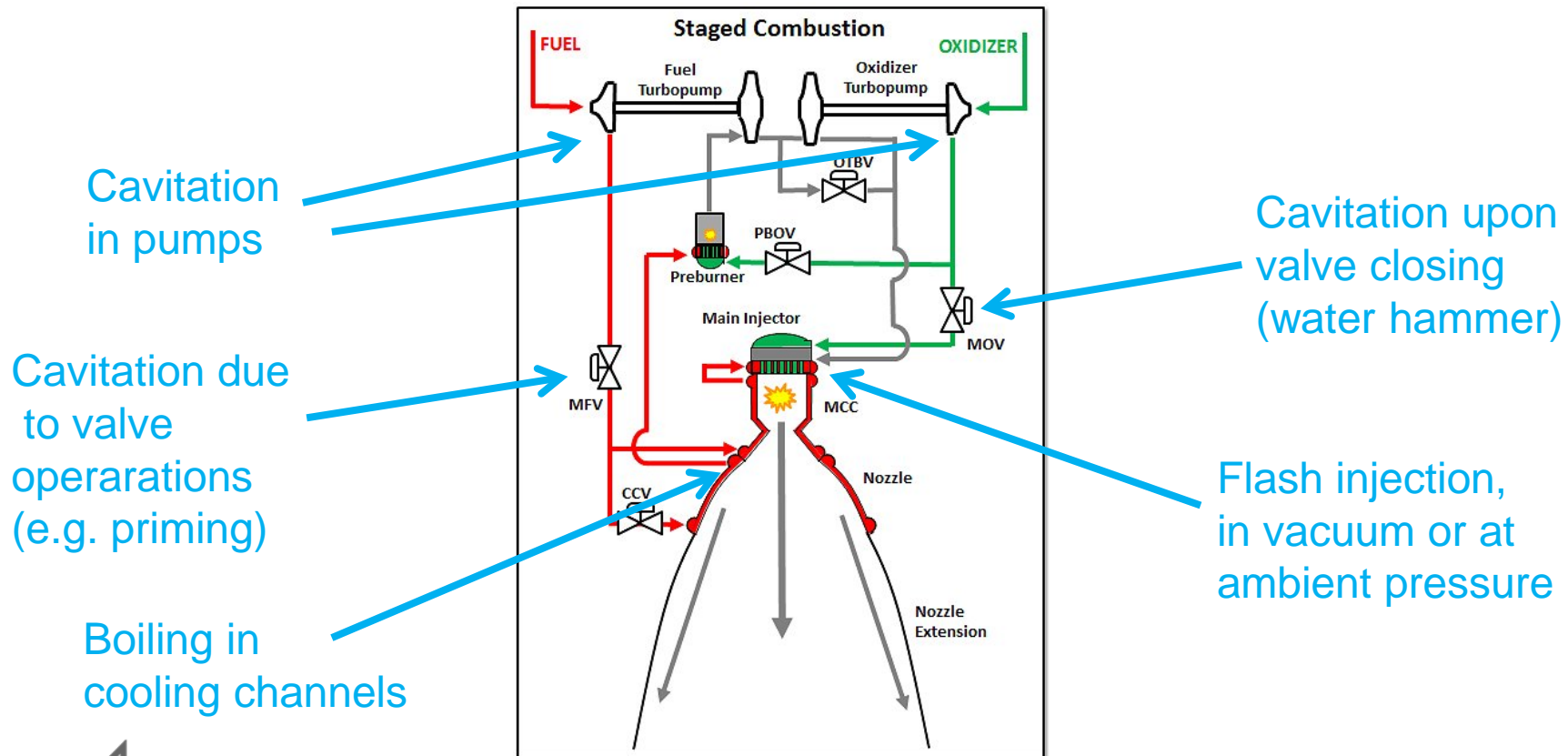
- Test cases:
 - Cavitation during water hammer
 - Priming
 - Numerical modeling



Introduction: Liquid Rocket Engines (LRE)

A LRE is a complex fluid network in which each propellant must be delivered from the tank to the combustion chamber.

Cryogenic propellants are stored near their saturation point => cavitation is likely to occur



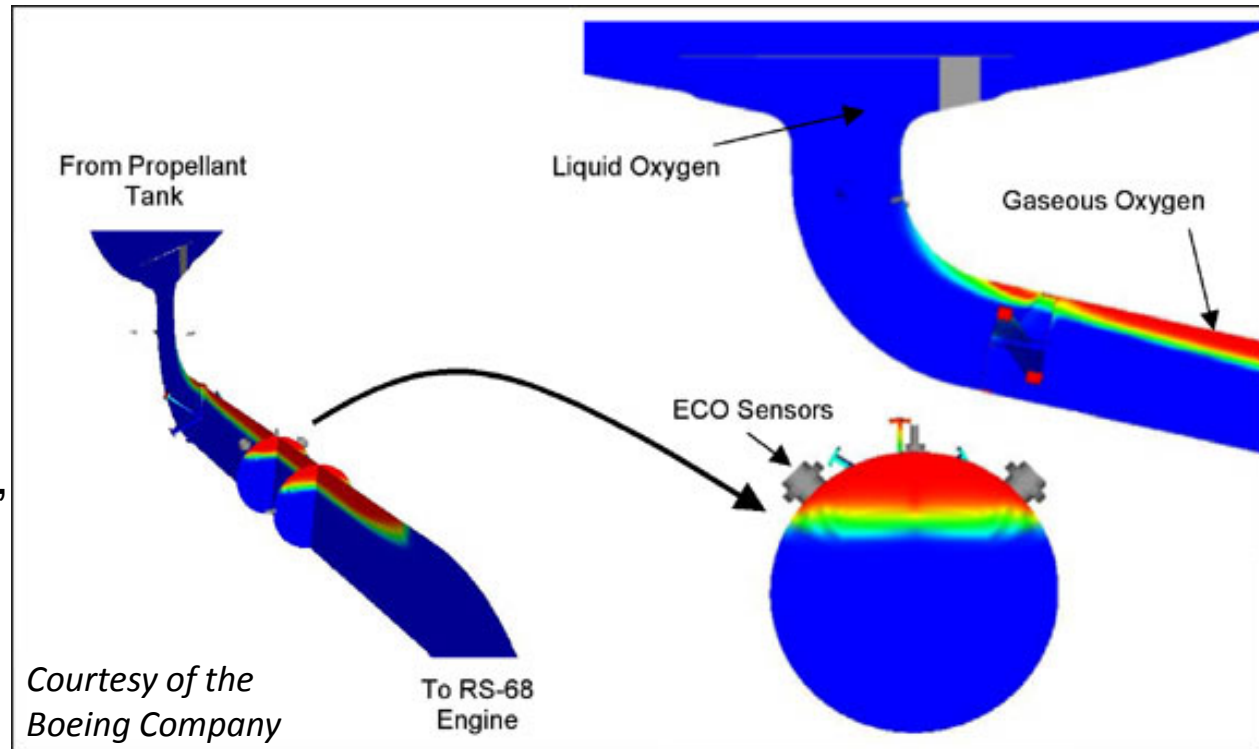
Real example of (expensive) cavitation: Delta IV Heavy



On 21 Dec 2004, cavitation in the LOX feedline caused a premature shutdown of the engine:

a pocket of gaseous oxygen formed and reached the Engine Cut-Off (ECO) sensor. This caused the ECO sensors to momentarily indicate dry, initiating then the shutdown sequence 8 sec earlier

Mission was a partial failure, since the payload was placed in a lower orbit (\$\$!)



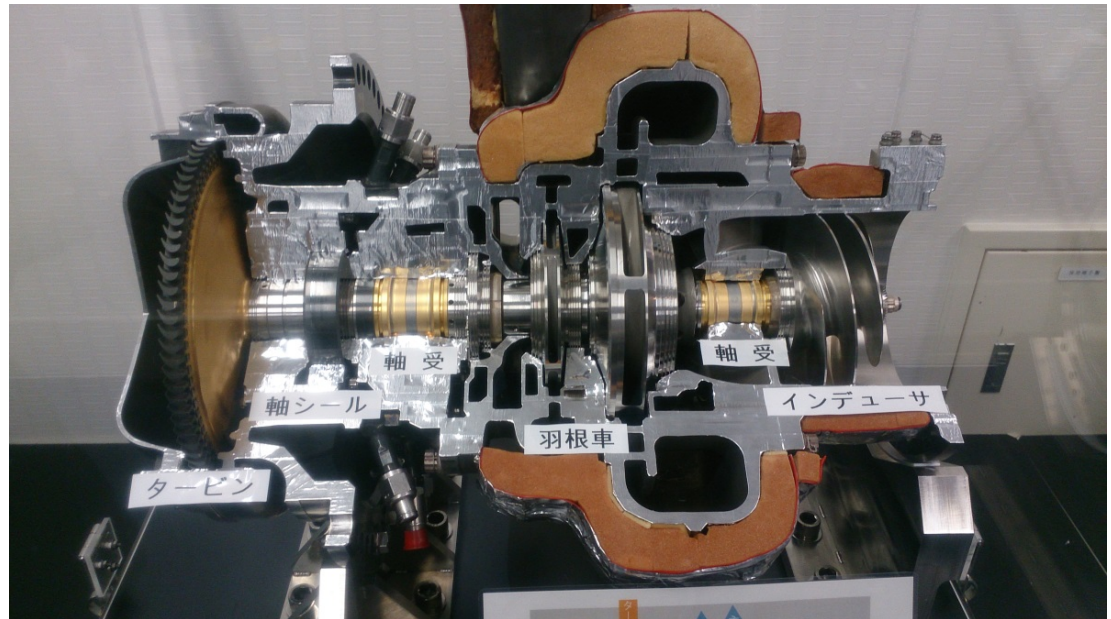
Cavitation in Turbopumps

Turbopump are key-components in LRE

Challenges:

- High pressure ratios
 - 5 to 130bar in single stage pump (Vulcain 2)
- Weight
 - High rotational speed
 - Low available NPSH (tank mass)
- Power density
 - 14.25MW (LH2 Vulcain2)
 - ~70x40x40cm
- Reactive Fluids
 - LOx fire hazard

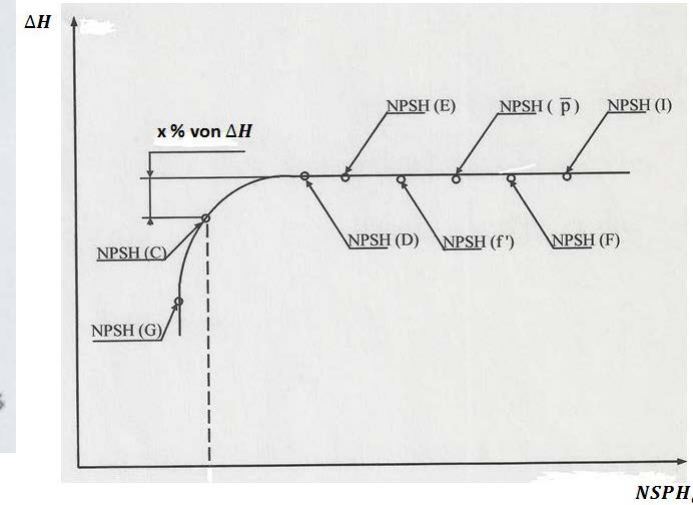
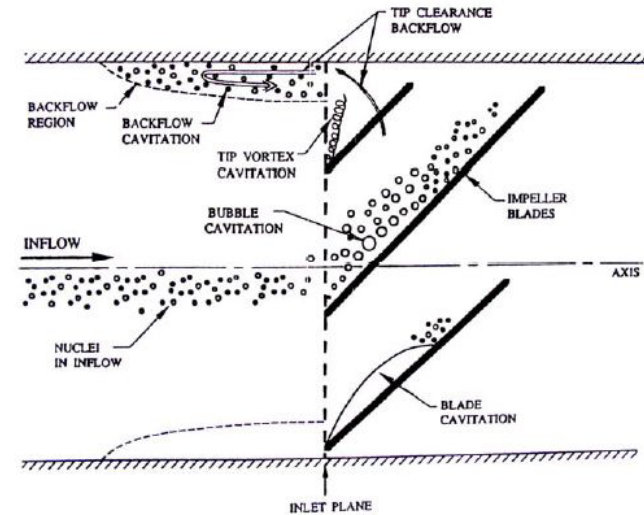
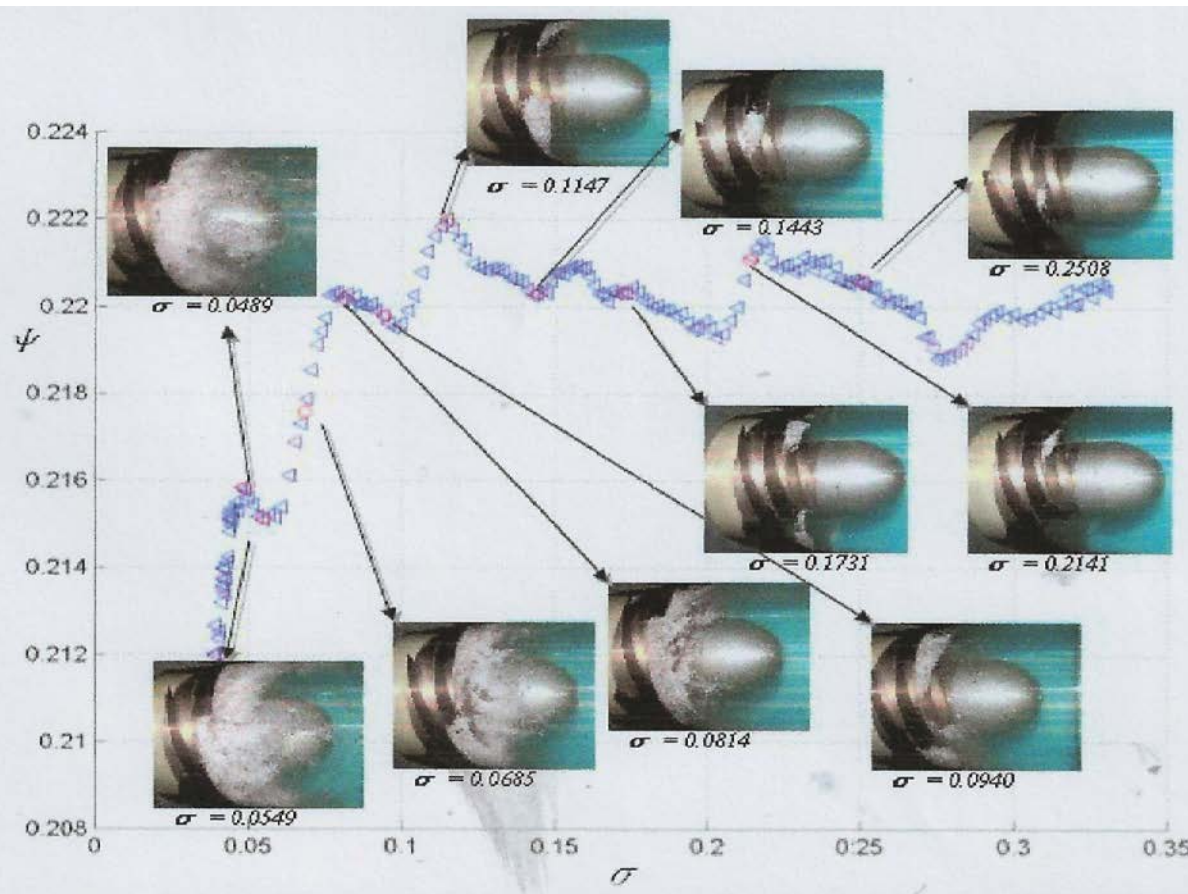
| | LH2-Pump [rpm] | LOX-Pump |
|---------------|----------------|----------|
| Vinci | 90000 | 18000 |
| Vulcain 2 | 36070 | 12300 |
| LE-7A (Japan) | 42000 | 18300 |



