

Concentrated Solar Radiation More than just a power source

MENAREC 6

04. - 06.04.2016, Kuwait

Prof. Dr. Christian Sattler

Christian.sattler@dlr.de

Knowledge for Tomorrow

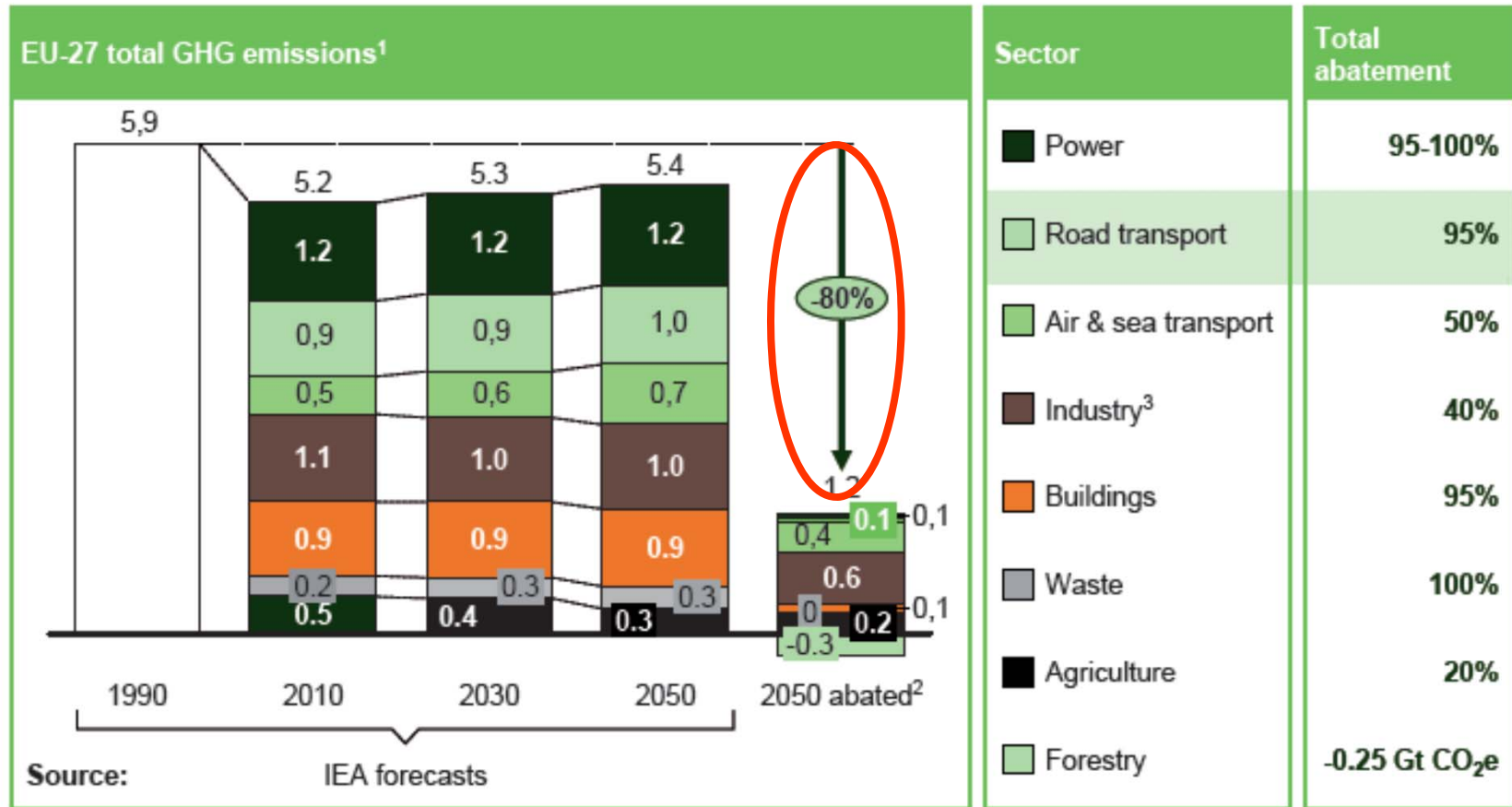


Overview

- Drivers:
 - Technical, Political, Economical, Ecological,
- Concentrating Solar Systems
- Solar technology developments and demonstrations
 - Thermochemical heat storage
 - Thermochemical fuels
 - Chemicals and materials
- Outlook



Development of EU GHG emissions [Gt CO₂e]



1 Large efficiency improvements are already included in the baseline based on the International Energy Agency, World Energy Outlook 2009, especially for industry

2 Abatement estimates within sector based on Global GHG Cost Curve

3 CCS applied to 50% of large industry (cement, chemistry, iron and steel, petroleum and gas, not applied to other industries)



SOURCE: www.roadmap2050.eu

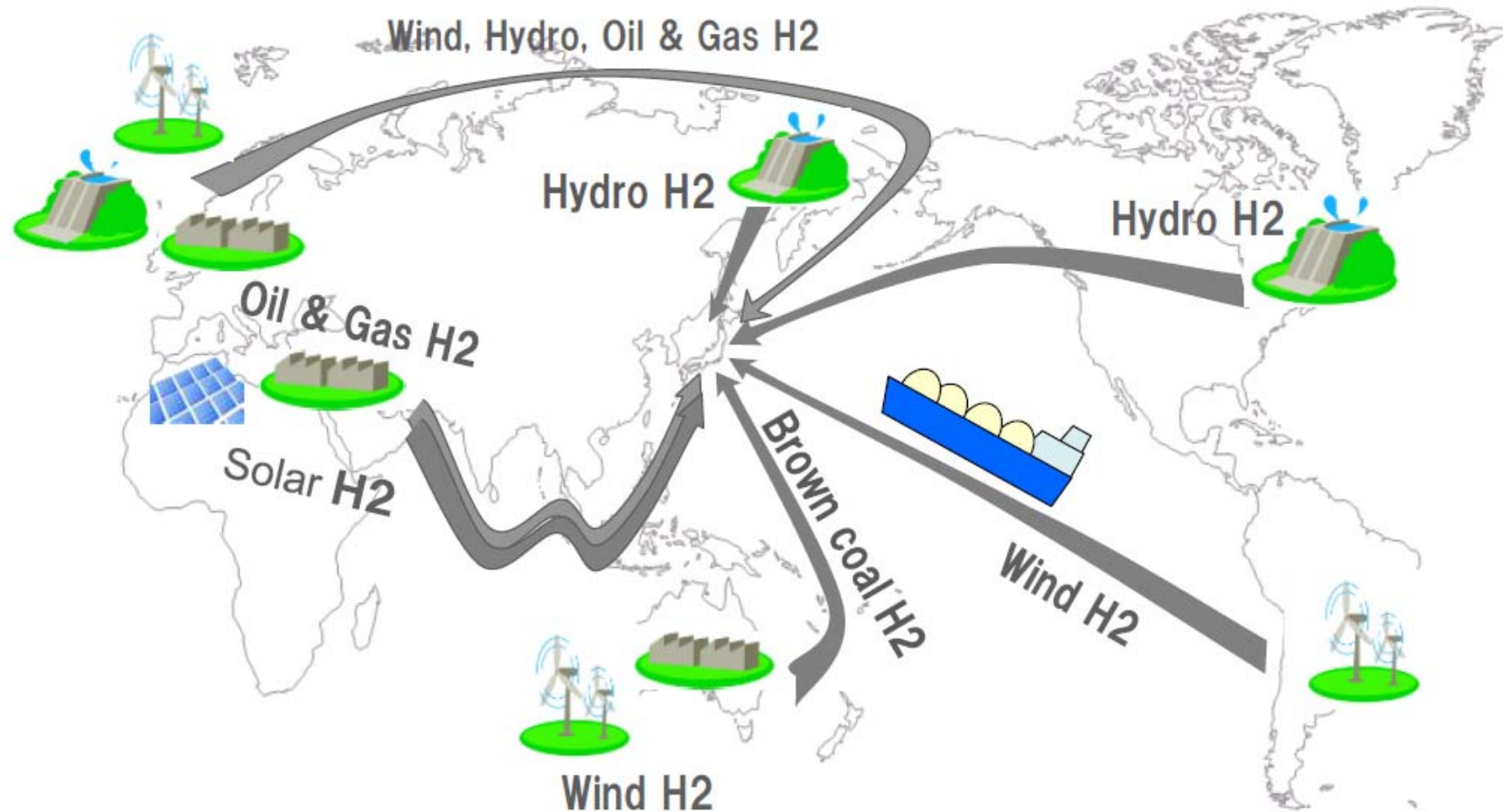


Political Drivers: Examples – EU Sustainable Energy Technology Plan (SET-Plan 2007) G7 Goals (2015)

- **Goals of the EU until 2020 (20/20/20)**
 - **20%** higher energy efficiency
 - **20%** less GHG emission
 - **20%** renewable energy
- **Goal of the EU until 2050:**
 - **80%** less CO₂ emissions than 1990
- **G7 Goals, Elmau, Germany**
 - **100%** Decarbonisation until 2100
 - **100 bln \$/year** for climate actions in developing countries, large share by industrial investment from 2020



Kawasaki Vision – Hydrogen Potential from Overseas



Kawasaki vision for the cryogenic liquid hydrogen market – team-up with Shell (March 15, 2016)

川崎重エグループは、国内で有数の大型水素貯蔵タンクや水素運搬車を製造している技術と経験を活かし、未来社会に向けての新しいエネルギー構想として「CO₂フリー水素コンセプト」を提案しています。



