

Demonstrating Cost Effective Thermal Energy Storage in Molten Salts: DLR's TESIS Test Facility

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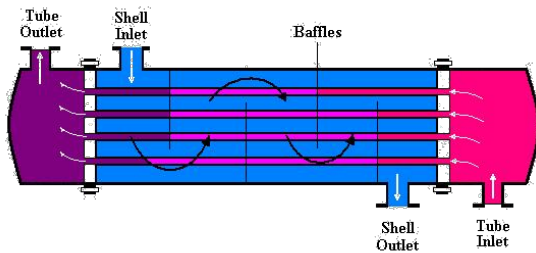


Knowledge for Tomorrow

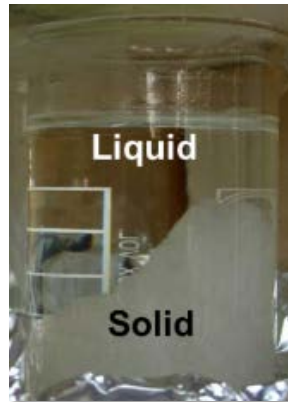


Advantages of Molten Salt

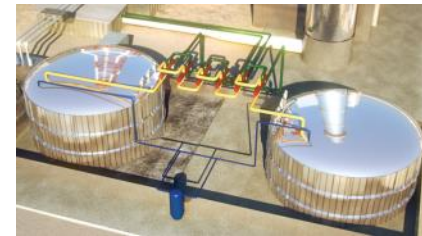
Molten Salt as Heat Transfer Fluid (HTF)



- ▶ Unpressurized (low vapor pressure)
- ▶ High heat transfer rates
- ▶ Low viscosity
- ▶ Operation temperature up to 560 °C
- ▶ Most common HTF in solar tower plants
- ▶ Trend for future parabolic trough plants



Molten Salt as Storage Material

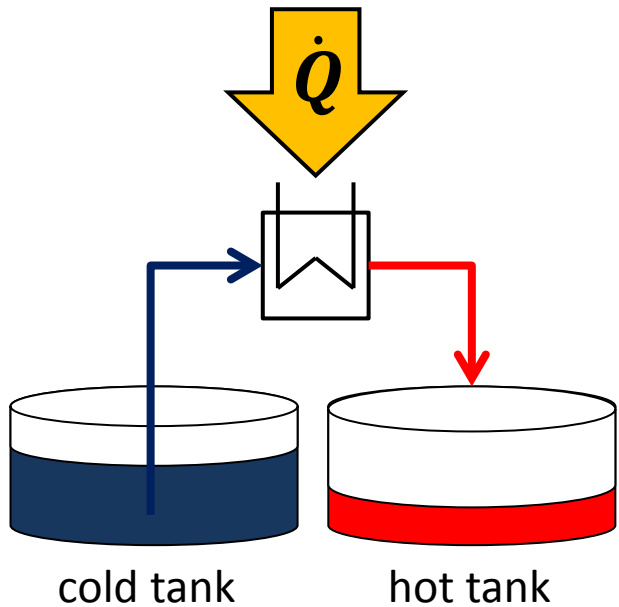


- ▶ Unpressurized
- ▶ Less expensive than synthetic oil
- ▶ No heat exchanger to HTF molten salt
- ▶ Nontoxic, nonflammable and no explosive phases
- ▶ Spec. heat capacity (liquid phase): about 1.5 kJ/(kgK)

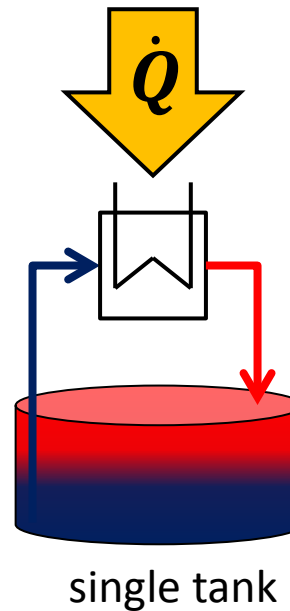


Overview of molten salt storage technology

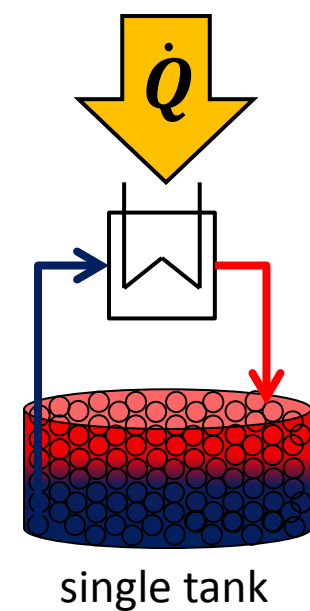
2-Tank (state of the art)