LE-7A LOx-Turbopump

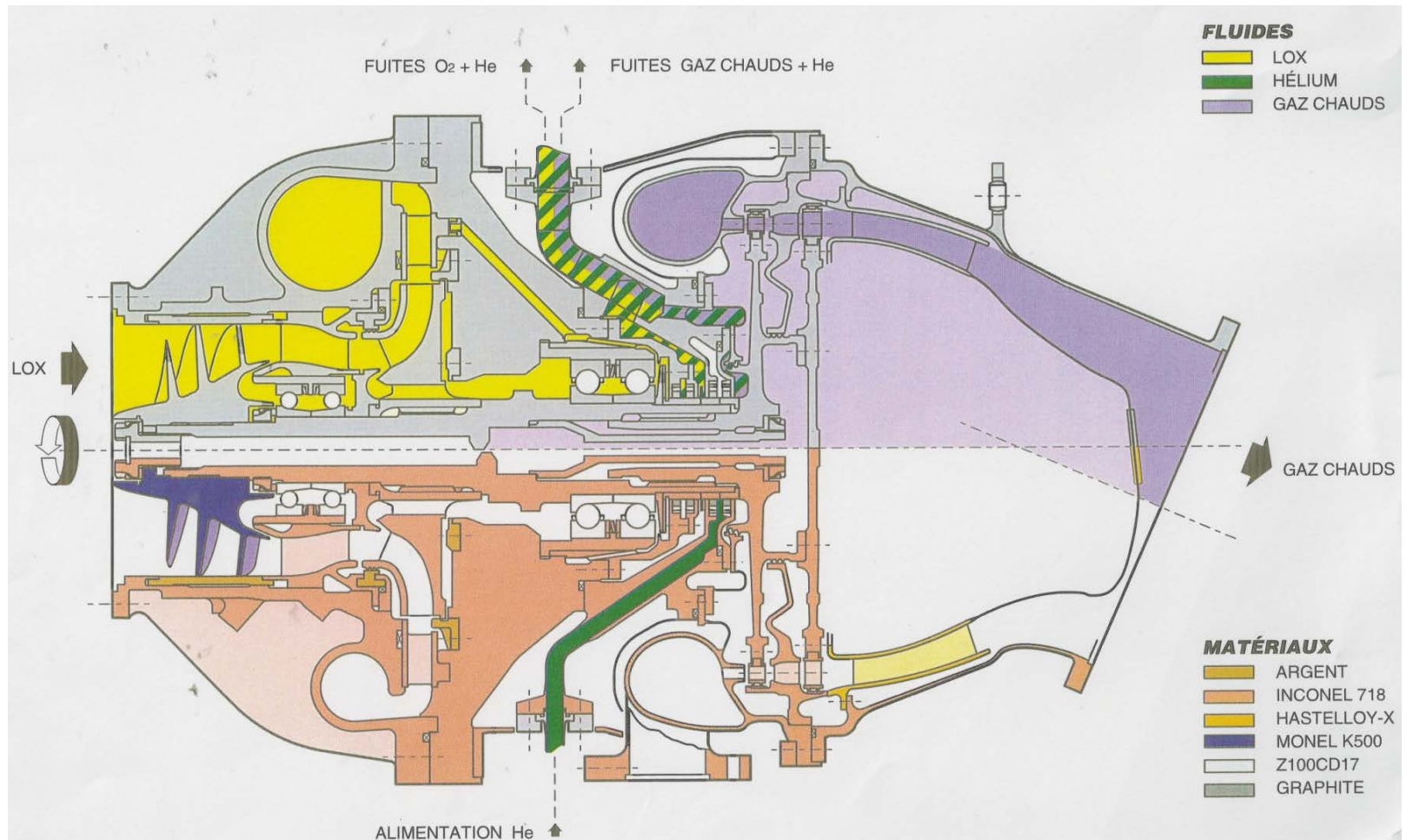


Cavitation at the inducer

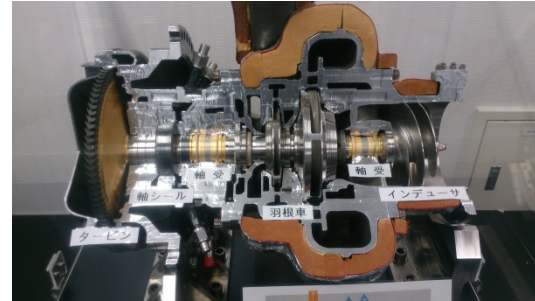


Cavitation Induced Vibration – LOx Turbopump

Fire hazard in case of LOX



Cavitation Induced Vibration: also difficult in LH2



Flashing: state of research

Flashing investigations

- with liquid hydrocarbons → Flash evaporation in jet dominated bubble nucleation; angle of spray as a function of pressure ratio and surface tension

DLR-Lampoldshausen:

- observation of flash evaporation during studies of transient ignition processes with LOX injection into vacuum

Cryogenic propellants (e.g. fuel LH2, CH4) might be already at supercritical conditions before injection

$$R_p = \frac{p_{\text{sat}}(T_{\text{inj}})}{p_c}$$



$R_p=0.949$



$R_p=1.298$



$R_p=2.310$



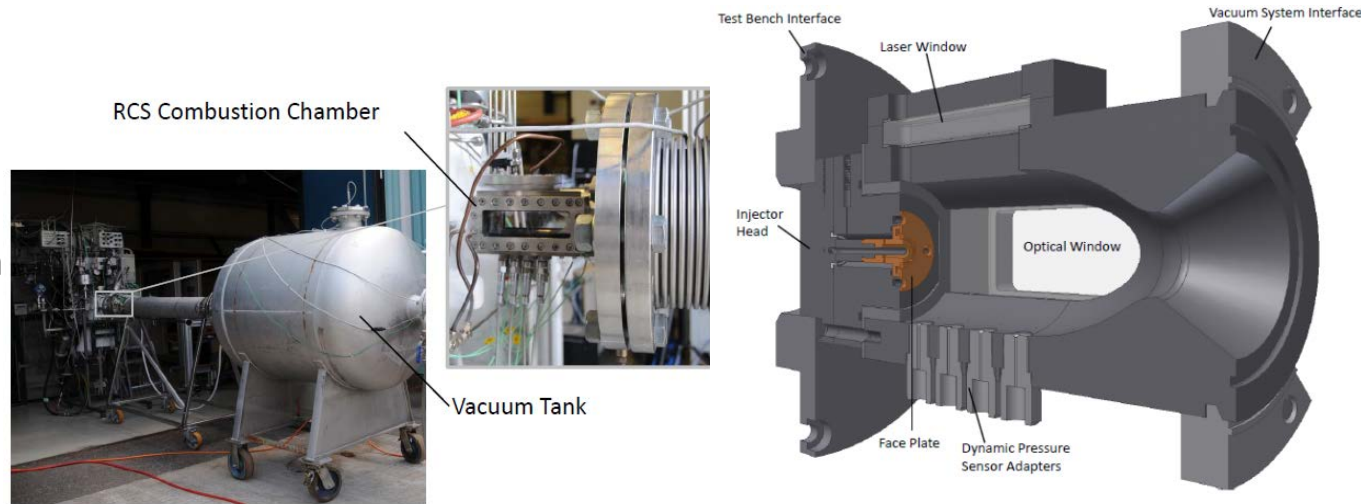
$R_p=37.980$

| | P critical | T critical |
|-----|------------|------------|
| LH2 | 13 bar | 33 K |
| CH4 | 46 bar | 190 K |



Flashing experiment at DLR M3.1

- Test bench M3.1:
 - 400N experimental thrust chamber with vacuum system
 - 2 configurations
 - High-Speed Shadowgraph imaging
 - Injection temperature T_{inj} not adjustable

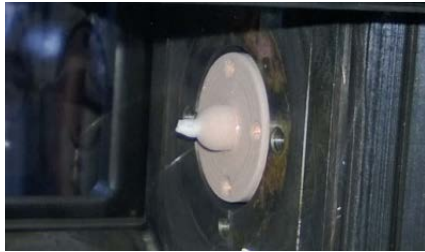


| | Injector diameter D_{inj} [mm] | Injection pressure p_{inj} [MPa] | Injection temperature T_{inj} [K] | Back pressure p_c [MPa] | L/D [-] |
|-------------|----------------------------------|------------------------------------|-------------------------------------|---------------------------|---------|
| config. #1: | 2,4 | 0,25 | 94 | 0,0035-0,03 | 21,9 |
| config. #2: | 0,3 | 1,7 | 113 | 0,0035-0,03 | 1,2 |



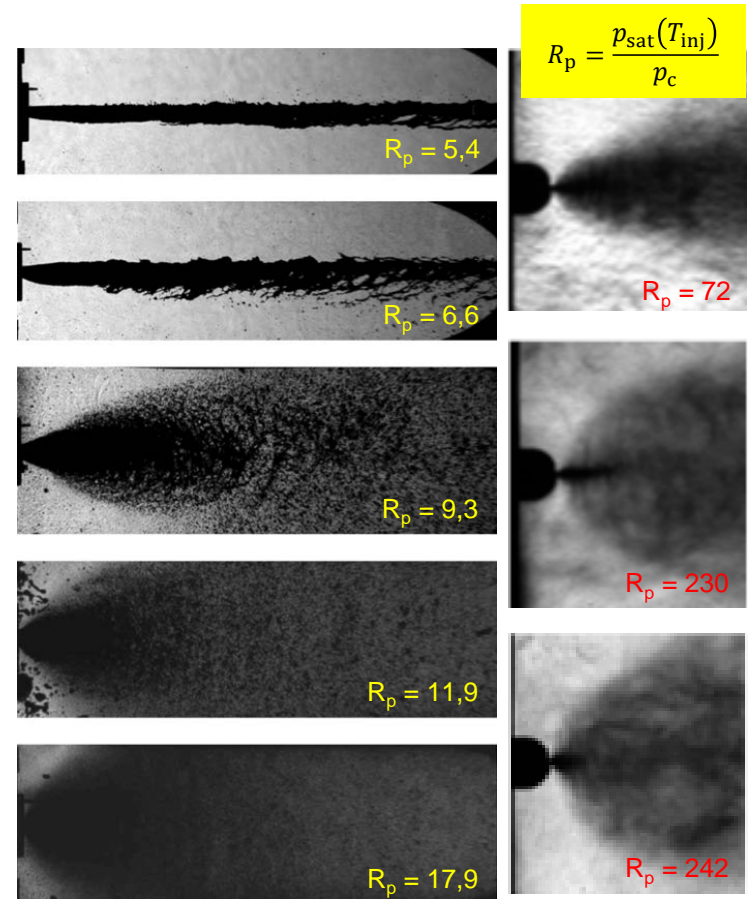
Flashing experiment at DLR M3.1

- Big challenges for the injection system concerning cryogenic environment :
 - cooling of the complete feed system including the injector with homogeneous temperature distribution
 - freezing air humidity → blocked injector or valves



- New cryogenic temperature adjustment and injection system (M3.3) was constructed

➔ detailed investigation of LN2 & LOX flash boiling, see poster *Cryogenic Flash Boiling in Liquid Rocket Engines*



Flash boiling of LOX at M3.1

left: config. #1 ($L/D \approx 22$, $T_{\text{inj}} = 94 \text{ K}$) → heterog. nucleation

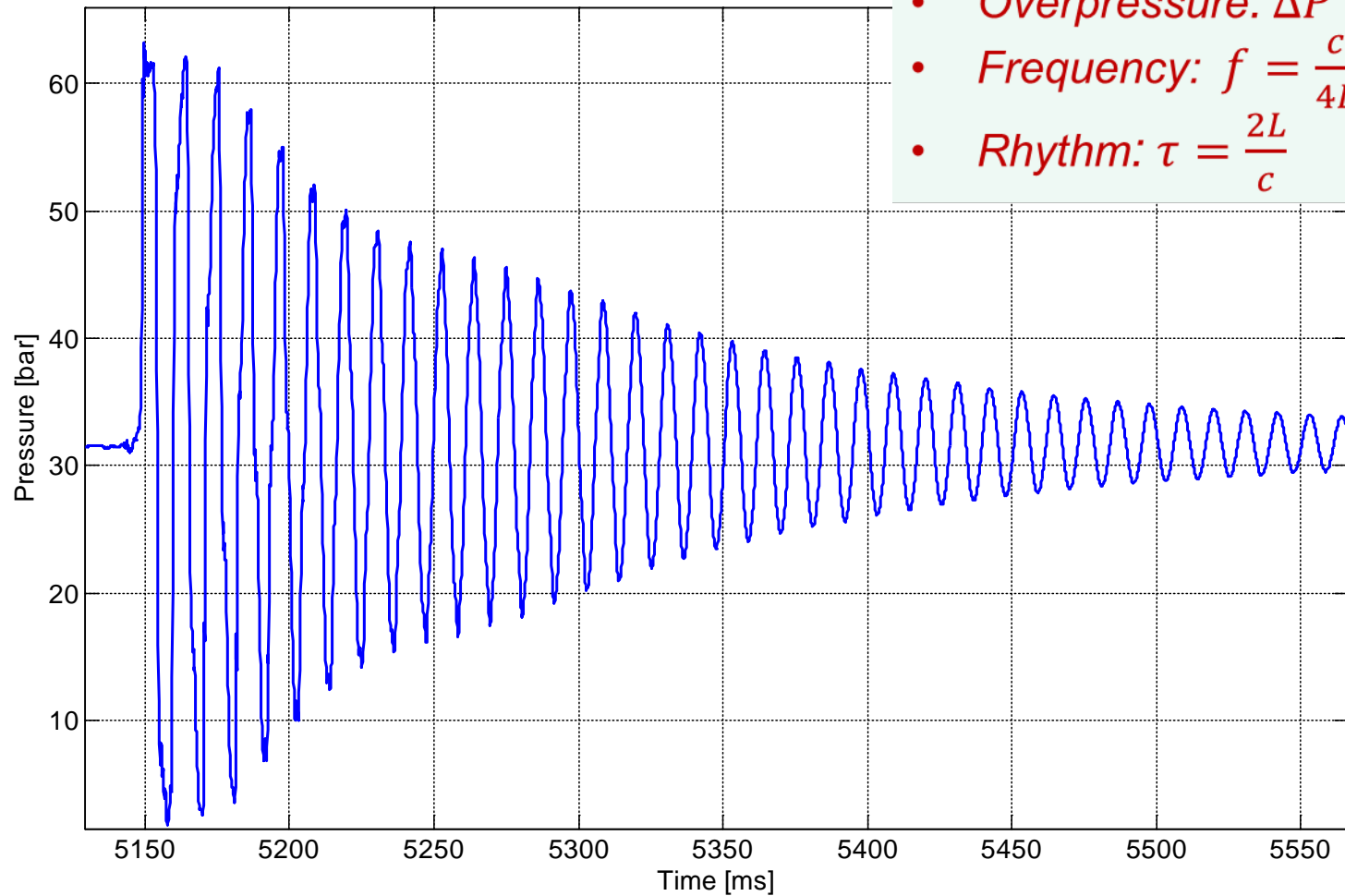
right: config. #2 ($L/D \approx 1$, $T_{\text{inj}} = 113 \text{ K}$) → homog. nucleation