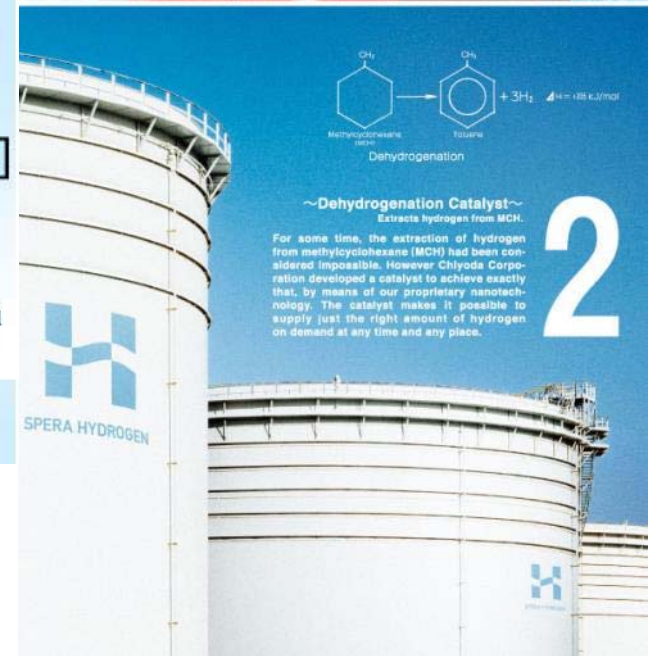
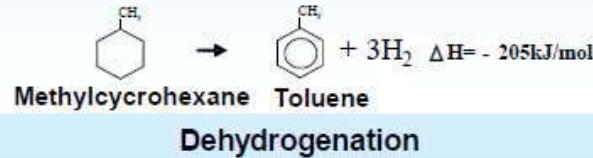
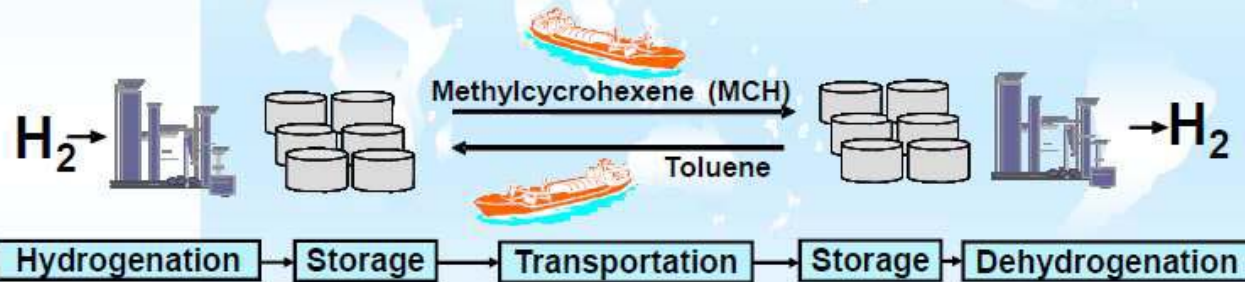
<http://global.kawasaki.com/en/stories/hydrogen/>



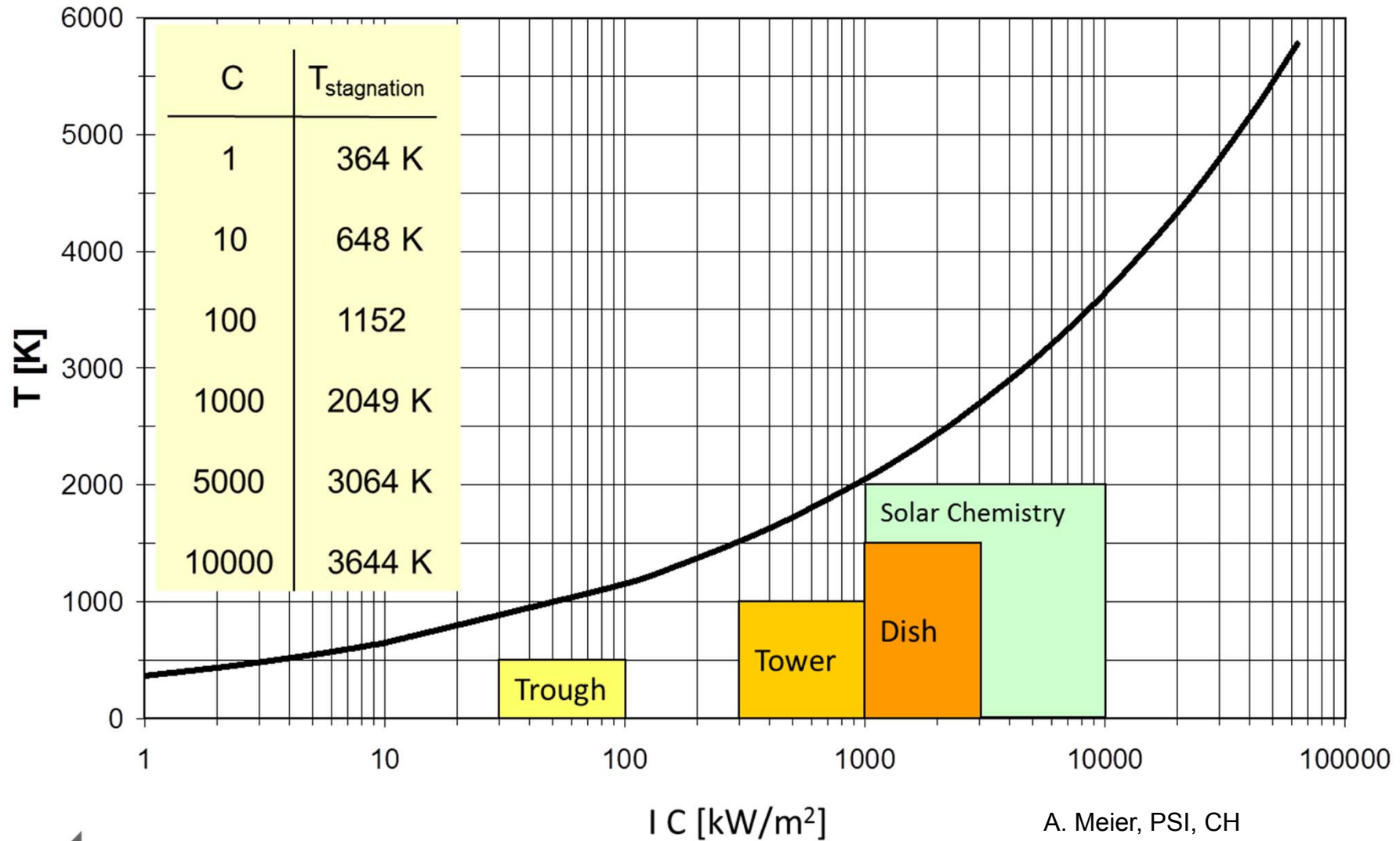


CHIYODA – Hydrogen Vision

The Methylcyclohexene(MCH) is considered one of the safety and economical hydrogen carriers because of the storage and transportation in the liquid phase under the ambient temperature and pressure.



Principle of Concentrating Solar Energy for Power and Chemistry



Solar Towers



On the Web:

<http://www.ivanpahsolar.com/>

<http://www.psa.es/webeng/index.php>

<http://www.torresolenergy.com/TORRESOL/home/en>

<http://www.solarreserve.com/en/global-projects/csp/crescent-dunes>

http://www.abengoasolar.com/web/en/plantas_solares/plantas_para_terceros/espana/

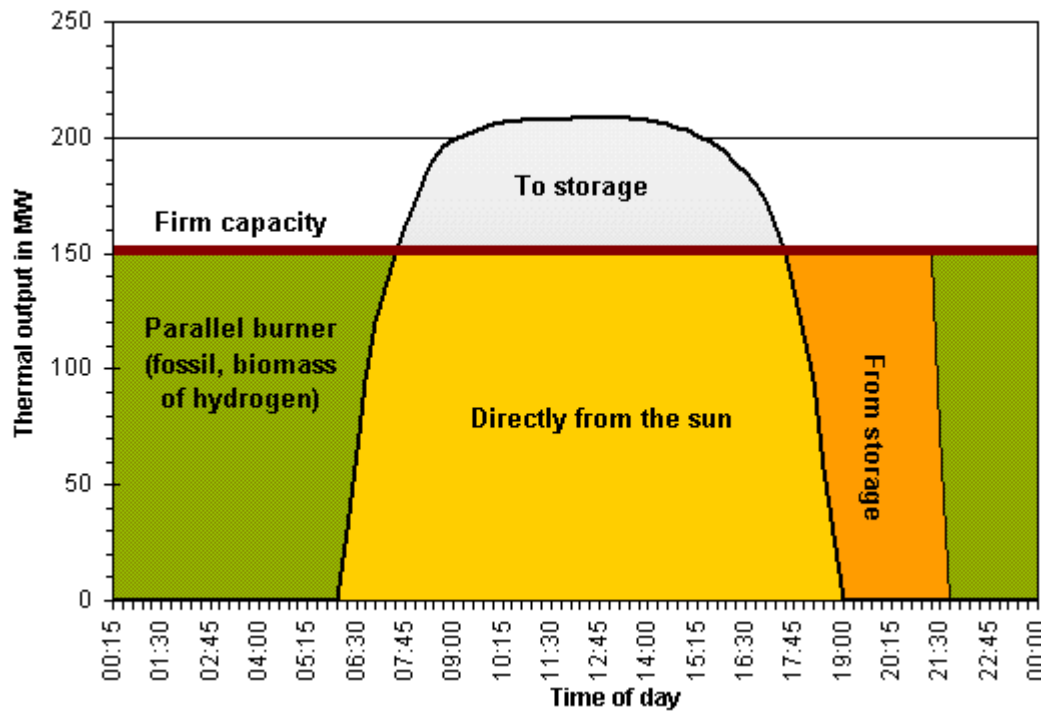


Centralized Energy Supply – Solar Troughs and Towers

Main Features

- Typical plant size: 10 – 200 MW_e
- Conv. thermal cycle efficiency: 35-42%

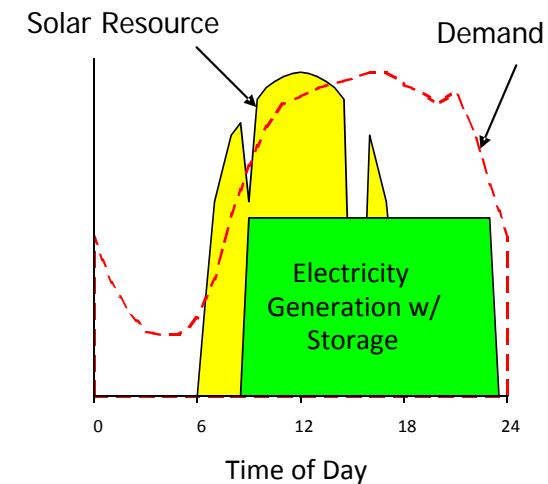
Typical solar plant operation



Thermal Energy Storage (TES)

Storage provides

- decoupling of energy collection and electricity generation
- helping *grid stability*
- higher value: power production can match utility needs



Thermochemical heat storage can provide very high energy storage densities

Technology	Energy Density (kJ/kg)
Gasoline	45000
Sulfur	12500
Cobalt Oxide	850
Molten Salt (Phase Change)	230
Molten Salt (Sensible)	155
Lithium Ion Battery	580
Elevated water Dam (100m)	1

- **High energy densities with low storage cost**
- **Ambient and long term storage**
- **Transportability**



Solar energy can be stored in elemental sulfur via a three step thermochemical cycle