Thermocline



Thermocline with filler

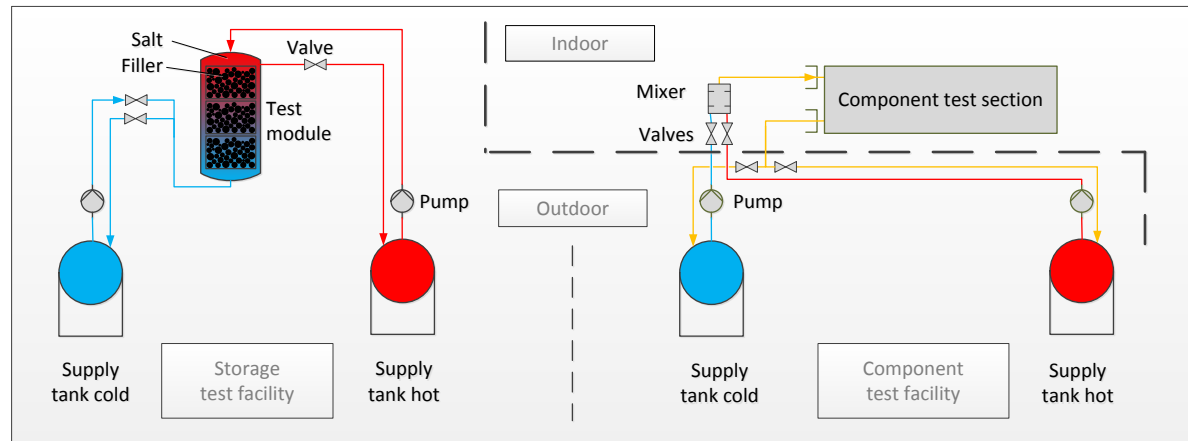


Research at DLR – TESIS Facility

Test facility for Thermal Energy Storage In Molten Salts

Test section for molten salt energy storage – TESIS:store

Test section for molten salt components – TESIS:com



- ▶ Flexible test section for alternative thermal energy storage concepts
- ▶ Long-term / permanent testing possible

- ▶ Flexible set-up for various components (e.g. valves, receiver tubes or instruments)
- ▶ Critical conditions possible



Research at DLR – TESIS Storage Test Section

TESIS:store

Molten salt medium

Nitrate - Nitrite salt mixtures

Min. operation temperature

150 °C

Max. operation temperature

560 °C

Max. mass flow rate

4 kg/s

Max. mass of filler material

45 t

Max. empty tank volume

22 m³

→ Behavior of storage system, model validation / refinement, molten salt chemistry on large scale

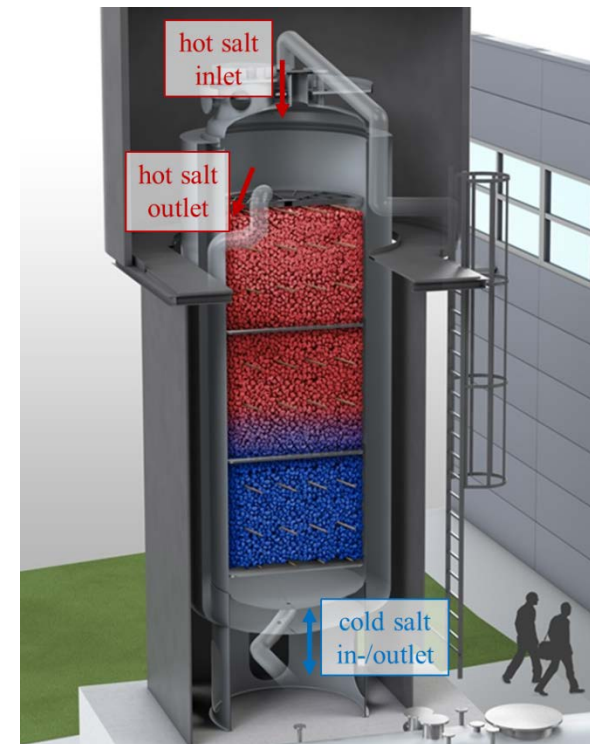
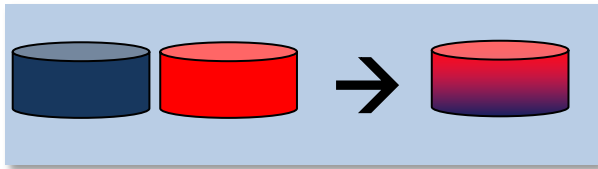