Test Case: Water Hammer with cavitation



Introduction: water hammer



- Overpressure: $\Delta P = \rho c \Delta V$
- Frequency: $f = \frac{c}{4L}$
- Rhythm: $\tau = \frac{2L}{c}$



Introduction: water hammer

In a LRE is of particular importance for LOx feedline (high density and speed of sound)

Cavitation => GOx : ignition hazard due to adiabatic compression

Physics can be very complex:

- Vaporous cavitation
- Gaseous cavitation (dissolved gas release)
- FSI

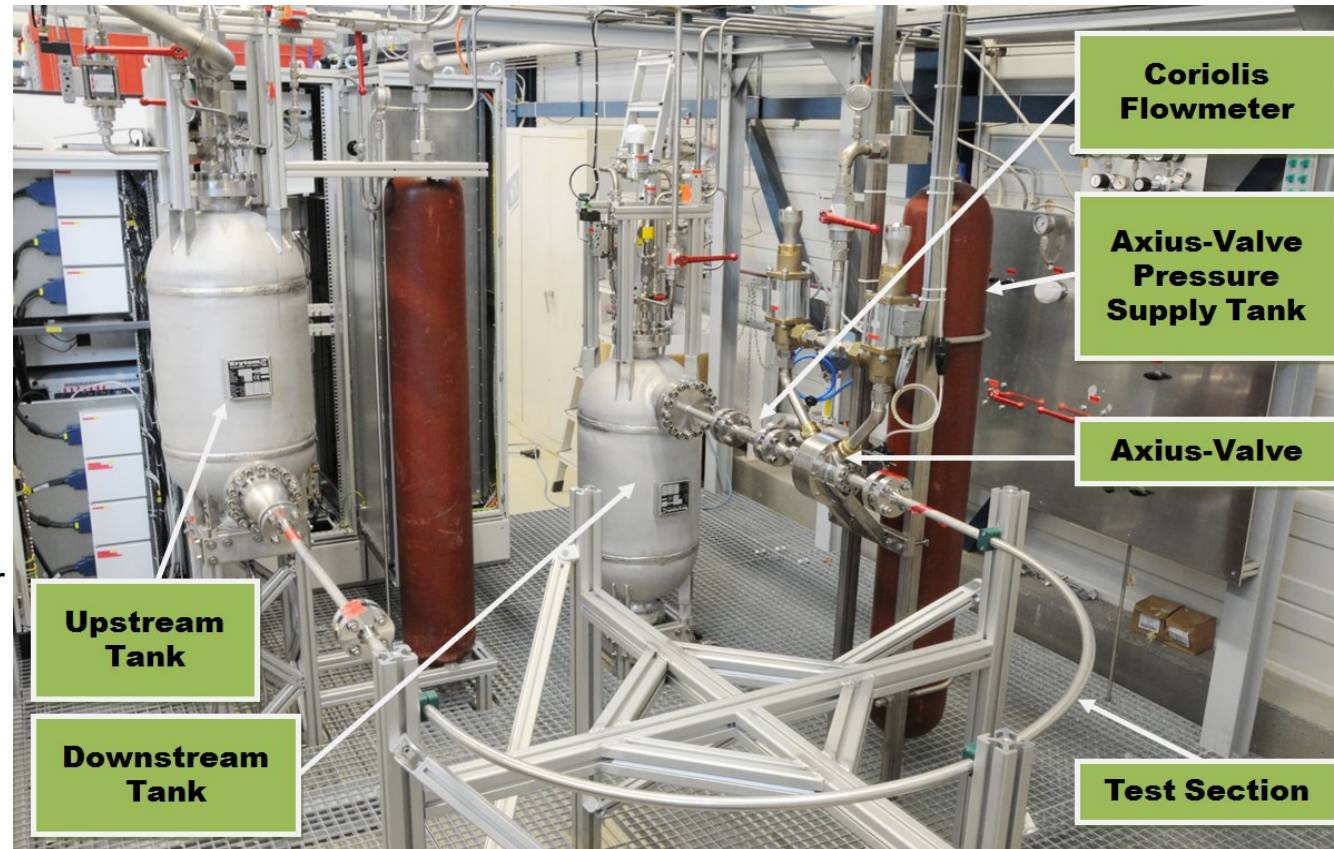
The flow not only two-phase but also *two-component*

Test data needed for validation of the numerical tools.

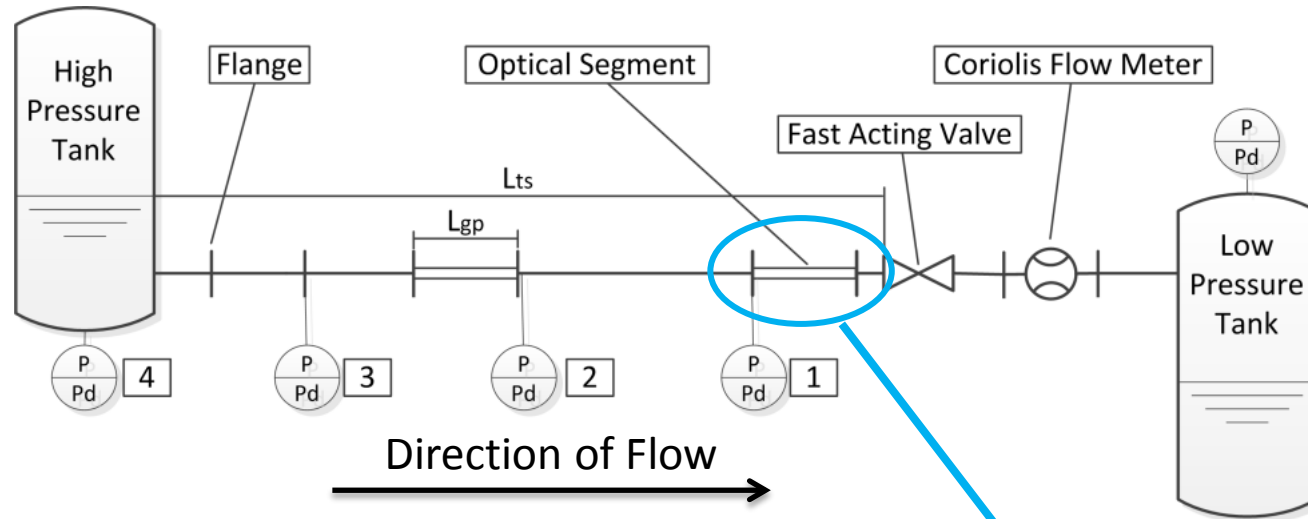


Fluid Transient Test Facility: Water hammer

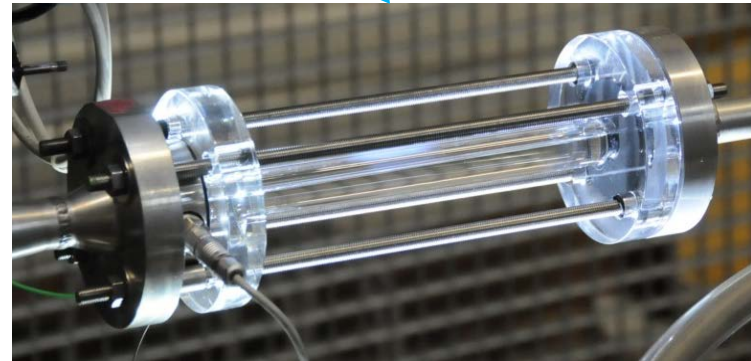
- Fluid: Water, Ethanol
- Tank pressure: 50bar
- Test section Pressure: 100bar
- Test section length, Valve to Tank: 7.34m
- Valve closure time: 11ms
- Pressurizing Gas: N₂, He
- Static and dynamic pressure sensors
- Strain gages and accelerometers for FSI
- Possibility of quartz window for optical investigation (high speed camera up to 100 kfps)
- Modularity for geometry changes, different test-sections



Experimental set-up for flow visualisation

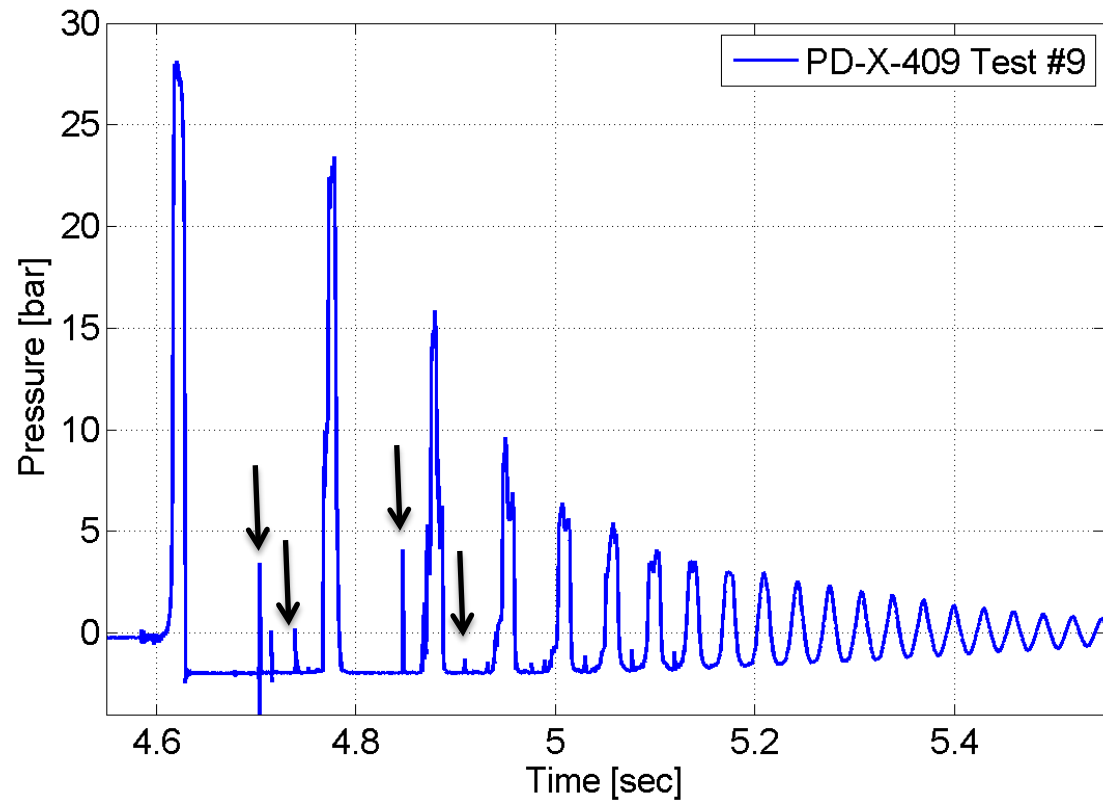


- Photron SA-X: 10000 fps
- Shutter: 1/18604s
- LED backlight
- Optical diffusor
- 710 x 115 pixels
- 0.28 mm/pixel

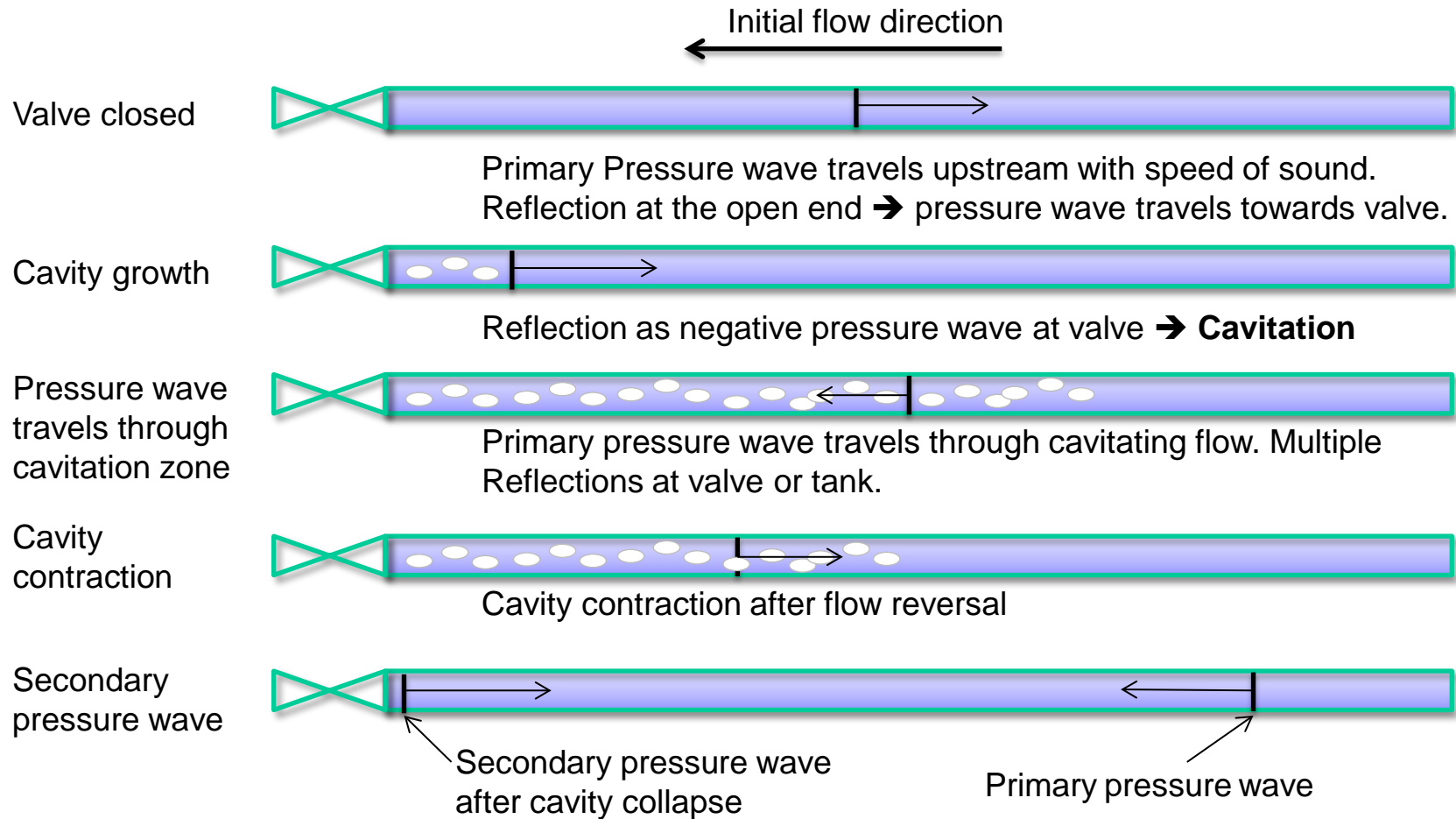


Water hammer with cavitation: pressure spikes

- Only in tests with cavitation
- Test #9:
 - Mean tank pressure: 2bar
 - Flow velocity prior to valve closing: 2.08m/s