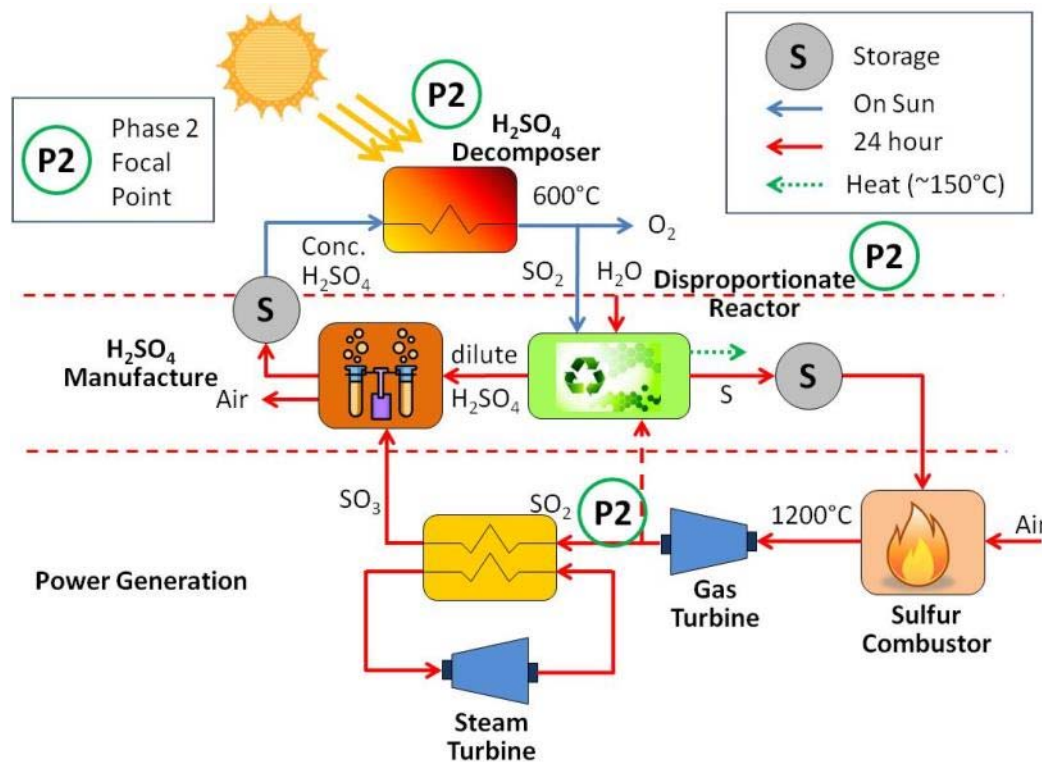


	Reaction	Temp (°C)
H_2SO_4 Decomposition	$2\text{H}_2\text{SO}_4 \rightarrow 2\text{H}_2\text{O}(\text{g}) + \text{O}_2(\text{g}) + 2\text{SO}_2(\text{g})$	800
SO_2 Disproportionation	$2\text{H}_2\text{O}(\text{l}) + 3\text{SO}_2(\text{g}) \rightarrow 2\text{H}_2\text{SO}_4(\text{aq}) + \text{S}(\text{l})$	150
Sulfur Combustion	$\text{S}(\text{s,l}) + \text{O}_2(\text{g}) \rightarrow \text{SO}_2(\text{g})$	1200



An improved flowsheet was established based on modeling and experimental

- Plant design incorporated established processes from sulfuric acid manufacturing plant



DOE Metric	LCOE (¢/kWh _e)
DOE Target	6.5
CSP w/Sulfur Storage	8.1*

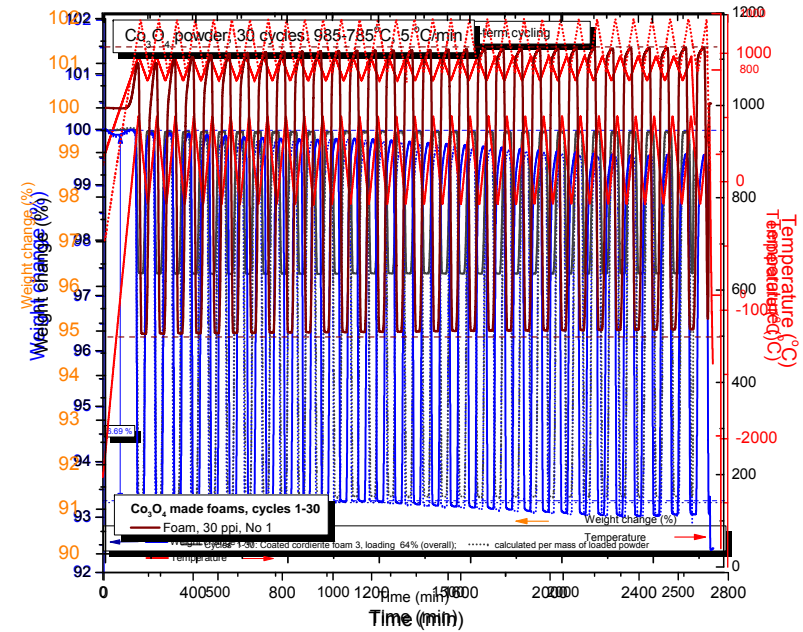
*SAM (NREL) using 2012 costs

- Storage cost is < \$2/kWh
- LCOE is ~6¢/kWh_e based on proposed Sunshot targets



Co₃O₄/CoO

- Co₃O₄ can operate in a quantitative, cyclic and fully reversible reduction/oxidation mode within 800-1000°C (950°C).
- As powder, coated on honeycombs/foams or shaped in foams.

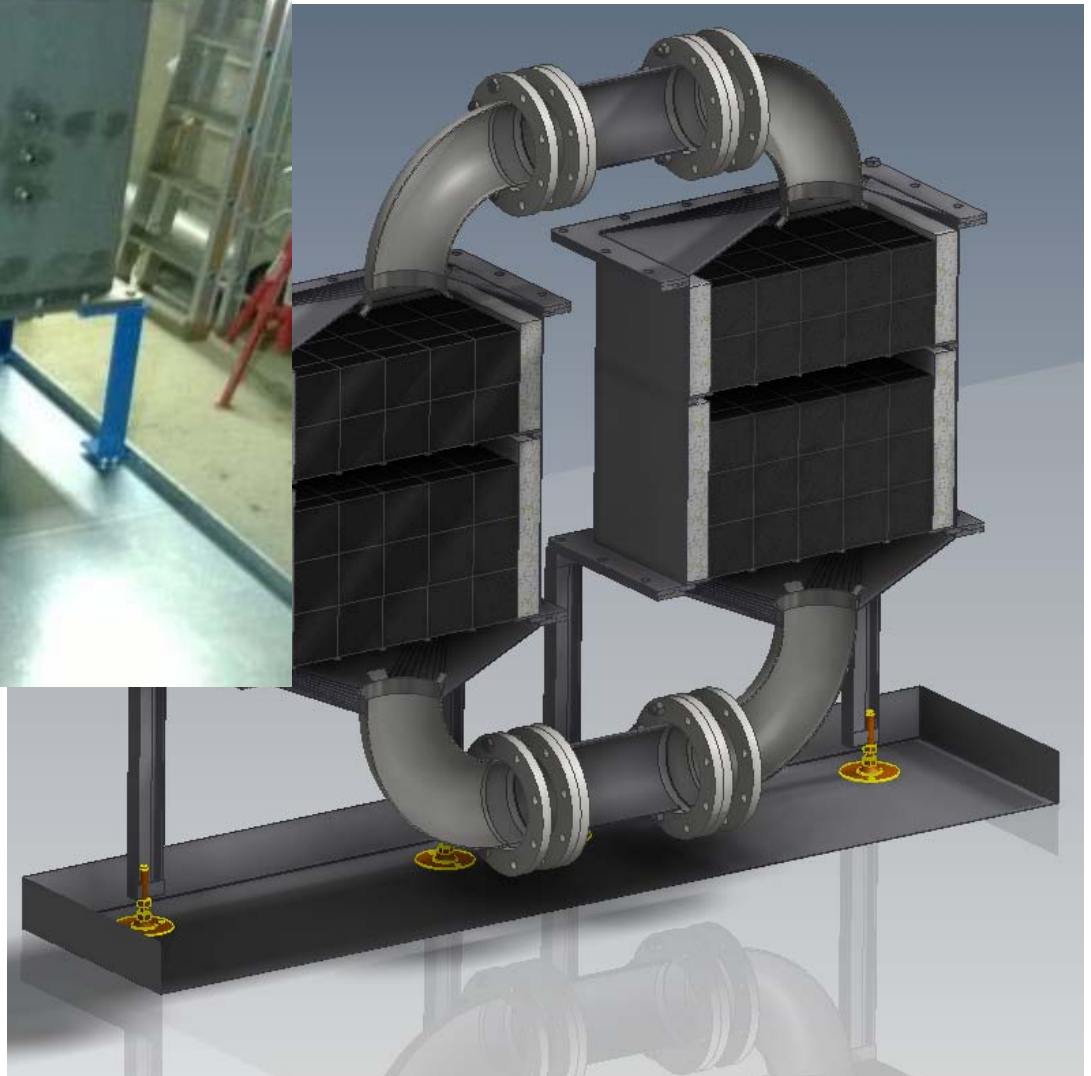


Agrafiotis, Roeb, Schmücker, Sattler, Solar Energy, (2014), (2015).