Photo of the TESIS Plant

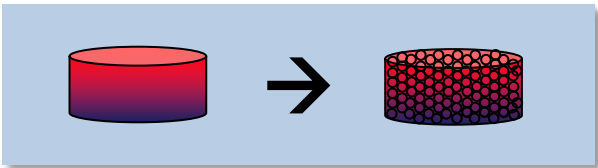


Potential for Cost-Reduction of Molten Salt Systems

Potential #1:



Potential #2:



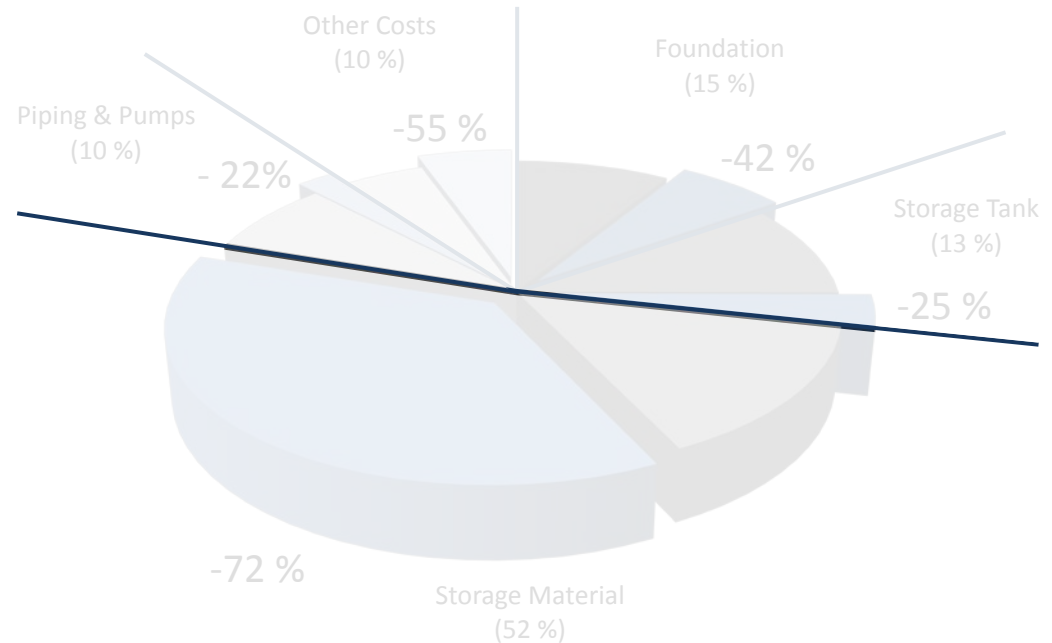
General potential:

Limited operational experience

Understanding of corrosion mechanisms

Understanding of molten salt degradation / small ΔT

Cost Reduction Potential for Thermocline Storage



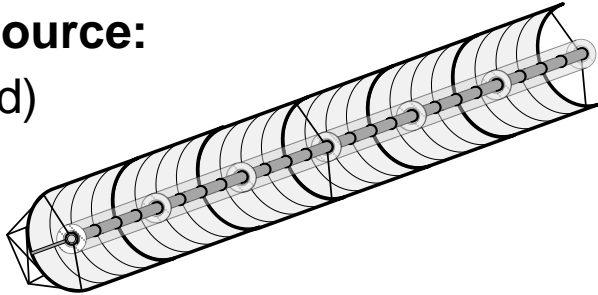
Source: 100 MWe power plant, DLR inhouse cost calculations



Example for Cost-Reduction: Exergy

Energy Source:
(Solar field)

$T_{in} =$
290 °C



$T_{out} =$
560 °C

Scenario:

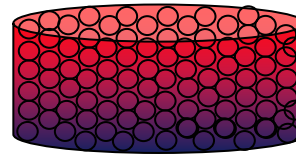


- 12 hours charging time
- 2.82 GWh thermal energy

Nominal Exergy:



~1.59 GWh



Regained Exergy:



< 1.59 GWh

Parametric study:

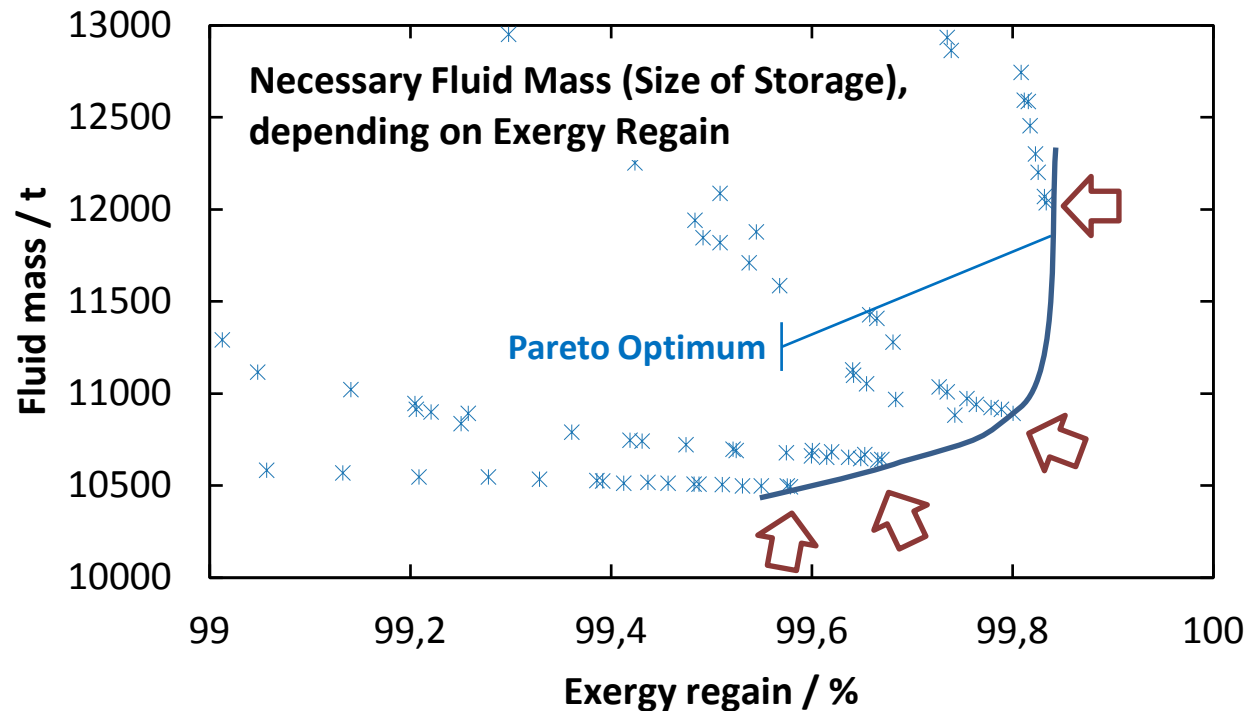
Adapt length of storage volume for

- 12 hours charge time and
- permitted drop of exit temperature

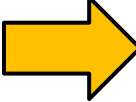


Result of Parametric study

- 100s of possible storage configurations
- Every configuration fits into the scenario
- Difference: Regained exergy vs. molten salt holdup (storage size)



Selected Results of the Parametric Study

System		Thermocline, $\varepsilon = 40\%$				2-Tank	-
Permitted change in exit temperature (ΔT_e)		10	30	50	70	0	K
	Exergy regain (Ξ)	99.8	99.8	99.7	99.6	100	%
	Storage volume (V_{stor})	16.7	14.9	14.6	14.4	13.7	10^3m^3
	Fluid mass (m_f)	12.2	10.9	10.7	10.5	25.1	kt
	Solid mass (m_s)	30.0	26.8	26.2	25.8	0.0	kt



Summary

Molten salt thermal energy storage is proven technology with large cost reduction potential

→ DLR has built two test facilities TESIS:store and TESIS:com, which help understanding storage behavior, salt chemistry and testing components for faster market application

Example based on exergy has shown that thermocline storage with filler can achieve

→ high exergetic efficiency and
→ significant reduction of salt inventory (investment cost)



Thank you for your attention

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