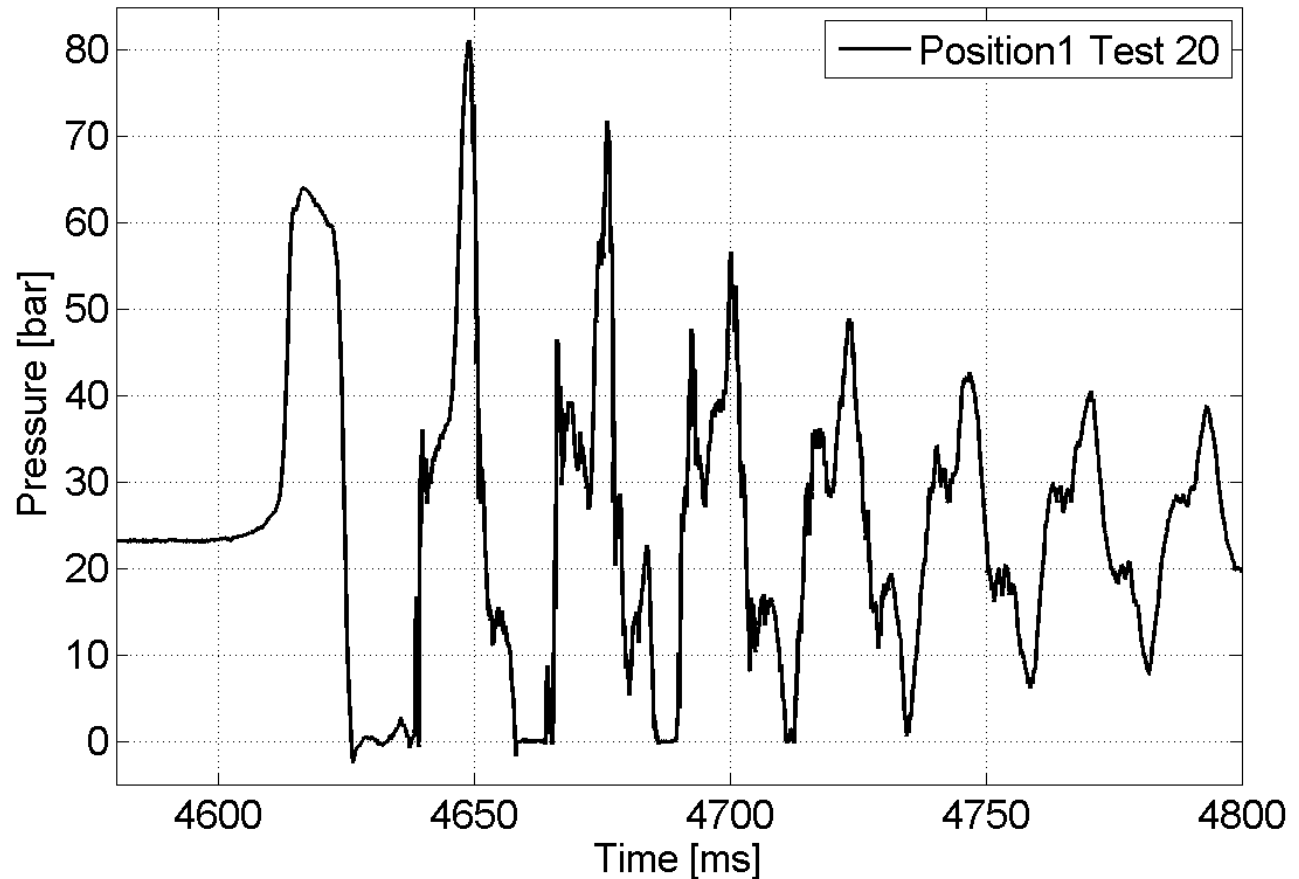


Water hammer with cavitation



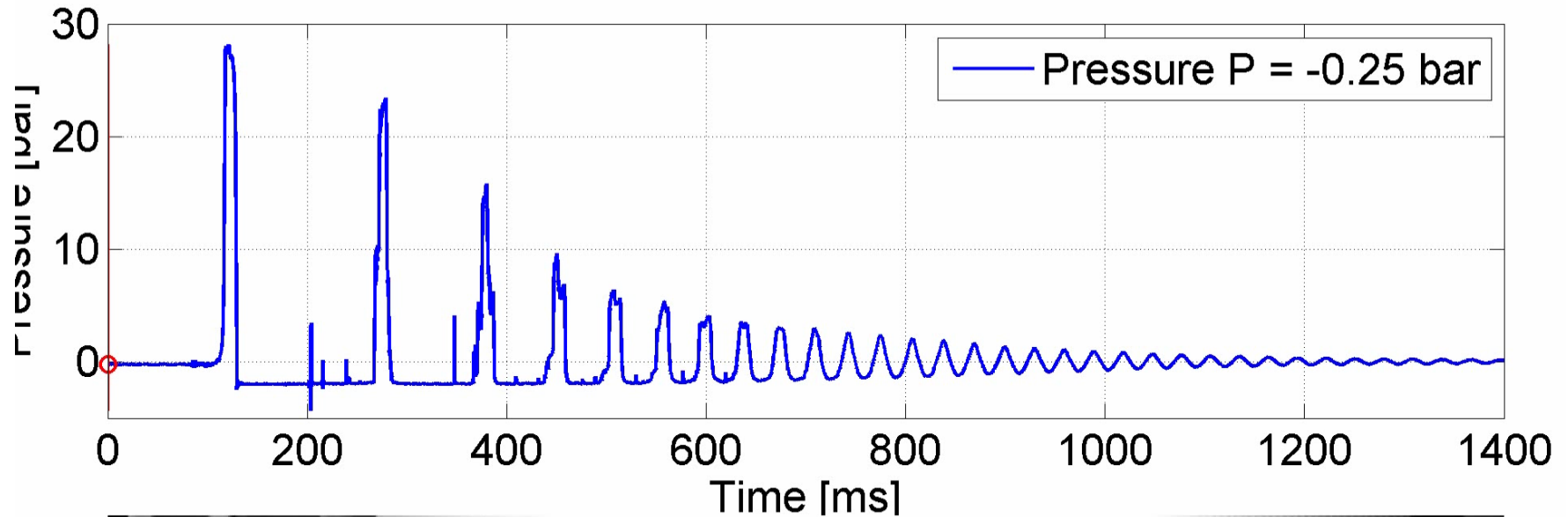
Water hammer with cavitation: higher 2nd peak

- Only in tests with cavitation
- Test #20:
 - Mean tank pressure: 23.8bar
 - Flow velocity prior to valve closing: 3.14m/s



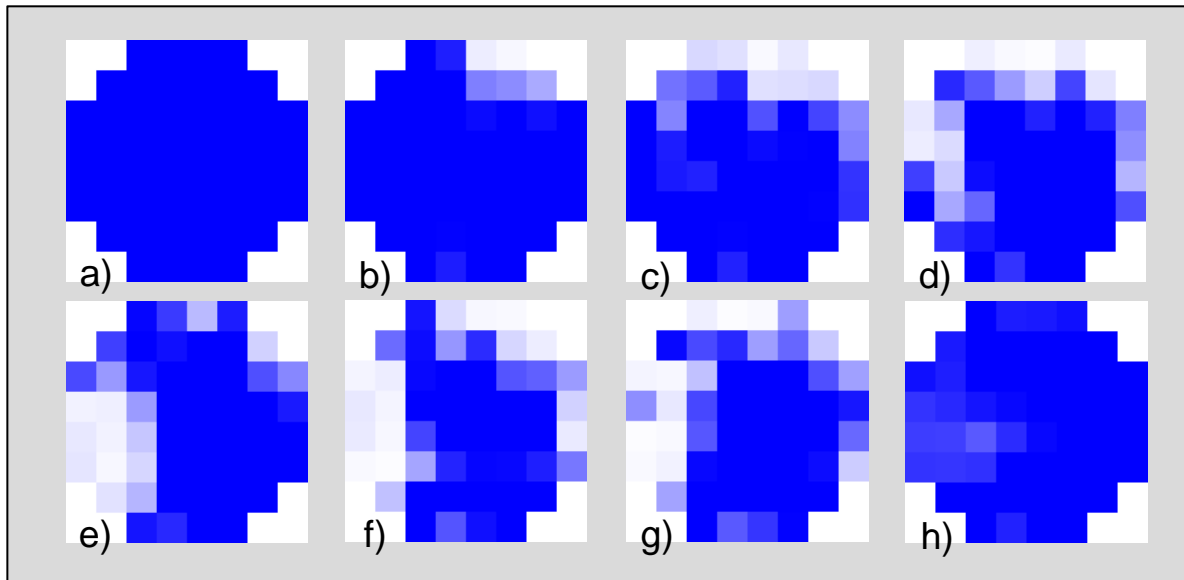
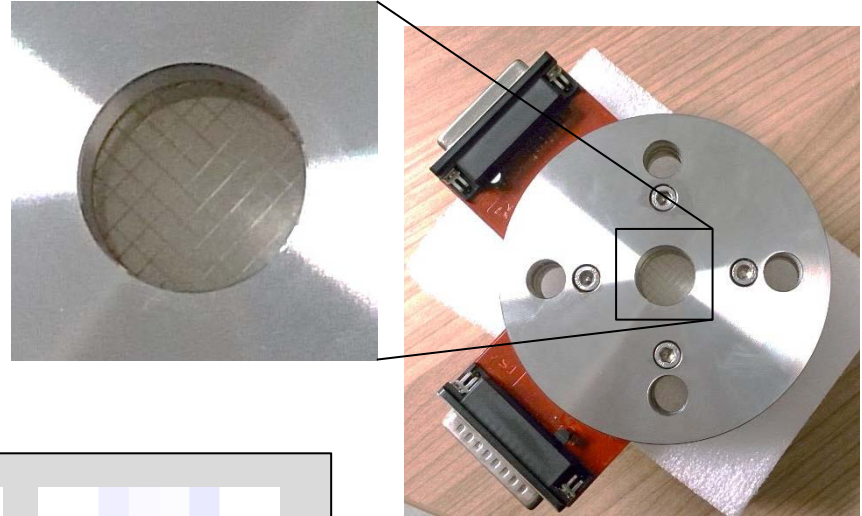
Water hammer with cavitation: flow visualisation

Pressure sensor PD-X-409 time $t = 0$ ms

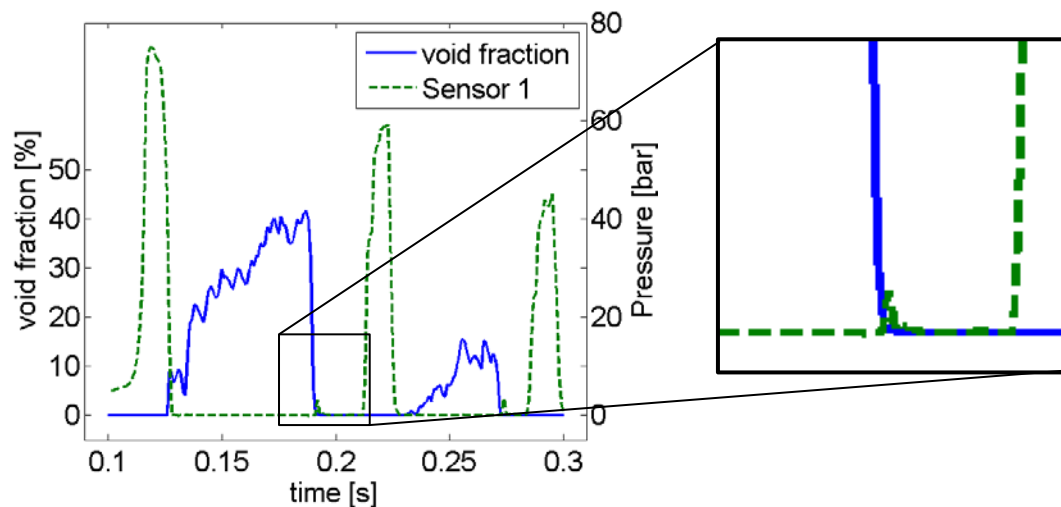
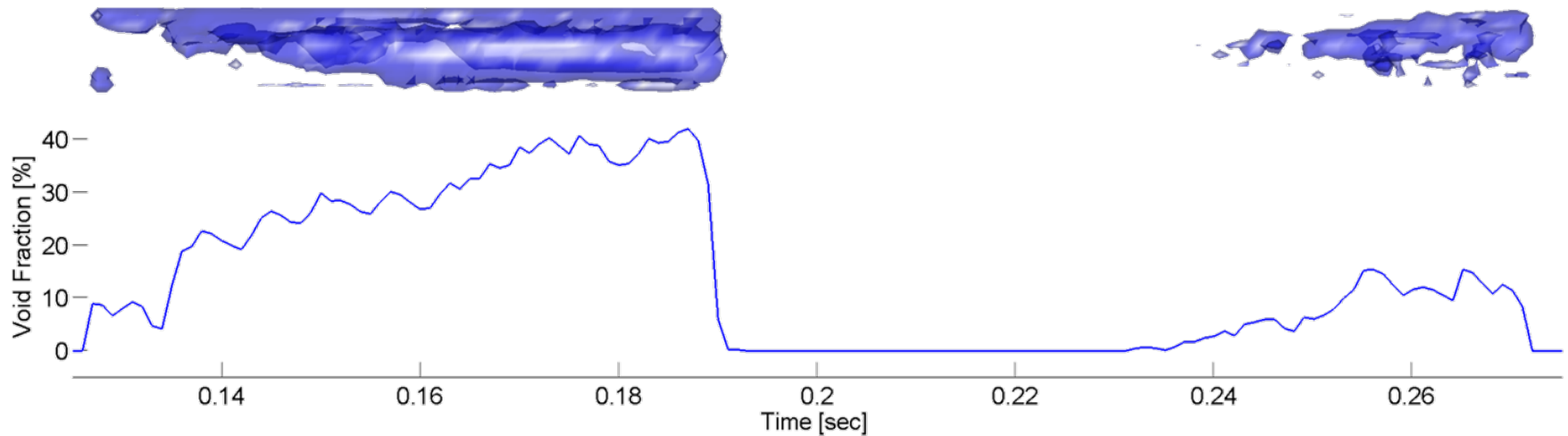


Water hammer visualisation technique: wire mesh sensor

- Sensor from Helmholtz Zentrum Dresden Rosendorf (HZDR)
- Two-dimensional void fraction over the cross section with a frame rate of 10000 fps
- 8x8 grid: 64pixel



Water hammer: wire mesh sensor



| | |
|-----------------------------|------|
| Test # | 9 |
| Mean tank pressure (bar) | 7 |
| Initial flow velocity (m/s) | 5.15 |

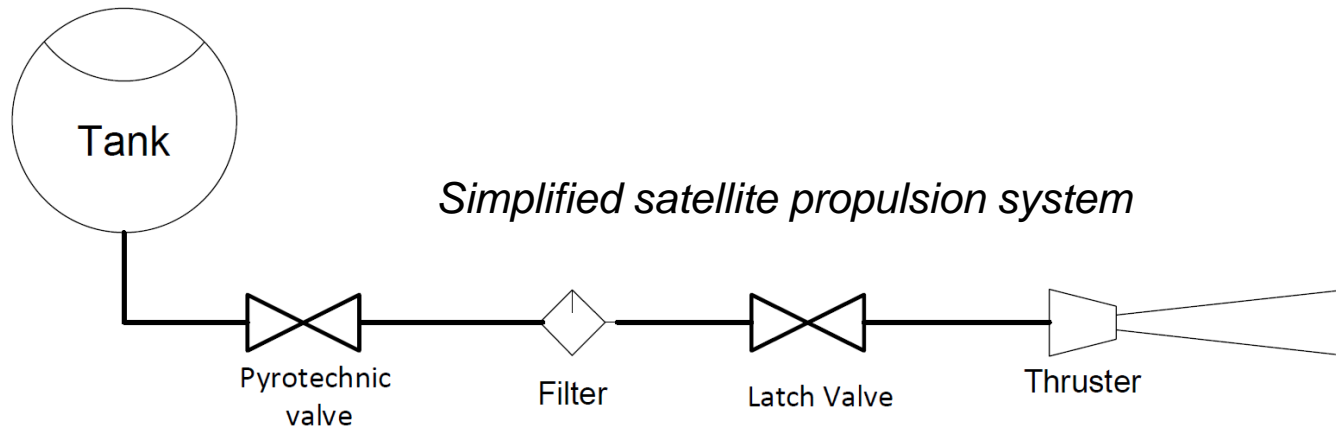


Test Case: Priming



Introduction: what is priming ?