Construction



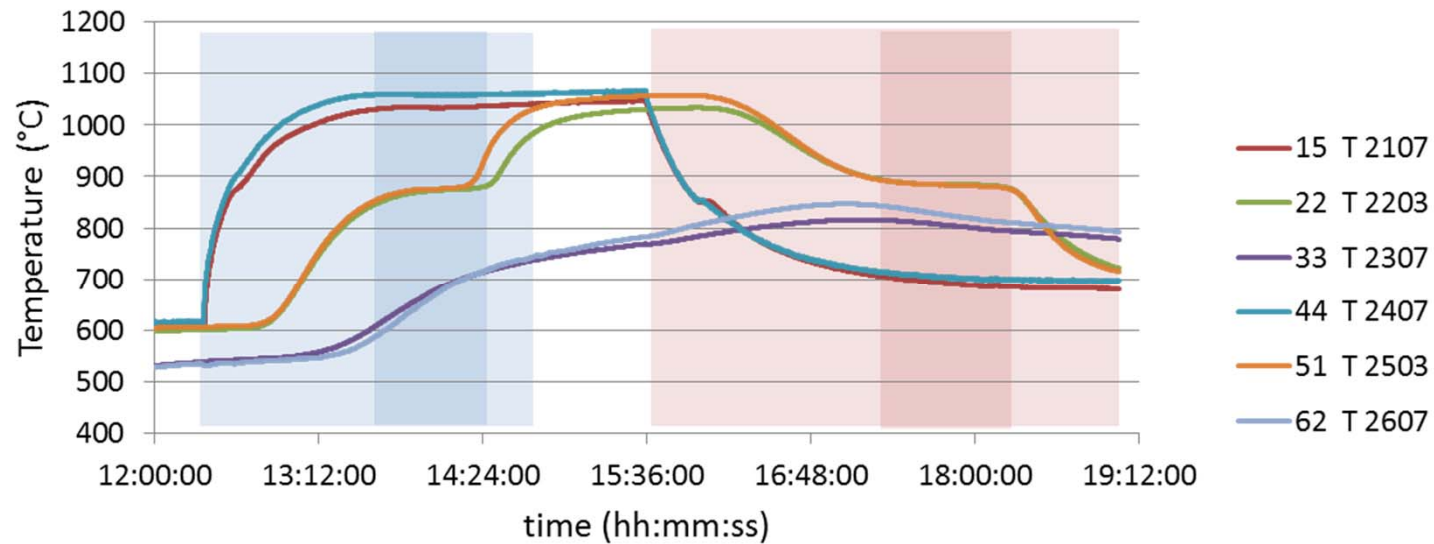
DLR solar tower juitch,
Germany



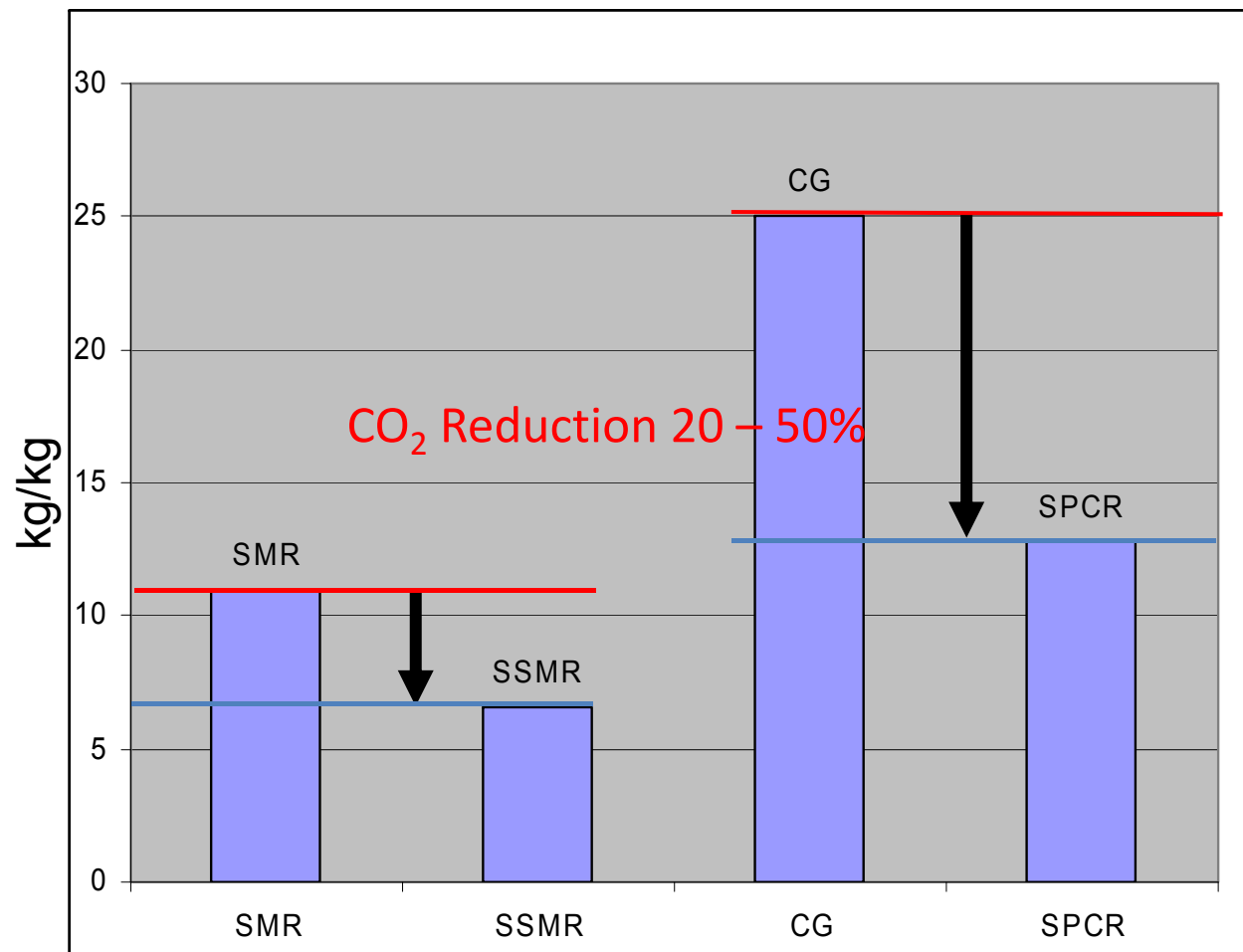
Chemical Tests

considering half of one chamber ($\approx 25\text{kg}$ cobalt)

	Energy stored (kWh)	Average Power (kW)	time	at constant temperature
Charge	38	11.2	3.5 h	1 h
Discharge	32	9.6	3.25 h	1 h

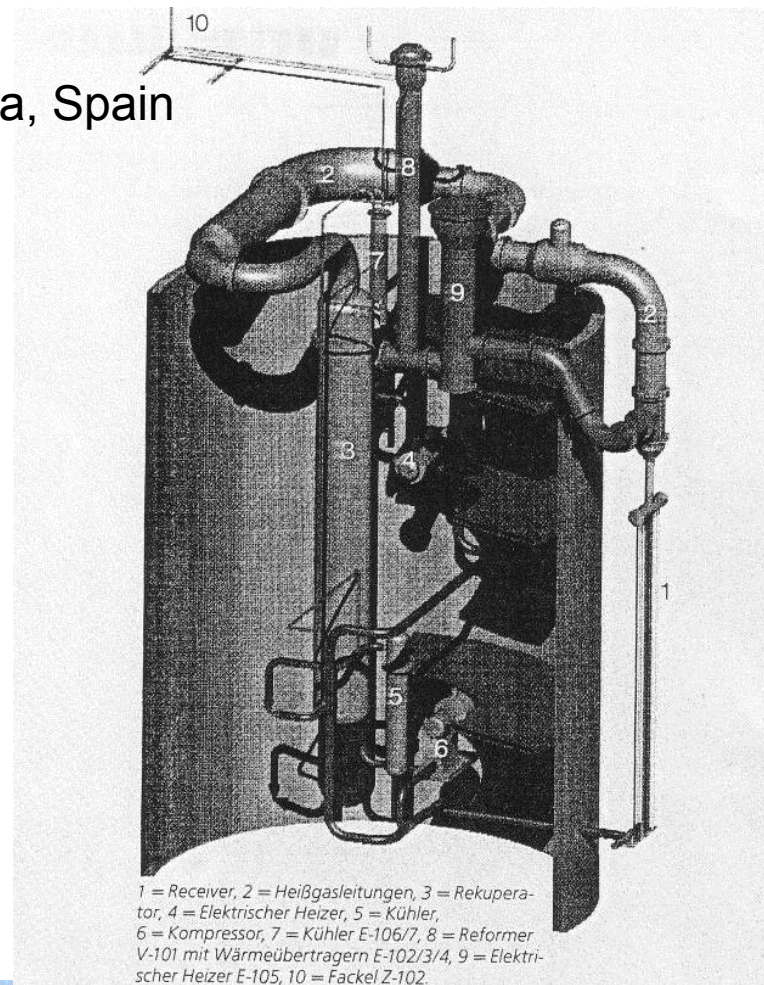


CO₂ Reduction by solar heating of state of the art processes like steam methane reforming and coal gasification



ASTERIX: Allothermal Steam Reforming of Methan

- DLR, Steinmüller, CIEMAT
- 180 kW plant at the Plataforma Solar de Almería, Spain (1990)
- Convective heated tube cracker as reformer
- Tubular receiver for air heating



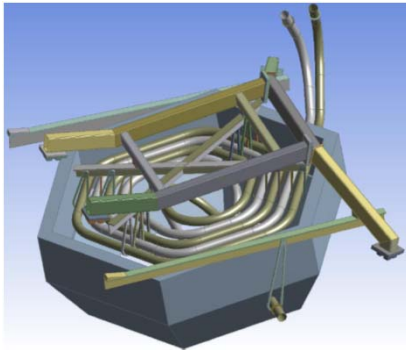
Near-term: Solar Production of Syngas (H₂ and CO)