Priming: opening of the isolation valve causes the filling of the evacuated feedline => severe pressure peak

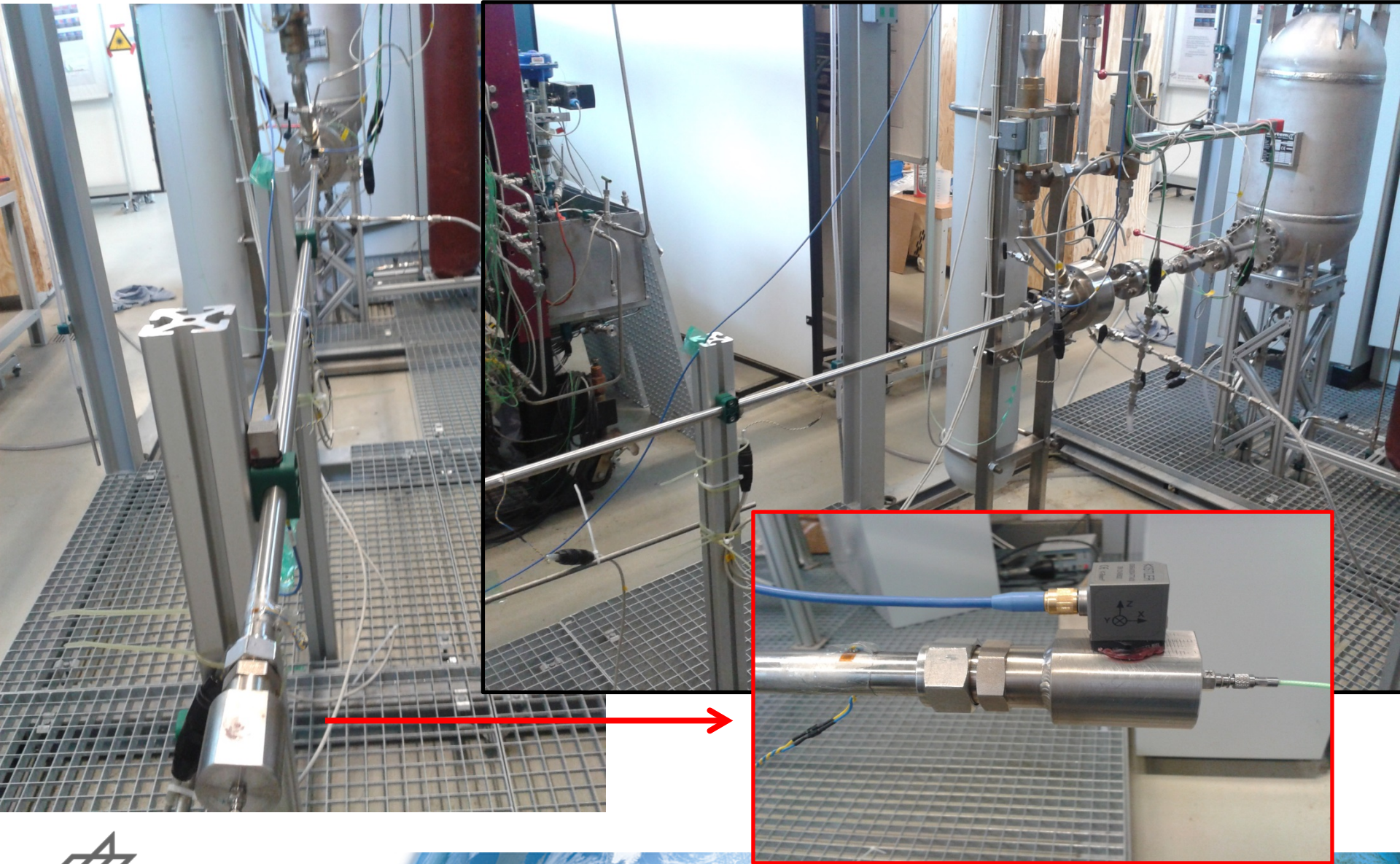


Pressure peak > 250 bar =>

1. Structural failure
2. Adiabatic compression detonation (monopropellant)

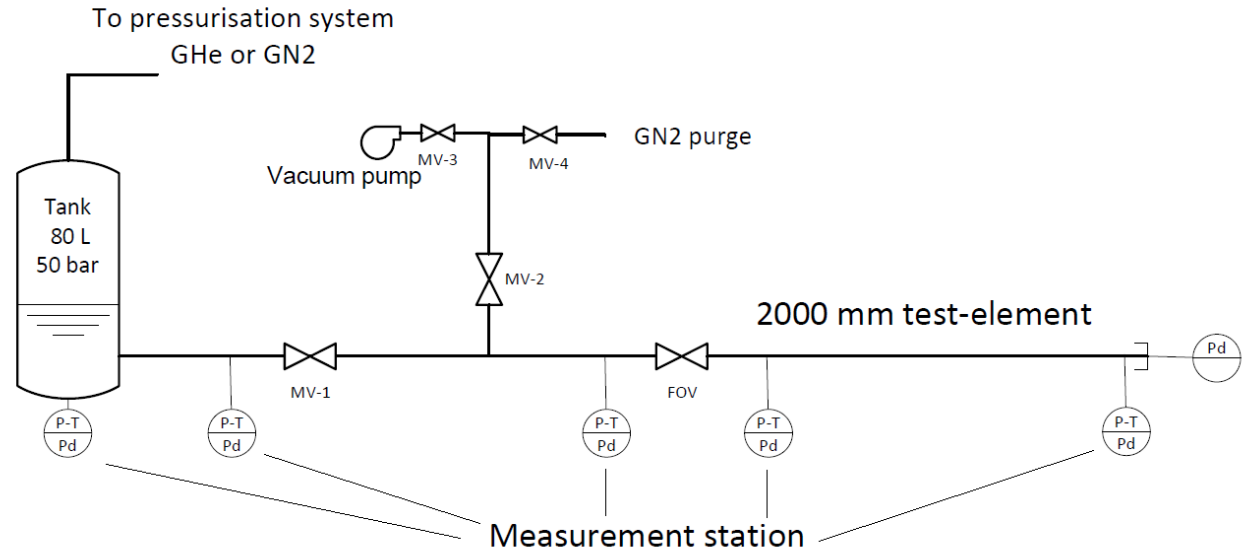


M3.5 Fluid transient Test-bench : priming configuration



Test procedure

- Purging GN2 via MV-2
- Evacuate
- Close MV-2 and FOV
- MV-1 open, manual prime
- Test run



*Test-element is a OD 2000mm long 19x1.44 mm pipe, stainless steel
High mass flow, e.g. ATV feedlines*

For satellite usually 6.35 mm x 0.41 mm titanium alloy



Test-matrix: effect of dissolved gas (gaseous cavitation, *aka Coca-Cola effect*)

tank pressure: 20 bar



| P line, water ($P_{\text{vap}} = 20 \text{ mbar}$) | P line, ethanol ($P_{\text{vap}} = 42 \text{ mbar}$) |
|---|---|
| Deaerated | Deaerated |
| 1 bar GN2 saturated | 1 bar GN2 saturated |
| 10 bar GN2 saturated | - |
| 20 bar GN2 saturated | 20 bar GN2 saturated |
| 20 bar GHe saturated | - |

Dissolved gas content

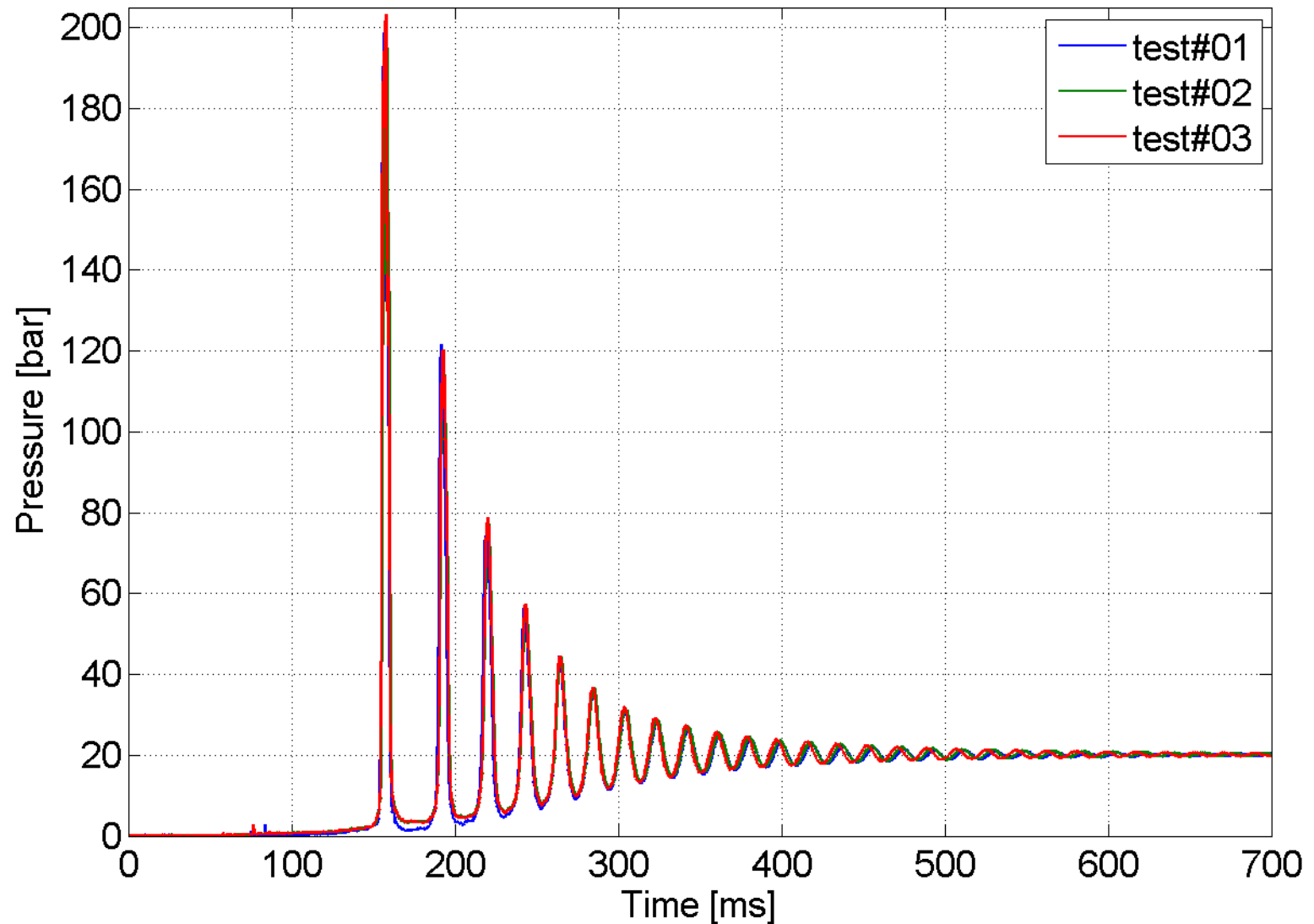
| Gas saturation pressure | water | ethanol |
|-------------------------------|------------|------------|
| 1 bar | 20.8 mg/kg | 220 mg/kg |
| 20 bar | 380 mg/kg | 4200 mg/kg |

Tests are repeated 3 times to examine reproducibility

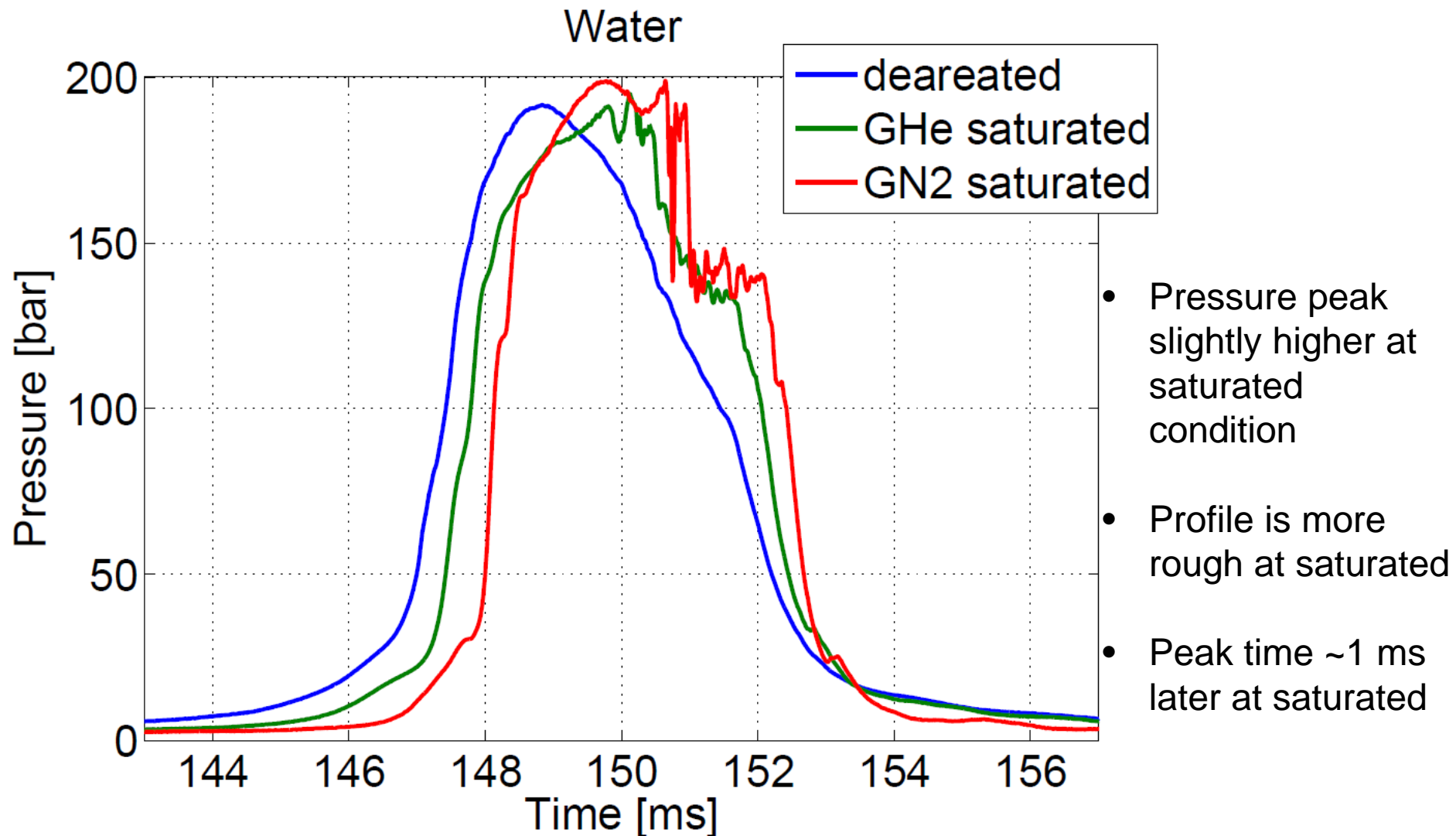


Priming, example

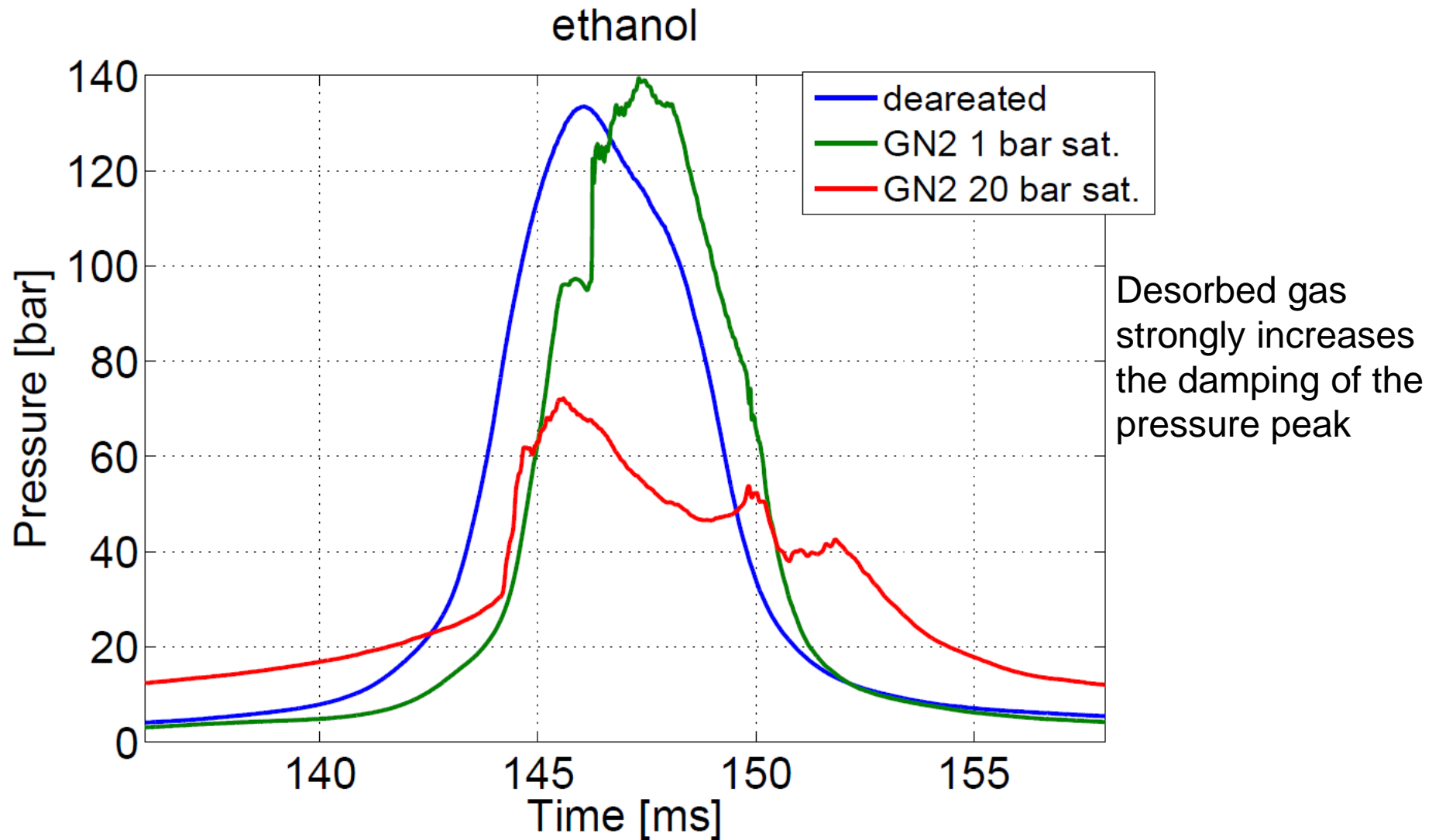
Pressure profile sensor : PDX507



Results for water



Results for ethanol



Priming

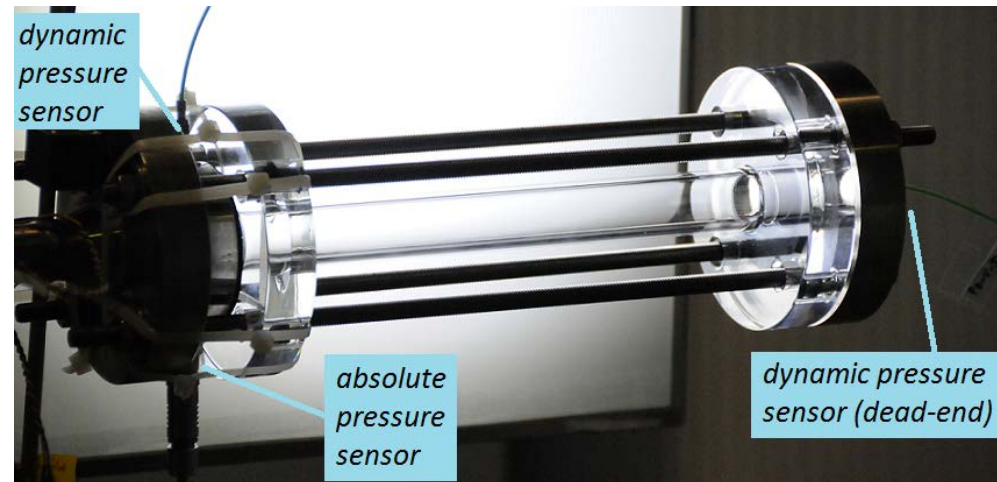
The effect of the dissolved gas is clear: but how does it act?

Hypothesized mechanism:

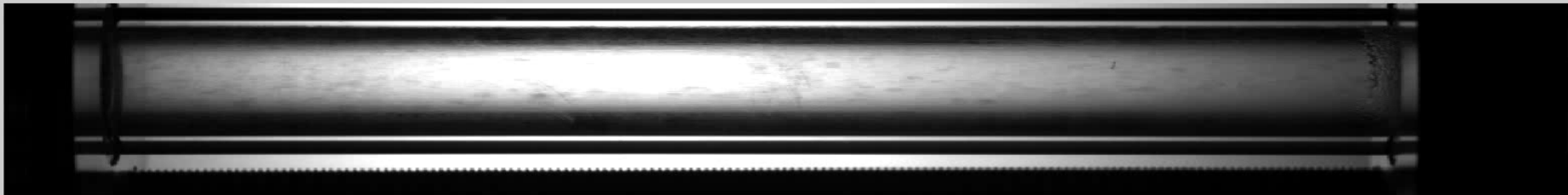
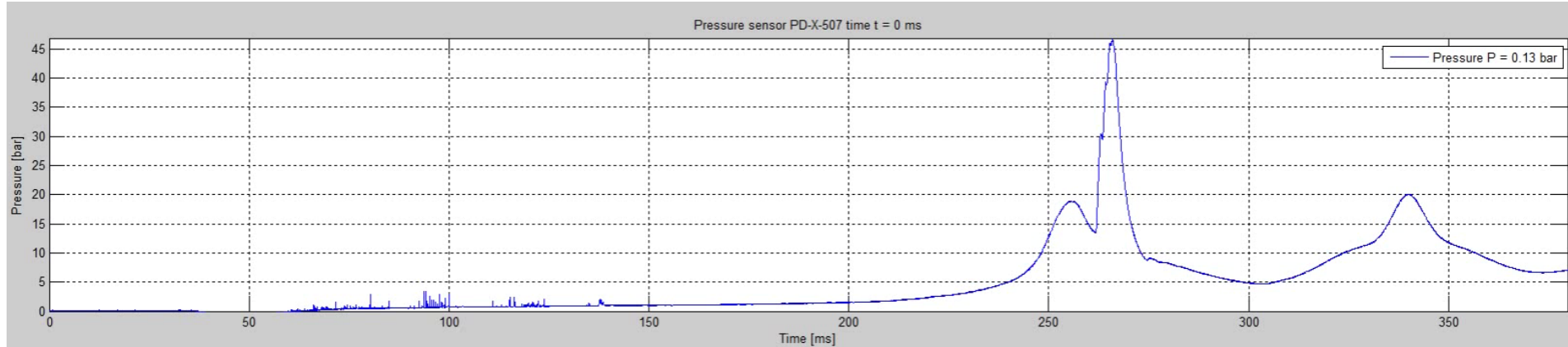
the desorption of the dissolved gas will create gas pocket inside the liquid, and the later could be modelled as multiple slugs that impinge one on the others resulting in the step-plateau profile

We need to see inside!

quartz pipe at the dead-end
+ high speed camera



Priming



Test conditions:

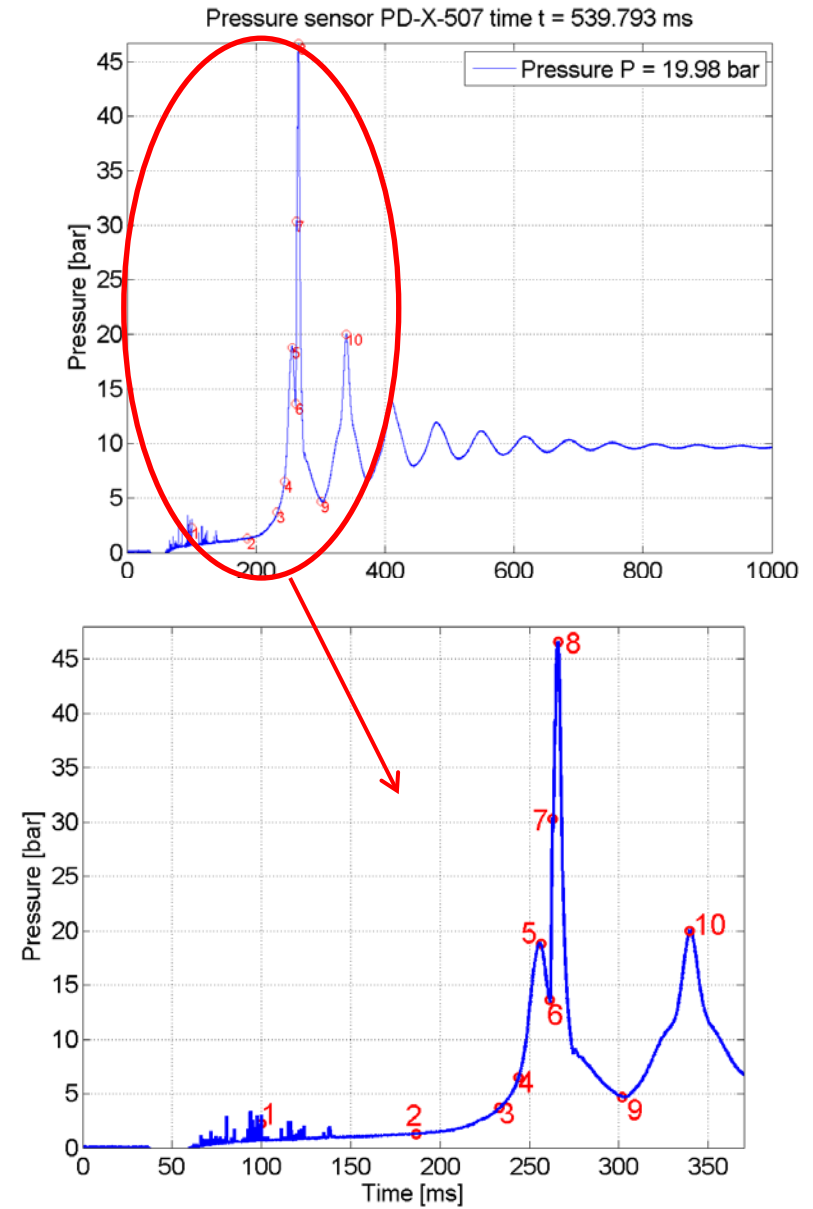
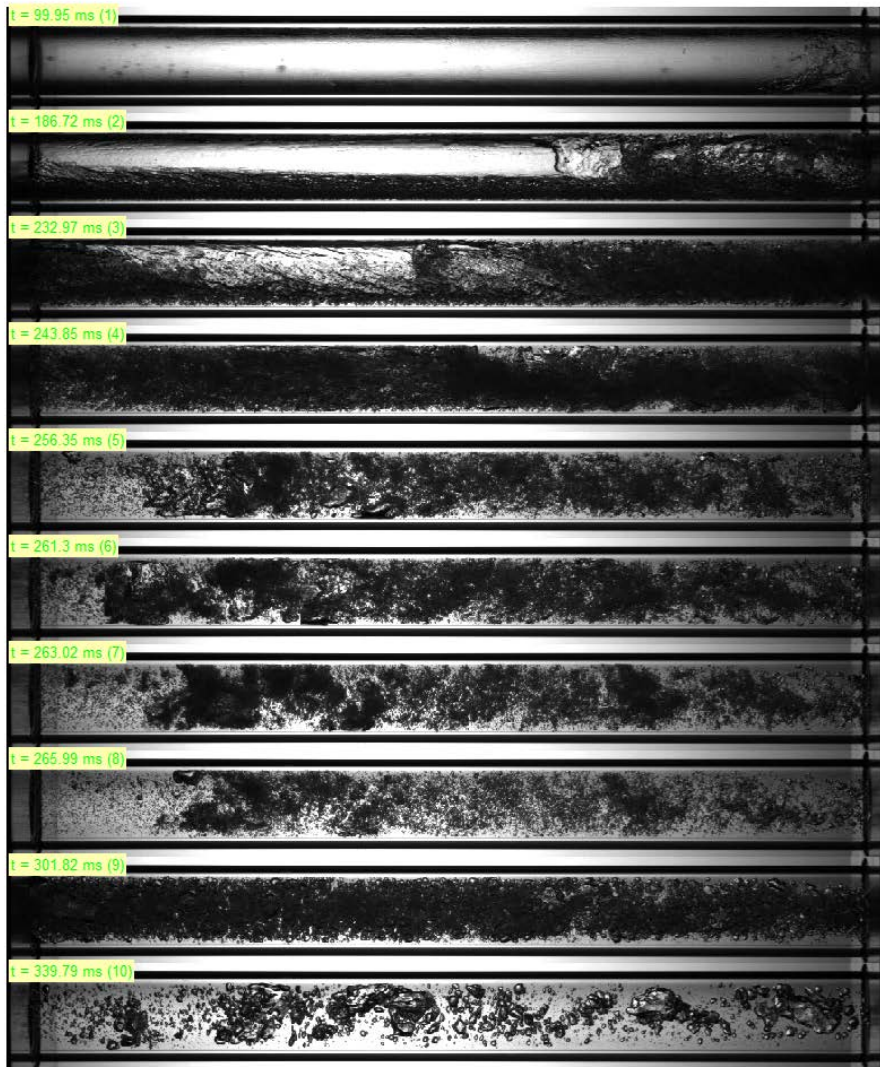
- Tank pressure : 9 bar
- saturated water
- Line pressure: 12 mbar