Solar pilot plants demonstrated in the power range of 200-500 kW_{th}

Solar steam reforming of natural gas / methane

Solar steam gasification of carbonaceous feedstock

SOLGAS (200 + 600 kW_{th})
CSIRO, Australia



SOLREF (400 kW_{th})
DLR, Germany



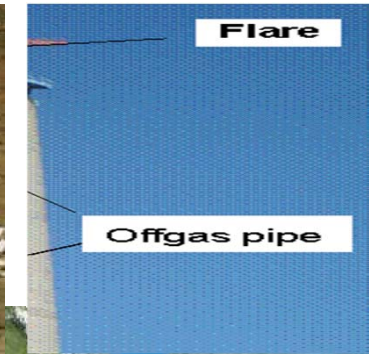
SYNPET (500 kW_{th})
CIEMAT, Spain



SOLSYN (250 kW_{th})
PSI, Switzerland



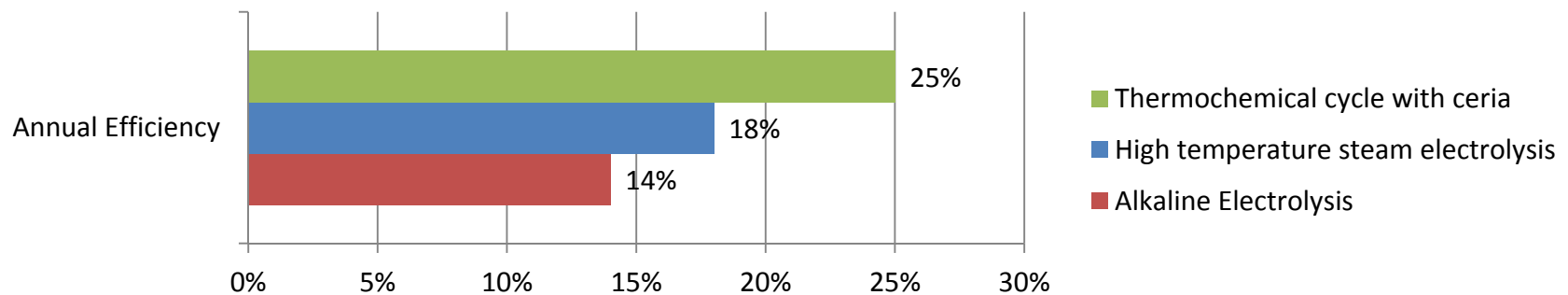
DLR



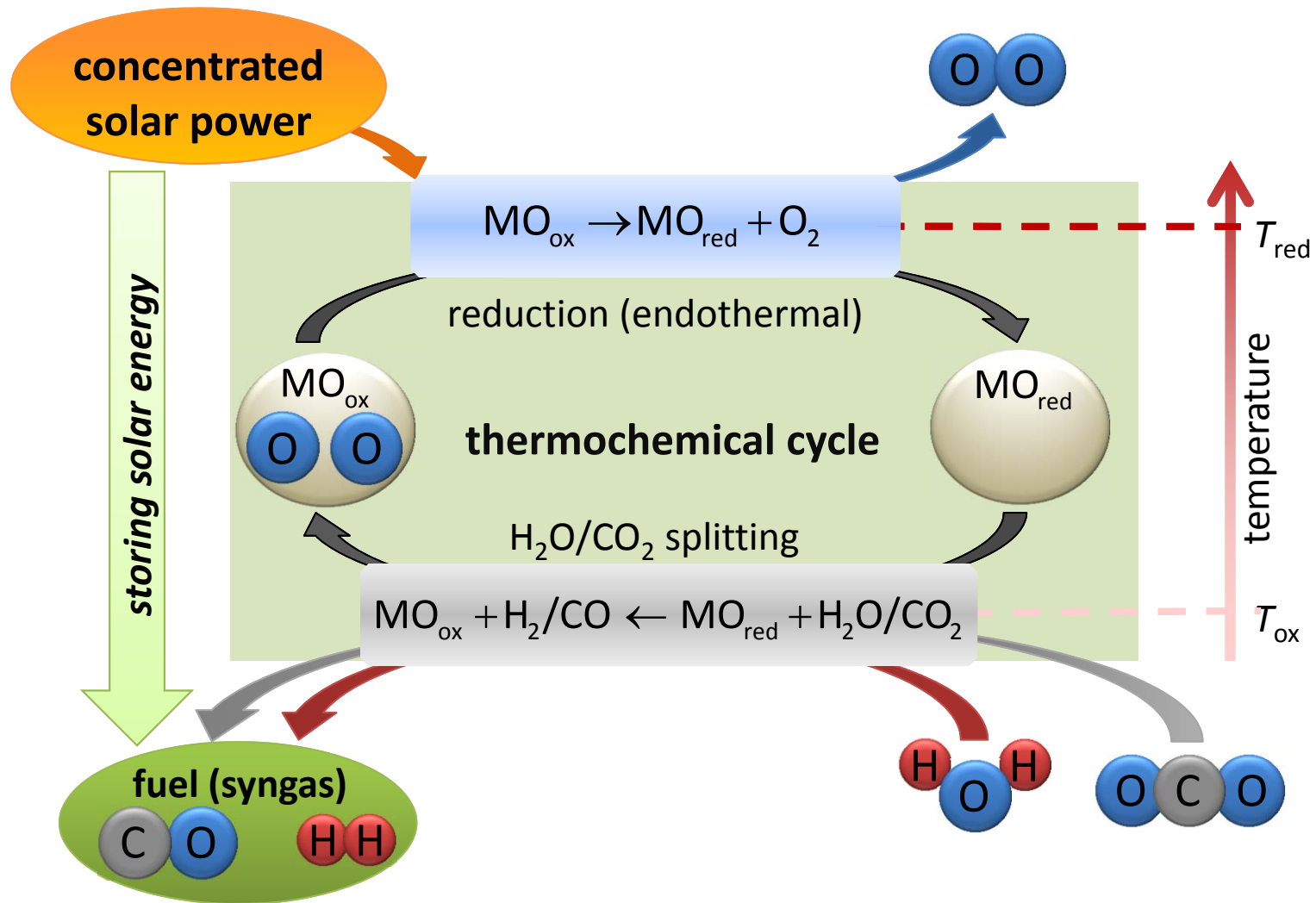
Solar Fuels: Efficiency Comparison vs. Benchmark

Process	temperature	Solar interface
	of the chemical reaction	receiver temperature
Alkaline Electrolysis	25°C	Solar PV
High temperature steam electrolysis	850°C	Future solar tower 1200°C
Thermochemical cycle with ceria	1500 / 1150°C	Future solar dish 1500°C

*G.J. Kolb, R.B. Diver SAND 2008-1900 / N. Siegel et al. I&EC Research May 2013



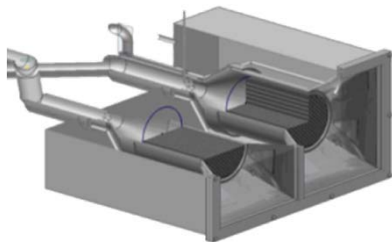
Thermochemical Cycles





HYDROSOL Development

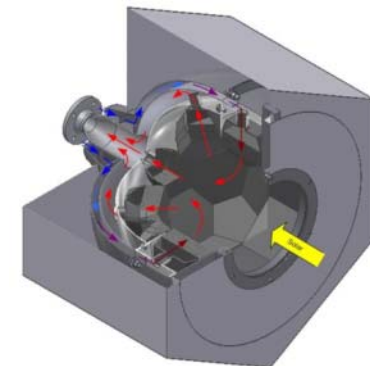
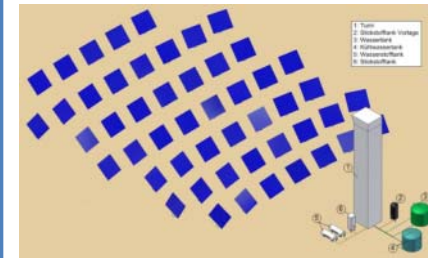
Hydrosol I
2002 – 2005
< 10 kW



Hydrosol II
2006 – 2009
100 kW



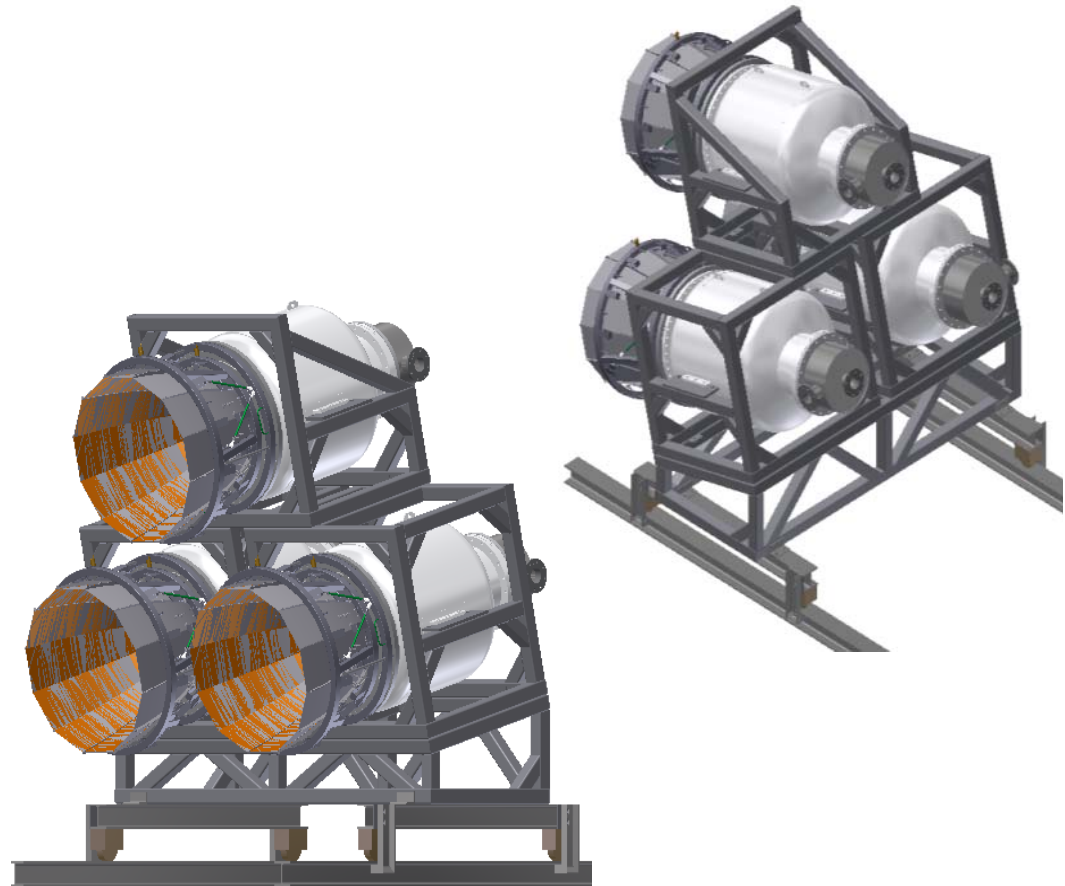
Hydrosol 3D
2010 – 2012
1 MW





Hydrosol Plant - Design for CRS tower PSA, Spain

- European FCH-JU project
- Partner: APTL (GR), HELPE (GR), CIEMAT (ES), HYGEAR (NL)
- 3 * 750 kW_{th} demonstration of thermochemical water splitting
- Location: Plataforma Solar de Almería, Spain, 2016
- Reactor set-up on the CRS tower
- Storage tanks and PSA on the ground





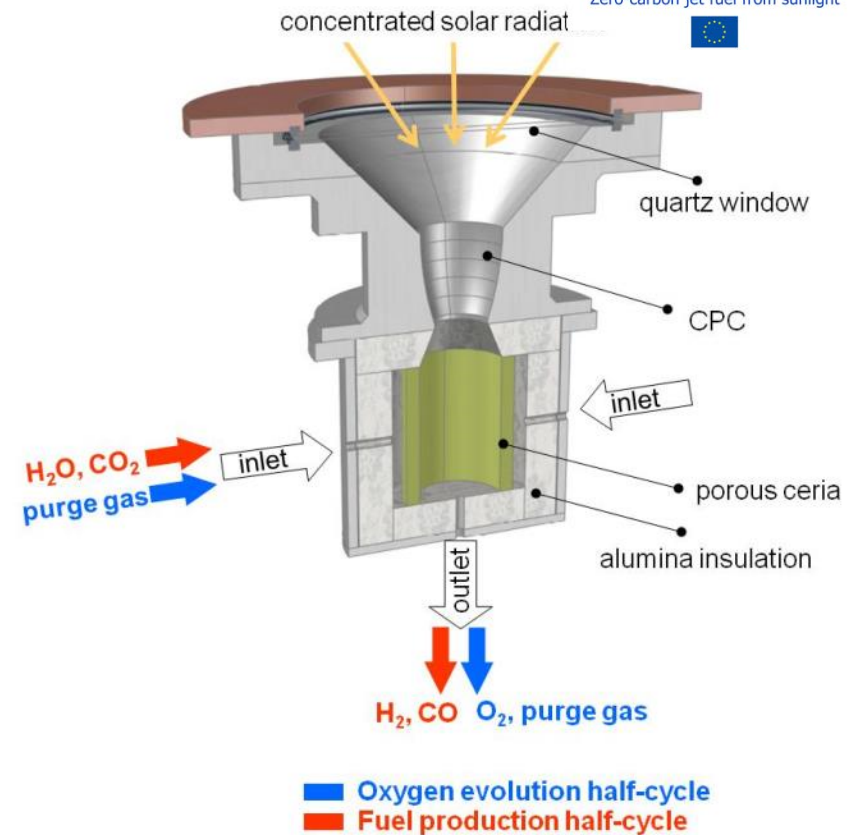
SOLAR-JET
Zero-carbon jet fuel from sunlight



H₂O/CO₂-Splitting Thermochemical Cycles

Solar Production of Jet Fuel

- EU-FP7 Project SOLAR-JET (2011-2015)
- SOLAR-JET aims to ascertain the potential for producing jet fuel from concentrated sunlight, CO₂, and water.
- SOLAR-JET will optimize a two-step solar thermochemical cycle based on ceria redox reactions to produce synthesis gas (syngas) from CO₂ and water, achieving higher solar-to-fuel energy conversion efficiency over current bio and solar fuel processes.
- **First jet fuel produced in Fischer-Tropsch (FT) unit from solar-produced syngas!**



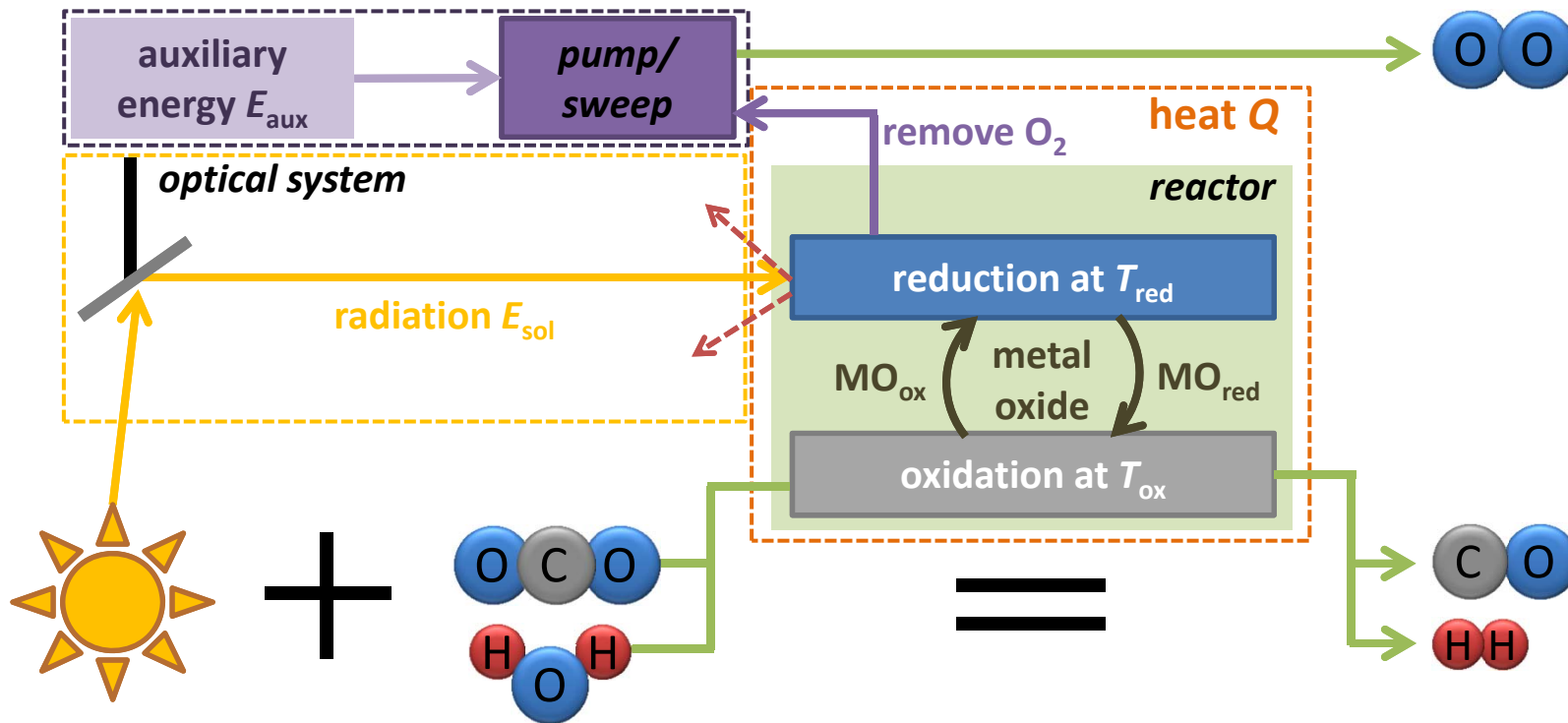
Int. J. Heat & Fluid Flow 29, 315-326, 2008.
Materials 5, 192-209, 2012.

Partners: Bauhaus Luftfahrt (D), ETH (CH),
DLR (D), SHELL (NL), ARTTIC (F)
Funding: EC

<http://www.solar-jet.aero/>



Challenges of the entire process



Production of CO_2 -neutral renewable fuels through solar-driven thermochemical cycles ($\$ + \eta$)

material side

- Determination of atomic mobilities in the redox materials
- Identification of methods to enhance long-term stability
- Improvement of hydrogen/ CO yield per cycle and conversion rate

process side

- Analysis and modelling of heat transfer mechanisms in the solar receiver
- Solar heat incorporation: Matching rates of chemical reaction and heat transfer
- Analysis and optimization of transport (conversion rates and residence times)





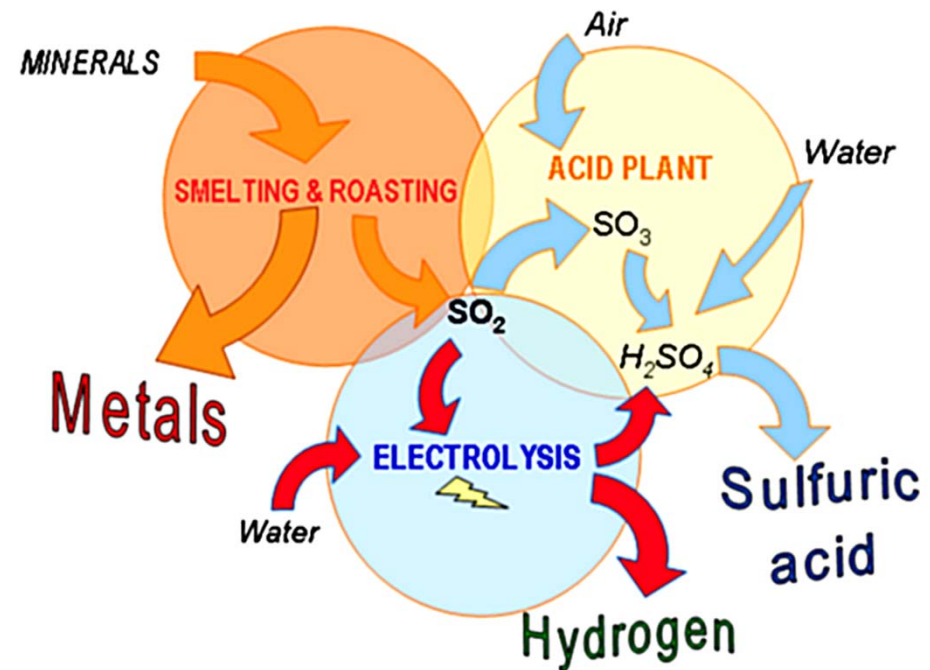
SOL2HY2 – Solar To Hydrogen Hybrid Cycles

- FCH JU project on the solar driven Utilization of waste SO_2 from fossil sources for co-production of hydrogen and sulphuric acid
- Hybridization by usage of renewable energy for electrolysis
- Partners: EngineSoft (IT), Aalto University (FI), DLR (DE), ENEA (IT), Outotec (FI), Erbicol (CH), Oy Voikoski (FI)
- >100 kW demonstration plant on the solar tower in Jülich, Germany in 2015