Camera setting:

- Frame rate: 19200 fps
- Resolution: 1024x84
- 250 ms at 120 fps (x160)



Priming



Priming/conclusions

Decreasing the line pressure causes *higher pressure peak, higher wave frequency, less wave attenuation* (as expected) but only down to P_{sat} :

- when the P line $< P_{sat}$ no remarkable differences any more

The effect of the dissolved gas is not negligible:

the desorption of the dissolved pressurizing gas affects the profile of the pressure peak :

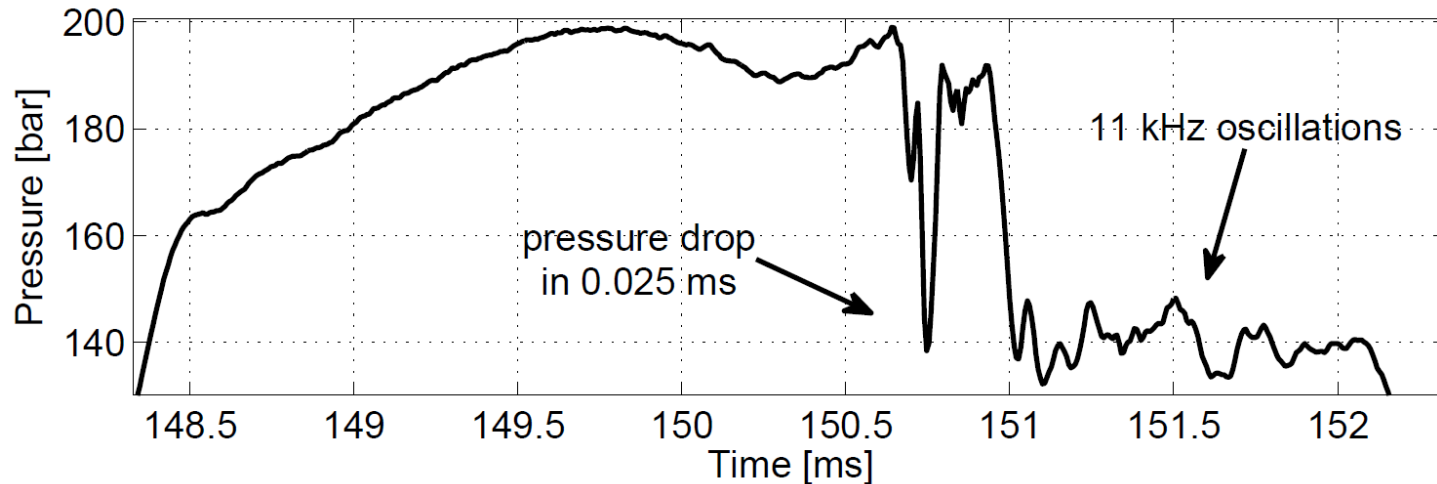
- rougher shape with a multiple step-plateau profile
- pressure peak is ~ 1 ms delayed
- pressure peak can be slightly higher!

Hypothesized mechanism : desorption of gas will create gas pocket forming multiple liquid slugs



Cavitation and bubble collapse

A strong pressure spike appears during the evolution of the first peak => cavitation



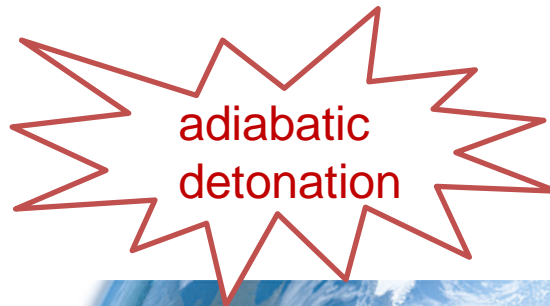
Cavitation occurred only with dissolved gas in liquid:

- 1 bar GN2 sat. : $P_{\text{tank}} \geq 20$ bar
- 20 bar GN2 sat. : $P_{\text{tank}} \geq 16$ bar
- 20 bar GHe sat. : $P_{\text{tank}} \geq 26$ bar



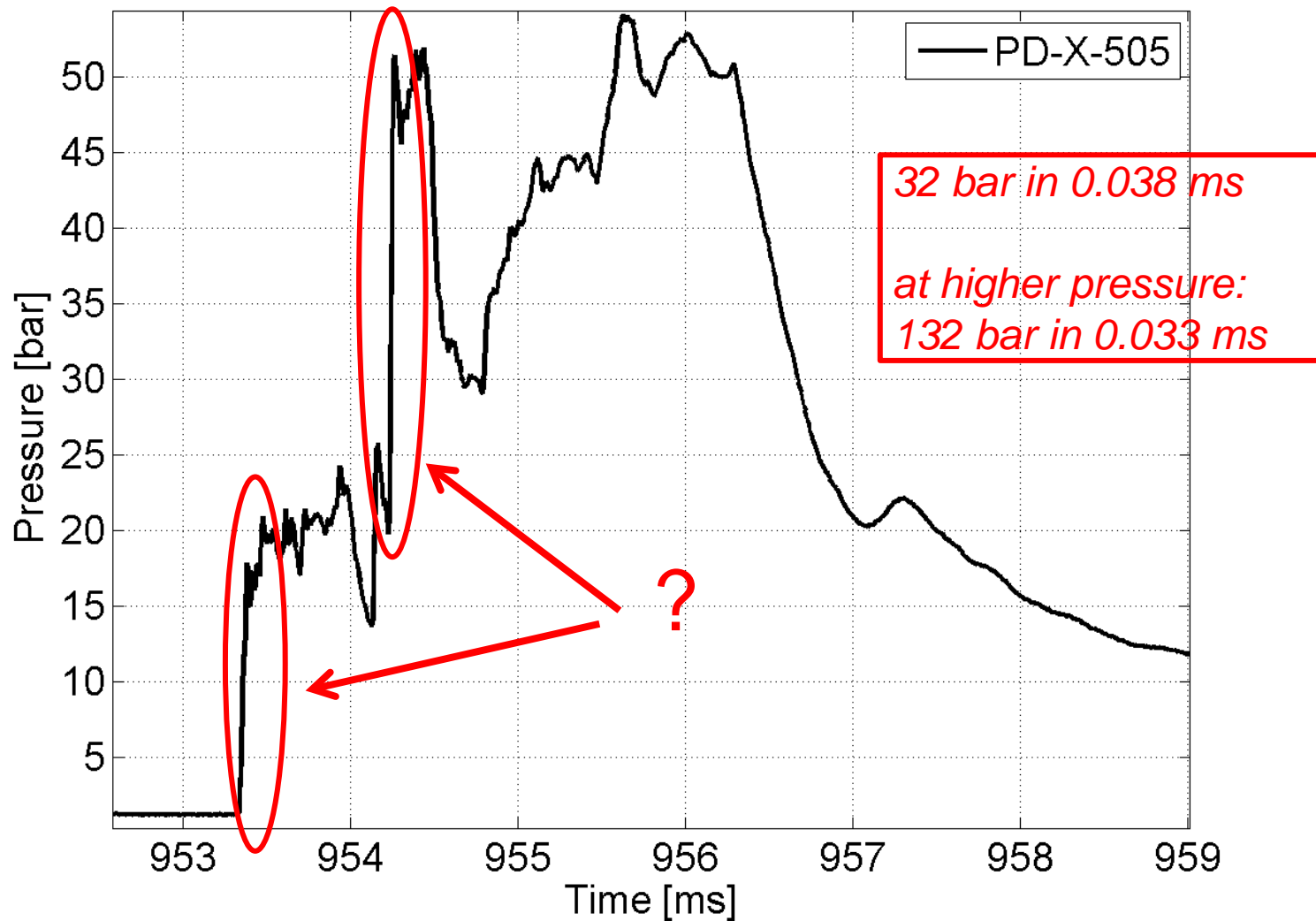
Clear effect of pressurizing conditions on the onset of cavitation

*in fact: nucleation rate increases;
surface tension decreases...*

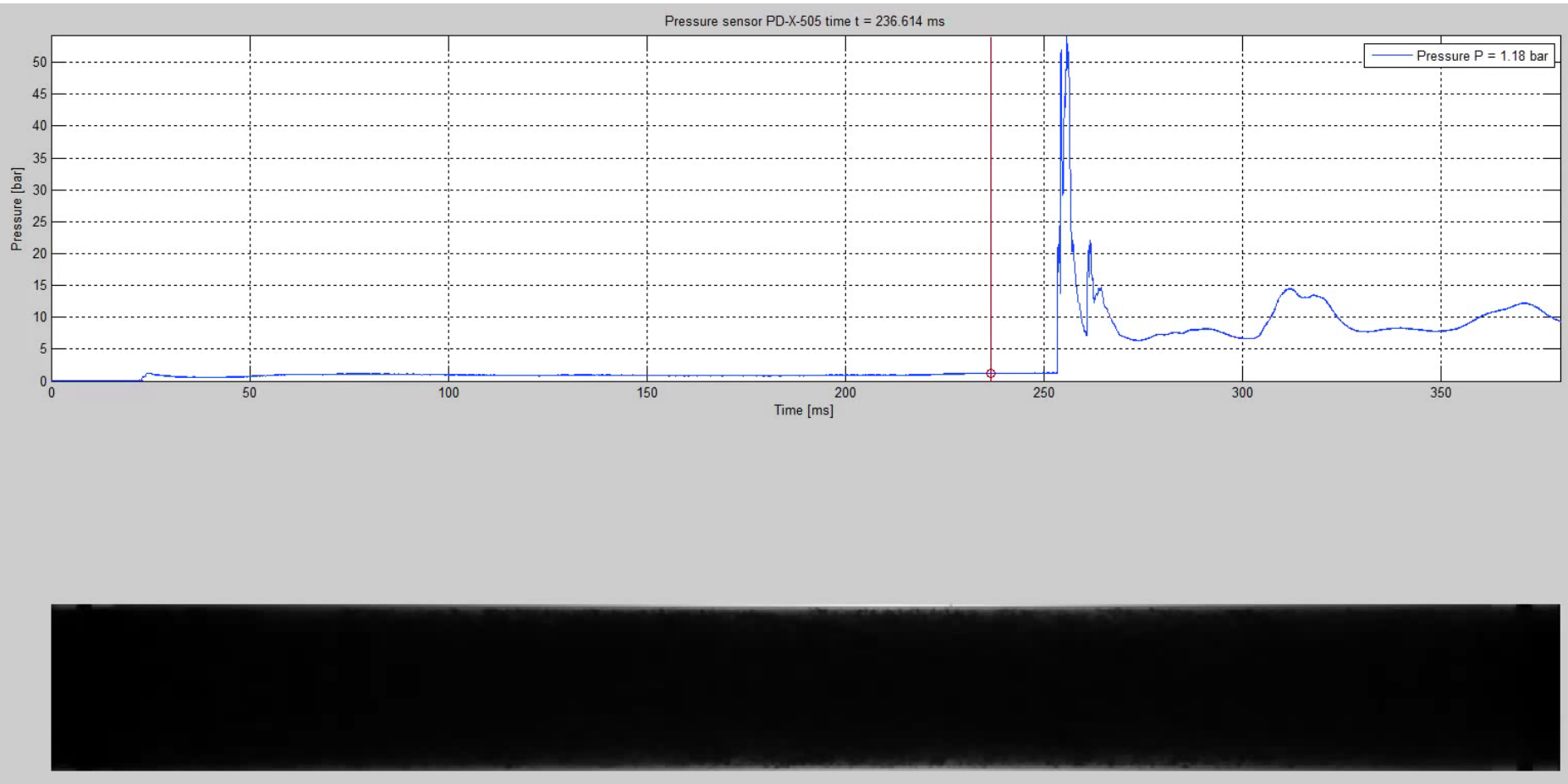


Priming: steep pressure gradient

Pressure after run valve



Priming: HSI

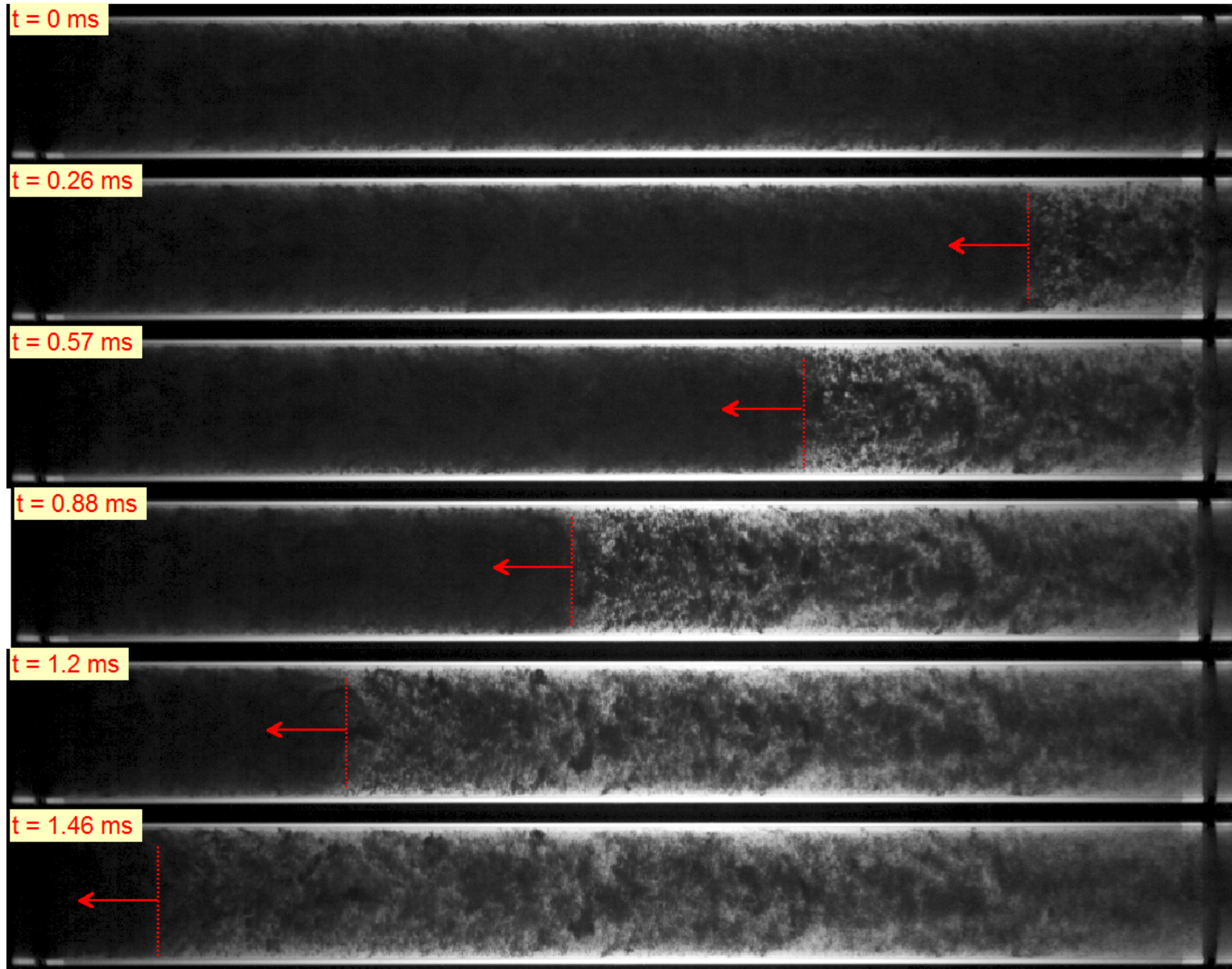


Cavitation-induced shock wave

Wave speed:
150 m/s

Mach 4 !