<https://sol2hy2.eurocoord.com>



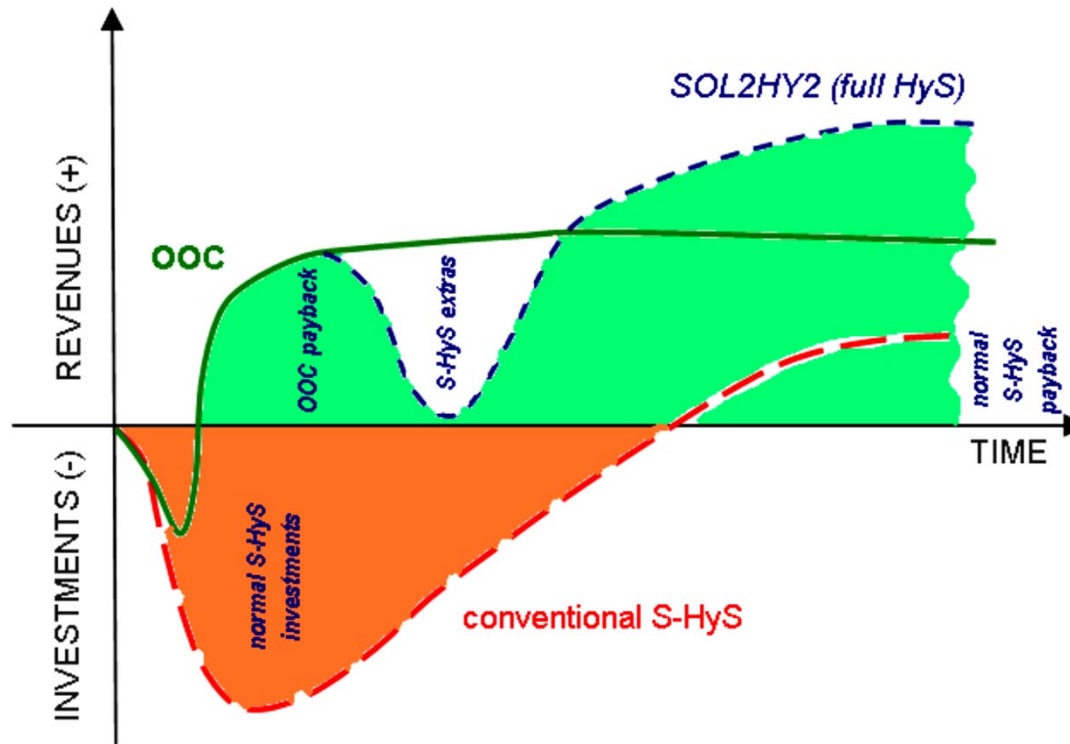
Outotec™ Open Cycle (OOC)



- Utilization of waste SO_2 from fossil sources
- Co-production of hydrogen and sulphuric acid
- Hybridization by renewable energy for electrolysis



Investments vs. revenues

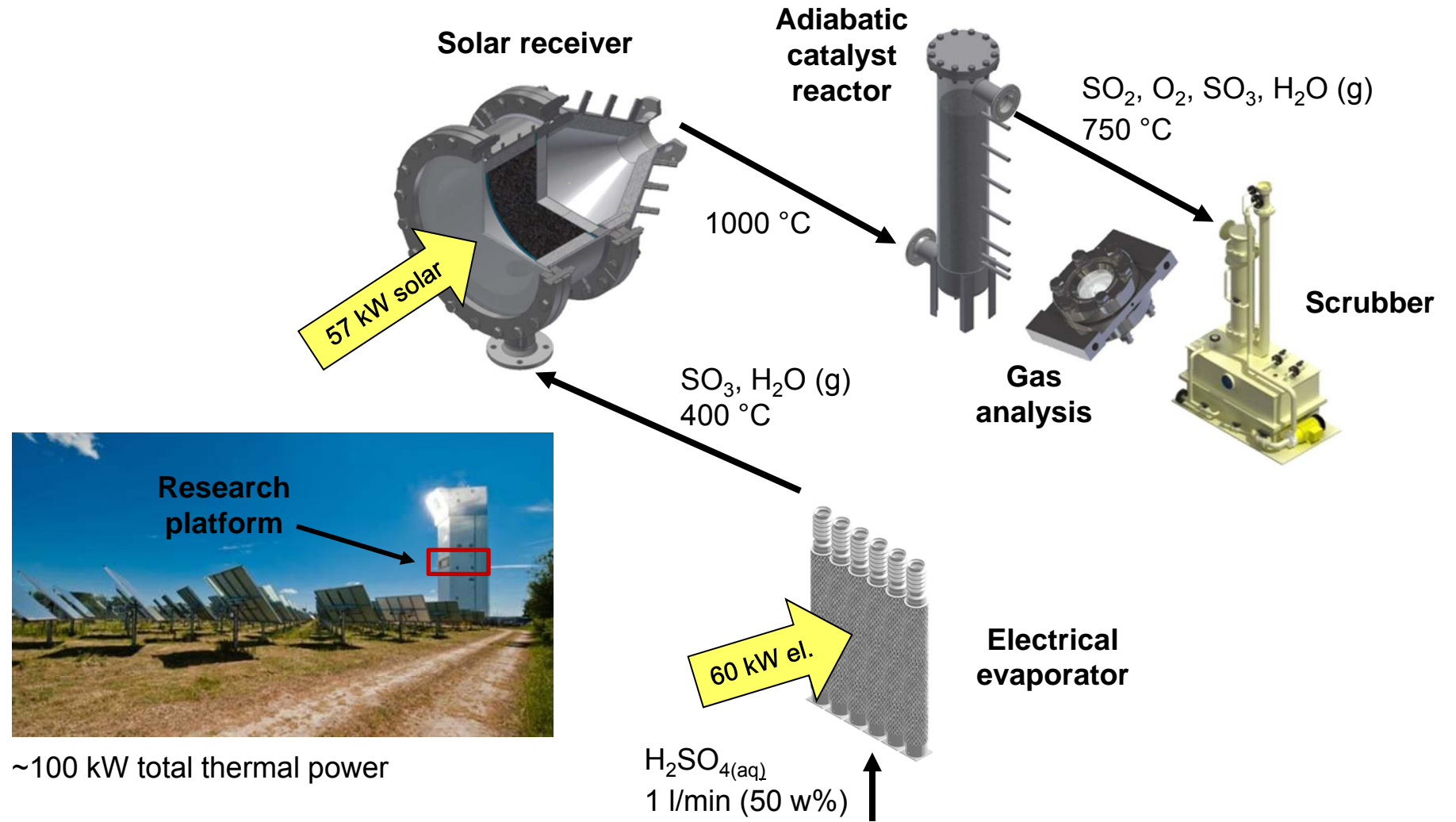


- Reduction of initial investments
- Financing of HyS development by payback of OOC
- Increase of total revenues





Design of SOL2HY2 pilot plant



~100 kW total thermal power



SOLAM

Solar Aluminium Melting in a Directly Heated Rotary Kiln

- **Aim**
- Demonstration of solar aluminium recycling in a 20 kW rotary kiln
- Develop process concept for a commercial pilot plant
- Driver: Reduce the electricity demand from the grid

South African partners

CSIR – Council for Scientific and Industrial Research

NFTN – National Foundry Technology Network

Eskom – South African National Electricity

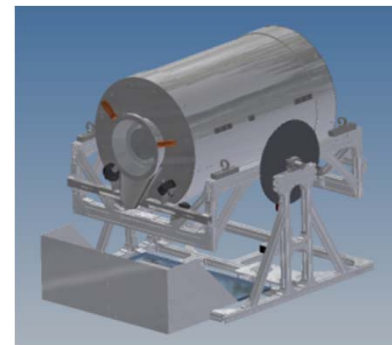
Generator and Distributor

DST – Department of Science and Technology

German partners

aixprocess

DLR



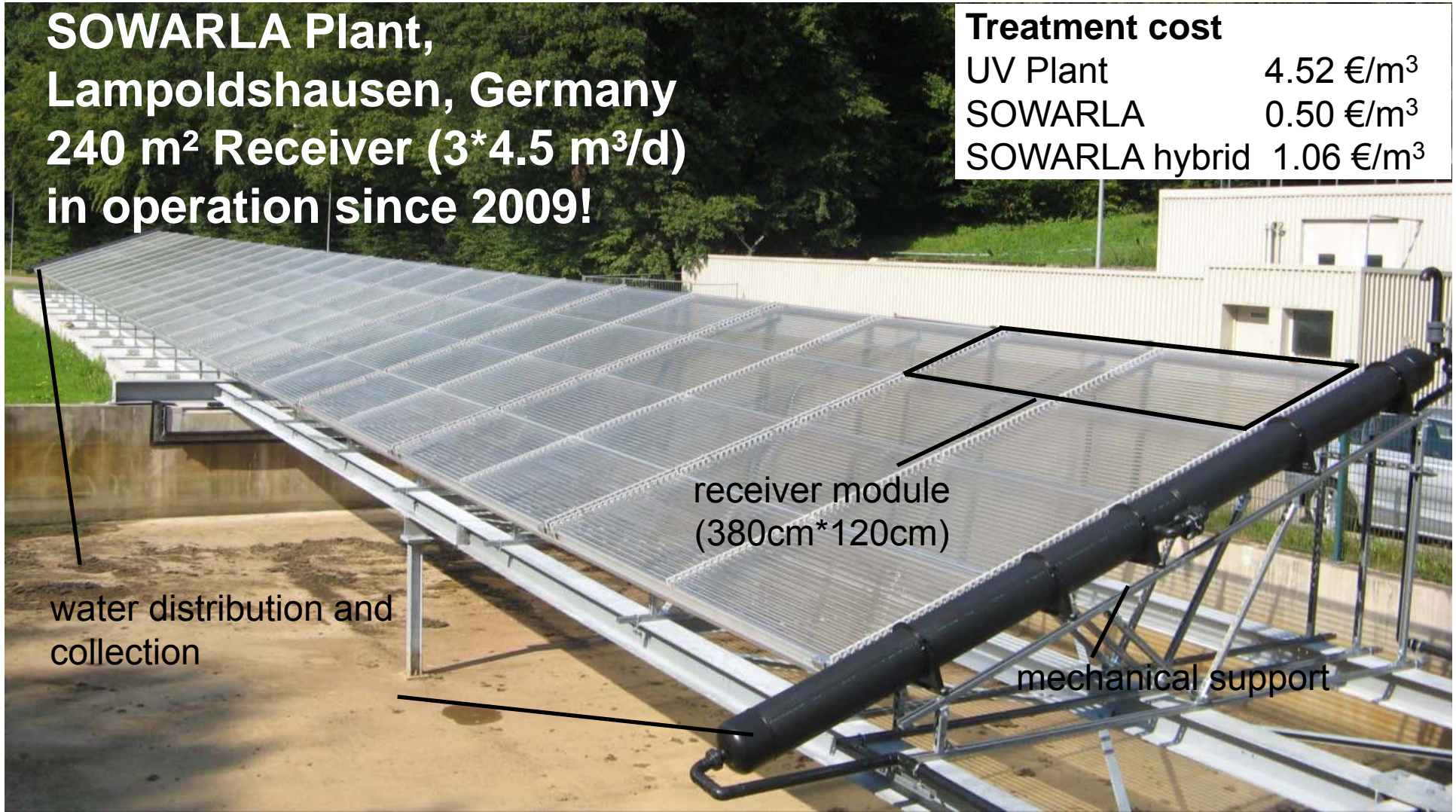


SOWARLA®

**SOWARLA Plant,
Lampoldshausen, Germany
240 m² Receiver (3*4.5 m³/d)
in operation since 2009!**

Treatment cost

UV Plant	4.52 €/m ³
SOWARLA	0.50 €/m ³
SOWARLA hybrid	1.06 €/m ³



STAGE-STE

Scientific and Technological Alliance for Guaranteeing the European Excellence in Concentrating Solar Thermal Energy (2014-2017)