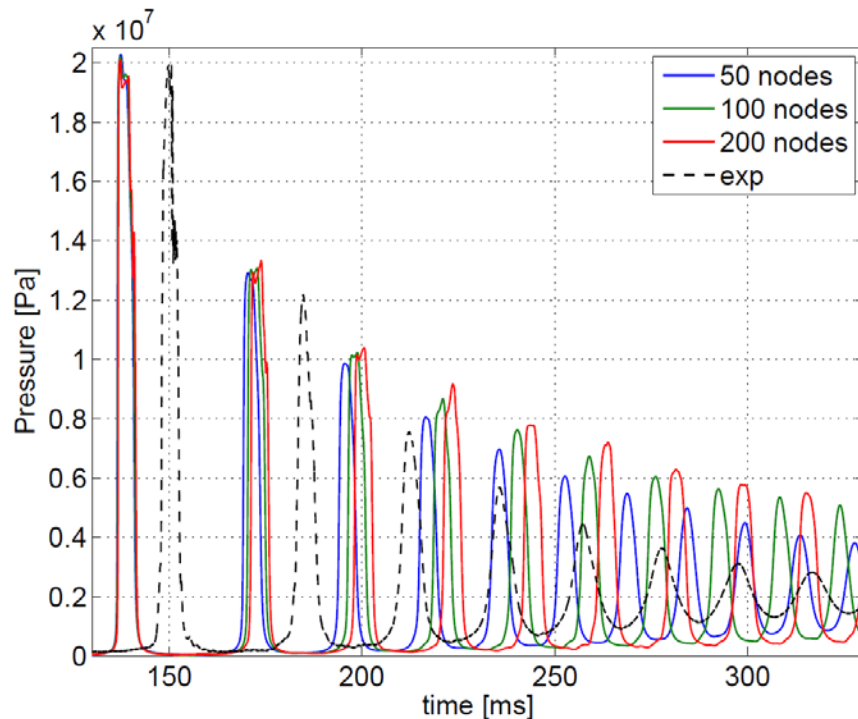
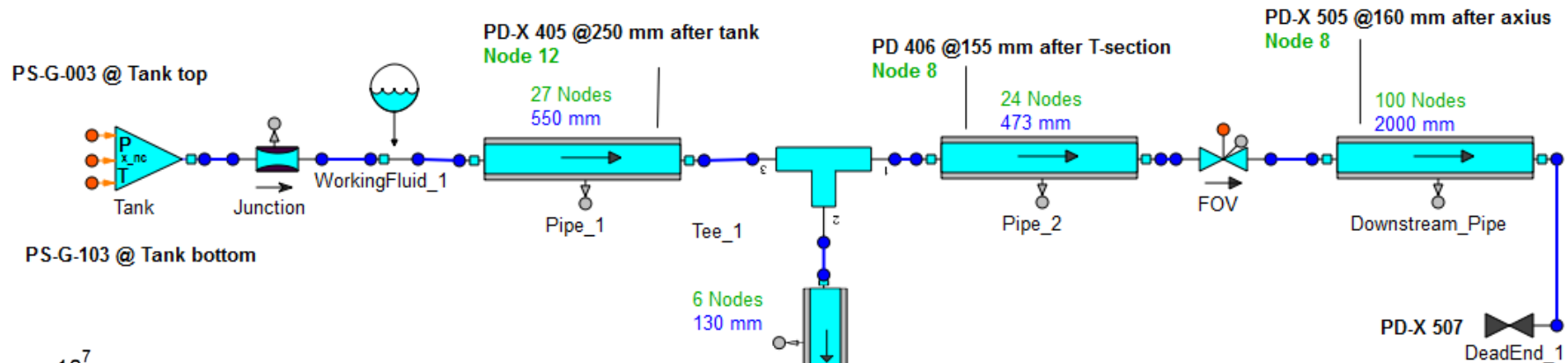
C. E. Brennen,
*Cavitation and
bubble dynamics*.
Oxford University
Press, 1995



Numerical Modelling



Numerical modeling with EcosimPro/ESPSS



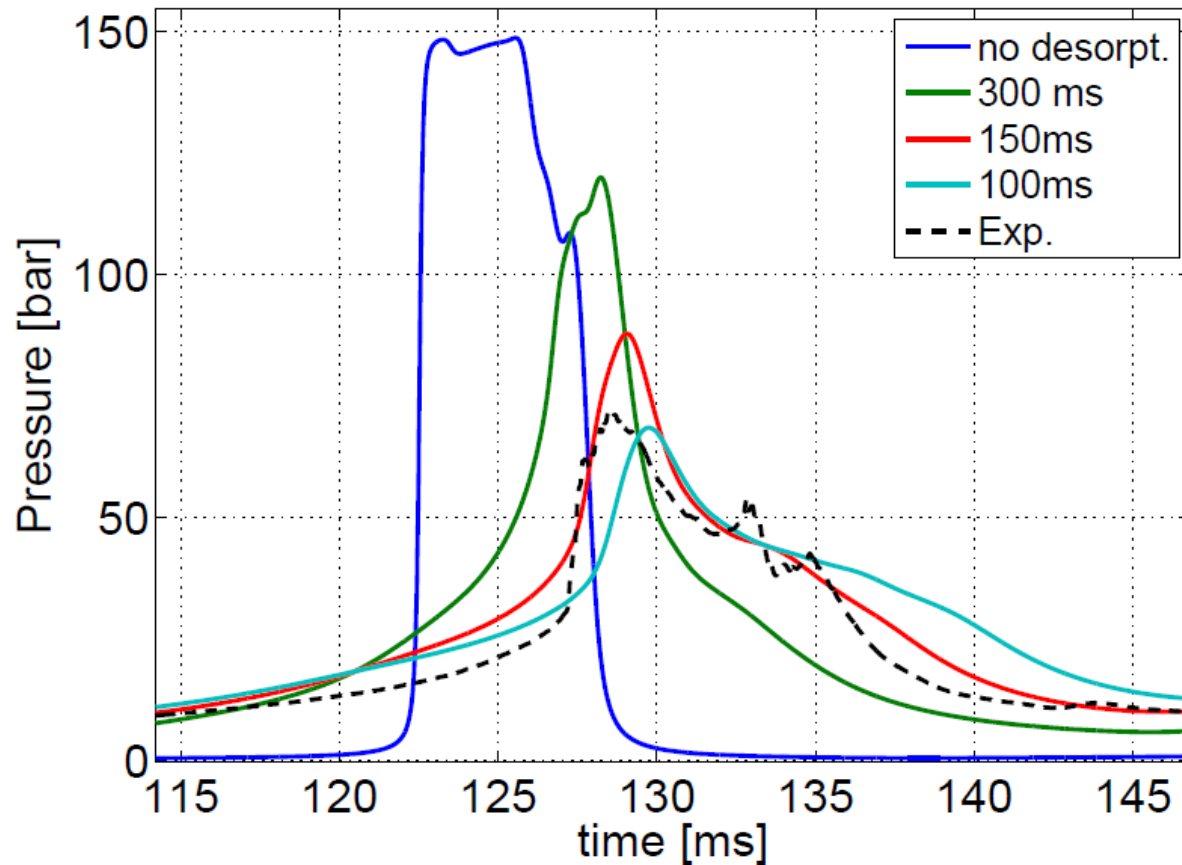
1D transient two-phase two-component flow, based on fluid conservation equations

Used in the design of propulsion systems, in particular for the pressurizing subsystem and feedline subsystem

Modeling of gas desorption

$$\dot{m}_{des} = C(P_{gas,sat} - P)$$

ethanol, dissolved mass fraction GN2: 4200e-6



A simple gas release model can be included: it needs some empirical parameters, e.g. the desorption time constant

It definitely improves the simulation in terms of pressure peak



Numerical Simulation of two-phase flow

Numerical analysis allows to investigate physical quantities which are difficult or impossible to measure, e.g. :

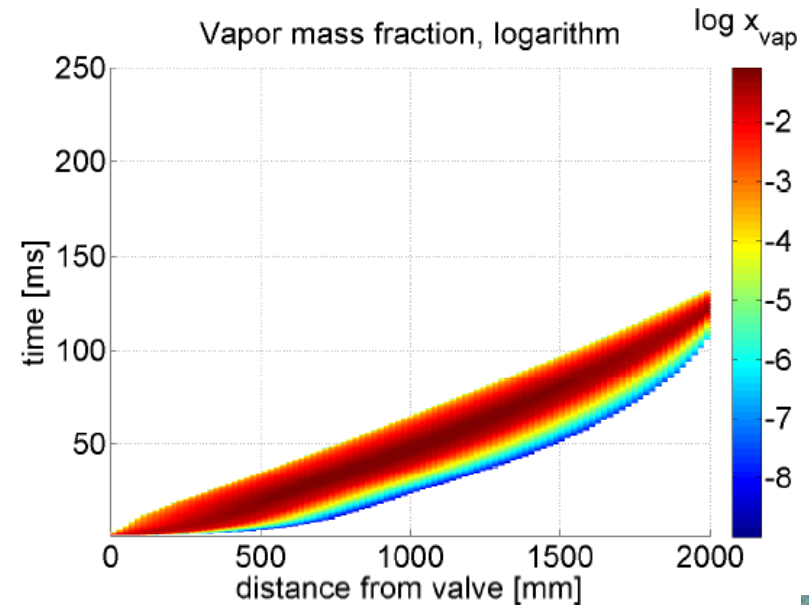
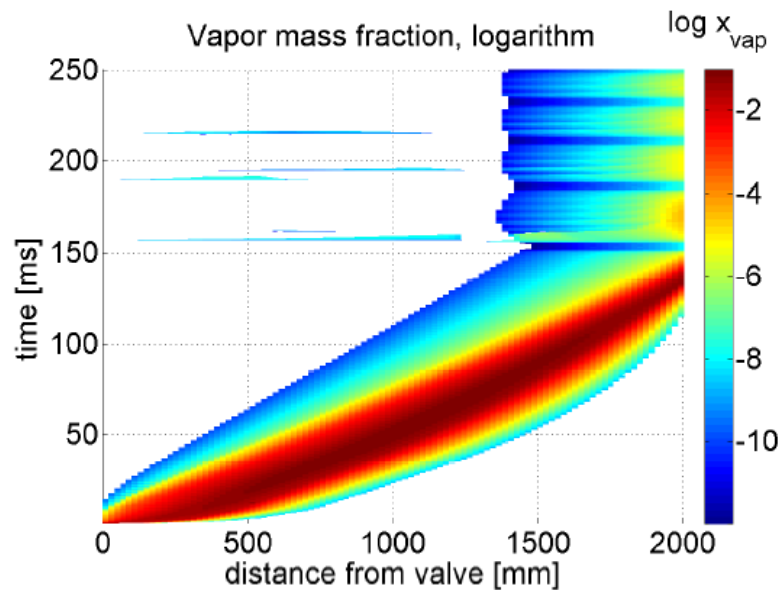
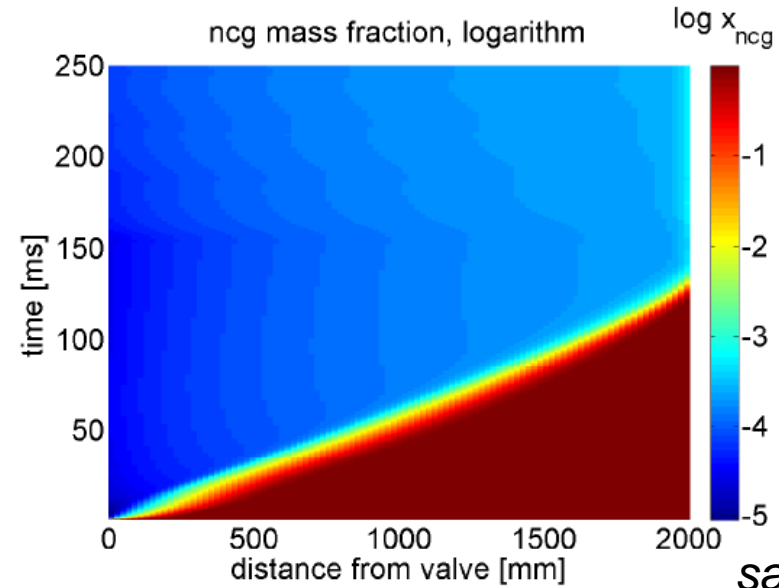
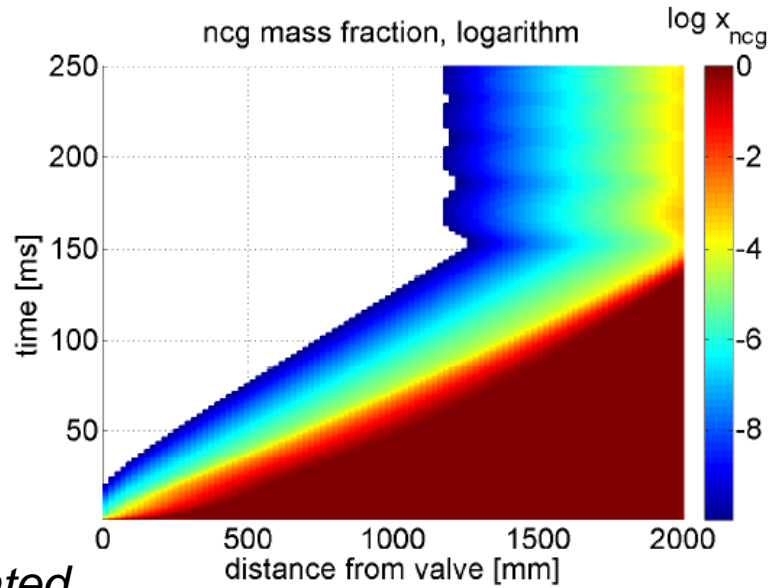
- Void fraction, α
- Non-condensable gas mass fraction, NCG
- Vapor mass fraction, x
- Speed of sound, c

Based on the values of α , NCG , x , different flow regions can be defined:

| region | α | x_{ncg} | x_{vap} |
|------------------|----------|-----------|-----------|
| gas | 1 | 1 | 0 |
| gas-vapor | 1 | >0 | >0 |
| vapor | 1 | 0 | 1 |
| liquid-vapor | <1 | 0 | >0 |
| liquid-gas | <1 | >0 | 0 |
| liquid-gas-vapor | <1 | >0 | >0 |
| liquid | 0 | 0 | 0 |



Numerical Simulation of two-phase flow



Priming/Conclusions

Propellant pressurizing conditions in tank play a not-negligible role:

- Pressure peak is affected by the gas saturation pressure
- Cavitation is intimately connected
- Formation of shock wave possible (detonation hazard)

Future work

- Further validation of the gas desorption model
- Inclusion of bubble dynamics



Thanks for your attention

Questions ?

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