WP1: Consortium Governance and Management Issues

WP2: Integrating Activities for Long-lasting Research Cooperation

WP3 Enhancement of STE Research Facilities Cooperation

WP4 Capacity Building and Training

WP5 Relationship with Industry & Transfer of Knowledge Activities

WP6 International Cooperation Activities

WP7: Thermal Energy Storage

WP8: Materials for Solar Receivers and STE Components

WP9: Solar Fuels

WP10: STE plus Desalination

WP11: Linear focusing STE Technologies

WP12: Point focusing STE Technologies

- WPs 7 to 12 involve 6 parallel individual research projects dealing with the whole current spectrum of STE research activities.
- Each WP is devoted to address the execution of considered most urgent research activities according to the defined EERA Subprogrammes, complemented with the missing elements to address the indicated whole spectrum of research activities

- [Contact: Dr. Julian Blanco](mailto:Julian.blanco@psa.es)
- Julian.blanco@psa.es
- <http://www.stage-ste.eu/>



STAGE-STE Consortium

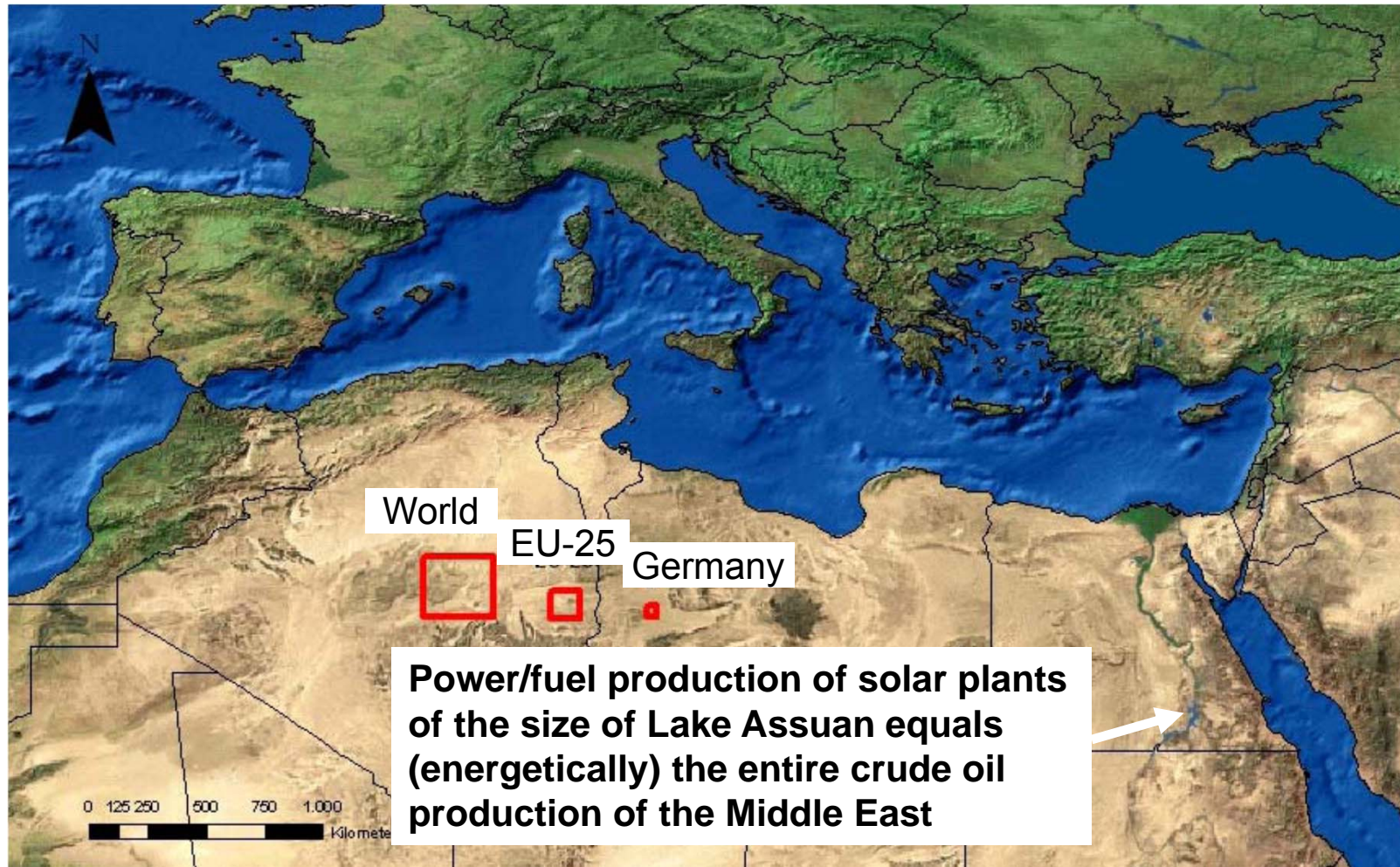


Participant no.	Organisation name	Country
1 (Coord.)	CIEMAT	SPAIN
2	DLR	GERMANY
3	PSI	SWITZERLAND
4	CNRS	FRANCE
5	FISE	GERMANY
6	ENEA	ITALY
7	ETHZ	SWITZERLAND
8	CEA	FRANCE
9	CYI	CYPRUS
10	LNEG	PORTUGAL
11	CTAER	SPAIN
12	CNR	ITALY
13	CENER	SPAIN
14	TECN	SPAIN
15	UEVORA	PORTUGAL
16	IMDEA	SPAIN
17	CRAN	UK
18	TKN	SPAIN
19	UNIPA	ITALY
20	CRS4	ITALY

Participant no.	Organisation name	Country
21	INESC-ID	PORTUGAL
22	IST-ID	PORTUGAL
23	SENER	SPAIN
24	CNIM	FRANCE
25	HITIT	TURKEY
26	ACCIONA	SPAIN
27	SCHOTT	GERMANY
28	ASE	ITALY
29	ESTELA	BELGIUM
30	ASNT	SPAIN
31	KSU	SAUDI ARABIA
32	UNAM	MEXICO
33	SUN	SOUTH AFRICA
34	CSERS	LYBIA
35	CSIRO	AUSTRALIA
36	FUSP	BRAZIL
37	IIECAS	CHINA
38	UDC	CHILE
39	UCAM	MOROCCO
40	FBK	ITALY
41	CNIM	France
42	COBRA	Spain

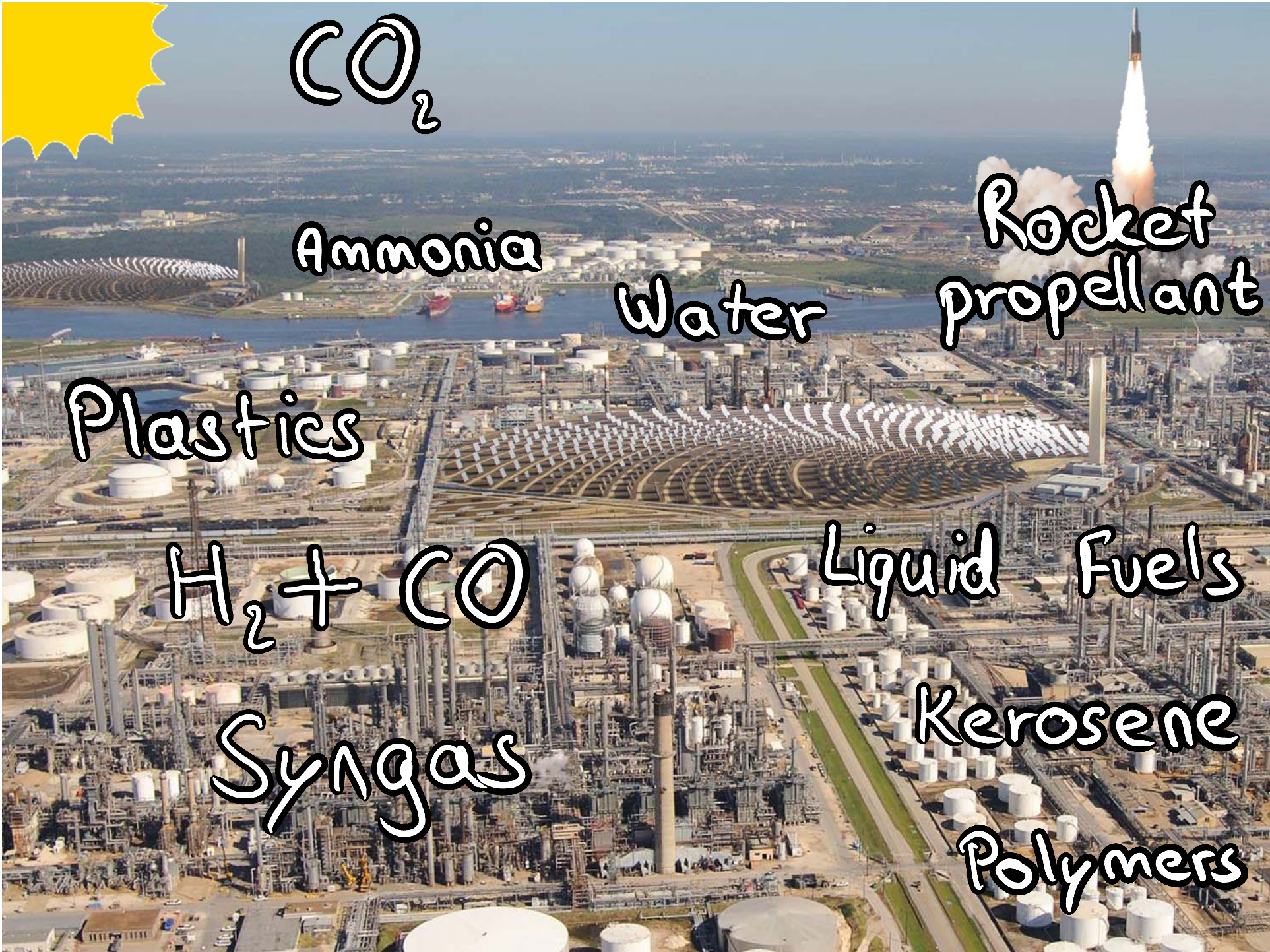


Potential of Solar Energy – the new economy?



M. Schmitz, TSK Flagsol





CO_2

Ammonia

Water

Rocket
propellant

Plastics

$\text{H}_2 + \text{CO}$

Syngas

Liquid Fuels

Kerosene

Polymers

Thank you very much for your attention!

